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Posted Date: 19 July 2023

doi: 10.20944/preprints202307.1313.v1

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Article

# Moroccan Citrus Clementina Peels: Optimization of Pectin Extraction, Chemical and Functional Properties

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**Abstract:** Citrus peels are considered as a rich source of valuable biomolecules like pectin as polymer of polysaccharide acid. In this study, response surface methodology was used to optimize pectin extraction from *Citrus clementina* peels using citric acid as extraction solvent. The effect of parameters conditioning the extraction process and pectin yield (pH, temperature, extraction time, solid/liquid ratio, and raw material particle size) was investigated using a Box-Behnken design. The quality of the extracted pectin was assessed both chemically (moisture, ash, protein, and sugar content) and functionally (gelling power and emulsifying activity). According to the screening experiment, the factors pH, temperature, and particle size were the main factors influencing the pectin yield. The adjusted mathematical model enabled us to plot response surfaces in order to determine optimal extraction conditions. The highest production yield of pectin (26.6%) was obtained at the optimal conditions of: pH = 1.5; temperature 100 °C and particle size = 0.1 mm for an extraction time of 30min. Compared to the predicted value of 26.6%, the experimental extraction yield was about 21.4% of pectin. Concerning the functional properties, the extracted pectin has a high gelling power of 164°SAG and an emulsifying activity of 38.5%.

**Keywords:** citrus by-products; pectin extraction; optimization; characterization; response surface methodology; technological properties

#### 1. Introduction

Many countries around the world largely depend on the socioeconomic contribution of the citrus industry. In Morocco, approximately 2.62 million tons of citrus are produced, of which 715,000 tons are destined for export, representing a value of more than 432 million dollars. Among these citrus fruits, clementines represent about 25% of the total planted area [1].

Citrus fruit production is intended for either direct consumption (fresh) or processing (drinks, jams, etc.) [2, 3]. Citrus juice manufacturing generates a significant amount of waste or byproducts. These by-products are underexploited in the agri-food sector and generally consumed as animal feed. However, these by-products are valuable sources of nutritional biomolecules, such as essential oils, phenolic compounds, flavonoids, and polysaccharides, like cellulose, or more specifically, pectins [4, 5]

Pectins are a class of complex polysaccharides that are found in plant cell walls. They are classified as food additives (registration number E440). The pectin chains are largely made up of  $\alpha$ -(1 $\rightarrow$ 4)-linked D-galacturonic acid units, connected by glycosidic linkages and a small amount of branched -L-rhamnose [6].

In the food industry, pectins are widely applied as thickeners, gelling agents, and emulsifiers in jams, jellies, fruit juices, desserts, and dairy products [7]. They are also used as reinforcement in

biomaterials [8, 9] and as an encapsulation agent for active substances in various fields (pharmaceutical, agri-food, cosmetics, etc.), thanks to their ability to envelop compounds of interest such as flavors and vitamins [10, 11, 12, 13]. The global demand for pectins exceeds 30,000 tons annually and is growing at about 4-5% per year [14].

Commercial pectin may be obtained by extractions from various plant sources, mainly from apple pomace and citrus peels [15, 16]. The extraction process includes hydrolyzing protopectin using acids, such as sulfuric, phosphoric, nitric, hydro-chloric, or citric acid, at high temperatures [17]. Many reports have demonstrated that the factors affecting pectin extraction are pH, temperature, extraction time, particle size, type of acid and solvent-to-sample ratio (SSR) [18, 2, 19]. Furthermore, researchers have optimized the yield of these extraction conditions using response surface methodology (RSM) [18, 2, 20]. RSM can be an effective tool for optimizing experimental conditions for a specific response while using a minimum number of experiments. [21, 22, 23, 24, 25].

The RSM helps reduce experimental trials and perform multiple factors analysis to optimize conditions for pectin extraction [26, 20]. However, to our knowledge, no previous data has been published on extracting pectin from Moroccan clementine peel. Therefore, the current study aims to (i) identify the optimal acidic conditions for the extraction of pectin from clementine by-products to obtain the maximum yield using a three-variable Box-Behnken response surface design, (ii) investigate the chemical and functional properties of the extracted pectin.

#### 2. Results and discussion

## 2.1. Experimental design

Substituting the variables coded as -1, +1, and 0 by their real values, the experimental conditions, and the corresponding experimental responses (pectin yield) were obtained and presented in Table 1. Fourteenth experiments with three independent variables (pH, temperature, and particle size) were performed to evaluate the corresponding pectin yield.

**Table 1.** Experimental conditions of the Box Behnken design and the corresponding experimental responses.

Ct 1	Factor 1	Factor 2	Factor 3	Response 1
Std —	X1:Particle size	X2: pH	X3: Temperature	Yield
	Mm		(°C)	%
4	1	3	80	3.8
2	1	1.5	80	18.7
11	0.55	1.5	100	22.8
13	0.55	2.25	80	14.7
9	0.55	1.5	60	21.5
1	0.1	1.5	80	25.4
10	0.55	3	60	6.5
14	0.55	2.25	80	14.6
8	1	2.25	100	19.3
7	0.1	2.25	100	18.7
3	0.1	3	80	10.5
5	0.1	2.25	60	17.4
6	1	2.25	60	10.8
12	0.55	3	100	7.8

Std: Sorting by Standard.

A similar result reported by Aina [27] shows that the maximum yield from *Citrus sinensis* was found to be 29.41% at pH 3.2 and a temperature of 70°C. The optimized extraction from *C. Limon* resulted in a maximum yield of 36.71% at pH 3.2 and a temperature of 60°C [28].

Thus, a pH of 3.2 appears to be optimal for the extraction of pectin from all the citrus peels studied. The optimal temperature for pectin extraction was observed to be 70°C for *Citrus sinensis* and *C. limetta*, but not for *C. Limon*, in which case a lower temperature of 60°C was preferred [28].

## 2.2. Estimated model

The observed responses were used to compute the model coefficients using the least square method. This allowed us to write the following estimated model:

## 2.3. Statistical analysis and validation of the model

The statistical 'model fit summary' confirms the suitability of the linear model compared with the quadratic or 2FI model (Table 2). Also, the predicted R<sup>2</sup> of 0.8556 and the insignificant lack-of-fit imply that the linear model was the best model to represent the parametric effects on the yield (Table 3).

Table 2. Fit Summary.

Source	Sequential p-value	Lack of Fit p-value	Adjusted R <sup>2</sup>	Predicted R <sup>2</sup>	
Linear	< 0.0001	0.0271	0.9130	0.8556	Suggested
2FI	0.3571	0.0271	0.9194	0.7681	
Quadratic	0.4610	0.0247	0.9212	0.6123	
Cubic	0.0247		0.9999		Aliased

2FI: two-factor interaction.

Table 3. Lack of Fit Tests.

Source	Sum of Squares	df	Mean Square	F-value	p-value	
Linear	36.83	9	4.09	818.41	0.0271	Suggested
2FI	23.87	6	3.98	795.62	0.0271	
Quadratic	13.33	3	4.44	888.67	0.0247	
Cubic	0.0000	0				Aliased
Pure Error	0.0050	1	0.0050			

Df: Degree of freedom.

The results illustrated in Table 4 indicate that the model F-value of 46.45 implies that the model is significant. Model terms are significant when the P-value is less than 0.0500. In this case, X1, X2, and X3 are significant model terms, and values greater than 0.1000 reveal that the model terms are not significant. The lack-of-fit F-value of 818.41 implies that the lack-of-fit is significant.

Table 4. ANOVA for Linear model.

Source	Sum of Squares	Df	Mean Square	F-value	p-value	
Model	513.27	3	171.09	46.45	< 0.0001	Significant
X1-Particle size	47.05	1	47.05	12.77	0.0051	
X2-Ph	447.01	1	447.01	121.36	< 0.0001	
X3-Temperature	19.22	1	19.22	5.22	0.0455	
Residual	36.83	10	3.68			
Lack of Fit	36.83	9	4.09	818.41	0.0271	Significant
<b>Pure Error</b>	0.0050	1	0.0050			
Cor Total	550.10	13				

The predicted  $R^2$  of 0.8556 is in reasonable agreement with the adjusted  $R^2$  of 0.9130, i.e., the difference is less than 0.2. A ratio greater than 4 is desirable. The ratio of 19.301 indicates an adequate signal (Table 5). Overall, this model can be used to navigate the design space.

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Std. Dev.	1.92	R <sup>2</sup>	0.9330
Mean	15.18	Adjusted R <sup>2</sup>	0.9130
C.V. %	12.64	Predicted R <sup>2</sup>	0.8556
		Adeq Precision	19.3009

Std.Dev: Standard deviation; C.V. %: Coefficient of variation.

The coefficient estimate represented in the Table 6 reveals the expected change in a factor's value per unit of response when the other factors are maintained constant. The average response of all the runs is the intercept in an orthogonal design. Based on the factor settings, the coefficients are changed to approximate the average. The variance inflation factor (VIF) is one if the factors are orthogonal. Multi-linearity is indicated by VIFs more than 1, and we have a stronger correlation with higher VIF. VIFs ranging less than 10 are generally acceptable.

Table 6. Coefficients in terms of coded factors.

Factor	<b>Coefficient Estimate</b>	Df	Standard Error	95% CI Low	95% CI High	VIF
Intercept	15.18	1	0.5129	14.04	16.32	
X1-Particle size	-2.43	1	0.6785	-3.94	-0.9131	1.0000
X2-pH	-7.48	1	0.6785	-8.99	-5.96	1.0000
X3-Temperature	1.55	1	0.6785	0.0381	3.06	1.0000

CI: Confidence intervals; VIF: Variance inflation factor.

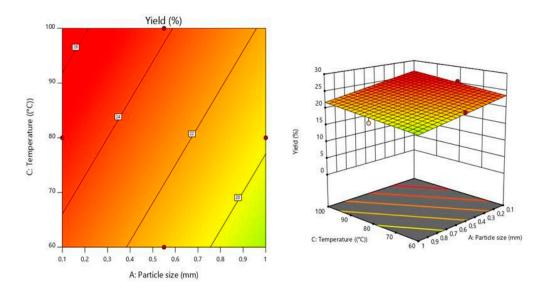
# 2.4. Interpretation of the response surface model

The response surface model graphically illustrates the relationship between the response and the experimental variables by plotting three-dimensional plots [2]. The graphics presenting the relationship between the response (extraction yield) and the experimental variables (pH, temperature, particle size) are shown in the Figures 1 and 2. Each of the two horizontal axes represents one of the three independent variables, while the vertical axes reflect the pectin extraction yield (%). By fixing a factor either in its lower or upper level, or at its average value, a graphical representation of the response as a function of the other two factors can be displayed.

The pectin yield variation as a function of pH variation (1.5 to 3) indicates that the pectin yield increased when decreasing the pH. This could be attributed to the fact that, at low pH, citric acid, can hydrolyze insoluble pectin and transform it into its soluble form, thus increasing the yield of pectin extraction [29]. Furthermore, low pH may decrease the molecular weight of pectin, and thus, increase its release from the plant tissue without degradation [30, 31, 32]. Similar results were published on apple pomace, sugar beet pulp, mango peels, and pomegranate peels by Canteri-Schemin [33], Yapo [34], Prakash Maran [7], and Moorthy [31], respectively.

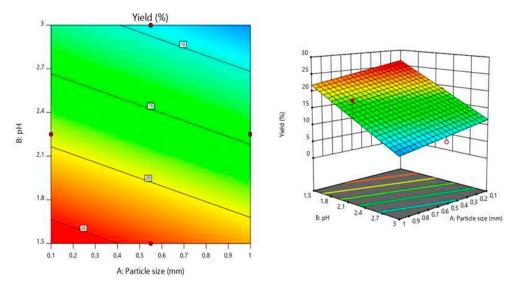
Temperature is considered to be one of the most crucial parameters affecting the pectin extraction yield. The effect of temperature is evaluated in Figure 1. The results show that when the pH was fixed at 1.5, the extraction yield increased relatively with increasing temperature.

According to Yang [35], the extraction yield of pectin increases when temperature increases due to the solvent's enhanced solubility and diffusivity in the plant tissue. These results are similar to those observed by Pagan [36] and Raji [18], who reported a significant improvement in the yield of pectin extraction from peach pomace and melon rind, respectively, with increasing temperature [32].



**Figure 1.** Three-dimensional response surface for the effect of temperature extraction and particle size at constant pH (1.5) on pectin yield extracted from dried Citrus clementina peels.

The results shown in Figure 2 reveal that particle size has a substantial impact on pectin yield. At a fixed temperature of 100°C, the production of pectin was greater for the 0.1 mm size raw material (26.64%). This could be because protopectin is more commonly available in small particles than in large ones. In other words, when the particle size is reduced, the surface area increases, which increases the exposure to the extracting agent [33].



**Figure 2.** Three-dimensional response surface for the effect of pH extraction and particle size at constant temperature (100°C) on pectin yield extracted from dried Citrus clementina peels.

# 2.5. Determination of optimum conditions

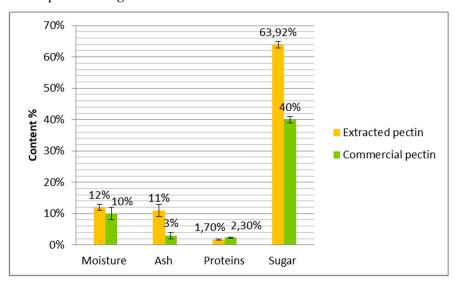
To select the optimal conditions, the particle size value was fixed at 0.1 mm and pH was plotted versus temperature. The conditions that obtained the highest yield (Y1 = 26.64%) were: a temperature of 100°C, a pH of 1.5, a grain size of 0.1 mm, a solid/liquid ratio of 1:50 (m/v), and an extraction time of 30 min.

The validation experiments that were performed under the selected conditions obtained an experimental yield of pectin (21.36%) that was lower than that calculated mathematically by the optimization model (26.64%). This difference of about 5% between the theoretical and experimental

values may be due to the difficulty of controlling the stability and precision of the experimental conditions.

## 2.6. Chemical characteristics

The comparison between extracted and commercial pectin based on moisture, ash, protein, and sugar contents is reported in Figure 3.



**Figure 3.** Chemical characterization of pectin extracted from clementine compared to commercial pectin.

The moisture content of extracted pectin was about 12%. This value is comparable to this reported by Baississe (2009) [37] who used aluminum chloride and aluminum sulfate to extract pectin from oranges and found moisture values of 8 and 13%. These values are still acceptable for good storage stability [37]. When compared to commercial pectin, the moisture content of extracted pectin is slightly higher with 2%. This difference may be attributed mainly to extraction conditions, species of used citrus, etc.

The ash content of the pectin obtained from clementine is 10.6%. This value is significantly higher than the commercial pectin (3%), it can be explained by the fact that in our extraction we used citric acid as extraction solvent, therefore in commercial pectin, the industrials use powerful acidic agents to extract and purify pectin. This result is similar to those obtained by Baississe [37] and Deluca and Joslyn [38] who showed that the ash content of pectins precipitated by mineral salts, especially aluminum sulfate and aluminum chloride, varied between 8 to 25%. Extraction conditions can also affect the precipitation of impurities with pectins and impact ash content. Thus, Yapo et al [34] concluded that pectins extracted at pH 1.5 are purer than those obtained by solubilization at pH 2.0 from beet pulp. Khotimchenko et al, [39] show that the sorption activity of pectin towards heavy metals is closely related to pH, where it varies in the range of 4-8.

The maximum protein content in pectins is 2.5%, according to LEU and FAO/WHO, which are cited by Herbstreith and Fox [40]. Regarding the recorded value of 1.7% obtained in this study, it indicates that the pectin extracted from clementines is still within the permitted range of 2.5%. Pectins extracted from apple pomace by Massiot and Renard [41] show protein content ranging from 2.1 to 7.5%, while those obtained by Schieber et al. (year) are about 4%. Yapo et al [34] obtained a protein content of 3.7% in pectins extracted from beet pulp by hydrochloric acid.

Moreover, the percentage of total sugars in the extracted pectin is 63.9% which is higher than that obtained for commercial pectin (40%). These results are comparable with those described by Baississe [37] who reported values of 70.8% and 74.1% in total sugars of pectins extracted by aluminum chloride and aluminum sulfate respectively. The study of Lekbir, [42] showed lower values than those of our study with a total sugar content that varies between 24.2 and 18.9% for

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orange pectins precipitated with aluminum chloride and aluminum sulfate respectively. Several studies have shown that parietal polysaccharides, especially pectins, are subject to qualitative and quantitative variations depending on: variety, maturity stage, geographical origin and storage [43, 44]. According to Seymour and Konx [45] and Thang et al. [46], the difference in total sugar levels can be explained by fundamental changes in fruit parietal polysaccharides during maturation and storage of raw materials, in addition to extraction conditions.

# 2.7. functional properties

According to Table 7, the analytical results showed that the pectin extracted from clementine peels had a significant gelling power (164°SAG) than the commercial one (150°SAG). This result is comparable to those of Benchabane [47], who reported that a good apple pectin has a gelling power of 177 to 220 ° SAG, while that of an orange pectin varies between 170 to 200 ° SAG. This difference can be explained by the structural difference between apple and orange pectins (molecular weight, content of neutral oses, and presence or not of acetyl groups). Several studies have shown that the sugar content, the distribution of non-esterified carboxyl groups and the charge of pectins, together with the content of neutral oses and the presence of acetyl groups, have a strong influence on the structural and textural properties of pectic gels [48,49].

**Table 7.** Functional properties of extracted pectin compared to commercial pectin.

	Gelling power	<b>Emulsifying activity</b>
Extracted pectin	164°± 2° SAG a	38,46%± 1,66%a
Commercial pectin	150°±1° SAG a	51% ± 2% <sup>b</sup>

<sup>\*</sup> Values followed by the same letters (a-b) are not significantly different a (P<0.05).

The emulsifying activity of the extracted pectin (38.46%) is significantly lower than that of the commercial pectin which has a value of (51%). Our results are comparable with those obtained by Leroux et al, [50] and Yapo et al, [34] which are respectively 43.2 and 47.1% for beet pectin and are higher than that found by Huang et al, [51] which is 30.3%. According to Yapo et al [34], this remarkable emulsifying activity of citric acid extracted pectins may be due to the fact that they are endowed with a tensioactive activity that increases the viscosity of the aqueous phase and reduces the tendency for the emergence of dispersed oil globules. Also, it is mainly time and temperature that have a major influence on surface activity. The most surface active pectins are those extracted at a temperature of 80°C, at a pH of 1.5 and for one hour.

# 3. Materials and Methods

## 3.1. Plant material

The clementine fruits (*Citrus clementina*) were harvested from the experimental station of the Regional Center of Agricultural Research of Tadla in Béni Mellal, Morocco (Latitude: 32.26, longitude: -6.52). The fruit peels were manually removed from the pulp, washed, and blanched at 90°C for 10 min to inactivate enzymes. Then, the peels were dried in a greenhouse at a controlled temperature (45°C) for 8 days. The dried peels were ground with an electric grinder (Retsch SR300, Germany) to obtain a fine and a homogeneous powder (0.1-1 mm). The obtained powder was stored in hermetically-sealed vacuum bags and protected from the light until experimental analysis.

# 3.2. Pectin extraction

Hot acid extraction of the pectin was carried out according to Canteri-Schemin [33] with the following modifications. The dried and ground peel powder (1:50 w/v) was soaked in distilled water and the pH was adjusted (pH 1.5-3) using an aqueous citric acid solution (25% w/v) and a pH meter (HANNA, hi 98161, France), under agitation. The solution was extracted at 60-100°C for 30 min. The obtained pectic extract was kept at 4°C for 24 hours. Pectins were precipitated by mixing the extracted

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pectic juice with two volume of 96% ethanol; the obtained pectic gel was washed with acetone (100%). Finally, the precipitated pectins were dried at 60°C to a constant weight in a vacuum oven (Memmert, GmbH, VO29, Germany).

Commercial pectin (pastry pectin, Louis Francois-France) was analyzed for comparison.

# 3.3. Experimental methodology

The pectin extraction parameters were optimized using RSM. A Box-Behnken design, an element of RSM, was used to identify the best experimental conditions.

Particle size (X1) (0.1-1 mm), pH (X2) (1.5-3), extraction temperature (X3) (60- $100^{\circ}$ C) were chosen as the independent variables. The extraction time was 30 min. For each factor, the experimental range was chosen based on the results from the literature and preliminary experiments.

In this study, to model the pectin extraction process, a linear model without interactions was used to approximate the relationship between the yield extraction and the three selected variables (X1, X2, and X3) as represented in equation 2:

$$Y = b0 + b1*X1 + b2*X2 + b3*X3$$
 (2)

Where: Y is the calculated response function; b1, b2, b3 are successively the coefficients of the parameters X1, X2, X3.

In order to validate the mathematical optimization model, the influencing factors and their variation ranges chosen for this study are illustrated in Table 8.

Table 8. Variation factors of the most influential factors.

	Factors	Lower level	Higher level	Medium level
X1	Particle size (mm)	0.1	1	0.55
X2	Ph	1.5	3	2.25
Х3	Temperature(°C)	60	100	80

It is important to note that all computation and graphics in this study were performed using Design Expert Statistical Software 10 by Stat Ease, Inc.

## 3.4. Validation of the model

Validation of the mathematical model is an important step. Thus, the validation was carried out by an appropriate analysis of variance (ANOVA), as described for the case of a composite design by Kamoun [52] and Masmoudi [2].

# 3.5. Chemical characterisation and pectin yield

#### 3.5.1. Moisture content

To determine the moisture content (H %), one gram (1g) of the sample is weighed (P1) in a tared porcelain crucible, then placed in an oven set at 105 °C. After 5h, the sample is transferred to a desiccator for 30 minutes and weighed; the operation is repeated until obtaining a constant weight [53].

The moisture content is calculated as follow:

$$H\% = (P2 - P1/P1) \times 100$$
 (3)

Where:

P1: Weight of the sample before drying,

P2: Weight after drying in the oven.

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## 3.5.2. Ash content

Ash content was determined using the AOAC method [54]. Pectin weighing 1g is placed in a previously tared porcelain capsule and placed in a muffle oven (NAHITA SERIE 642, France) for 24 hours at 550 °C. Then, the capsule is cooled in a desiccator and weighed. The ash content was calculated as the percentage of sample weights before and after muffle oven-drying.

#### 3.5.3. Protein content

The protein content was assessed using Micro-Kjeldahl apparatus (Kel plus, Pelican, India), in accordance with AOAC method [55]. A total of 0.2 g of pectin powder was digested in a solution of catalyst (1 g) and 5 mL of H2O2 and conc. H2SO4. The digested sample was allowed to boil before collecting the distillate of ammonia liberated in boric acid. The distillate was titrated with hydrochloric acid until the blue color was completely removed. The protein content was estimated using the formula below.

$$N\% = \frac{(S - B) \times N \times 14.007 \times Volume \ made \ (mL)}{\text{Weight of sample } (g) \times Volume \ taken \ (mL)} \times 100$$
 (4)

Where:

S = mL of HCl required for sample titration

B = mL of HCl required for blank titration,

N = Normality of HCl (0.02 N)

Protein 
$$\%$$
= Nitrogen $\%$  x 6.25 (5)

# 3.5.4. Carbohydrate content

The procedure described by Dubois in 1956 [56] was used to determine the amount of carbohydrates in the sample. After 0.5ml of a pectin extract and 0.5ml of a phenol solution at 5% for 15–30 minutes in darkness and ambient cooling, 3ml of concentrated sulfuric acid was added. Galactose is used to generate the standard range, and a UV-Visible spectrophotometer is performed to measure the optical density (OD) at 485 nm.3.5.5. Pectin yield

The pectin extraction yield, subject of this study, was calculated as follows:

Yield (%) = (weight of dried pectin /weight of dried clementine by-product) 
$$\times 100$$
 (6)

3.6. functional properties

## 3.6.1. Determination of gelling power

The traditional SAG method was used to measure the strength of gels formed under the following conditions: 65.0% soluble solids (sucrose), 0.70 wt% pectin, and a pH of 2.3 to determine the gelling capacity (or power) of pectins [57] .In order to prevent evaporation, the jelly mixture was placed entirely within a Ridgelimeter glass. It was then left undisturbed at ambient temperature for 2 hours before aging for a further 22 hours in a water bath at 30 °C. The gel was then delicately demolded onto a Ridgelimeter glass plate without causing any damage. The pointer of the device (Ridgelimeter) was gently lowered until it contacted the gel surface after exactly 2 minutes of standing, and the percentage of sagging under its specific gravity was measured. The following equation was used to determine the gelling power:

$$^{\circ}SAG = (A/B) \times F$$
 (7)

Where A, B, and F are the amounts of sugar and pectin in gel and the factor of sagging percentage, respectively.

# 3.6.2. Emulsifying activity analysis

The extracted pectin's emulsion activity (EA) was determined using the method reported by Hosseini et al. [58]. In a brief, 5 mL sunflower oil, 5 mL of extracted pectin solution (0.5% w/v), and 0.02% sodium azide (NaN3) were combined and subjected to 4000 g centrifugation for 5 min. Finally, EA was determined as follows:

$$EA\% = VE/VT \times 100$$
 (8)

Where VE was the volume of the emulsion layer and VT was the total volume.

# 3.7. Statistical analysis

All experiments were performed in triplicate, and results were expressed as the means  $\pm$  standard deviation (SD). Analysis of variance was performed using (SPSS Corporation, Northampton, MA, USA). The significant level was set as p < 0.05 throughout the study.

## 4. Conclusions

In this work, the optimal yield of pectin extraction from Citrus clementina peel with citric acid solvent was investigated using a Box-Behnken design for three independent variables, consisting of the temperature (60-100°C), particle size (0.1-1 mm), and pH (1.5-3). The results revealed that increasing temperature and reducing particle size and pH considerably improved the extraction yield. The optimal conditions determined using the response surface designs were : pH = 1.5, T =  $100^{\circ}$ C and particle size = 0.1 mm for a solid/liquid ratio of 1:50 (m/v) and an extraction time of 30 min. Under these conditions, the response value (extraction yield) that the model predicts is 26.64%. The chemical composition of the extracted pectin was statically similar to the commercial pectin. In terms of functional properties, the extracted pectins had significantly higher gelling power (164°SAG) than commercial pectin (150°SAG). Inversely, the extracted pectins' emulsifying activity (38.46%) was lower than commercial pectin (51%).

Further studies must be focused on determining the effect of extracted pectin from the clementine peel on the preparation of food products, such as jams and jellies, to confirm their effectiveness as gelling and emulsifying agents, as well as their environmental and chemical stability.

Author Contributions: Conceptualization, Hanane Azzouzi, Souad Salmaoui and Elfazazi Kaoutar; Data curation, Hanane Azzouzi, Loubna Elhajji and Mouad Achchoub; Formal analysis, Hanane Azzouzi, Loubna Elhajji, Mouad Achchoub and Hasnaa Harrak; Methodology, Hanane Azzouzi, Loubna Elhajji, Abdelilah Ammadi and Elfazazi Kaoutar; Resources, Rachid Touzani and Younes Noutfia; Software, Abdelilah Ammadi; Supervision, Elfazazi Kaoutar; Validation, Elfazazi Kaoutar; Visualization, Rachid Touzani and Younes Noutfia; Writing – original draft, Hanane Azzouzi and Elfazazi Kaoutar; Writing – review & editing, Hasnaa Harrak and Rachid Touzani.

**Funding:** This study was fully funded by the National Institute of Agricultural Research of Morocco (INRA) under the Medium-Term Research Program (MTRP 2021-2025) - Citrus Megaproject. **Data Availability Statement:** Data other than presented in this paper are available upon request. Please send all communications to Dr. Elfazazi Kaoutar at Kaoutar.elfazazi@inra.ma or Mrs Azzouzi Hanane hananeazzouzi94@gmail.com.

**Acknowledgments:** The authors would like to thank the staff of Afourer experimental station of CRRAT- INRA for providing samples and their support during this study.

**Conflicts of Interest:** The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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