

Specification and classification of pelletised dried sewage sludge: Identifying its key properties as a renewable material for enabling environmentally non-harmful energy utilisation

Supplementary Materials: Wastewater treatment efficiency at the CWWTPL, pellets preparation, and their assessment as non-hazardous waste.

Mislej Vesna* and Novosel Barbara

* Correspondence: corresponding author: Vesna.Mislej@vokasnaga.si, JP VODOVOD KANALIZACIJA SNAGA d.o.o., Vodovodna c. 90, Ljubljana, 1000-SI

1. Evaluation of the Wastewater treatment efficiency at the CWWTPL

1.1. Wastewater sampling and characterisation

At the CWWTPL [1], the wastewater flow at the inlet and outlet is continuously measured with a Venturimeter and an inline flow meter Prosonic S, Endress + Hauser, based on an ultrasound distance meter between the water level and the sensor, according to the accredited methods: i) DIN 19559-1:1983, Measurement of flow of wastewater in open channels and gravity conduits; General information and ii) DIN 19559-2:1983, Measurement of flow of wastewater in open channels and gravity conduits; venturi flumes. Partial wastewater samples are automatically sampled time-proportionally using the CSF48 Liquistation, Endress+Hauser. Samples are prepared, cooled, and stored by i) ISO 5667-10:1992, Water quality, Sampling, Part 10: Guidance on sampling of wastewaters, and ii) ISO 5667-3:2012, Water quality, Sampling, Part 3: Preservation and handling of water samples [2].

Table 1: Overview of the performed Sampling campaigns.

Sampling campaign N ^o	Year	Date	Inflow, m ³ day ⁻¹	Outflow, m ³ day ⁻¹
1	2010	The 6 th July	86,500	86,600
2		The 12 th October	73,700	71,800
3	2011	The 17 th May	86,500	86,600
4		The 17 th October	73,700	71,800
5	2012	The 27 th September	83,100	82,496
6	2013	The 14 th May	79,700	79,900
7		The 21 st October	59,600	58,400
8	2014	The 25 th May	56,900	52,200
9		The 24 th September	70,700	70,800
10	2015	The 9 th April	62,500	64,500
11		The 27 th October	58,312	59,566
12	2016*	The 24 th May	65,148	64,882
13		The 16 th October	50,194	51,720
14	2017	The 3 rd July	66,814	69,950
15		The 5 th July	55,252	58,690
16		The 9 th July	43,352	46,730
17	2021	The 12 th July	60,110	65,080
18	2022	The 7 th June	65,000	68,700

*[2].

From 2010 - 2022, additional representative samples were collected in the spring, summer and autumn (Table 1). 24-hourly, time-proportional representative sub-samples

were taken at the influent and effluent to determine the removal efficiency of potential toxic metals (PTMs) (As, Cd, Cr, Cu, Hg, Mo, Ni, Pb and Zn), and metals Sb, Co, Mn, Tl and V from the raw wastewater (from Table 2 to Table 8).

The content of the heavy metals in the raw wastewater and treated effluent is monitored by standardised physicochemical measurements: i) digestion of the wastewater sample is made according to EN ISO 15587-2:2003, Water quality – Digestion for the determination of selected elements in water – Part 2: Nitric acid digestion, ii) determination of heavy metals (except mercury) is performed with ISO 17294-2 (relevant edition), Water quality – Application of inductively coupled plasma mass spectrometry (ICP-MS) – Part 2: Determination of selected elements including uranium isotopes and iii) mercury is determined with EN ISO 12846:2012, Water quality – Determination of mercury – Method using atomic absorption spectrometry (AAS) with and without enrichment.

Most of the used methods are accredited according to the Technical Standard EN ISO/IEC 17025 (relevant edition), General requirements for the competence of testing and calibration laboratories and performed by authorised contractors.

1.2. The treatment efficiency for heavy metals evaluation/ calculation

$$\text{Treatment efficiency, \% m/m} = [(Q_{\text{inlet}} * C_{\text{inlet}} - Q_{\text{outlet}} * C_{\text{outlet}}) / (Q_{\text{inlet}} * C_{\text{inlet}})] * 100 \quad (1)$$

$Q_{\text{inlet}}, Q_{\text{outlet}}$ – the inflow of the raw wastewater/ the outflow of the treated wastewater in $\text{m}^3 \text{ day}^{-1}$

$C_{\text{inlet}}, C_{\text{outlet}}$ – the concentration of heavy metal in the raw wastewater/ the treated wastewater

Heavy metal concentration for results with values <LOQ or <LOD [3, 4]:

$$C_{\text{inlet}}, C_{\text{outlet}} = \text{LOQ}/2 \text{ or } \text{LOD}/2 \quad (2)$$

1.3. The Heavy metals concentration in wastewater and their biological treatment efficiency with the active sludge

Tables 2 to 8 show results with values lower than LOQ and higher than LOD as <.... Results with a value lower than the LOD are given by [...]. The treatment efficiency could not be assessed in the case of equally low inlet and outlet concentrations.

Table 2. Overview of the removal efficiency for arsenic and cadmium.

Sampling campaign, N ^o	As			Cd		
	Inlet concentration, mg L ⁻¹	Outlet concentration, mg L ⁻¹	Treatment efficiency, % m/m	Inlet concentration, mg L ⁻¹	Outlet concentration, mg L ⁻¹	Treatment efficiency, % m/m
1	[0.007]	[0.007]	n. e.	[0.0003]	[0.0003]	n. e.
2	[0.007]	[0.007]		[0.0003]	[0.0003]	
3	[0.007]	[0.007]		<0.0010	[0.0003]	
4	[0.007]	[0.007]		[0.003]	[0.0003]	
6	[0.007]	[0.007]		[0.0003]	[0.0003]	
7	[0.007]	<0.010	0	[0.0003]	[0.0003]	n. e.
8	0.0005	[0.0003]	72.5	[0.0003]	[0.0003]	
9	0.00076	0.00048	36.8	[0.0003]	[0.0003]	
10	0.0010	0.0037	0	[0.0003]	[0.0003]	
11	0.00080	0.00043	45.1	[0.0003]	[0.0003]	
12*	0.00093	0.00046	50.7	[0.0003]	[0.0003]	
13*	0.0018	0.00043	75.4	0.00068	[0.0003]	77.3
17	0.0011	0.00077	24.2	[0.0003]	[0.0003]	n. e.
18	0.00093	0.00061	30.7	0.00019	[0.0003]	16.6

* [2].

In general, the content of heavy metals in municipal wastewater is low, most often at the limit of quantification. The methods for sample decomposition and determination of the heavy metals and mercury improve all the time. That resulted in the results' quality and lowered the LOQ and LOD. After 2014 (since campaign 8), the quality of results has improved, and fewer results are as <LOQ or [LOD]. The latter is especially true for As, Sb, Co, and Mn. The Cd, Sb, and Tl concentrations are mostly [LOD]. Mercury concentration at the outlet of the CWWTPL is on the level of ng L⁻¹ or as [LOD].

Table 3. Overview of the removal efficiency for antimony and cobalt.

Sampling campaign, N°	Sb			Co		
	Inlet concentration, mg L ⁻¹	Outlet concentration, mg L ⁻¹	Treatment efficiency, % m/m	Inlet concentration, mg L ⁻¹	Outlet concentration, mg L ⁻¹	Treatment efficiency, % m/m
6	[0.005]	[0.005]	n. e.	[0.003]	[0.003]	n. e.
7	[0.005]	[0.005]	n. e.	[0.003]	[0.003]	n. e.
8	[0.001]	[0.001]	n. e.	0.00096	0.00071	32.2
9	[0.001]	[0.001]	n. e.	0.0016	0.00073	54.3
10	[0.001]	[0.001]	n. e.	0.0022	0.0040	0
11	[0.001]	[0.001]	n. e.	0.0015	0.00033	77.5
12*	[0.001]	[0.001]	n. e.	0.0024	0.00059	75.5
13*	0.0021	[0.001]	75.5	0.0048	0.00053	88.6
14				0.0015	<0.0005	82.6
15		no a.		0.0014	<0.0005	81.0
16				0.00094	<0.0005	71.3
17	[0.001]	[0.001]	n. e.	0.00085	0.00033	58.0
18	<LOD=0.00035	<LOD=0.00037	0	0.0029	0.0005	81.8

* [2].

Table 4. Overview of the removal efficiency for chromium and copper.

Sampling campaign, N°	Cr			Cu		
	Inlet concentration, mg L ⁻¹	Outlet concentration, mg L ⁻¹	Treatment efficiency, % m/m	Inlet concentration, mg L ⁻¹	Outlet concentration, mg L ⁻¹	Treatment efficiency, % m/m
1	0.014	0.012	14.2	0.009	<0.005	72.2
2	<0.010	<0.010	n. e.	0.026	<0.005	90.4
3	0.014	0.011	21.3	0.034	<0.0050	92.8
4	0.032	[0.003]	95.4	0.039	0.0065	83.7
5	0.027	0.027	0.73	0.041	<0.0050	87.8
6	0.016	<0.010	68.7	0.029	0.0052	82.5
7	0.011	[0.003]	86.6	0.033	<0.0050	92.4
8	0.011	0.0056	53.3	0.065	0.0091	86.4
9	0.039	0.0088	96.1	0.022	<0.0050	88.7
10	0.041	[0.005]	93.7	0.041	0.0069	83.1
11	0.021	[0.005]	87.8	0.30	0.024	92.2
12*	0.026	[0.005]	90.4	0.012	[0.01]	61.8
13*	0.049	[0.005]	94.7	0.061	[0.01]	91.8
17	0.0068	0.0015	76.1	0.068	[0.01]	92.4
18	0.019	[0.005]	86.1	0.015	[0.01]	64.8

* [2].

Table 5. Overview of the removal efficiency for thallium and vanadium.

Sampling	Tl	V
----------	----	---

campaign, N°	Inlet concen- tration, mg L ⁻¹	Outlet concen- tration, mg L ⁻¹	Treatment efficiency, % m/m	Inlet concen- tration, mg L ⁻¹	Outlet concen- tration, mg L ⁻¹	Treatment efficiency, % m/m
6	[0.00025]	[0.00025]	n. e.	[0.030]	[0.030]	n. e.
7	[0.00025]	[0.00025]		[0.030]	[0.030]	
8	<0.01	<0.001	90.8	0.0014	0.00081	46.9
9	[0.005]	[0.005]	n. e.	0.0016	0.00056	65.0
10	[0.005]	[0.005]		0.0075	0.00034	95.3
11	[0.005]	[0.005]		0.0025	0.00043	82.4
12*	[0.005]	[0.005]		0.0030	0.00055	81.7
13*	[0.005]	[0.005]		0.0075	0.00032	95.6
17	[0.005]	[0.005]		0.0028	0.00066	74.5
18	[0.005]	[0.005]		0.0031	0.00059	79.9

* [2].

Table 6. Overview of the removal efficiency for mercury and zinc.

Sampling campaign, N°	Hg			Zn		
	Inlet concen- tration, mg L ⁻¹	Outlet concen- tration, mg L ⁻¹	Treatment efficiency, % m/m	Inlet concen- tration, mg L ⁻¹	Outlet concen- tration, mg L ⁻¹	Treatment efficiency, % m/m
1	[0.00015]	[0.00015]	n. e.	0.29	<0.10	65.5
2	<0.00020	[0.00015]	26.9	0.20	<0.10	75.6
3	<0.00020	[0.00015]	24.9	0.26	<0.10	80.7
4	0.00065	[0.00015]	88.8	0.31	<0.10	84.3
5	[0.00015]	[0.00015]	n. e.	0.14	<0.10	64.5
6	0.00025	[0.00015]	69.9	0.19	<0.10	73.6
7	0.00079	[0.00015]	90.7	0.35	<0.10	86.0
8	0.00032	[0.00003]	95.7	0.21	0.098	57.2
9	0.00014	[0.00003]	89.3	0.18	[0.05]	86.1
10	0.00019	0.000093	49.5	0.25	0.087	64.1
11*	0.00013	[0.000007]	97.2	0.20	0.074	62.2
12*	0.00011	0.000016	85.5	0.24	0.10	58.5
13	0.0080	0.000042	99.5	0.61	0.065	89.0
17	no a.	[0.000007]	n. e.	0.12	0.047	57.6
18	0.00019	0.000039	78.3	0.28	0.065	75.5

* [2].

Table 7. Overview of the removal efficiency for nickel and lead.

Sampling campaign, N°	Ni			Pb		
	Inlet concen- tration, mg L ⁻¹	Outlet concen- tration, mg L ⁻¹	Treatment efficiency, %	Inlet concen- tration, mg L ⁻¹	Outlet concen- tration, mg L ⁻¹	Treatment efficiency, %
1	0.011	<0.010	54.5	0.031	[0.0030]	95.2
2	<0.010	<0.010	n. e.	0.010	[0.0030]	85.4
3	0.015	<0.010	66.6	0.0097	[0.0030]	84.5
4	0.028	0.017	40.9	0.016	[0.0030]	90.9
5	0.049	0.014	71.6	0.0078	[0.0030]	80.9
6	0.015	0.010	33.2	0.015	[0.0030]	90.0
7	0.063	<0.010	92.2	0.029	[0.0030]	94.9
8	0.0073	0.0079	0.72	0.010	[0.003]	86.2
9	0.018	0.0075	58.3	0.018	[0.003]	91.7
10	0.044	0.027	36.7	0.016	[0.003]	90.3
11	0.011	0.0058	46.1	0.010	<0.005	74.5
12*	0.021	0.0056	73.4	0.018	[0.003]	91.7

13*	0.033	0.0067	79.1	0.060	[0.003]	97.4
17	0.01	0.0066	28.5	0.006	[0.003]	70.5
18	0.017	0.0074	54.0	0.024	[0.003]	93.4

* [2].

Table 8. Overview of the removal efficiency for manganese and molybdenum.

Sampling campaign, N°	Mn			Mo		
	Inlet concentration, mg L ⁻¹	Outlet concentration, mg L ⁻¹	Treatment efficiency, %	Inlet concentration, mg L ⁻¹	Outlet concentration, mg L ⁻¹	Treatment efficiency, %
6	<0.10	[0.025]	74.9	no a.		
7	<0.10	[0.025]	75.5			
8	0.043	0.017	63.7			
9	0.054	0.017	68.5			
10	0.064	0.029	53.2			
11	0.058	0.0069	87.8			
12*	0.057	0.015	73.8			
13*	0.11	0.011	89.7			
17	0.041	0.0083	78.1	0.0018	0.00091	45.3
18	0.25	0.029	87.7	0.00054	0.00024	53.0

* [2].

2. Pellets production at the CWWTPL (JP VOKA SNAGA, 2019)

Raw surplus sludge is discharged daily from the biological system. After gravitational and mechanical pre-thickening with the addition of flocculants, the excess sludge contains 5.5 to 6.5 % of dry matter. It is then alternately taken to one of two identical parallel digesters capable of holding a total volume of 14,800 m³ and processed through anaerobic mesophilic digestion. The digested sludge contains 3.0 - 3.5 % dry matter. It is collected into a 1,850 m³ secondary thickening tank. When the tank is full, the digestate dehydration process starts. Afterwards, it is transported to the mixer, where dry granulates are added. This mixture reaches a moisture content of 55 – 65 % dry matter. In this rheological form, it is suitable to be exposed to thermal treatment in a convectional rotating drying drum (Figure 1). The latter process is not continual but is in batch mode connected with the running of the centrifuge. Drum performs mixture drying up to 92 % m/m of dry matter, pelleting, and hygienisation simultaneously. Final pellets have 2 mm to 4 mm in diameter. Until taken over by the stakeholder, pellets are temporarily stored in a silo (Figure 1) with a volume of 50 m³.

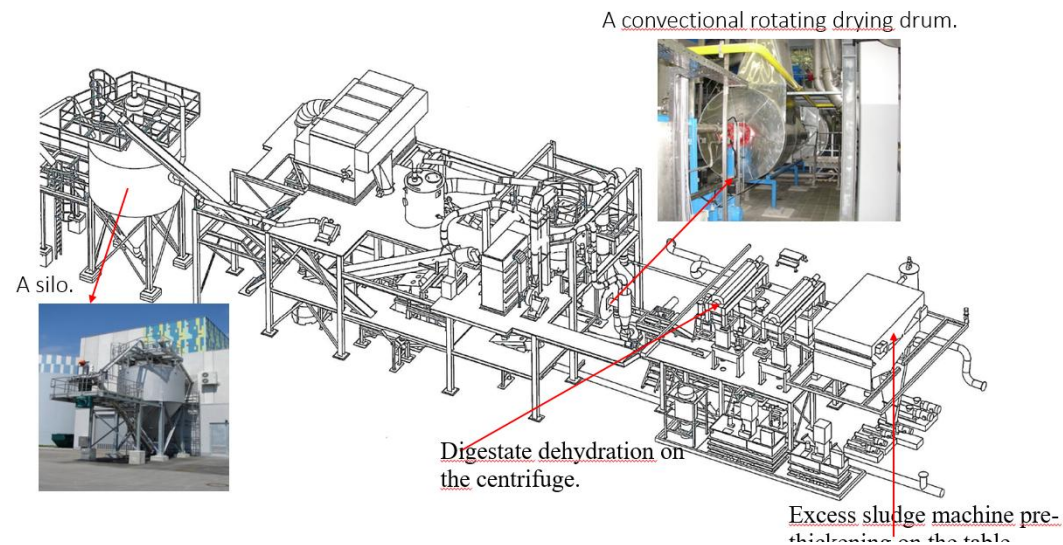


Figure 1. Schematic representation of mechanical pre-treatment of excess sludge and digestate at the CWWTPL [5, 6].

3. The pellets assessment according to hazardous waste characteristics

»Hazardous waste« means waste which displays one or more of the hazardous properties listed in Annex III of Directive 2008/98/EC [7]. Based on the review of pellets generation technology at the Central wastewater treatment plant, the review of input raw materials, pellets composition, and assessment of analysis results on the annual representative samples, the report was prepared regarding the content of hazardous matter. Official reports NLZOH [8] and NLZOH [9] state that the waste in question does not contain substances that could be classified under one of the hazard statements [10], and designated as additional hazardous items related to HP 15 [7, 10, 11]. 'Hazard statement' means a phrase assigned to a hazard class and category that describes the nature of the hazards of a hazardous substance or mixture, including, where appropriate, the degree of risk. By the EU Commission Regulation [11], the hazardous properties H 1 to H 15 defined in Annex III to Directive 2008/98/EC [7] are renamed to HP 1 to HP 15 to avoid potential confusion with the hazard statement codes defined in EC Regulation [10] (Table 1). Directive 2008/98/EC [7] states that the classification of waste as hazardous should be based, among other things, on the EU Union legislation on chemicals, in particular concerning the type of preparations as hazardous, including concentration limit values used for that purpose.

Table 9. The evaluation of pellets according to hazardous waste characteristics [7, 8, 9].

Properties of waste which render it hazardous	Description	Assessment report (Yes/No)
HP 1	"Explosive": waste is capable of chemical reaction of producing gas at such a temperature and pressure and at such a speed as to cause damage to the surroundings.	No
HP 2	"Oxidising": waste, which may, generally by providing oxygen, cause or contribute to the combustion of other materials.	No
HP 3	"Flammable": flammable solid waste, which is readily combustible or may cause or contribute to fire through friction.	No
HP 4	"Irritant — skin irritation and eye damage" waste on the application can cause skin irritation or damage to the eye.	No
HP 5	"Specific Target Organ Toxicity (STOT)/Aspiration Toxicity" can cause specific target organ toxicity either from a single or repeated exposure or cause acute toxic effects following aspi-	No

	ration.	
HP 6	“Acute Toxicity” can cause acute toxic effects following oral or dermal contact or inhalation exposure.	No
HP 7	“Carcinogenic” : waste, which induces cancer or increases its incidence.	No
HP 8	“Corrosive” : waste, which on the application can cause skin corrosion.	No
HP 9	“Infectious” : waste containing viable micro-organisms or toxins reliably believed to cause disease in man or other living organisms.	No
HP 10	“Toxic for reproduction” : waste affects sexual function and fertility in adult males and females, as well as developmental toxicity in the offspring.	No
HP 11	“Mutagenic” : waste may cause a mutation, a permanent change in the amount or structure of the genetic material in a cell.	No
HP 12	“Release of an acute toxic gas” : waste releases acute toxic gases in contact with water or acid.	No
HP 13	“Sensitising” : waste contains one or more substances known to cause sensitising effects to the skin or the respiratory organs.	No
HP 14	“Ecotoxic” : waste presents or may present immediate or delayed risks for one or more sectors of the environment.	No
HP 15	“Waste capable of exhibiting a hazardous property listed above not directly displayed by the original waste” .	No

4. The SRF classification into Quality classes

The Technical Report [12] summarises a classification system, classes, and specification procedure to evaluate the treated waste as an SRF by the decision of CEN/TC 343 Working Group 2, Fuel Specification and Classes.

Table 10. Classification of SRFs [12].

Classification characteristic	Statistical measure	Unit	Classes ^a				
			1	2	3	4	5
NCV	Arithmetic	$\text{MJ kg}^{-1}_{\text{ar}}$	≥ 25	≥ 20	≥ 15	≥ 10	≥ 3
Chlorine (Cl)	mean	% m/m _{DM}	≤ 0.2	≤ 0.6	≤ 1.0	≤ 1.5	≤ 3
Mercury (Hg)	Median	$\text{mg MJ}^{-1}_{\text{ar}}$	≤ 0.02	≤ 0.03	≤ 0.08	≤ 0.15	≤ 0.50
	80th percentile		≤ 0.04	≤ 0.06	≤ 0.16	≤ 0.30	≤ 1.00
Cadmium^b (Cd)	Median	$\text{mg MJ}^{-1}_{\text{ar}}$	≤ 0.1	≤ 0.30	≤ 1.0	≤ 5.0	$\leq 15^c$
	80th percentile		≤ 0.2	≤ 0.60	≤ 2.0	≤ 10	$\leq 30^c$

^a Values refer to a minimum of 10 analyses. ^bProposed classes for Cd. ^cFor the SRF with high ash content and therefore a higher raw material substitution in the clinker production with a maximum of 100 mg kg⁻¹_{ar}.

Technical Report [12] introduced a list of three operational parameters essential for the successful operation of a combustion facility: i) economics aspects (NCV), ii) corrosion (Cl) and emission indicators (Hg and Cd). Cadmium is added as a proposal to supplement the classification system, which can be used if needed. The classification system presents five classes (Table 10). At least ten representative samples of treated waste, sampled evenly over a calendar year, must be analysed to specify the Class code. The highest class (the worst SRF Quality class) is reserved for the SRF derived from, e.g. sewage sludge and filter cakes. Technical Standard [13], superseded with Technical Standard [14] in May 2021, determines the quality classes based only on NCV, Cl, and Hg. Both documents determine the method of evaluating the energy and environmental sui-

tability of treated waste for use as SRF and set the statistical procedures for generated analytical results.

Reference

- [1] JP VOKA SNAGA, 2019, vokasnaga.si/o-druzbi/centralna-cistilna-naprava-ljubljana. Website, accessed on 25 March 2022.
- [2] Mislej, V., Grilc, V., Novosel, B., Mladenovič, A., Zalar, Serjun, V., 2022. Sewage sludge management at the central wastewater treatment plant Ljubljana—Characterization of its properties, possibilities for sustainable utilization and legislative obstacles. The Holistic Approach to Environment. doi: org/10.33765/thate.12.1.2.
- [3] Directive 2013/39/EU of the European Parliament and of the Council of 12 August 2013 amending Directives 2000/60/EC and 2008/105/EC as regards priority substances in the field of water policy Text with EEA relevance OJ L 226, 24.8.2013, p. 1–17.
- [4] Commission Directive 2009/90/EC of 31 July 2009 laying down, pursuant to Directive 2000/60/EC of the European Parliament and of the Council, technical specifications for chemical analysis and monitoring of water status (Text with EEA relevance), OJ L 201, 1.8.2009, p. 36–38.
- [5] JP VOKA SNAGA, 2019, vokasnaga.si/o-druzbi/centralna-cistilna-naprava-ljubljana/obdelava-odvecnega-blata. Website, accessed on 25 March 2022.
- [6] Publication »Ljubljana Waste Water Treatment Plant«, 2009, KROG, Ljubljana.
- [7] Directive 2008/98/EC of the European Parliament and of the Council of 19 November 2008 on waste and repealing certain Directives (Text with EEA relevance). OJ L 312, 22.11.2008, p. 3–30.
- [8] Report on the investigation of hazardous properties of waste for the company JP VODOVOD KANALIZACIJA SNAGA d.o.o., Waste 19 08 05 - Sludge from municipal wastewater treatment, Document N° 88-62/19-1, National Laboratory of Health, Environment and Food, Department for Waste and Soil.
- [9] Report on the investigation of hazardous properties of waste for the company JP VODOVOD KANALIZACIJA SNAGA d.o.o., Waste 19 08 05 - Sludge from municipal wastewater treatment, Document N° 54-51-1/22, National Laboratory of Health, Environment and Food, Department for Waste and Soil.
- [10] Regulation (EC) No 1272/2008 of the European Parliament and of the Council of 16 December 2008 on classification, labelling and packaging of substances and mixtures, amending and repealing Directives 67/548/EEC and 1999/45/EC, and amending Regulation (EC) No 1907/2006 (Text with EEA relevance), OJ L 353, 31.12.2008, p. 1–1355.
- [11] Commission Regulation (EU) No 1357/2014 of 18 December 2014 replacing Annex III to Directive 2008/98/EC of the European Parliament and of the Council on waste and repealing certain Directives Text with EEA relevance, OJ L 365, 19.12.2014, p. 89–96.
- [12] Technical Report, 2006, CEN/TR 15508:2006, Key properties on solid recovered fuels to be used for establishing a classification system, ICS: 75.160.10.
- [13] Technical Standard, 2011, EN 15359:2011, Solid recovered fuels – Specification and classes, ICS: 75.160.10.
- [14] Technical Standard, 2021, EN ISO 21640:2021, Solid recovered fuels – Specification and classes, ICS: 75.160.10.