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Review

Rare Earth Elements: Their Geological Sources and the Potential of Organosulfonic Acids for Rare Earth Elements Leaching from Coal Ash and Process Optimization

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Abstract: The orbital electronic structure of Rare Earth Elements (REEs) contains many unpaired electrons which render them capable of storing large amount of magnetic energy in addition to being critical for hitech applications. Geological deposits are their conventional sources, and the current supply chain relies on production from these deposits. However, given their critical roles in the anticipated global energy transition, there is the need to explore other viable sources to supplement current and future supplies chains. REEs occur in coal as accessory minerals and their concentration in coal ash to levels that rival those of geological deposits has been established by sophisticated analytical chemical methods. Conventional hydrometallurgical processes rely on acid leaching, using toxic mineral acids. Meanwhile, organosulfonic acids have pKa values that rival those of conventional mineral acids and can, therefore, be used in hydrometallurgy but their uses in this regard are not well documented in the literature. In this extensive review, we have covered geological sources of REEs exhaustively in addition to showing the potential of organosulfonic acids as environmentally benign lixiviants for REEs extraction from coal ash. We have also shown how process optimization can be achieved using advanced technologies while using organosulfonic acids. Moreover, we have shown current and future global market trends regarding the production of select organosulfonic acids, and the anticipated global increase in their production motivates the use of organosulfonic acids as viable lixiviants for REEs extraction from coal ash deposits.

Keywords: coal ash; mineral acids; organosulfonic acids; lixiviants; hydrometallurgy; rare earth elements

1. Introduction

Rare Earth Metals (REEs) are a group of chemically similar metallic elements, usually consisting of the lanthanides series and yttrium, and the first extended row of chemical elements below the main body of the periodic table: cerium to lutetium (Pecharsky & Gschneidner, 2023). Their characteristic unsaturated 4f electronic structure accords them such unique properties of luminescence, magnetism, and unique electronic properties suitable for the development of new hi-tech materials (Generalic, 2012). Besides, these unique properties of REEs make them universally acclaimed precursors for the manufacture of products vital for a broad spectrum of industrial uses. Europium, for instance, provides a phosphor for televisions and computer monitors, having no known substitute (Resende & Morais, 2015). Thus, REEs are vital for products related to electronics, chemical analysis, computer screens, automotive catalytic converters, glass polishing and ceramics, permanent magnets, petroleum refining and others (USGS, 2014; Balaram, 2019). Therefore, considering their vital and unparalleled uses as permanent magnets, they are critical and above all, strategic for the global energy transition to environmentally benign energy generation and utilization (IRENA, 2022). Moreover, recognition of over dependence on REEs by automakers has prompted the development of alternatives for permanent magnets (Cambridge-University, 2022) that have poor performance indices, notably a reduction in driving range which is a critical factor in automobile evaluation (Reuters, 2021).

Considering their trivalent charge and similar ionic radii, REEs naturally occur together in the geosphere not individually like gold or copper, but as either minor or major constituents (USGS,2014). However, despite being genetically associated with a wide range of minerals in the paragenetic sense (Silyanov, et al., 2022), economically important sources of REE minerals are bastnaesite, monazite, loparite, and through lateritic ion-adsorption clays. Consequently, there are over 250 minerals which contain REEs as vital constituents in their chemical formula and crystal structure (Dostal, 2017). The global mean value for REEs concentration in the Earth's crust is estimated to be between 150 to 220 parts per million, indicating a higher value than the concentration of other metals mined for industrial uses, such as Cu or Zn (Mission-2016, 2016; Long et al.2016; Sowerbutts, 2013). Normally, an economically feasible source contains at least 5 percent rare earths, except where it occurs with other minerals, such as zirconium, uranium, or iron which justify economic recovery of deposits with concentrations as low as 0.5 percent by weight (Bititannica, 2023). While magmatic rock settings are known to host averagely higher concentrations of REEs, coal deposits are also known to be geologically associated with to them, but their concentrations are relatively lower causing them not to be directly useful. For instance, Vilkavic (1983) (Valkovic, 1983) estimated the total concentration of rare earth elements in coal deposit as 46.3 $\mu\text{g/g}$, with the total concentration of rare earth elements in US coal deposits being reported as 62.1 $\mu\text{g/g}$ (Finkelman, 1993).

The current global supply of REEs from magmatic rock and weathered rock sources (LI & YANG, 2014) is dominated by China, accounting for 63 percent of the world's rare earth mining, 85 percent of rare earth processing, and 92 percent of rare earth magnet production with its supply of REEs alloys and magnets being critical components in missiles, firearms, radars and stealth aircraft (Seligman, 2022). Therefore, considering the enormous strategic importance of REEs, diversification of their sources is the current global focus (Canada, 2014). However, Ilankoon, et al., (2022), have identified 13 factors as constraints to develop REEs supply chains outside China which have been rated by suppliers and experts. Moreover, survey results obtained from the REEs industry experts have been thoroughly subjected to statistical analysis to ascertain key factors affecting the development of independent and supply chains beside the Chinese dominance. Four statistically important factors were identified in addition to constraints relating to business uncertainties (Ilankoon, et al., 2022). Nevertheless, while magmatic deposits are the dominant sources of REEs, their concentrations in coal ash deposits due to combustion induced volume changes have, in recent times, been considered as promising for their extraction (Eterigho-Ikelegbe,2021; Park, et al., 2021; Bishop et al., 2023; Choudhary et al.,2023). In this regard, the average total REE content, consisting of lanthanides, yttrium, and scandium) from Appalachian derived coal ash sources was 591 mg kg^{-1} , significantly greater than that from ashes in Illinois and Powder River basin coals (403 and 337 mg kg^{-1} , respectively). Moreover, the percentage of critical REEs (Nd, Eu, Tb, Dy, Y, and Er) in the fly ashes was reported as 34–38% of the total and considerably higher than in conventional ore deposits, which typically averages 5%. Taggart et al. (2016)..

In another study, it was found that REY are concentrated in fine particle size, non-magnetic and middle density fractions, and using combined physical separation techniques, their concentration in coal fly ash was enriched from 782 $\mu\text{g g}^{-1}$ to 1025 $\mu\text{g g}^{-1}$ (Pan et al., 2020). Currently, there are over 3 *billion tons* of coal ash in landfills and coal ash ponds facilities across the U.S. and over 100 million tons of additional coal ash generated per year (FIBERS, 2023). In Canada, 6% of electricity was generated, using coal combustion in 2020, while electricity generation consumed 18.4 Mt of coal in 2021 (Canada.ca, 2023). In addition, the first thermal power plant based on coal combustion that generated 1 million kW was established in 1954 in Toronto (-Canada, 2022). Therefore, considering the significant proportion that coal combustion accounts for global electricity generation, oscillating around 40% since 2000 (IEA, 2023), coal ash as a resource for REEs will likely be realized in several countries with coal fired power plants.

To technically and economically render global coal ash deposits resourceful for REEs, significant research input in industry and academia on a global basis is essential, and such an initiative will be a stepping stone for greener alternatives to producing REEs (Liu, et al., 2023), given the

environmental pollution associated with conventional mining practices (Zapp et al., 2022; Yin et al., 2021; 2013). Consequently, the scientific literature on the extraction of REEs from coal ash abounds (Seferinoğlu, 2003; Honaker et al., 2019; Dahan, et al., 2022; Prihutami et al., 2021; Pan et al., 2020). While significant breakthrough in research and commercialization of research findings is yet to be realized, intensive research has reported the advantages and shortfalls in light of technical and economic viabilities (Huang et al., 2019; Miranda et al., 2022; Das et al., 2018; Kim et al., 2019). Moreover, the development of suitable chemical and physical extraction process for the extraction of REEs from coal ash draws on knowledge of their occurrence in these ashes. Rather than occurring as individual minerals dispersed in the ash, it has been reported that most REEs are homogeneously distributed in a glassy phases amorphous aluminosilicate matrices (Ward & French, 2005; Pan et al., 2018; Wang et al., 2019). Generally, wet leaching has been the most common technique to extract REEs from coal ash (Tang, et al., 2019; USDE, 2020; Honaker et al., 2019; Imaz & Ottosen, 2022), where acid leaching, based on the application of strong mineral acids at elevated temperatures, is one of the most prevalent ways to extract REEs from coal ash matrix (Franus et al., 2015; Peiravi, et al., 2017). However, strong mineral acids have been found to be highly corrosive to the skin and eyes, which poses occupational health risk (VDH, 2023; National-Cancer-Institute, 2022) (VDH, 2023). Therefore, organic acids are being researched as alternatives for acid leaching in mineral beneficiation (Belfqueh et al., 2023). For instance, Belfqueh et al., (2023) have shown that acetic acid (CH_3COOH) has the highest leaching performance of REEs, allowing leaching yields over 90% for Nd, Dy and Pr in the acid concentration range of 1.6–10 mol/L and the S/L ratio range of 0.5%–5% at a temperature of 60 °C, using NdFeB permanent magnets from end-of-life HDDs of computers. Their results demonstrated not only the efficiency of organic acids, but also their ecofriendly manner. Xiao et al. (2022) have also researched the efficiency of organic acids and mineral acids for leaching in the remediation of protogenetic lead contaminants in soils (Xiao et al., 2022). In their study, hydrochloric and citric acid produced the best results. Therefore, given the toxicity of strong mineral acids, environmentally and health wise, exploring organic acids as potential substitutes is necessary but apart from a most recent research work that documents the potential of Methane sulfonic acid and p-toluene sulfonic acid (PTSA) for REEs leaching from coal ash (Banerjee et al., 2022), the usefulness of organosulfonic acid by the research community has yet to be realized. Herein, we report the potential of organosulfonic acids, notably MSA and PTSA for the leaching of REEs from coal ash. Accordingly, we also report on the potential of these acids for heap leaching of REEs from coal ash. Currently, coal ash is a valuable resource for the construction industry, considering its use as a concrete aggregate (Karala et al., 2022; Mangi et al., 2019; Maliki, et al., 2017). Therefore, in the event of coal ash proving to be a viable resource for REEs extraction, the construction industry will be negatively impacted in terms of the concrete aggregate supply chain involving coal ash. In this regard, our extensive literature review has enabled us to report the applicability of REEs leached coal ash as concrete aggregate after REEs extraction, which is an added advantage of using Organosulfonic acid in place of environmentally toxic mineral acids as lixiviants.

2. Geological Resources of Rare Earth Elements

2.1. Regolith Hosted Deposits

One economically attractive geological resource of REEs is related to regolith deposits. (Borst, et al., Adsorption of rare earth elements in regolith-hosted clay deposits, 2020), that form through ion-adsorption clay (IADs) deposits arising from subtropical weathering processes of igneous rocks, and they are the world's primary sources for heavy rare earth elements (Weng, Jowitt, Mudd, & Haque, 2015), (Jowitt, Wong, Wilson, & Gore, 2017). In these accumulations, the REEs are thought to be weakly adsorbed onto clay minerals, consisting predominantly of kaolinite and halloysite, in addition to oxides, at variable structural sites consisting of broken edge sites, charged aluminol or siloxane groups at defects and isomorphic substitutions (Schoonheydt & Johnston, 2013). Beside these mechanisms, dissolution of nanoparticulate secondary REE-bearing phosphates is a precursor to the formation of deposits (Zhou & Keeling, 2013). Major economically recoverable

IADs occur in Southern China, being hosted in weathered igneous crusts associated with granitic rocks, providing about 35% of China's total REEs production, and roughly 80% of Heavy Rare Earth Element supply on a global basis (Borst, et al., Adsorption of rare earth elements in regolith-hosted clay deposits, 2020). Compared to hard rock deposits associated with carbonatites and alkaline igneous rocks, IADs deposits consist of relatively low tonnages Smith et al., (2016). Economic exploitation of IADs is mostly carried out through low-cost in situ leaching or Heap leaching ((Sanematsu & Watanabe, 2016; Wall et al., 2017) resulting in significant environmental impact in China (Yang et al., 2013). Generally, the majority of IADs are readily leachable deposits. As mentioned earlier, hard rock deposits of primary geological origins account for sizable global production and supply (Verplanck et al., 2016) and the following section will be devoted to reviewing their origin, global production, and current supply status.

2.2. Rare Earth Elements from Carbonatites

Carbonatite-hosted rare-earth-element (REE) occurrences (Wang et al., 2020) with notable Cenozoic deposits in China constitute the most significant source of the world's REEs supply albeit their geologic processes of origin still remains obscure (Hou et al., 2015). These deposits occur as stock-works of dykes associated with syenites, being extremely rich in Barium, Strontium and REEs (Shunda et al., 2008) and showing the ratio of the isotope of Strontium 87 to that of Strontium 86 above 0.7055n (Hou et al., 2015). Genetically, these carbonatites were likely formed by melting of the sub-continental lithospheric mantle which had previously undergone metasomatism (Chikanda et al., 2019) characterized by high-flux of REEs and carbon dioxide rich hydrothermal fluids derived from subducting marine sedimentary environments (Wang et al., 2021). Generally, monazite is the most important source of REEs in carbonatites, and this has been demonstrated in relationship to the Kangankunde carbonatite Complex (Zhou et al., 2017). Globally, carbonatite deposits have resulted in 53% of global projects while 86.5% of active mines are centered on them (Lin et al., 2023). Apart from ion adsorption clay deposits and carbonatite source related ones; there are several minor but economically important deposits on a global basis, the distribution of which can be represented by the following Figure 1., while Figure 2 shows major world producers of REEs.

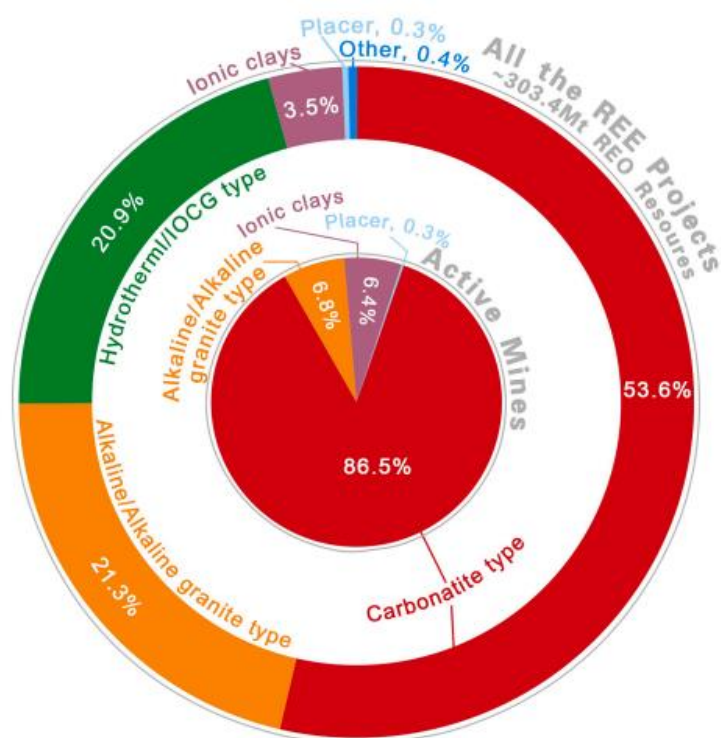


Figure 1. The proportion of different types of REE resources. The outer ring chart represents all the REE projects. The inner pie chart represents the active mines. It is the proportion of resources rather than the number of projects (Liu et al., 2023).

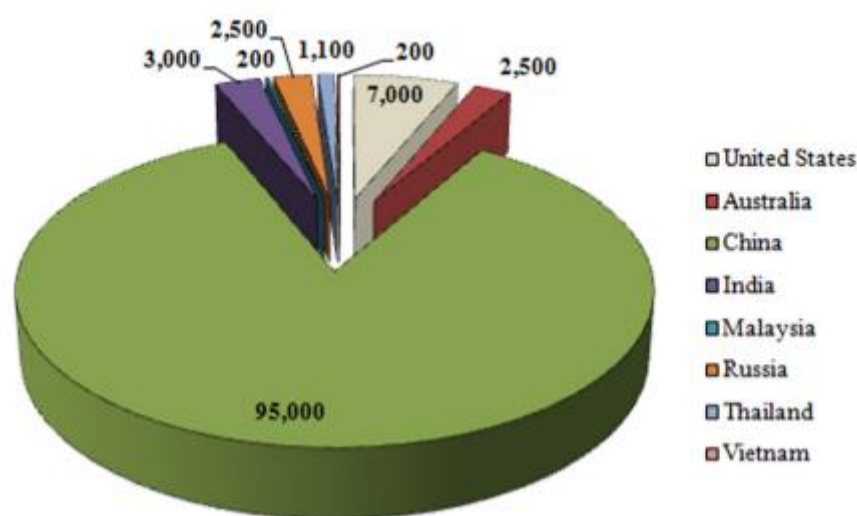


Figure 2. Global mine production of rare earth metals in different countries (USGS, 2015).

It is obvious from Figure 1 that next to carbonatites resources, Alkaline /granitic types deposits provide significant resources for active mine development, followed by ion adsorption type.

2.3. Primary sources of REEs in Geologic Systems

Similar to the concept of paragenesis (Yan, et al., 2022) in ore deposits, REEs occurring in crusts as mixtures in magmatic rocks, such as granites, gneiss, basalts and in sedimentary rocks (Krishnamurthy & Gupta, 2015). Generally, REEs have strong affinity for oxygen, which cause them to exist predominately in the trivalent states as cations associated with carbonates, oxides, phosphates, and silicates (Hedrick, 1992). Literature show that nearly 95% of all REEs resources occur in only three minerals, namely monazite ($(\text{Ce, La, Nd}) \text{PO}_4$), bastnasite ($(\text{Ce, La, Y}) \text{CO}_3\text{F}$), and xenotime ($(\text{Y, Yb}) \text{PO}_4$), being the main sources of REEs in the paragenetic sense (Cotton, 2006). The concentration of REEs in these principal sources vary. For instance, in monazite, the rare earth oxide (REO) concentration ranges between 35 and 71%, while in xenotime and bastnasite it ranges between 52 and 54% and between 70 and 74%, respectively (Kanazawa & Kamitani, 2005; Jordens et al., 2013) (Kanazawa & Kamitani, 2005). The following text summarizes the characteristics of each principal source of REEs.

2.3.1. Bastnasite

This is a fluorocarbonate mineral containing approximately 70% rare earth oxide in the form of Light REEs, being the principal source of most REEs. This source of REEs is easier to treat compared to other sources (Jordens et al., 2013; Ozbayoglu, 2000; Huang et al., 2005). Bastnasite is genetically associated with vein deposits, metamorphic zones, igneous carbonatites deposits, being the principal ore of the most giant REEs mines. Typical of such mines are the Mountain Pass, USA and the Bayan Obo mine in China (Gupta & Krishnamurthy, 1992; Gupta and Krishnamurthy, 2005). La, Ce, Pr and Nd are the most abundant elements of Bastnasite (See Figure 3). In the hydrometallurgical context, Bastnasite is processed by numerous operations, which include gravity and magnetic separation to produce intermediate rare earth concentrates, which are further processed through solvent extraction and selective precipitation.

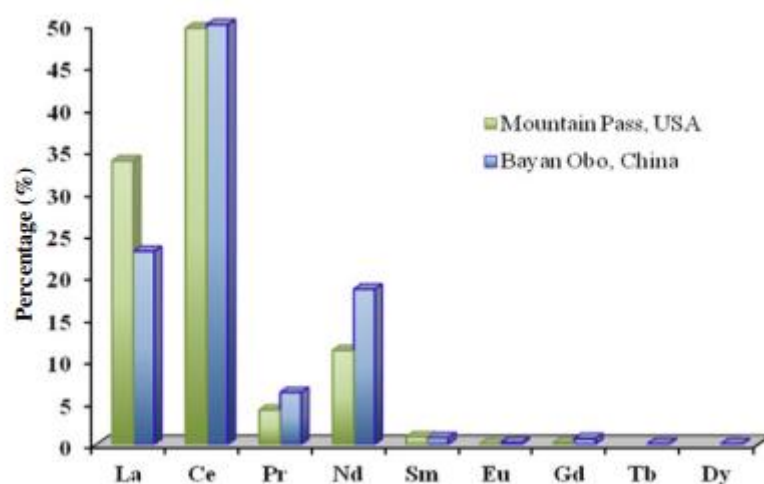


Figure 3. Distribution of REEs in Bastnasite (Chen, 2011; Jordens et al., 2013).

2.3.2. Monazite

Monazite is a designated REE phosphate mineral. It is the principal sources of Light Rare Earth (LREEs) (Kumari, Panda, Jha, & Kumar, Process development to recover rare earth metals from monazite mineral: A review, 2015). Monazitic sources of REEs are characterized by high proportions of radioactive thorium, normally (4–12 wt.%) with variable amount of uranium and these characteristics underscore the environmental hazards associated with mining such deposits. Globally, beach sands are the predominant sources of monazitic sands from which REEs are sources (Saha et al., 2023; Kumari et al., 2015) (Saha, Eliason, Golui, Masud, Bezbaruah, & Iskander, 2023).

2.3.3. Xenotime

Xenotime is the principal source of REEs oxides, which are the sources of yttrium and HREEs (Alex, Suri, & Gupta, 1998). Granites, crystalline metamorphic rocks, and pegmatite deposits are the principal sources of xenotime (Amli, 1975). Ore beneficiation is carried out using flotation, magnetic or gravity separation methods followed by hydrometallurgical or pyrometallurgical processes (Dinh et al., 2022).

3.4. REEs Resources of Coal Derived Ashes

REEs occur in coal deposits (Lia et al., 2008; Scott & Kolke, 2019)), but with low concentrations for commercial exploitation (Valkovic, 1983). For instance, the concentrations found in coal deposits, on average, barely approach levels judged commercially viable when extracting the rare earths alongside another mineral (Ekmann, 2012). These elements occur in clay phases mainly as sorbed forms (by organic matter and clay particles) and fine-grained authigenic minerals (Seredin et al., 1996; Birk & White, 199; Zhang et al., 2018) associated with coal deposits. Normally, combustion of coal under different conditions results in the concentration of REEs in feed coal ash due to imminent volume changes, Taggart et al., 2016), with concentrations reaching 33 ppm Maity et al., 2022) and 400 ppm (Dugin et al., 2022). However, while coal deposits generally contain lower concentrations of REEs, coal seems containing 300 to 1000 ppm REEs have been reported in some Russian Far East deposits (Seredin et al., 1996). Geochemically, REEs can be classified into two groups, namely light (LREE, from La to Gd) and heavy (HREY, from Tb to Lu), this distinction being based on their atomic number (Jordens et al., 2013). Moreover, based on the abundance and utilization prospects, they can be further categorized as critical (Y, Nd, Eu, Tb, Dy, Er), excessive (Ce, Ho, Tm, Yb, Lu), and uncritical (La, Pr, Sm, Gd) as suggested (Seredin & Dai, 2012). In the following sections, we will focus on coal

ash geochemistry, current research for extracting technical REEs from coal ash deposits on a commercial basis and the challenges so far, using hydrometallurgical routes.

3.5. The Chemistry of Coal Ash

3.5.1. Major Oxides of Coal Ash

The major components of coal ash consist of oxides of Si, Fe, Al, and Ca, and residual carbons with bottom and fly ashes containing 185.8 mg/kg and 179.2 mg/kg of REEs, respectively (Park, et al., 2021), (USDT, 2016). The following Table 1 shows the major oxides of coal fly ash (Hauashdh et al., 2020) while Figure 4 shows trends in coal ash generation based on statistics data from six energy-intensive economies.



Figure 4. Indicators of generation and disposal of CFA in the developed countries (Dmitry et al., 2022).

Table 1. Major oxides of bottom and fly ash (Hauashdh et al., 2020).

Chemical composition %	Fly Ash	Bottom ash
SiO ₂	44.40	48.00
Al ₂ O ₃	27.50	26.60
CaO	11.50	8.73
Fe ₂ O ₃	6.21	8.51
TiO	1.79	1.95
MgO	2.36	1.76
K ₂ O	0.99	1.05
P ₂ O ₅	1.37	0.45
SO ₃	1.01	0.25
Na ₂ O	1.38	0.84
BaO	0.42	0.28

Three types of REY occurrences in coal ash can be identified as, Si-Al glassy association, discrete minerals or compounds, and organic association (bound with unburned carbon), with glassy association occurring through binding to the glass an also as a dispersion throughout the glassy structure (Fu et al., 2022). Discrete phases are inorganic in nature, occurring as phosphorus in coals, especially in higher rank coals (Buchill al.,1990). The phosphorus-containing mineral phases in coals include: apatite, most (Swaine, 1977); crandallite-series minerals; monazite; and xenotime (Finkelman, 1980), including phosphates, dispersed throughout the organic matrix, as important sites for trace elements in coal. Therefore, acid digestion method widely used in mineral processing for the analysis of mineral contents (Palm et al., 2015) is an ideal choice as one of the methods for determining the REEs potential of coal ash deposits as has been used for apatite/phosphate based REEs ores (Kim et al., 2016)..

3.5.2. Trace Elements of Coal Ash

Coal ash also contains minor amounts of trace elements, such as chromium (Cr), nickel (Ni), zinc (Zn), arsenic (As), selenium (Se), cadmium (Cd), antimony (Sb), mercury (Hg), and lead (Pb). uranium (U) can also be a common trace element occurring at concentrations ranging from 10 to 30 ppm, similar to the upper limit of concentrations found in a naturally magmatic rock such as granite and the sedimentary rock known as black shale (Zielinski et al., 2007). The presence of trace elements in coal ash is directly linked to their occurrence in coal during the process of its formation in the sedimentary environment (Raask, 1985; Gluskoter et al., 1997; Sorokin et al., 2019). The concentrations of these trace elements increase, following the reduction in volume accompanying the combustion process. Therefore, their concentrations, measured as parts per million (ppm) in coal derived ash are higher compared to background concentration in the original coal samples (Carlson & Adriano, 1993); Jankowski et al., 2006).

3.6. Natural Evidence of REEs Leaching from Waste

Canada, for instance, is one of the world's leading producers of economic minerals. The mining of base and precious metals results in the production of immense quantities of waste rock, mill tailings, and waste related to refining processes Moncur,2023). Consequently, the generation of acid mine drainage (AMD) and the resulting release of water containing substantial concentrations of metals from mine wastes has long been proven to pose environmental problems on a global scale (Luís, et al., 2022). AMD is caused by the oxidation of sulfide minerals in the mine waste that occurs when these materials are exposed to atmospheric oxygen oxidation processes that continue to release acid and metals to the surrounding environment for decades to millennia (Moncur et al., 2005). Therefore, evidence of natural leaching of metals from waste piles is a motivation for the drive towards the adoption of acid leaching as a potential route for the recovery of rare earth elements from coal ash as it substitutes for the waste encountered in the case of mining (Banerjee et al., 2022; Pan et al., 2021; Honaker et al., 2019; Banerjee et al., 2023).

3.7. Hydrometallurgical Profiles of Conventional Mineral Acids

In hydrometallurgy, Sulfuric acid is by far the most widely used in leaching metals from their ores, in addition to being the acid of choice in electrolytes for the electrowinning and electrorefining of metals (Free, 2013). The acid possesses several advantages that motivate its extensive use in hydrometallurgy. The following summarize its benefits ((Binnemans & Jones, 2023):

It is abundant through large scale production, which drive lower cost, rendering it the topmost chemical in terms of quantity produced by the chemical industry.

Metallurgical plants produce their own sulfuric acid from the sulfur dioxide that is released during the roasting of sulfur-based ores in hydrometallurgical units.

- Its less corrosive nature gives flexibility in the choice of materials for the building of process units.
- The use of sulfuric acid comes with no concern for odor and volatility of toxic gases. Moreover, electrowinning processes based on sulfuric acid electrolytes have the advantage that oxygen gas is formed at the anode.

While the above mentioned qualities underscore the benefits of sulfuric acid in hydrometallurgy, metal sulfate salts have a relatively low solubility in aqueous solutions compared to chlorides and nitrates salts, with lead and calcium sulfate being insoluble. This limitation in aqueous solubility poses a problem in hydrometallurgical processes related to these metals. Beside, calcium sulfate scaling is a problem. In addition, experience has revealed that the relatively low solubility of $\text{CuSO}_4 \cdot 5\text{H}_2\text{O}$ in sulfuric acid solutions sets a limit to the maximum copper concentration, causing an inefficient electrowinning and electrorefining of the metal (Schlesinger, King, Sole, & Davenport, 2011).

Consequently, the solubility limitations of metal sulfates in hydrometallurgy has inspired the development of nitrate (Demopoulos et al., 2008) and chloride hydrometallurgy, where the former has more solubility. However, while metal chloride salts are generally more soluble than sulfate salts, there exist poorly soluble ones like Lead and Silver. Due to the corrosive nature of chloride solutions there exists a limitation to the choice of material for hydrometallurgical units. Another shortfall of chloride hydrometallurgy stems from the fact that chloride gas evolves at the anode instead of oxygen gas, which is corrosive. Nitrate reduction at the cathode is also a problem associated with the use of nitrate salts in electrolysis.

Considering the hydrometallurgical application limitations of conventional mineral acids, viable options that come with less concern for environmental toxicity and process unit corrosion are essential, and that is where Organosulfonic acids come in, and the following sections will be devoted to reviewing the potential of such acids and their salts in the recovery of REEs from coal ash. Already, evidence exists for the use of Methanesulfonic acid as a sustainable acidic solvent for recovering metals from the jarosite residue of the zinc industry (Palden et al., 2019) as for its use in hydrometallurgical processes related to several metals (Binnemans & Jones, 2023).

3.8. The Potential of Organosulfonic Acid

Organosulfonic acids are a member of organosulfur compounds of sulfonic acid (et al., 1941) with an organic functional group substitution and it is a derivative of sulfonic acid, (Scientific, 2023). Already, the potential of Organosulfonic acid-functionalized mesoporous silicas as a catalyst for the esterification of fatty acid has been demonstrated (Mbaraka et al., 2003; Chen et al., 2021). Sulfonic acid derivatives have also been used in cosmetics (Newsted & Jones, 2005). In petroleum production engineering, the use of ester derivatives of sulfonic acids as anti-sludge agent during acidization of petroleum reservoir formations has been reported (Looney & McDougall, 1984). In the field of mineral beneficiation, while other organic acids have been researched as potential leaching acids for coal, the use of Organosulfonic acids is less documented. Recently, Banerjee et. al. (2022) investigated the leaching efficiency and potential of Methanesulphonic acid and *p*-toluenesulphonic acid in the extraction of REEs from coal ash, where they showed that the optimum condition for extraction was 90°C and process duration of 60 min

using a liquid to solid ratio of 100 and a stirring speed of 600 rpm. Accordingly, using 0.5 M acid concentration Light REEs were leached out with extraction yield of 65-70% whereas Heavy REEs has a leaching yield of 12-20%. Their study further demonstrated, based on X-Ray diffraction analysis that Organosulfonic acids did not destroy the aluminosilicate matrix of coal ash and that the kinetics of leaching was diffusive, following the shrinking core model. They concluded that the leaching potential of Organosulphonic acid is comparable with those of mineral acids (HNO_3 and HCl), demonstrating its potential as a green alternative to mineral acids which are conventionally widely used in REE extraction from coal ash wastes.

Spent catalysts can pose environment and human health if poorly managed. To mitigate the problems, novel environmentally friendly flowsheet based on deep eutectic solvents (DESs) have been developed to enhance nickel recovery from spent hydroprocessing catalysts. In this regard, P-toluenesulfonic acid-based DES-1 (PEG-400: PTSA) and DES-8 ($\text{ChCl}:\text{EG}:\text{PTSA}$) has been shown to enhance high nickel extraction (>90 %). from spent hydroprocessing catalysts via deep eutectic solvents (Ebrahimi et al., 2023).

3.9. Properties of Methane Sulfonic Acid

Methanesulfonic acid (MSA, Figure 5) is usually described as a “green acid” due to its environmental benefits (Gernon et al., 1999; Kulkarni, 2025). Its molecular structure is characterized by two sulfur to oxygen double bonds. It is a strong organic acid ($\text{pK}_a = 1.9$) with a low potential for oxidation of organic compounds, having a melting point around -55°C and high thermal stability, and these qualities render it applicable as a liquid over a wider temperature range.

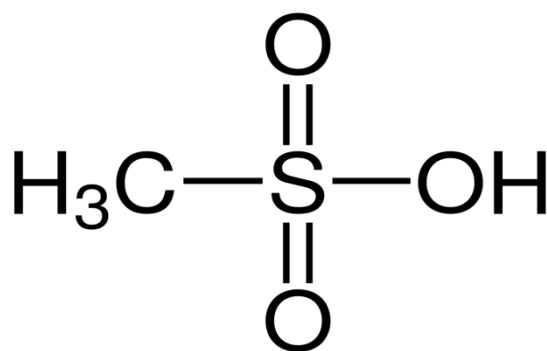


Figure 5. Molecular structure of methane sulfonic acid.

Under normal atmospheric conditions, its aqueous form is odour-free, due to its low vapor pressure, with no tendency to evolve dangerous volatiles, making it safe to handle. Its salts are characterized by high solubility, which makes it suitable for use in cleaning applications, such as removal of calcium carbonate scale. MSA is far less corrosive and toxic than the usual mineral acids employed in diverse industrial processes including hydrometallurgy (Martyak & Ricou, 2004). A cost-effective and efficient solid Brønsted acid catalyst was synthesized by loading Methanesulphonic acid (MSA) on silica, and used for the acid-catalyzed Pechmann reaction meant for investigating the catalytic activity and reusability. Accordingly, derivatives of 4-methylcoumarin were successfully synthesized with good yields, using short reaction times in the presence of environmentally friendly higher *n*-alkanes as solvents (Joshi et al., 2011). Currently, MSA is used extensively in areas related to catalysis/reagent for organic reactions including the production of biodiesel, in the pharmaceutical industry, as a solvent for high molecular polymeric materials (Roitman et al. 2004), in cleaning fluids and removal of rust (Lafitte & Monguillon, 2013), and for pipe descaling in the downstream petroleum industry (Bertkau et al., 2015).

The sulfonic acid group is highly polar (Liu et al. 2007) and it can greatly enhance the water solubility of compounds as seen with the sulfonic acid derivative of triphenyl phosphine (TPPTS). Its metal complexes are used as homogeneous catalysts for the syntheses of organic compounds in a two-phase-organic water systems. Considering this extensive application at industrial and domestic

scales, the annual production is projected to increase above 50,000 tons (Ewe & Scheible, 2017) and a recent environmental assessment of alternative Methanesulfonic acid production using direct activation of methane will likely give impetus to its production (Kappenthuler et al. 2018).

4. Use of Organosulfonic Acid Derivatives in Extractive Metallurgy

In the context of thermodynamics and electronic structure, REEs are located in the sub-group of periodic table. Because of the unique 4f-electronic configuration, their inner layer has a strong shielding effect on the outer layer and the atomic nucleus of RE elements is less attractive to electrons of the outer layer, causing them to be active metals. The standard equilibrium electrode potential of the electrode reaction of the 15 elements (from La to Lu) is -2.52-2.25 V (Zhou et al., 2021). This thermodynamic aspect of the REEs makes their recovery by electrolysis as attractive as by other hydrometallurgical process and the use of highly soluble RREs salts will be an advantage for their electrolytic recovery.

4.1. Solubility of REEs Organosulfonate Salts and the Potential for Their Recovery by Electrolysis

MSA has toxicity that is relatively lower compared to many commercially available acids, having a LD₅₀ (oral, cat) of 1158 mg kg⁻¹ compared to 238–277 mg kg⁻¹ for hydrochloric acid (Springborn-Laboratories, 1997). It is highly biodegradable, producing sulfate and carbon dioxide (Thompson et al., 1995), 1995 degradation products, and part of the natural sulfur cycle. MSA is considered to be a natural product, and it is part of the natural sulfur cycle (Baker et al., 1991). MSA is a strong acid, having a pK_a value of -1.19 which is close to those of mineral acids, viz nitric acid (pK_a = -1.3) and sulfuric acid (pK_{a1} = -3) and higher than those of conventional organic acids, such as formic acid (pK_a = 3.82), acetic acid (pK_a = 4.76) and citric acid (pK_{a1} = 3.09) (Rappoport & Patai, 1991).

Recovery of metals based on the electrolysis of their molten salts is an established practice in metals recovery from their corresponding salts (Li, et al., 2021; Xi et al., 2020; Oishi et al., 2010; Li et al., 2023). Moreover, in the recovery of REEs, their molten salts have been employed in electrolysis (Oishi et al., 2010; Joo et al., 2020; Yang et al., 2023). In the research work of Joo et al., (2020), Amperometry electrodeposition experiments were performed between, using variable voltages to recover REEs over the Ni sheet. Recovered REEs were fully characterized using scanning electron microscopy, energy dispersive X-ray spectroscopy, Fourier transform infrared spectroscopy, X-ray photoelectron spectroscopy, and photoluminescence spectroscopy.

However, while metal recovery using molten electrolysis is beneficial and efficient, the energy cost is substantial (Thonstad, 1990; Yan & Fray, 2010). One principal driver of the hydrometallurgical electrowinning of a metal is the solubility of its salts which maximizes extraction. The application MSA derivative in the form of REEs-Organosulfonates has the potential to produce salts that will maximize their electrolysis recovery due to the use of the parent strong acid. Besides, its use is encouraged by its non-oxidizing nature, high conductivity and the excessively high solubility of methanesulfonate salts in water (Florence et al., 2011). Consequently, the averagely high solubility of its salts is an incentive for the use of RREs sulfonates for their electrolysis based recovery.

5. Process Optimization

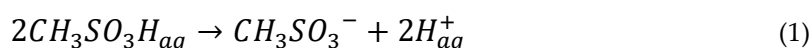
5.1. Hydrometallurgical Aspects

Organosulfur acids contain a functional group characterized by a sulfur atom doubly bonded to two oxygen atoms (See Figure 5), a hydroxyl group, and a carbon atom of any hybridization (Anderson et al., 2014a). The recovery of metals in general by acid leaching is a well-established hydrometallurgical route, both circular (Binnemans & Jones, 2023b) and non circular in nature (Xie, et al., 2023), where reagents regeneration is possible and where it is not possible, respectively. The sulfonic acid moieties are effective hydrophilic molecular components (Ohtake et al., 2022) and this, coupled with the high solubility of its salts and ease of proton donation (Alaba, Sani, & Daud, 2016) has inspired recent applications of its organic derivatives metal leachants in hydrometallurgy

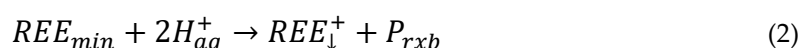
((Binnemans & Jones, 2023a). For instance, the unique chemistry of the sulfonic group has inspired its application for several industrial processes, such as organosulfonic acid functionalized montmorillonites as solid catalysts for transesterification of free fatty acid and waste (Silva et al., 2020) and highly active organosulfonic aryl-silica nanoparticles as efficient catalysts for biomass derived biodiesel and fuel additive (Peixoto, et al., 2021). Moreover, in line with the exponential demand for RREs to fuel the globally anticipated energy transition to environmentally benign and sustainable energy supplies, their recovery from industrial wastes has been proven to be technically feasible (Elbashier et al., 2021; Castro et al., 2021; Binnemans et al., 2016; Gulliani et al., 2023; Kozakiewicz et al., 2019; Brahim et al., 2022) (Elbashier, Mussa, Hafiz, & Hawari, 2021). The following sections will be devoted to the roles organic derivatives of sulfonic acids in REEs extraction from coal ash.

5.2. Recovery Using Methane Sulfonic Acid (MSA)

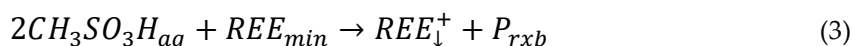
In light of non RREs extraction, the potential of MSA has been explored through research. In this regard, in the recovery of lead and silver from zing leaching residue, MSA has been found to have a proven hydrometallurgical potential (Rodriguez, Onghena, & Binnemans, 2019) as has its potential for the leaching of silver granules (Hopf, Weigelt, Bombach, Stelter, & Charitos, 2021). The detailed chemistry of metal leaching by MSA is described by the following equations (Feng et al., 2015):



Equation (1) refers to the dissociation of MSA in aqueous solution. The dissolution is then given as:



In Eq. (2), REE_{\downarrow}^+ is RRE ion in the aqueous phase and P_{rxb} is the sum of reaction byproducts. Using Eq. (1) and Eq. (2), the total dissolution reaction gives:



Therefore, based on Eq.(1) through Eq.(3), MSA provides the leaching potential characteristic of traditional mineral acids for the recovery of REEs from coal ash deposits, considering its low toxicity, which does not necessitate the choice of specific equipments to mitigate corrosive degradation in hydrometallurgy extraction of metals.

The most recent demonstration of REEs extraction from coal ash using MSA has been published (Banerjee et al., 2022). In this research work, two organosulfonic acids (MSA and PTSA) were selected for performance comparison. Prior to their study, leaching of REEs from lamp phosphor using high concentrations of MSA had been reported (Gijsemans et al., 2018; Palden et al., 2019; Rodriguez et al., 2021). Therefore, the prime objective of Banerjee et al. (2022) was to explore optimum leaching using lower acid concentration ranging from 0.025 M to 1.5 M for both toluene sulfonic acid and MSA. Results of the two structurally different organosulfonic acids in coal ash leaching based on Banerjee et al. (2022) can be summarized as follows:

- Using 1 M MSA, close to 70% of REEs can be leached from coal at 90 °C in one hour. With minimal (<10%) prominent coal ash minerals being leached.
- Using optimum experimental conditions PTSA showed only 60% leaching efficiency with 0.5 M concentration.

5.3. Optimization of Coal Ash Leaching Using Oxidative Assisted Leaching Methodology

The principal mechanism of leaching using MSA is through complexation reactions mediated by a bidentate ligand (Aricó et al., 1997). Moreover, the complexation reactions of lanthanides with PTSA, on the other hand, is known to be complicated, varying with the type (Parac-Vogt & Binnemans, 2004). Therefore, considering the geochemical variability and complexity of coal ash, it falls within the class of difficult-to-leach ores (Kopecky et al., 1986; EL-Bar & Barkat, 2018). Detailed analysis of coal ash review its geochemical complexity (Anggara et al., 2020; Riddell, 2020).

Experience from hydrometallurgical processes show that some ores are difficult to acid-leach without reductants due to their complexities (Zheng et al., 2023; Xin et al., 2022). For instance, compared to copper minerals, cobalt minerals are generally difficult to leach without a reductant. The problem arises due to the fact that some cobalt present in both sulfide and oxide minerals is in the trivalent state, CO^{+3} , with low solubility in aqueous solutions, resulting in a lower rate of leaching. Therefore, to optimize the leaching process, a reductant is usually added to the leaching reactors to reduce CO^{+3} to CO^{+2} (Chong et al., 2008; Ferron, 2008)).

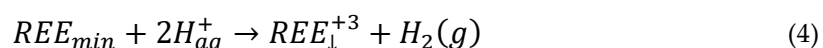
Hydrogen peroxide is one of the most powerful and commercially available oxidizing agents with a standard reduction potential of 1.76 V for the reaction (Nicol, 2020).

However, a detailed literature review shows that its used in connection with oxidative leaching of metals has been mostly associated with the leaching of sulfide ores (Balaz & Ebert, 1991; Gosch et al., 2008; Pecina et al., 2008; Taylor et al., 2015; Adebayo & Olasehinde, 201).

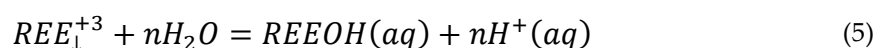
MSA is a non-oxidizing acid. However, its mixtures with hydrogen peroxide have demonstrated strong oxidizing potentials which can be used to dissolve difficult-to-dissolve non-REEs related ores (Zhang, Xiaojiao, et al, 2020; Zhang et al, 2017). This advantage can be exploited for REEs leaching from coal ash.

5.4. Potential for Oxidative Dissolution of REEs in Hydrogenated Hydrothermal Solutions

Different kinds of ore deposits have been associated with submarine hydrothermal systems (Halbach et al, 1993; Ishibashi et al., 2015 (Halbach, Pracejus, & Maerten, 1993), hosting Zn–Pb-rich sulfide ore, Ba–Zn–Pb sulfide ore, massive Zn–Cu-rich sulfides. Moreover, evidence abounds for the leaching of metals from rocks adjacent to conduits for hydrothermal transport (Goldfarb & Marsh, 2010). For instance, Fuchida, et al. (2017) (Fuchida, et al., 2017) have determined the leaching potential of metals (Zn + Pb, As + Sb, and Zn + Cu) and metalloids from four hydrothermal ores collected from the Okinawa Trough into aerobic seawater in addition to evaluating the toxic nature of the leachates phytoplanktons. The geochemistry of the leaching reactions can be summarized as follows (Ziemniak et al., 2007):



Eq. (4) is followed by a sequential hydrolysis reaction as:



Reaction 5 is followed by the addition ammonia to form metal complexes reaction as follows:



Reaction 6 requires excess ammonia addition (Reinhardt, 1998). REEs extraction can then be achieved by solvent extraction, using non aqueous methods (Wang et al., 2018; Amjad et al., 2022).

In the research work of Ziemniak et al., (2007), solubility measurements were made using the flowing autoclave while the feed tanks, pump, filter holder, and tubing between the feed tanks and autoclave were of stainless steel. Other features of their experimental set up show that it can be adopted for research of REEs extraction based on the Hydrogenated Hydrothermal Solutions approach.

5.5. Optimization of Leaching Process: Microwave Assisted Option

In conventional mining and metal extraction from ores, **mineral processing** involves the liberation and concentration of economical metals and minerals from ores (Lottermoser, 2010), where an aspect known as comminution involves the reduction of ore sizes to facilitate easy metal leaching/extraction. Experience from the mining industry has shown that the industry is energy intensive, with comminution by grinding being responsible for consuming about 40% of the energy in the whole mining chain. Moreover, Inefficiency in grinding has proven to be an outstanding problem, this being augmented where the production of fines and ultra-fines are the

main objectives. Therefore, to reduce energy intensity of process units, the mining industry has shifted the comminution process towards the crushing (MEI, 2018). In hydrometallurgy, the microwave assisted leaching of metals from ores was introduced decades ago (Al-Harashsheh & Kingman, 2004), with researchers demonstrating experimentally that microwave technology has great potential to improve the extraction efficiency of metals by reducing leaching time while increasing time recovery of valuable metals. Research experience shows that the application of Microwave-Assisted Leaching (MAL) does not require additional milling to reduce particle sizes for efficient leaching. The microwave-assisted leaching experiments for REEs leaching can be performed in a Milestone Flexi-Wave laboratory set-up, equipped with 2 magnetrons (950 W) designed to provide an overall power of 1.8 kW at a 2.45 GHz frequency (Suoranta et al., 2015). Wouter et al., (2021) have demonstrated experimentally that a 6 M HCl has remarkable dielectric properties and a suitable oxidation environment (Atia et al., 2021). Atia et al. (2021) have reported the metal leachability as high as $104\pm3\%$ for Ce using this kind of MAL approach.

Microwave heating of dielectric materials lies in the ability of an electric field to polarize the charge of the material where polarization is unable to follow the rapid change of the electric field (Metaxas & Meredith, 1998). To optimize acid leaching using microwave assisted technology, the porosity of coal ash particles can be increased by as follows:

In geologic systems, evidence of thermal pressurization has been cited as one of the principal causes of overpressure (Barker, 1972; Zhifeng et al., 2016; Shi & Wang, 1986). In this regard, the differential thermal expansion mismatch between pore water and rock grain is the principal cause of pressure development in geologic porous systems. Therefore, to optimize the leaching efficiency of coal ash using microwave heating technology, coal ash can be made to imbibe water prior to heating. The idea is to cause the faster thermal expansion of water in ash particles against the slower expansion of the latter to induce multiple cracking which can even generate fines. Under such conditions cracking occurs when stresses are induced in materials by restraint to deformation imposed by adjacent materials (Baker, 1964).

5.6. Enhance Lixiviant Diffusion due to Microwave Assisted

In porous systems, transport by advection is dominated by high porosity and permeability systems while in low porosity systems, diffusion transport mechanism persists (Shena, Shen, & Chen, 2007). Detailed characterization of coal ash particles based on surface area measurements and morphological studies of different sizes of samples reveal that small ash particles are predominately nonporous spheres with irregular surface morphology (Schure, Soltys, Natusch, & Mauney, 1985). The leaching kinetics studies under varying experimental temperature conditions concluded that the process of acid leaching of REEs from coal ash is diffusion controlled (Banerjee et al., 2023, in addition to following the shrinking core model 9 Pritzker, 1996; Rahimi et al., 202). In addition, activation energies obtained from the kinetic studies of acid leaching of REEs from coal ash, backed by Scanning Electron Microscopy combined with X-ray Dispersive analysis confirm the diffusive nature of the leaching process (Shopper, et al., 2023). The leaching potency of organosulphonic acid was found to be at par with mineral acids (HNO_3 and HCl), and hence it could be considered as a green alternative to mineral acids which are conventionally widely used in REE extraction from coal ash wastes (Banerjee et al 2018).

In sediments, or in any porous systems, the presence of solid particles causes the diffusion paths of species to deviate from straight lines, causing lower diffusion rates. To show the role of porosity on diffusion in porous systems, the effective diffusion coefficient has been scaled with porosity (Peng et al., 2012) and tortuosity (Yong et al., 2014). The relationship between effective diffusivity in biologic porous systems (Backer & Baron, 1993) and in sediment porous systems (Boudreau, 1996; Epstein, 1989; Tjaden et al., 2016)) have been correlated with a porosity-tortuosity factor. Meanwhile, the relationship between tortuosity, porosity and shape factors is given (Du Plessis & Masliyah, 1991), based on analytical model from an idealized granular pore microstructure. It reads:

$$\tau = 1.23 \frac{(1 - \theta)^{4/3}}{\xi^2 \theta} \quad (7)$$

In which is tortuosity[-], θ is the porosity of sediment[-] and ξ is the shape factor [-].

To account for the effect of sediments porosity and tortuosity on effective diffusivity, the following equation shows the effect of combined tortuosity and porosity and diffusivity (Boudreau, 1996; Epstein, 1989; Tjaden et al., 2016):

$$D_{eff} = D_0 \frac{\theta \delta}{\tau_d^2} \quad (8)$$

In which D_{eff} is the effective diffusion coefficient[m²s⁻²], D_0 is diffusion coefficient in air[m²s⁻²], and δ is the constriction coefficient due to the variation of pore diameter along the diffusion pathway, with a value depending on the ratio of the solute to the pore diameter.

Equation (7) permits prediction of the effect of tortuosity and porosity on acid diffusion coefficient during organosulfur acid leaching of coal ash following the application of microwave assisted leaching. Thus, the effect of microwave assisted leaching is to induce more fracturing of coal ash particles in addition to producing more fines. The net effect is an increase in porosity. Tortuosity is defined as the effective flow path divided by the total flow path available in a porous system (Cai et al., 2017). From Eq. (7), porosity increase translates to practically reducing tortuosity for a given shape factor. Therefore, from Eq. (8), the net effect of microwave assisted activation of coal ash is to increase effective diffusivity in acid leaching, which enhances efficient REEs leaching from coal ash.

5.7. Optimization of Acid Leaching Process by Reducing Acid Consumption

5.7.1. Triboelectrical Technology Option

The quality of coal ash used for concrete is determined by the loss on ignition (LOI) which (Ngo, Huynh, Le, & Mai, 2018), which measures the carbon content (Vandenberghe, et al., 2010). Therefore, coal ash is a major carbon flux that poses environmental hazards (Li et al., 2021). Consequently, ASTM standards exist for the limit of LOI regarding the use of coal ash for concrete works (ASTM, 2017). In hydrometallurgical processes involving acid leaching, the consumption of reagents other than for leachable target minerals is a common occurrence, which increases extraction cost. To optimize acid leaching while reducing processing cost, the carbon content of coal ash must be reduced to the barest minimum where the LOI is excessively high. Two known methods exist for decarbonization of coal ash, namely thermal and triboelectrical approaches. In the triboelectrical approach, coal ash is fed into a thin gap between two parallel planar electrodes in the separation process unit (Baker et al., 2022). The particles are triboelectrically charged via interparticle contact, causing the positively charged carbon and the negatively charged mineral to be attracted to opposite electrodes. The particles are then transported up by a continuous moving belt in opposite directions towards the opposite ends of the separator. In the triboelectrical method, the high belt speed enables very high throughputs which can lead to 36 tons per hour on a single separator. By regulating pertinent process parameters, such as belt speed, feed point, and feed rate, the concrete/aggregate industries have demonstrated that the method can produce low LOI fly ash at carbon contents of less than 1.5 to 4.5% from feed with LOI ranging from 4% to over 25%. Therefore, this technology of beneficiation can be put to use to substantially reduce the carbon content of coal ash, which will reduce acid consumption in the leaching phase of REEs extraction from coal ash.

5.7.2. Thermal Decarbonization Option

In this method, the carbon content of coal ash is reduced by heating to temperatures in excess of 500°C (Shen & Zeng, 2021; Badenhorst et al., 2019). To reduce acid consumption during REEs leaching from coal ash by organosulfonic acid, thermal treatment is a technically viable potential strategy.

5.8. Advantages of REEs Leaching from Coal Ash Using Organosulfonic Acids

While coal is a viable source of REEs, its use as a suitable concrete aggregate in the construction industry is well-established. Consequently, in the United States, coal ash in landfills have been sampled to determine their suitability for construction purposes (Baker et al., 2022). The utility of coal ash as a concrete aggregate stems from its structural suitability in addition to its appreciable aluminosilicate content, regarding certain coal ranks (Law, Gunasekara, & Setunge, 2022). Detailed XRD analysis of coal ash after leaching with MSA led to the conclusion that coal ash matrix remained unperturbed during the process, unlike mineral acids. Consequently, MSA leaching of coal ash provides the opportunity for extracting REEs while maintaining its potential as a viable resource for the construction industry.

5.9. Global Market Trends of Organosulfonic Acids

5.9.1. Methane Sulfonic Acid

Due to its wide-spread uses in hydrometallurgy in addition to lower cost, sulfuric acid has the highest global annual production compared to other acids (Speight, 2017). Methane sulfonic acid lies between sulfuric acid and methyl sulfonyl methane, having excellent compatibility between water and oxygenated solvents in addition to behaving in aqueous solutions as a potent acid (SkyQuest, 2022). Considering its non-volatile nature and excellent solubility, MSA serves as a catalyst in a variety of organic synthesis ((Luong, et al., 2004; Kulkarni, 2015; Tian et al., 2012). Presently, the dominant segmented nature of the MSA market is apportioned between industrial and pharmaceutical grade sectors, with the industrial grade portion being the most dominant. The following Table 2) sums up the pharmaceutical and industrial grade portion of MSA market.

Table 2. MSA applications (Fortune, 2020).

ATTRIBUTE	DETAILS
By Product Type	<ul style="list-style-type: none">Pharmaceutical GradeIndustrial Grade
By Application	<ul style="list-style-type: none">ElectroplatingPharmaceutical & MedicinesOrganic SynthesisOthers
By Geography	<ul style="list-style-type: none">North America (U.S., and Canada)Europe (Germany, UK, France, Italy, and Rest of Europe)Asia Pacific (China, India, Japan, and Rest of Asia Pacific)Latin America (Mexico, Brazil, and Rest of Latin America)Middle East & Africa (UAE, South Africa, and Rest of Middle East & Africa)

The market driver of MSA is governed by two factors, namely expansion in its uses and the replacement of its salts with conventional ones in electrowinning of metals (Lu & Dreisinger, 2021). From the hydrometallurgical perspective, the demand for MSA stems from its increased uses in sectors that include pharmaceuticals and ceramics. In the field of organic synthesis, its use as a greener solvent is receiving global attentions, particularly in esterification reactions (Sangsiri et al., 2022; Thakkar & Chudasama, 2008). In light of its growing uses the Following Figure 6 sums of the projected market growth until 2028 (SkyQuest, 2022).

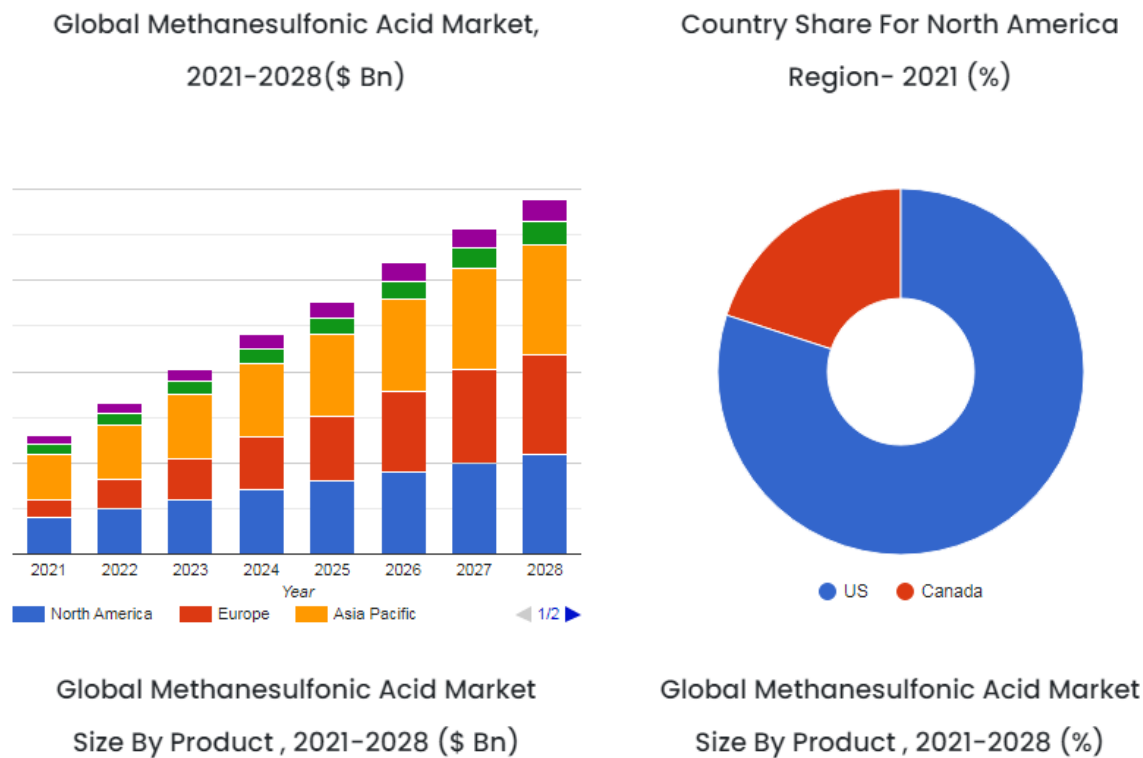


Figure 6. Global market insight and share of MSA.

5.9.2. P-Toluene Sulfonic Acid (PTSA)

P-Toluenesulfonic acid is a white crystalline organic solid with excellent solubility in water, alcohol, and ether (KYTE-RESEARH, 2023). From the industrial perspective, PTSA is widely used as a catalyst in chemical synthesis such as esterification, alkylation, and condensation (Zhang, et al., 2018; (Mahindaratne & Wimalasena, 1998; Liang et al., 2008). One of the major factors driving the market growth of PTSA is the increasing demand in the pharmaceutical industry. PTSA is used as a reagent in the synthesis of various pharmaceutical drugs, making it a crucial component in the production of medicines. Generally, the market is categorized into four major types based on purity level as, industrial grade (<95%), pharmaceutical grade (95-97%), extracted grade (97-99%). A Reagent grade, above 99%, is the purest form used primarily for laboratory analysis and research purposes.

6. Prospects of Organosulfonic Acids for in REEs Hydrometallurgy

Extensive use of MSA and PTSA in hydrometallurgical recovery of metals is yet to be realized. However, thanks to the recent extensive review work of Binnemans & Jones (2022), that integrate the potential of MSA for base metals and REEs in addition to the anticipated global production growth, the following hold true:

Enhanced Recovery of REEs from Methane Sulfonic Acid Salts by Electrowinning Processes

One route to the recovery of REEs from coal ash using mineral acids is by acid digestion followed by electrowinning (NETL, 2020; Argumedo et al., 2020). In such conventional approaches, the resulting RREs salts are less water soluble compared to those of Organosulfonic acids. Therefore, the use of MSA and PTSA in a research designed to explore coal ash as viable resources for REEs provides the opportunity to maximize REEs recovery in electrowinning processes, where the sulfonate salts REEs are the feedstocks. Accordingly, maximization of RREs extraction where their concentrations in coal ash samples are below the global average is equally guaranteed in the electrowinning process.

Potential for Organosulfonic Acid Uses in REEs Heap Leaching from Coal Ash

Considering its cost-effective nature (Thenepalli et al., 2019), heap leaching has prevailed as the preferred option for mineral beneficiation, particularly in settings where ore grade is low or has been proven to be uneconomic. In this regard, its attractiveness stems from low capital investment and operating costs, fast payback, no tailings disposal, lower energy and water requirements, applicability to tailings and waste piles, viable in a wide range of climates, simple setup and operation (FEECO, 2023). Therefore, considering that the concentrations of REEs in original coals vary globally, their concentrations in coal ash has variability with the possibility of lower than average REEs concentrations in some ashes. Therefore, the potential of Organosulfonic acids for REEs beneficiation and recovery by heap leaching is huge for different concentrations in the ash. Moreover, the inherently strong acidity of MSA as evidence by the pKa value that rivals those of conventional mineral acids is another attractive factor for its potential use in REEs heap leaching from coal ash.

7. Summary and Conclusion

REEs are critical for the anticipated global energy transition, but the established global monopoly in their supply raises global concerns, both politically and economically. To diversify supply as well as meet the anticipated exponential global demand for both energy transition and other industrial purposes, production from both geological and waste resources is critical, a fact that has been acknowledged by the United States government (USGS, 2017). Considering that the basic principle of ore genesis is inherent in its concentration through ore forming process such as wall rock alteration, hydrothermal processes and other metasomatic processes (Hedenquist & Lowenstern, 1999; Wu, & Liu, 2022) the potential of coal ash to act as a viable resource for REEs is huge, due to their accumulation in ash to concentrations similar to those associated with geological processes. For instance, in REEs deposits associated with the ion adsorption clays, the deposits originate from their leaching from rocks as REEs ions followed by their adsorption by clays through electrostatic processes based on ion exchange (Wu, et al., 2023; Sobri et al., 2023).

In the literature, an earlier research effort designed to extract REEs from coal ash has been reported (Hower et al., 1998). Following that, other research efforts have been documented in the literature (Smolka-Danielowska, 2010; Long et al., 2013). Much of these research works have centered on the application of environmentally hazardous and corrosive mineral acids as lixiviants. Meanwhile, the pKa of Organosulfonic acids are known to rival those of conventional mineral acids. To the best of our knowledge, the usefulness and potential use of organosulfonic acids as greener lixiviants for non REEs has yet to be realized, let alone their use for the extraction of REEs from coal ash deposits. Therefore, our review centered on the potential of Organosulfonic acids for the extraction of REEs from coal ash as well as on yet-to-be-realized advantages of using these acids in REEs hydrometallurgy. The following sum up the conclusions of this extensive review work:

1. Coal ash deposits are potential sources of REEs due to their combustion induced concentration, this concentration being dependent on the source of coal and the operational parameters of coal combustion chambers,
2. Organosulfonic acids hold the potential for optimized REEs extraction from coal ash due to the enhanced solubility of their salts,
3. While the use of conventional mineral acids as lixiviants lead to REEs extraction with reported efficiencies in the literature, their uses will render leached coal ash residues unsuitable for the construction industry because they destroy the aluminosilicate structure of amorphous phases of coal ash, which prompt their use as concrete aggregate,
4. The use of Organosulfonic acids as lixiviants will preserve the amorphous aluminosilicate structure to maintain the geotechnically important aspect of coal ash for concrete aggregate,
5. The use of organosulfonic acids for REEs extraction from coal ash has the same potential to optimize the leaching process due to the rival nature of its pKa value as reported in the literature compared to those of conventional mineral acids,
6. The global market production of organosulfonic acids is poised to grow, given their increased uses for diversified industrial process, which will give impetus for their use as lixiviants for REEs extraction from coal ash,

7. The high solubility of Organsosulfonic acids coupled with their high pKa values are indicators for the potential use in hydrometallurgical processes involving RREs extraction from coal ash.

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