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Article

Examination of Kinetic Parameters for Dyeing of Polyamide Fabrics with Acid Dyestuff in Microwave and Conventional Heating Media

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Abstract

In this study, the dyeing kinetics of polyamide fabrics with acid dyes, Telon Blue M2R, under both conventional and microwave-assisted heating conditions were comprehensively investigated. While the conventional dyeing reaction was completed in 30 minutes, microwave-assisted dyeing was performed in the microwave device for 10 minutes. Dyeing kinetics were investigated as a function of reaction time, reaction concentration and dyeing temperatures. The K/S values (color depth) of the dyed fabrics were correlated with the concentration. A significant reduction in the dyeing process time for polyamide fabric was observed with microwave heating compared to the conventional method. Kinetic analysis revealed that the PSO kinetic model provides a better fit to the experimental data on the diffusion process of acid dye in polyamide fabrics, as evidenced by higher correlation coefficients (R^2) compared to the PFO model. The activation energy of the reaction in dyeing was found to be 63.27 kJ/mol, and the Arrhenius constant was determined as $7,20 \times 10^{10}$ L/g.min in conventional media and $18,70 \times 10^{10}$ L/g.min in microwave media. The Arrhenius factor in the microwave medium was more than two times higher than in the conventional one.

Keywords: Polyamide; microwave; acid dyes; kinetic parameters; Arrhenius constant; activation energy

1. Introduction

Polyamide fibers, particularly nylon 6 and nylon 6.6, are among the most important synthetic fibers in the textile industry due to their excellent mechanical properties, including high tensile strength, elasticity, and abrasion resistance. These characteristics make polyamide fabrics suitable for various applications ranging from apparel to technical textiles [1–4].

The conventional dyeing process of polyamide fabrics typically involves prolonged heating at elevated temperatures (50–95 °C) for extended periods, resulting in high energy consumption and long processing times [2]. Microwave-assisted dyeing has emerged as a promising alternative technology that addresses many of the limitations associated with conventional dyeing methods. [5–7].

The principle of dielectric heating operates, where electromagnetic radiation at 2450 MHz frequency causes rapid molecular vibration of polar molecules, particularly water, resulting in uniform and rapid heating throughout the dyeing bath. Microwave energy can penetrate molecules and heat them instantly, reducing heat transfer problems. Conventional dyeing methods are inherently limited by slow, non-uniform heat transfer, often leading to thermal gradients within the dye bath. This phenomenon can cause uneven dye uptake, resulting in defective dyeing known as “barre” or abruption [8–11]. Microwaves are one of the most effective non-contact heating techniques because high-dielectric materials are energetically heated by vibration and rotation of fixed dipoles in the microwave field [12–14] Microwave irradiation offers a transformative heating mechanism

characterized by rapid, volumetric, and selective energy deposition [15–18]. Microwaves interact with polar molecules, such as water and the ionic dye molecules themselves, through dipole rotation and ionic conduction, achieving the target temperature within seconds and ensuring exceptional thermal uniformity [19–21]. Microwaves eliminate thermal imbalances in the dyeing bath and lead to an increase in the rate of dye diffusion into the fiber. Furthermore, the rate constants of the kinetic dyeing reaction increase [22–24].

The Arrhenius constant values in the Arrhenius rate equation vary depending on the microwave power and control the rate of dyeing. The ionic structure and polarity of the dye are observed to be affected by microwaves. Therefore, it is necessary to obtain quantitative and qualitative data on the relationship between the microwave environment and polarity or ionicity [25–28].

Acid dyes represent the most commonly used class of dyes for polyamide fiber dyeing due to their excellent affinity and color fastness properties. The dyeing mechanism involves ionic interactions between the sulfonic acid groups of the dye molecules and the amino groups present in the polyamide fiber structure. The dyeing process is typically conducted under acidic conditions (pH 4-6) to protonate the amino groups in the fiber, thereby enhancing the electrostatic attraction between the dye and fiber [29].

Recent studies have demonstrated the potential of microwave technology in textile dyeing applications. Rahman et al. [9] reported significant reductions in dyeing time and improved color yield when applying microwave energy to cotton dyeing with reactive dyes. Similarly, Zhang et al. [10] observed enhanced dye penetration and reduced energy consumption in wool dyeing processes using microwave assistance. However, limited research has been conducted specifically on the kinetics of polyamide dyeing with acid dyes. In addition, we could not find any studies that investigated the kinetics of dyeing reactions in a microwave environment and determined the kinetic parameters.

Understanding the kinetics of dyeing processes is crucial for optimizing dyeing conditions and predicting dyeing behavior under various operational parameters [30–34]. Kinetic studies provide valuable insights into the rate-controlling mechanisms, equilibrium conditions, and the effects of process variables on dyeing performance [35–37]. Several kinetic models have been proposed to describe dyeing processes, including PFO, PSO, and intraparticle diffusion models [39–42]

In this study, conventional heating and microwave heating were investigated for the dyeing process of polyamide fabric with acid dyestuff (Telon Blue M2R). A pivotal and novel aspect of this research is the investigation into the interaction between microwave fields and the ionic structure/polarity of the dye molecules a subject for which, as noted in the literature, quantitative data is currently lacking. This study seeks to generate foundational data on this relationship.

2. Materials and Methods

Commercial 100% polyamide 6 fabric (e.g., plain weave, 150 g/m², supplied from Nurel Group) was used in this study. Telon Blue M2R (Figure 1) (supplied from DyStar) was selected as the model acid dye. Acetic acid was used for pH adjustment. Detergent - Bianco HS New F.T.R Chemicals and Levelling Agent Seragal N-FS Eco Dystar was supplied from Nurel Group.

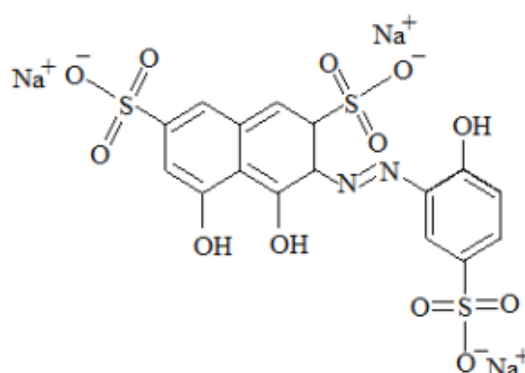


Figure 1. Telon Blue M2R.

2.1. Microwave-Assisted Dyeing Setup

Dyeing experiments were conducted using a modified microwave oven (START D Microwave Digestion System). Dyeing baths were prepared in microwave-transparent 100 ml capacity tubes to ensure uniform microwave energy absorption.

2.2. Dyeing Procedure

Polyamide fabric samples (e.g., 1 g each) were cut into uniform sizes. Dyeing baths were prepared with specific concentrations of Telon Blue M2R (e.g., 2% on weight of fabric), acetic acid for pH adjustment. The liquor ratio (fabric weight to bath volume) was maintained at 1:50 throughout all experiments.

For microwave-assisted dyeing, the prepared dyeing bath containing the fabric sample was placed inside the microwave system. Experiments were performed at microwave power level of 160 W, dyeing times (1, 2, 3, 4, 5, 6, 7, 8, 9, 10 minutes), target temperatures (50 °C, 60 °C, 70 °C, 80 °C, 95 °C), and pH value 6.5 (without acid donor). Temperature was measured immediately after the experiment ended.

After the specified dyeing time, the fabric samples were removed, thoroughly rinsed with cold distilled water to remove unfixed dye, and air-dried at room temperature.

For comparison, conventional dyeing experiments were carried out in a heating system under similar conditions (Temperature, pH, Liquor Ratio, Dye Concentration). Conventional dyeing were studied in 5, 10, 15, 20, 25, 30 minutes.

In experimental studies, polyamide fabric was used for dyeing. Acid donor, levelling agent and Bianco HS New were used as auxiliary materials for dyeing. START D Microwave Digestion System is used. The reflectance values of all dyed fabrics were measured using a Data Color SF 600 spectrophotometer.

2.3. Dyeing Kinetics Analysis

Dye uptake was determined by measuring the color strength in the fabric at predetermined time intervals using a Data Color SF 600 spectrophotometer at the maximum absorption wavelength of Telon Blue M2R ($\lambda_{max} = 630$ nm). A calibration curve was established using known concentrations of the dye. The percentage dye exhaustion (Dye Exhaustion is proportional with K/S) was calculated using the following equations:

$$\% \text{ Exhaustion} = \frac{(C_0 - C_t)}{C_0} \times 100 \quad (1)$$

$$K/S \propto \frac{(C_0 - C_t)}{C_0} \times 100 \quad (2)$$

$$\frac{K}{S} = \frac{(C_0 - C_t)}{C_0} \times A \quad (3)$$

where C_0 is the initial dye concentration and C_t is the dye concentration in the bath at time t .

The difference between the initial concentration and the dye concentration remaining in the bath at time (t) gives the dye concentration absorbed by the fabric. A linear regression was performed between this value and the K/S value read by the spectrophotometer to convert the K/S value into concentration. This conversion coefficient (A) was determined to be approximately 15. This coefficient depends on the type of dye and the initial dye concentration. The time-dependent calculation of dye concentration (C_t) in water was determined by using spectrophotometric measurements of the dye-water mixture and the proportionality of the K/S value to dye consumption.

Color strength (K/S value) of the dyed fabric samples was measured using a reflectance spectrophotometer (Data Color 1000 spectrophotometer.) according to the Kubelka-Munk equation:

$$\frac{K}{s} = \frac{(1-R)^2}{2R} \quad (4)$$

where R is the reflectance value at the maximum absorption wavelength.

To analyze the dyeing kinetics, the experimental data were fitted to pseudo-first-order (PFO) and pseudo-second-order (PSO) kinetic models.

The PFO rate equation is given by:

$$k_1[C] = -\frac{d[C]}{d(t)} \quad (5)$$

$$\ln(C_t) = \ln C_0 - k_1 t \quad (6)$$

The PSO rate equation is given by:

$$k_2[C]^2 = -\frac{d[C]}{d(t)} \quad (7)$$

$$\frac{1}{C_t} = \frac{1}{C_0} + k_2 t \quad (8)$$

C_0 is the initial concentration value, while C_t is the instantaneous concentration value during the experimental process and at time t , respectively; k_1 (min^{-1}) is the PFO rate constant; and k_2 ($\text{g}/\text{lt}.\text{min}$) is the PSO rate constant

Using the k rate constants, A and E_A values were calculated from the Arrhenius Equation:

$$k = A \cdot e^{-(E_A/RT)} \quad (9)$$

$$\ln(k) = -\frac{E_A}{RT} + \ln(A) \quad (10)$$

Then, PFO and PSO were converted into variables of the equations. The rate constants k for PFO and PSO were calculated from the data obtained from each equation [40–42]

3. Results and Discussion

3.1. Effect of Conventional Heating on Dyeing Kinetics

The influence of conventional heating on the dyeing kinetics of polyamide fabric with Telon Blue M2R was investigated at a different temperatures (50, 60, 70, 80 and 95 °C), different times (5, 10, 15, 20, 25, 30 minutes) within pH value 6.5 (without acid donor) and constant dye concentration (0,1%).

PFO and PSO figures (Figures 2 and 3) were drawn from the concentration data in our study as seen below. In order to further explore the dyeing kinetics of acid dye in the polyamide fabrics, the PFO and PSO models were applied to analyze the experimental data in conventional heating system. The correlation coefficient (R^2) of the PSO kinetic model of polyamide fabrics adsorption was greater than that of the PFO kinetic model. Analysis of the obtained data revealed that the reaction was second-order [5]. As shown in Table 1, increasing the temperature from 50 °C to 95 °C significantly accelerated reaction rate.

Table 1. Reaction Rate Constant Data according to Conventional Heating.

Temperature	First order		Second Order	
	k_1 (1/min)	R^2	k_2 (L/g.min)	R^2
50 °C	0,0275	0,9874	4,1579	0.9999
60 °C	0,0396	0,9648	8,556	0.9998
70 °C	0,0581	0,9379	17,660	0.9998
80 °C	0,0711	0,9022	30,298	0.9999
95 °C	0,0931	0,8387	76,063	0.9997

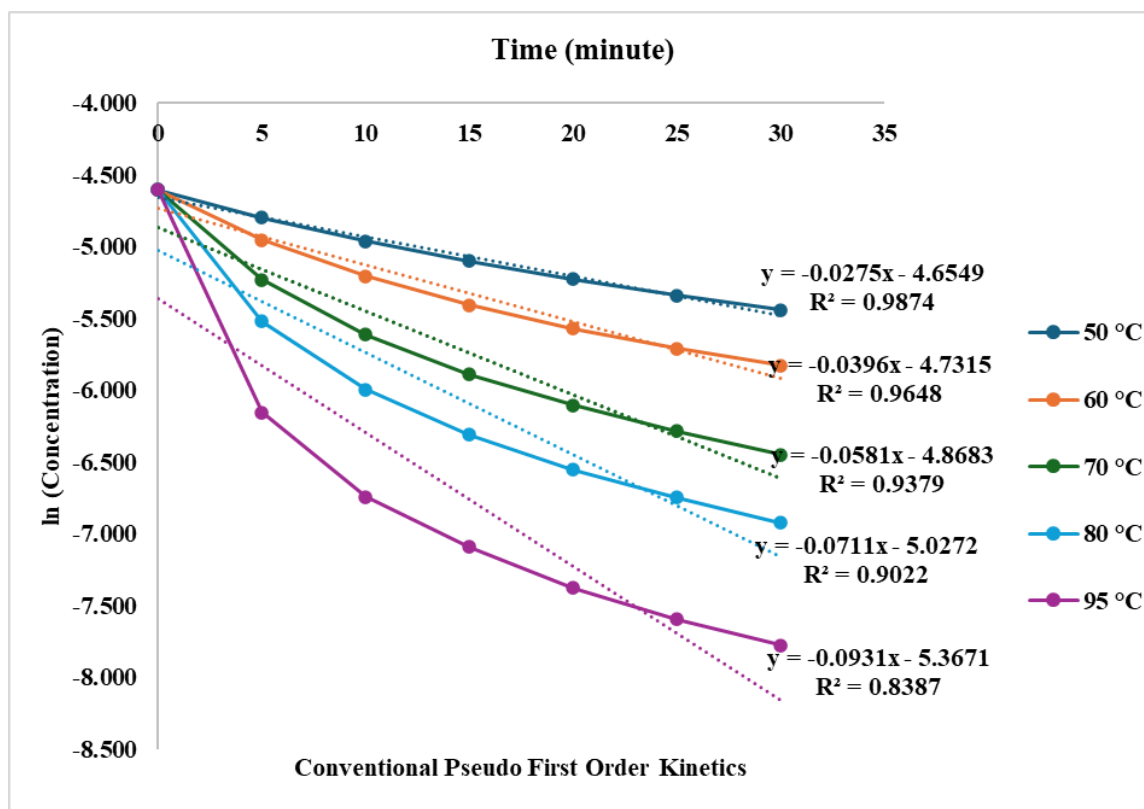


Figure 2. PFO Kinetic Model (LN (Concentration) – Time) at Conventional Heating.

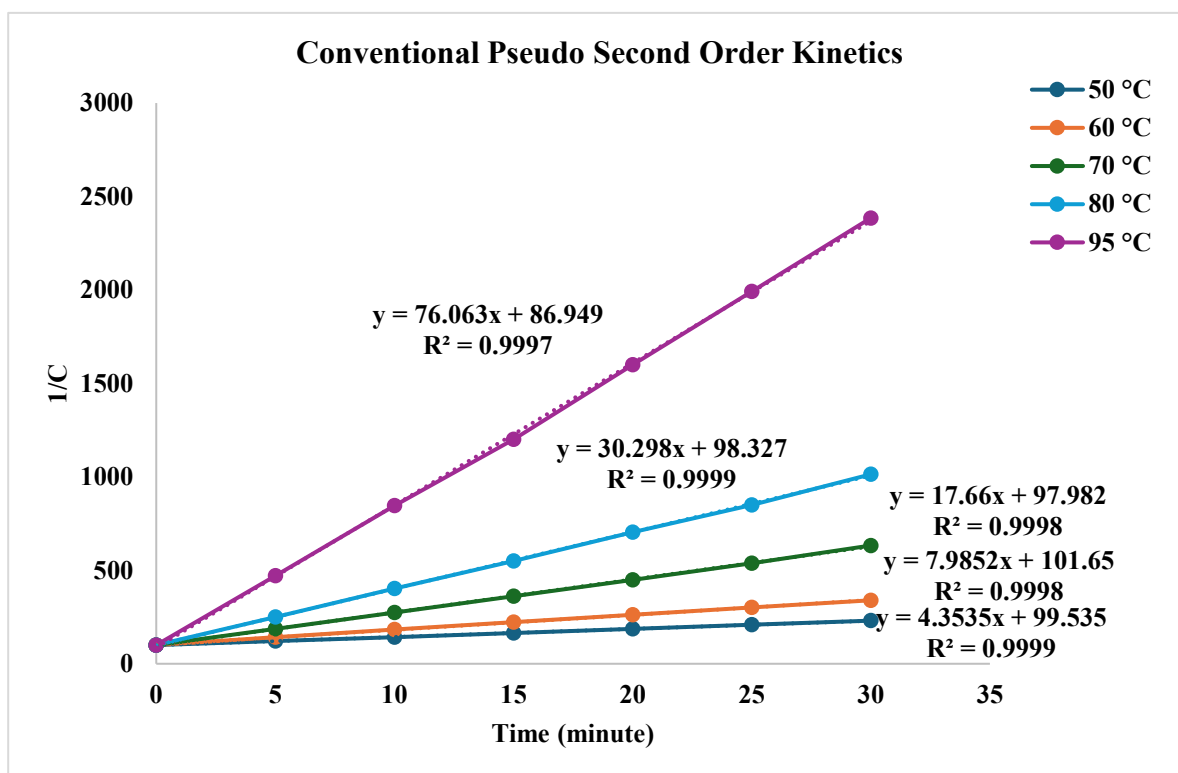


Figure 3. PSO Kinetic Model (1/Concentration) – Time) at Conventional Heating.

Figures 4 and 5 illustrates the evolution of Color Strength (K/S) and dye concentration over time (min.) for a polyamide substrate, dyed at different temperatures. The K/S value, derived from the Kubelka-Munk theory, is a fundamental metric in color science that quantifies the depth of color; a higher K/S value indicates a darker or more intense color. For all temperatures, the K/S value

increases with time, which is the expected behavior for a dyeing process. Initially, the rate of dye uptake is high, leading to a rapid increase in color strength. Over time, as the system approaches equilibrium (saturation of the fiber with dye), the rate of increase in K/S slows down, and the curves begin to plateau. Temperature is a critical factor significantly influencing the dyeing kinetics and the final color depth. The curve representing the highest temperature consistently yields the greatest K/S value at any given time and reaches the highest final color strength. In addition, the curves for progressively lower temperatures lie beneath the higher-temperature curves, resulting in lower final K/S values. The data conclusively shows that both the rate of dyeing and the final color depth (K/S) on polyamide are strongly dependent on the process temperature. Operating at a higher temperature dramatically shortens the time required to achieve a deep shade and results in superior color yield. These figures provide crucial optimization guidelines, indicating that for maximum efficiency and color strength, the dyeing process should be conducted at the highest temperature compatible with the stability of the fiber and dye.

Table 2. K/S values according to Time/Temperature (Conventional Heating).

K/S (Color Strength)	50 °C	60 °C	70 °C	80 °C	95 °C
0	0	0	0	0	0
5	2,151	3,745	6,980	9,000	11,820
10	3,671	5,764	9,527	11,270	13,228
15	4,802	7,026	10,846	12,276	13,750
20	5,675	7,889	11,653	12,867	14,063
25	6,371	8,518	12,208	13,235	14,247
30	6,938	8,995	12,629	13,520	14,371

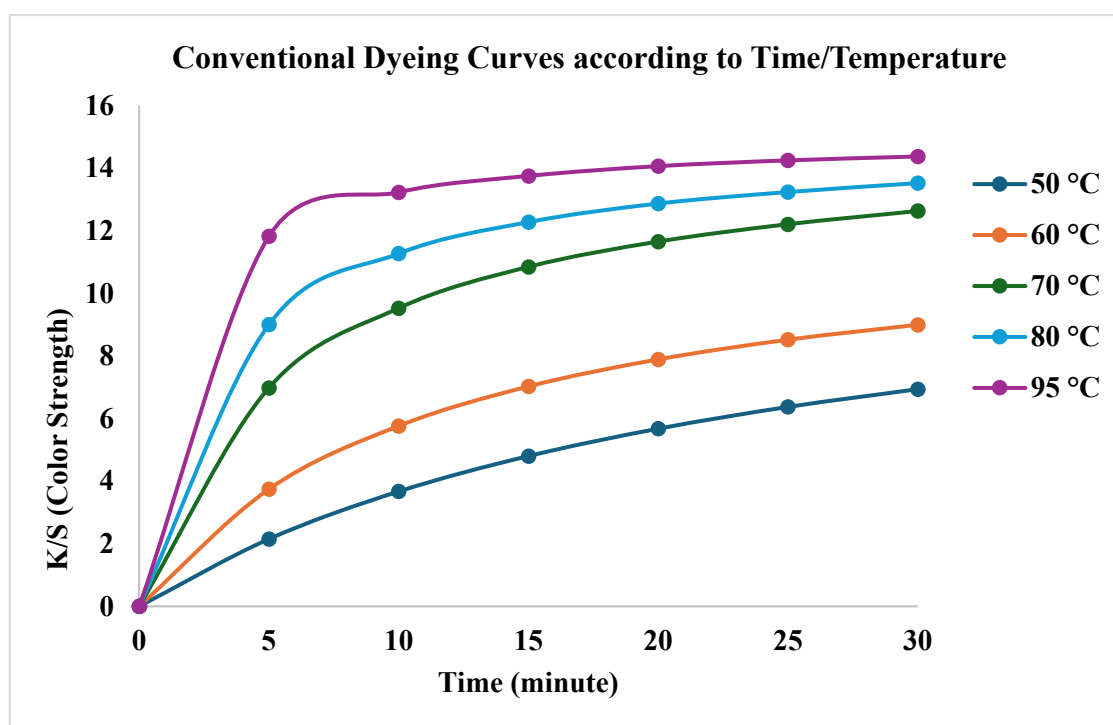


Figure 4. Dyeing curve at different temperatures for conventional heating.

Figure 5 presents the conventional concentration curves, illustrating the change in dye concentration in the bath over a 30-minute period at five different temperatures: 50 °C, 60 °C, 70 °C, 80 °C, and 95 °C. The initial concentration for all experiments was consistently set at 0.01000 gr/100 ml.

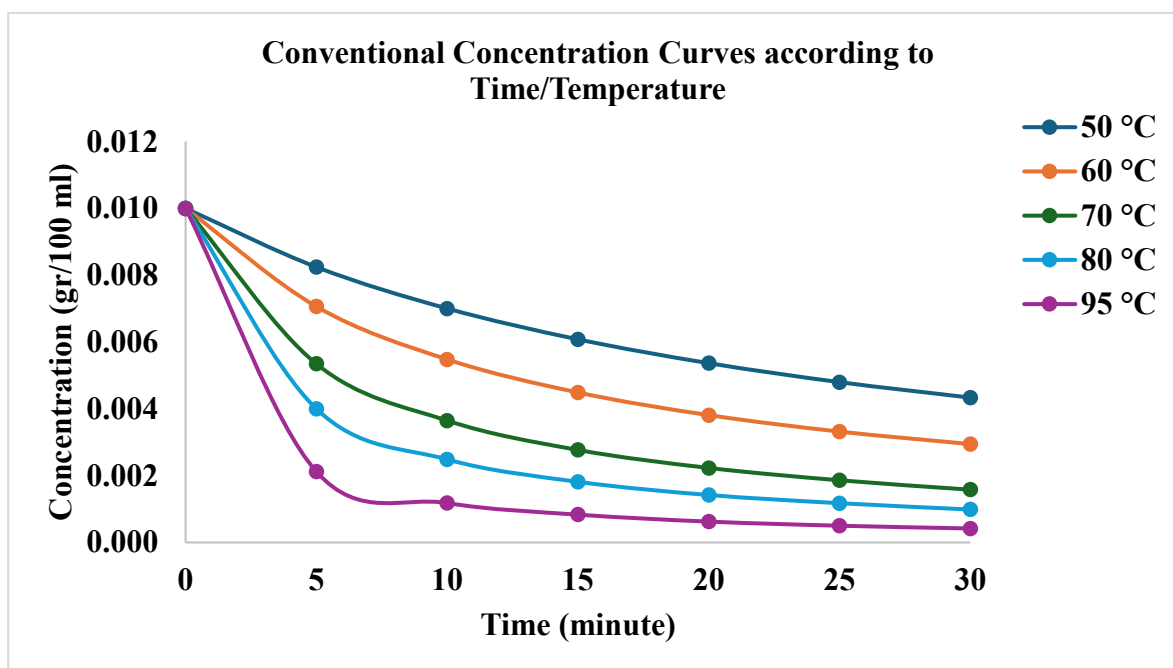


Figure 5. Conventional Concentration Curve for the Dyeing Process at Various Temperatures.

A clear trend of decreasing dye concentration in the solution is observed across all temperatures, which is characteristic of the dye exhaustion process onto the substrate. The kinetics of the process appear to be two-phased: a rapid initial uptake phase within the first 5 minutes, followed by a significantly slower approach to equilibrium from 5 to 30 minutes. This suggests that the initial stage is likely governed by rapid surface adsorption, while the later stage is controlled by the slower diffusion of the dye into the internal structure of the material.

The influence of temperature is highly significant, affecting both the rate and the extent of the dyeing process:

Effect on Rate of Uptake: As the temperature increases, the rate of dye uptake is markedly enhanced. This is evidenced by the steeper initial slope of the curves at higher temperatures. For instance, the concentration drop is most dramatic at 95 °C, where the near-equilibrium state is achieved much faster compared to the lower temperatures (e.g., 50 °C). This acceleration is consistent with the general principle that increasing thermal energy provides the necessary activation energy for the dye molecules to overcome energy barriers and diffuse more rapidly.

2. Effect on Extent of Exhaustion: The final concentration values at the end of the 30-minute period demonstrate that higher temperatures lead to a greater extent of dye exhaustion.

At the lowest temperature (50 °C), the final concentration remains highest (approximately 0.00420). Conversely, at the highest temperature (95 °C), the final concentration is lowest (approaching 0.00010), indicating maximum dye exhaustion from the bath. This relationship confirms the endothermic nature of the dyeing process, where higher temperatures shift the equilibrium towards the adsorbed state, resulting in a higher equilibrium dye uptake.

The data in Table 3 unequivocally demonstrates that temperature is a critical control parameter for the conventional dyeing process. The enhanced rate of uptake and the greater extent of dye exhaustion observed at elevated temperatures (up to 95 °C) are indicative of a process that is both kinetically accelerated and thermodynamically favored by heat. The rapid initial uptake followed by a diffusion-controlled tail suggests that future kinetic modeling should consider a pseudo-second-order or similar model that accounts for both surface and internal diffusion mechanisms.

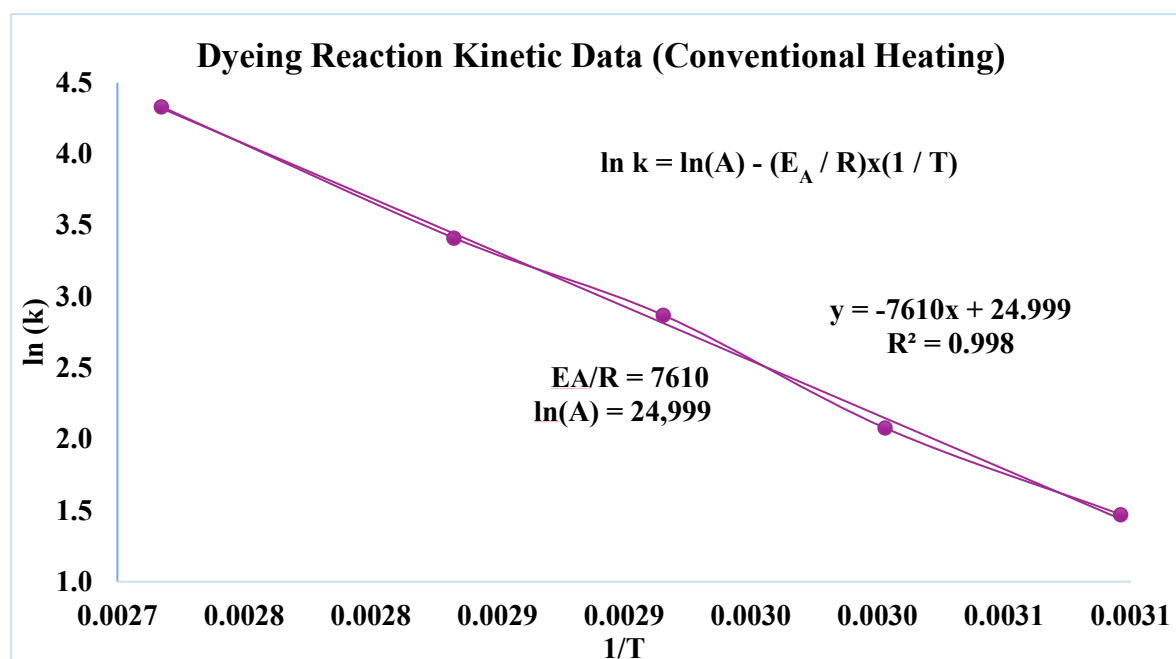
Table 3. Dye Concentration according to Time/Temperature (Conventional Heating).

Concentration (gr/100 ml)	50 °C	60 °C	70 °C	80 °C	95 °C
0	0,01000	0,01000	0,01000	0,01000	0,01000
5	0,00824	0,00706	0,00535	0,00400	0,00212
10	0,00700	0,00548	0,00365	0,00249	0,00118
15	0,00608	0,00449	0,00277	0,00182	0,00083
20	0,00537	0,00381	0,00223	0,00142	0,00062
25	0,00480	0,00332	0,00186	0,00118	0,00050
30	0,00434	0,00294	0,00158	0,00099	0,00042

Figure 6 shows the kinetic analysis of dyeing of polyamide with acid dye at conventional heating. The Arrhenius plot as seen Figure 6 obtained for the conventional heating process shows a strong linear relationship between $\ln(k)$ and $1/T$, with an R^2 value of 0.998, indicating excellent conformity to the Arrhenius model. The slope of the fitted line (-7610) corresponds to $-E_A/R$, from which the activation energy (E_A) can be calculated. This relatively steep negative slope suggests a moderately high activation energy, implying that the reaction rate is strongly dependent on temperature.

The intercept of the line (24.999) represents $\ln(A)$, which reflects the pre-exponential factor (A). A high $\ln(A)$ value indicates a high frequency of successful molecular collisions leading to product formation. Overall, the linearity of the plot confirms that the reaction kinetics under conventional heating follow Arrhenius behaviour, and the calculated kinetic parameters (E_A and A) provide reliable insight into the temperature sensitivity and mechanistic characteristics of the reaction system.

The activation energy of the dyeing reaction was determined to be 63.27 kJ/mol for both conventional and microwave dyeing processes. Arrhenius constant was determined to be A 7.20×10^{10} for conventional dyeing processes.

**Figure 6.** Kinetic Analysis of Dyeing of Polyamide with Acid Dye at Conventional Heating (Arrhenius Plot).

3.2. Effect of Microwave Power on Dyeing Kinetics

The influence of microwave power on the dyeing kinetics of polyamide fabric with Telon Blue M2R was studied at a different temperatures (50 °C, 60 °C, 70 °C, 80 °C, 95 °C), different times (1, 2, 3, 4, 5, 6, 7, 8, 9, 10 minutes) within a certain pH value 6.5 (without acid donor) and constant dye concentration (0,1%).

PFO and PSO figures (Figures 7 and 8) were drawn from the concentration data in our study as seen below figures. In order to further explore the dyeing kinetics of acid dye in the polyamide fabrics in microwave media, the PFO and PSO models were applied to analyze the experimental data. The correlation coefficient (R^2) of the PSO kinetic model of polyamide fabrics adsorption was greater than that of the PFO kinetic model. Analysis of the obtained data revealed that the reaction was second-order [5].

As shown in Table 4, increasing the temperature from 50 °C to 95 °C significantly accelerated reaction rate. This enhanced performance is attributed to the more rapid and uniform heating provided by higher microwave power, which facilitates faster diffusion of dye molecules into the fiber structure. The volumetric heating mechanism of microwaves ensures that the entire dyeing bath is heated simultaneously, minimizing temperature gradients and promoting efficient dye transfer.

Table 4. Reaction Rate Constant Data according to Microwave Power Level.

Temperature	First order		Second Order	
	k_1 (1/min)	R^2	k_2 (lt/g.min)	R^2
50 °C	0,0646	0,9734	9,3013	0,9938
60 °C	0,0977	0,9803	17,925	0,9932
70 °C	0,1451	0,9796	33,52	0,9967
80 °C	0,1708	0,9179	61,509	0,9819
95 °C	0,2344	0,8504	174,94	0,9638

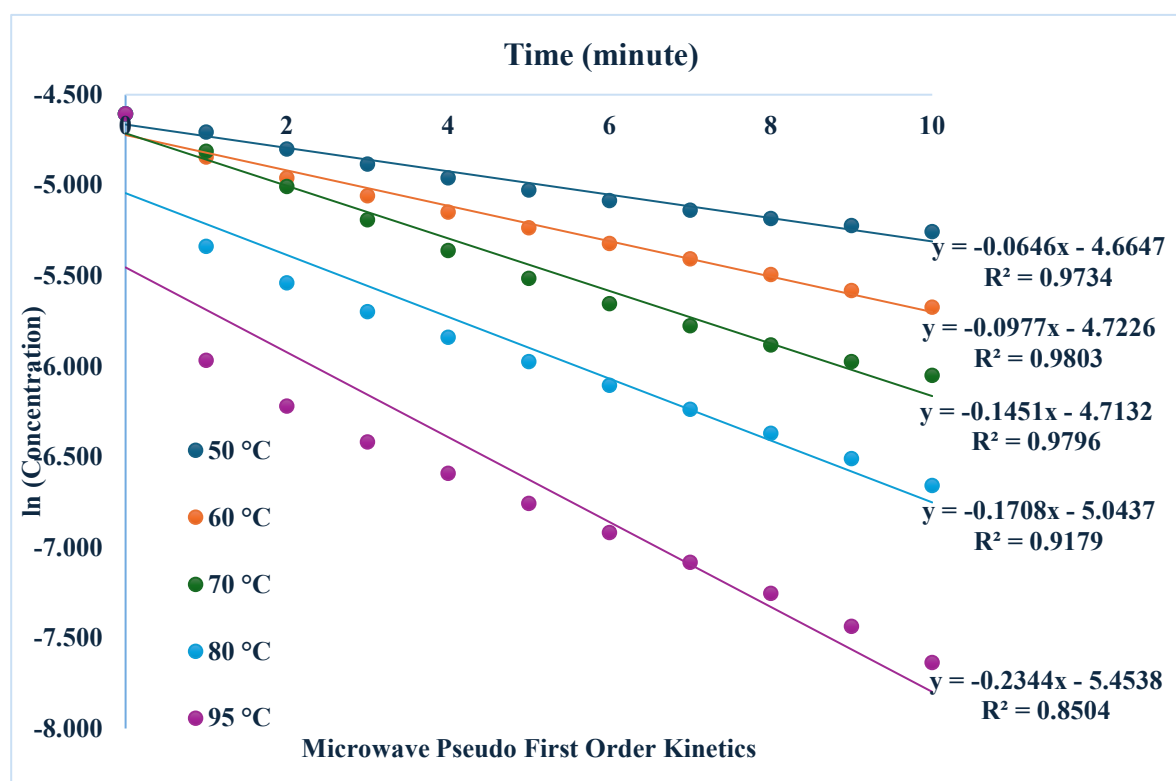


Figure 7. Microwave PFO Kinetics in Microwave Media.

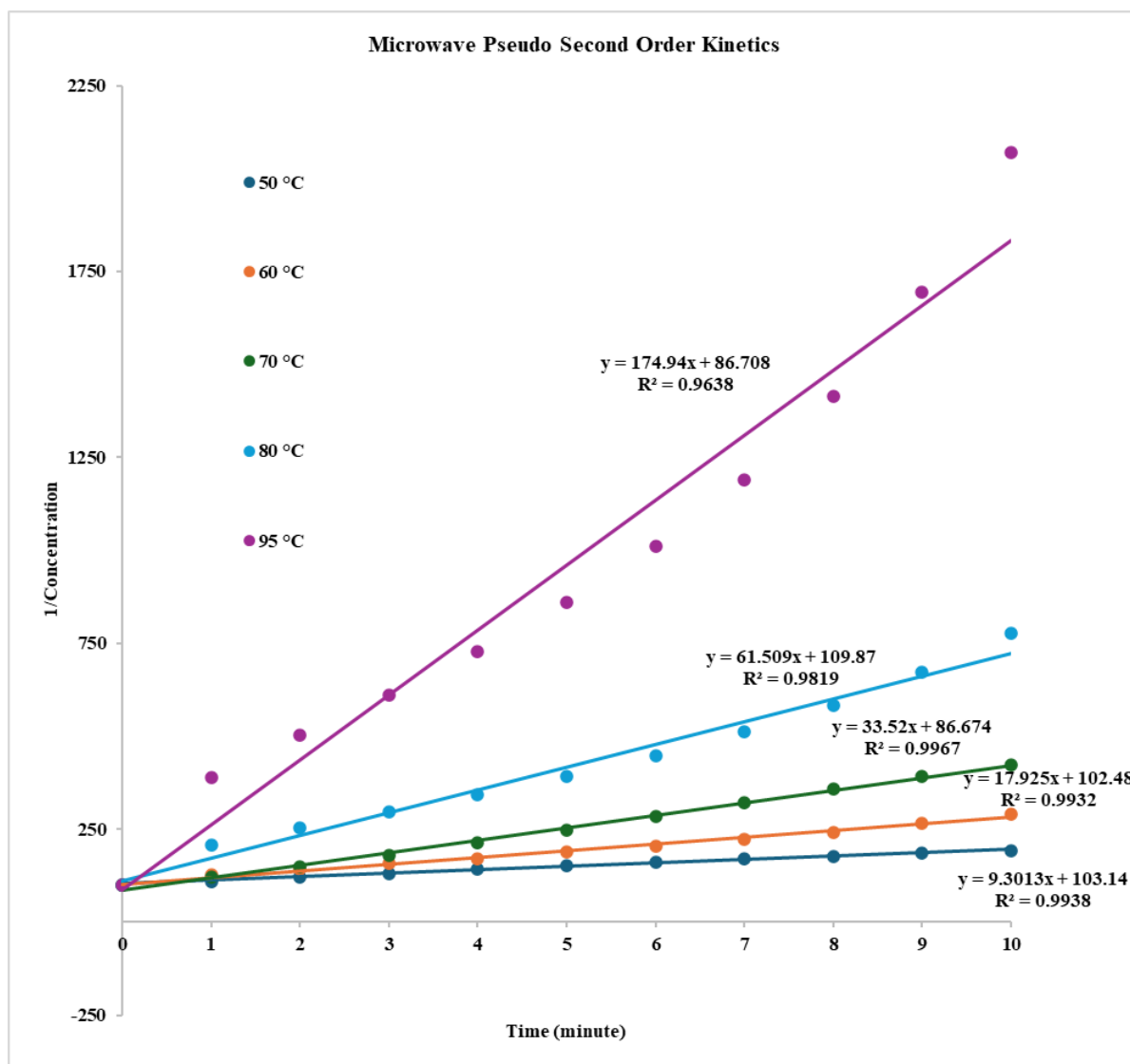


Figure 8. PSO Kinetic Model (1/C-Time) in Microwave Media.

Figure 9 titled “Color Strength (K/S) Curve of Polyamide (at Different Temperatures in Microwave Media)” illustrates the relationship between the dyeing time and the resulting color strength (K/S) of a polyamide (nylon) fabric, under the influence of microwave irradiation at different temperatures. For all temperatures, the Color Strength (K/S) increases with time, which is a classic behavior in dyeing processes. This indicates that more dye molecules are diffusing into the polymer and being fixed as time progresses. Temperature is the dominant factor influencing the rate and final depth of dyeing. The graph clearly demonstrates a direct correlation: higher dyeing temperatures lead to significantly higher K/S values in a shorter time. A higher temperature dramatically improves the dye uptake rate and the final color depth.

Table 5. K/S values according to Time/Temperature (Microwave Heating).

K/S (ColorStrength)	50 °C	60 °C	70 °C	80 °C	95 °C
0	0	0	0	0	0
1	1,399	3,085	2,892	8,308	11,530
2	2,559	4,330	5,134	9,710	12,418
3	3,521	5,280	6,870	10,637	12,968
4	4,319	6,077	8,216	11,347	13,374
5	4,981	6,778	9,259	11,931	13,697
6	5,530	7,411	10,068	12,431	13,967

7	5,985	7,991	10,694	12,869	14,199
8	6,363	8,530	11,179	13,262	14,403
9	6,676	9,036	11,555	13,618	14,586
10	6,936	9,514	11,847	13,944	14,751

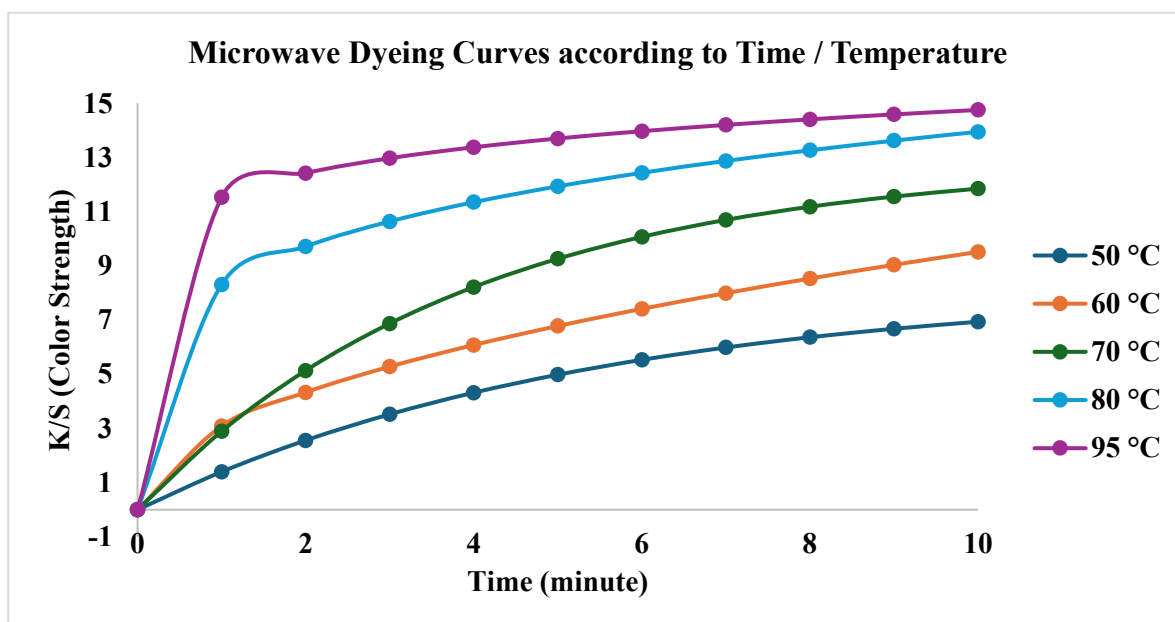


Figure 9. Dyeing rate (K/S) curve of polyamide according to time at different temperatures in Microwave Media.

As shown in Table 6 and Figure 10, the microwave concentration profiles clearly demonstrate that both temperature and processing time exert a pronounced influence on the depletion of the target compound. At all temperatures, the concentration decreases rapidly during the initial stage of treatment, reflecting the high reaction rate promoted by microwave-induced energy absorption. This initial sharp decline is especially evident at 80 °C and 95 °C, where the concentration drops almost immediately to less than half of its initial value, indicating strong thermal and non-thermal microwave effects.

As the process continues, the rate of concentration loss becomes progressively slower, suggesting that the easily degradable or reactive fraction is consumed early in the treatment while the remaining fraction degrades more gradually. Higher temperatures consistently result in lower residual concentrations at any given time, confirming the strong positive correlation between reaction rate and temperature. Notably, at 95 °C the concentration approaches a minimal asymptotic level within only a few minutes, while at lower temperatures such as 50 °C and 60 °C the decline is more gradual and extended over the entire 10-minute period.

Table 6. Dye Concentration according to Time/Temperature (Conventional Heating).

Concentration (gr/100 ml)	50 °C	60 °C	70 °C	80 °C	95 °C
0	0,01000	0,01000	0,01000	0,01000	0,01000
1	0,00904	0,00787	0,00813	0,00481	0,00256
2	0,00824	0,00701	0,00669	0,00393	0,00199
3	0,00757	0,00636	0,00557	0,00335	0,00163
4	0,00702	0,00581	0,00470	0,00291	0,00137
5	0,00656	0,00533	0,00403	0,00254	0,00116
6	0,00619	0,00489	0,00350	0,00223	0,00099
7	0,00587	0,00449	0,00310	0,00196	0,00084
8	0,00561	0,00412	0,00279	0,00171	0,00071

9	0,00540	0,00377	0,00255	0,00149	0,00059
10	0,00522	0,00344	0,00236	0,00128	0,00048

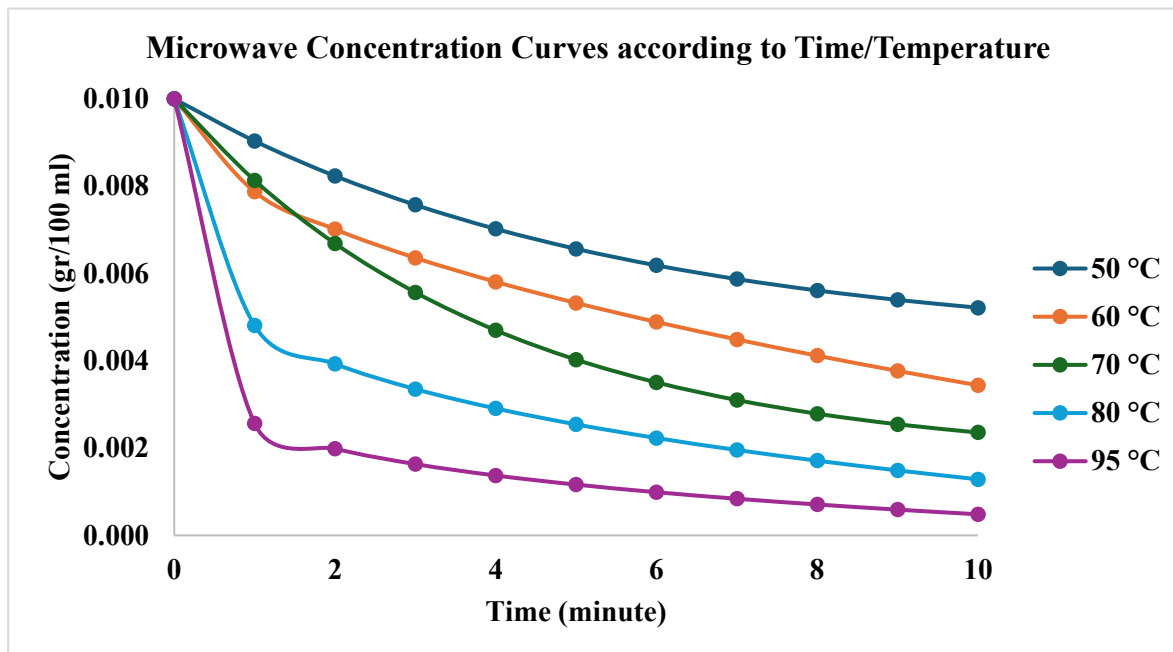


Figure 10. Conventional Concentration Curve for the Dyeing Process at Various Temperatures.

Overall, the results indicate that microwave heating significantly accelerates the reaction or degradation mechanism, and the temperature-dependent trends observed are consistent with typical kinetic behaviour in thermally activated processes. These findings highlight the effectiveness of microwave energy in enhancing reaction kinetics, particularly at elevated temperatures, and provide a strong basis for subsequent kinetic modelling and Arrhenius analysis.

Figure 11 shows the kinetic analysis of dyeing of polyamide with acid dye at microwave heating. Activation energy of the dyeing reaction was determined to be 63.27 kJ/mol, and the Arrhenius constant A was determined to be $18,70 \times 10^{10}$ lt/gr.min at microwave media.

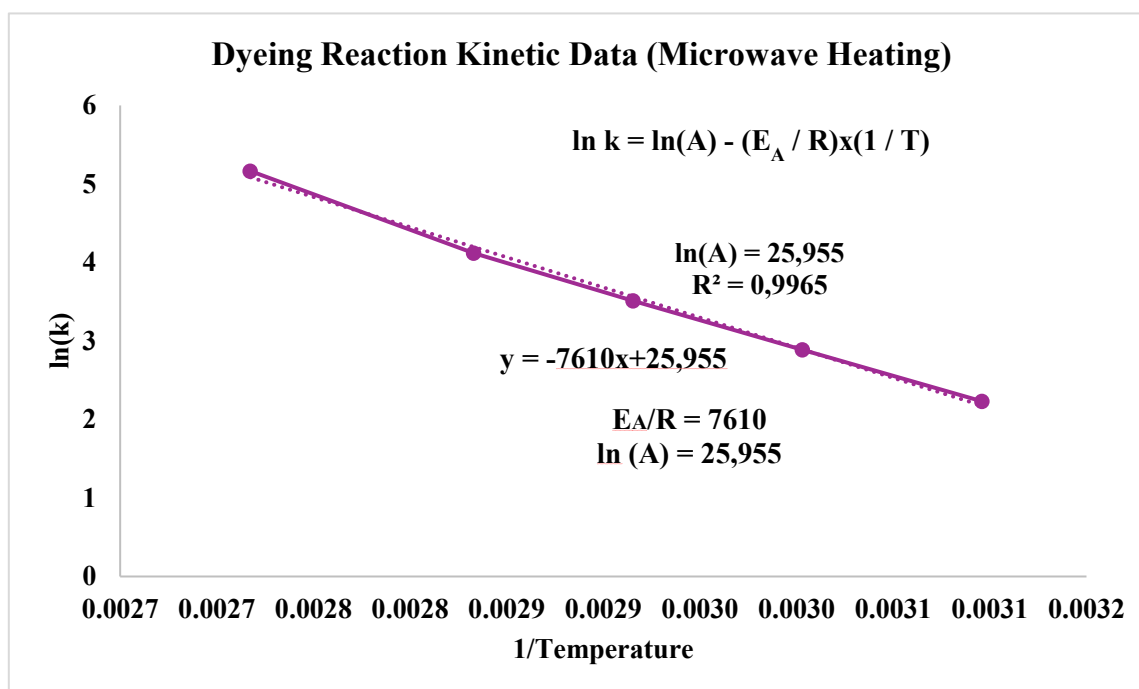


Figure 11. Kinetic Analysis of Dyeing of Polyamide with Acid Dye in Microwave Media (Arrhenius Plot).

The Arrhenius plot obtained for the microwave-assisted dyeing process shows a clear linear relationship between $\ln(k)$ and $1/T$, indicating that the reaction kinetics follow Arrhenius behavior under microwave conditions. The high coefficient of determination ($R^2 = 0.9965$) demonstrates excellent linearity, confirming that temperature has a strong and predictable influence on the reaction rate.

The extrapolated intercept provides the pre-exponential factor, $\ln(A) = 25.955$, suggesting a relatively high frequency of effective molecular collisions during the dyeing process. This is consistent with the enhanced energy transfer characteristic of microwave heating, which can promote rapid dipole rotation and localized superheating within the system. As a result, dye-fiber interactions may occur more efficiently compared to conventional heating.

The negative slope of the line indicates the expected decrease in reaction rate with increasing $1/T$, corresponding to higher rates at higher temperatures. The magnitude of this slope (though not numerically provided here) would be directly related to the activation energy (E_A), and its linearity implies that microwaves do not introduce anomalous or non-thermal effects that disrupt classical Arrhenius behavior. Instead, the data suggest that microwave heating accelerates the dyeing process primarily by increasing the effective temperature and improving energy distribution within the medium.

Overall, the Arrhenius analysis confirms that microwave-assisted dyeing is thermally activated and exhibits strong kinetic consistency. The high $\ln(A)$ value and excellent model fit support the conclusion that microwaves enhance reaction kinetics, potentially offering advantages such as faster dye uptake, reduced processing times, and improved energy efficiency.

3.3. Comparison of Microwave and Conventional Heating on Dyeing Kinetics

Figures 12–14 present a direct comparison of the Reaction Rate Constant (k) as a function of Temperature ($^{\circ}\text{C}$) for the same chemical reaction conducted under Microwave Heating and Conventional Heating. In addition, it provides compelling and direct evidence that microwave irradiation is not merely a faster method to heat a reaction mixture, but it actively enhances the reaction kinetics. The consistently higher rate constants demonstrate a clear advantage over conventional heating, leading to more efficient and rapid chemical synthesis.

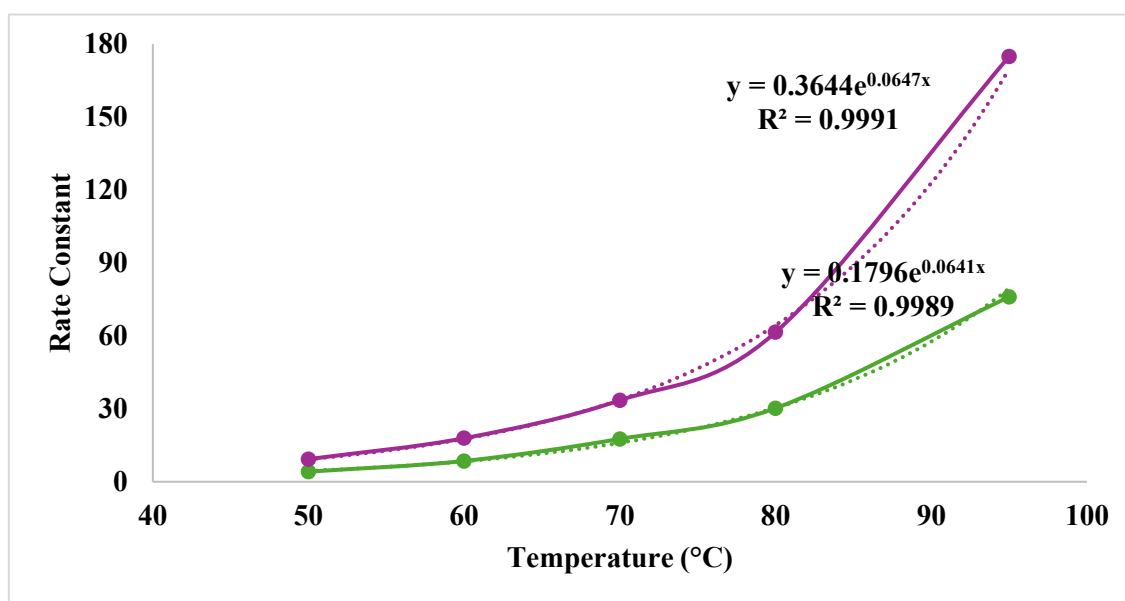


Figure 12. Effects of Temperature on Reaction Rate Constant (k) on Both of Microwave and Conventional Heating.

From the slopes in Figure 14, it is understood that the activation energy is the same, and the Arrhenius constants are different for Microwave and Conventional Heating. The fact that the Arrhenius constant is approximately more than two times higher in the microwave environment provides strong evidence that microwaves act not only as a simple heat source but also as a “specific” or “non-thermal” effect. Microwaves accelerate the dyeing process by potentially inducing more frequent and/or more effective molecular interactions in the reaction zone. This allows molecules to collide at a higher frequency and more effectively.

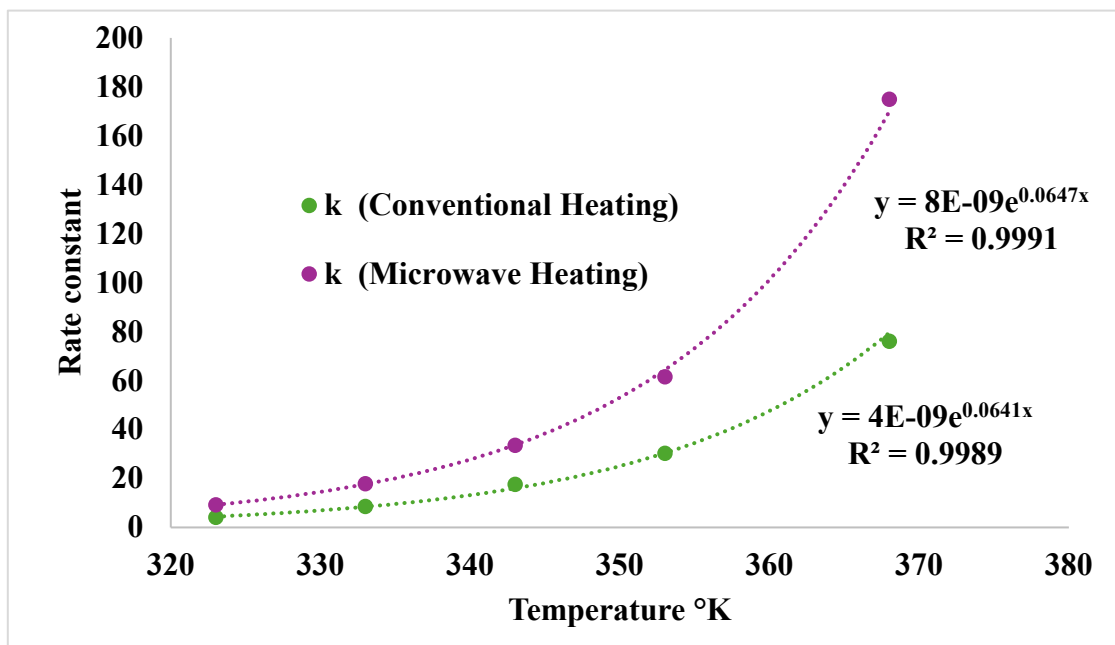


Figure 13. Effects of Temperature on Reaction Rate Constant (k) on Both of Microwave and Conventional Heating.

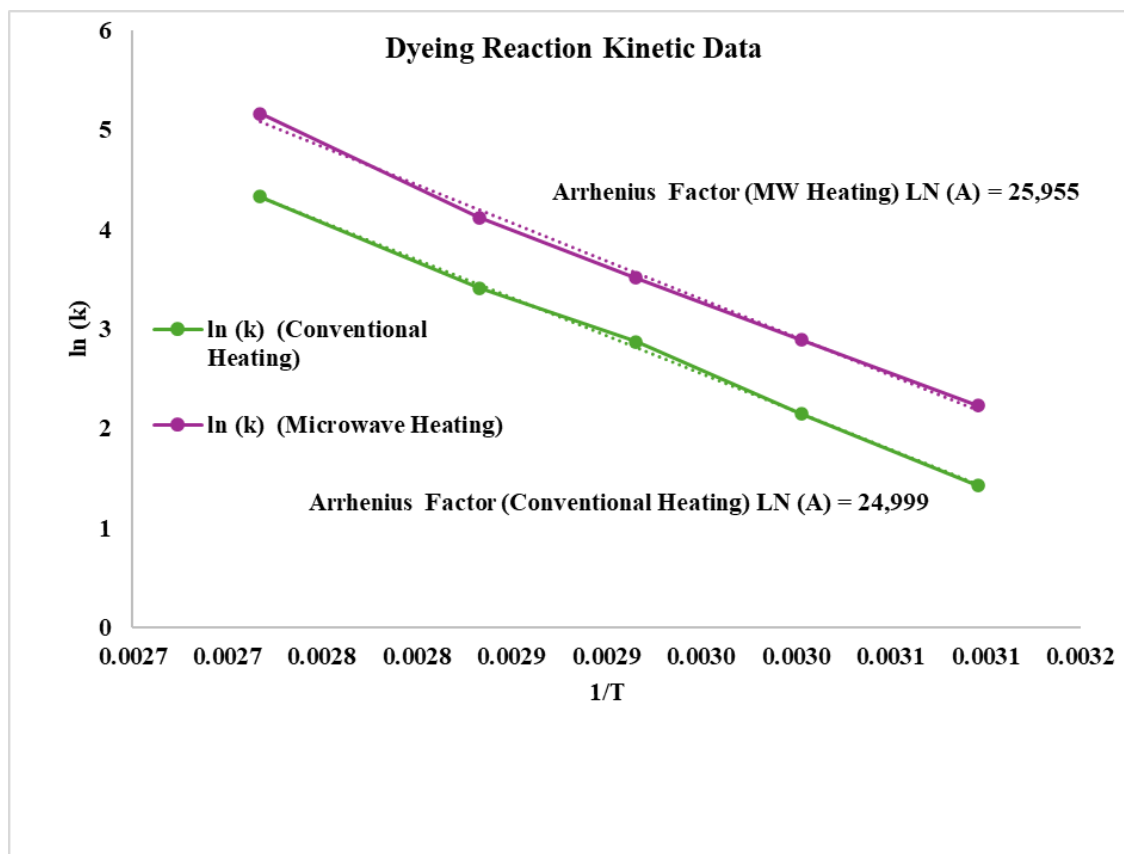


Figure 14. Comparison of Arrhenius Plot for Microwave and Conventional Heating.

4. Conclusions

This study investigated the dyeing kinetics of acid dyes on polyamide fabric in a microwave-assisted environment. The microwave-assisted dyeing process demonstrated significant advantages over conventional methods, particularly in terms of reduced processing time and enhanced dye uptake. While conventional dyeing required 30 minutes, the microwave-assisted technique achieved comparable results in only 10 minutes.

This notable reduction in processing time is attributed to the microwave heating mechanism, which provides rapid, volumetric, and homogeneous heating throughout the dye bath. This minimizes thermal gradients and promotes efficient dye transfer. A key finding was the more than two times increase in the pre-exponential factor (A) in the Arrhenius equation for the microwave medium (18.70×10^{10} L/g·min) compared to the conventional one (7.20×10^{10} L/g·min). Since factor A is related to the frequency of molecular collisions, this increase suggests a specific, potentially non-thermal microwave effect that induces more frequent and/or effective molecular interactions at the reaction site, beyond mere bulk heating.

Miklavc observed a decrease in activation energy during the microwave-assisted decomposition of sodium bicarbonate. Exposing substrates (dielectric materials) to microwaves causes molecules to rotate rapidly. This generates heat due to friction and also increases the contact probability between reactive molecules, thus reducing the activation energy and increasing the reaction rate [47].

Subsequently, Cross found an increase in molecular mobility in the presence of microwaves. The increase in the reaction rate was attributed to a rise in the Arrhenius (A) factor.

$$A = \gamma \lambda^2 \Gamma$$

- γ : The number of adjacent jump sites (The number of possible neighboring positions to which an atom or molecule can migrate)
- λ : The jump distance (The average distance an atom or molecule travels in a single diffusion jump)
- Γ : The jump frequency (The rate at which an atom or molecule makes successful jumps from one site to another) [48].

In our study, the Arrhenius factor in the microwave medium was more than two times higher than in the conventional one, which supports the view expressed by Cross. In accordance with the increase in the Arrhenius (A) factor, the pre-exponential factor is dependent on the vibrational frequency of atoms at the reaction interface and is therefore influenced by microwave irradiation. Kappe and colleagues conducted a thorough investigation of this microwave effect for ring-closing metathesis and the Biginelli reactions, where no significant difference was observed between conventional and microwave heating. It is crucial to note that this finding is specific to those particular reactions and cannot be generalized. In addition to the debated “thermal” and “non-thermal” microwave effects, employing microwave irradiation in aqueous processes offers several distinct practical advantages [48–50].

This demonstrates that higher energy input and longer exposure to the dye solution lead to accelerated dye absorption by polyamide fibers. Kinetic analysis revealed that the PSO kinetic model provides a better fit to the experimental data on the diffusion process of acid dye in polyamide fabrics, as evidenced by higher correlation coefficients (R^2) compared to the PFO model [51].

As a result, microwave technology offers a viable and promising alternative for the sustainable and efficient dyeing of polyamide fabrics. Future research could focus on exploring the applicability of the microwave-assisted dyeing method to other fiber types and dye classes, and on conducting comprehensive economic and environmental life cycle assessments to validate its industrial feasibility and sustainability benefits on a larger scale. The significant reduction in dyeing time, improved process efficiency, and elucidation of kinetic parameters underscore that microwave

technology should be implemented in the textile industry as a sustainable alternative to conventional dyeing methods.

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