## Biogas Production from Organic wastes and Iron as an Additive - A Short Review

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### **ABSTRACT**

The world is facing a serious energy crisis and environmental pollution problems due to a sharp increase in the world population. Bioenergy is an eminent solution to these problems. Anaerobic digestion is a green energy technology used worldwide for the conversion of organic waste to biogas. It is reported that organic wastes are hard to digest and need some technical improvement in the anaerobic digestion process to improve biogas yield. Iron-based additives, due to their electron acceptance and donation capabilities, have been emphasized as being exceptional in improving anaerobic digestion process efficiency amongst all other enhancement options. This study reviews the major available types of iron-based additives, their characteristics, and their preparation methods. The preferred iron-based additive that has a significant effect on the enhancement of biogas yield is also discussed. The use of iron-based additives in the anaerobic digestion process with varying dosages and their impact on the biogas generation rate is also being studied. Substrates, operating parameters, and types of anaerobic digesters used in recent studies while researching the effects of iron-based additives are also part of this review. Lastly, this study also confirms that iron-based additives have a significant effect on the reduction rate of the volatile suspended solids, methane content, biogas yield, and volatile fatty acids.

# **KEYWORDS**

Anaerobic digestion, iron additives, biogas, catalyst, bioenergy

### 1 - INTRODUCTION:-

Due to a significant increase in the world population during the last decade, lots of problems have arisen, including deforestation, increased energy requirements, environmental pollution, and global warming. Around 82% of the world's energy requirements are fulfilled by burning conventional fossil fuels like natural gas, oil, and coal, which are the main causes of environmental pollution and increased GHG emissions in the atmosphere, resulting in global warming (BP, 2019; World Bioenergy Association (WBA), 2019). Bioenergy is a prominent option to mitigate these environmental concerns and to reduce dependency on fossil fuels. It is obtained by the biological conversion of biomass (organic matter) into biofuels (Basu, 2018).

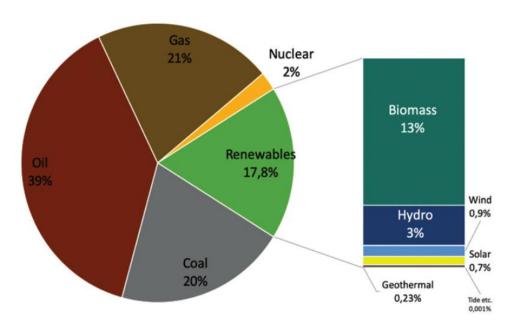


Figure 1: World Energy Mix - World Bioenergy Association (WBA) Report-2019

Biomass is considered a renewable energy resource as green plants receive power from sunlight to initiate chemical reactions that store energy. The consequence of these chemical reactions results in the generation of numerous types of energy-rich resources, including plants and trees, forestry residues, fruits and vegetable residues, and animal wastes (Maletta & Díaz-Ambrona, 2020). Technologies used for biological conversion of organic matter are combustion, gasification, pyrolysis, anaerobic digestion, and microbial fermentation, and the biofuels obtained as a result are syngas, bio-oil, bio-diesel, charcoal, biogas, methanol, and ethanol (Gao et al., 2018). Biogas is one of the cleanest sources to generate electricity and for cooking and heating applications. The preferable technology used for biogas generation is anaerobic digestion (Omer, 2012).

The anaerobic digestion (A.D.) process is an innovative technology for waste management that involves the conversion of organic wastes to biogas in the absence of oxygen. Organic content present in organic waste contains a large amount of lignocellulosic matter, which is hard to digest due to its complex structure. This leads to low substrate biodegradability and, ultimately, longer time required for digestion (Li et al., 2018). Pretreatment of organic wastes has proven to be a feasible option to improve process performance by facilitating lignocellulosic

breakdown, enhancing biogas yield, and reducing hydraulic retention time (HRT) (Carlsson, 2015). Pretreatment has a number of drawbacks, including a high energy cost and suppression of the methanogenic process owing to excessive salt production and an extreme pH value (Zhang et al., 2016).

Anaerobic decomposition driven by microbiology is a sophisticated, multi-stage set of biochemical events. Bacteria and Archaea are two species of microorganisms that primarily digest organic material, resulting in biogas production. Because these microorganisms are oxygen-intolerant, the process takes place in an anoxic environment. The final product contains approximately 60% methane, 30%–40% carbon dioxide, and trace quantities of gaseous water, hydrogen sulfide, and ammonia (Liu et al., 2011). Hydrolysis, acidogenesis, acetogenesis, and methanogenesis are the four steps of the AD process, as shown in Fig. 2.

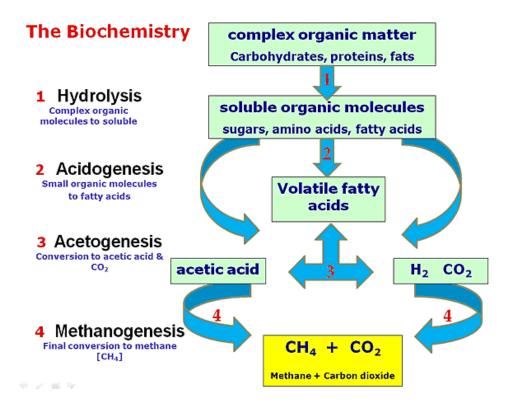


Figure 2: Biochemical process flow diagram of Anaerobic digestion process - Adapted from Waste to Energy (Ogejo, 2013)

Hydrolysis is the hydrodriven lysis of bulk molecules into soluble monomers. Carbohydrates, polysaccharides, proteins, nucleic acids, lipids, and other insoluble high-molecular-mass components are broken down by enzymes. Acidogenesis includes acid-forming essential and heterotrophic anaerobes convert the soluble end-products of the hydrolysis. Acetic acid, butyric acid, propionic acid, ethanol, carbon dioxide, and hydrogen are some of the end products. Acetogenesis is the third phase, which consists of anaerobic oxidation processes. Acetate is created from the alcohol and acids released during acidogenesis. Methanogens mediate the creation of methane from acetate (aceticlastic methanogenesis), carbon dioxide, and hydrogen gas during this stage (hydrogenotrophic methanogenesis). Methane-forming bacteria do not use any of the chemicals from previous phases that have not been converted to acetate, thus they accumulate in the digester (Ganzoury & Allam, 2015).

According to previous studies, adding additives to the A.D. process speeds up starting, decreases contaminants, enhances biogas rate of production, lowers HRT, replenishes lacking nutrients, raises methane content, and improves reactor stability (Kim et al., 2017; Ward et al., 2008). Additives used for the A.D. process cover a wide variety of materials and can be chemical, biological, organic, or inorganic, and can also have variability in their size (Abdelwahab et al., 2020). Nickel, Cobalt, Iron, Selenium, Sulfur, and Carbon, etc. can be used as an additive for improvement of the A-D process (Samson Nnaemeka Ugwu & Enweremadu, 2020).

Iron is one of the cheapest ways to boost methane production from anaerobic digestion since industrial businesses create around 18,895 thousand tons of iron waste each year, with only 8000 thousand tons recycled. The remaining leftover iron scrap is disposed of in landfills (BP, 2019). If iron proves to be a critical answer for enhancing biogas yield, then biogas from the anaerobic digestion process will be a cost-effective solution, as we have approximately 10,000 tonnes of waste iron ready to be used as an addition in the A-D process.

Iron is a vital element for the methanogenesis process as it replicates the DNA structure and provides an environment for the survival of cells. Iron has exclusive ionization ability for Fe<sup>2+</sup> and Fe<sup>3+</sup> and it acts as both a donor and an acceptor of electrons. Iron-based additives have been reported to have unique advantages amongst all, like supplementation of nutrients, improvement of methane yield, improvement of substrate digestibility, control of H2S toxicity, etc. (Chen et al., 2018). Iron-based additives can also improve the hydrolysis enzyme activity by reducing oxidative-reductive potential and support the biological growth of enzymes (Feng et al., 2014). This article highlights all of the key advancements in biogas production that have been made by employing iron as an addition for the A-D process. This study also goes into different types of iron that may be used as an additive, substrates that can handle iron additives, optimum operating conditions with iron additives, digester types that can be employed, and the pros and disadvantages of employing iron as an additive.

# 2 - BENEFITS OF ADDTIVE MATERIALS: -

Figure 3 summarized the effects of additives in anaerobic digestion process. In commercial full-scale AD plants, process stability is a critical concern, as inadequate process stability typically leads to uneven methane output. In addition, prolonged periods of instability might lead to process failure. As a result, a number of research projects have been undertaken to address the causes of AD instability. Different forms of inorganic component and packing materials (clay materials and zeolites) are often used to immobilize and retain microbial communities to manage and diminish AD inhibition. Depending on particle size, porosity, surface area, absorbent capacity, and electric conductivity, different materials may influence the abundance and retention of diverse microbial communities at their surface. The AD process's reaction kinetics are considerably improved by the support materials, allowing for higher COD conversion rates even at high OLR and low HRT. By preserving the microbial flora, removing inhibitory elements, and serving as catalysts in metabolism, support materials play a critical role in manipulating the reaction kinetics of even resistant substrates and methane production (Arif et al., 2018).

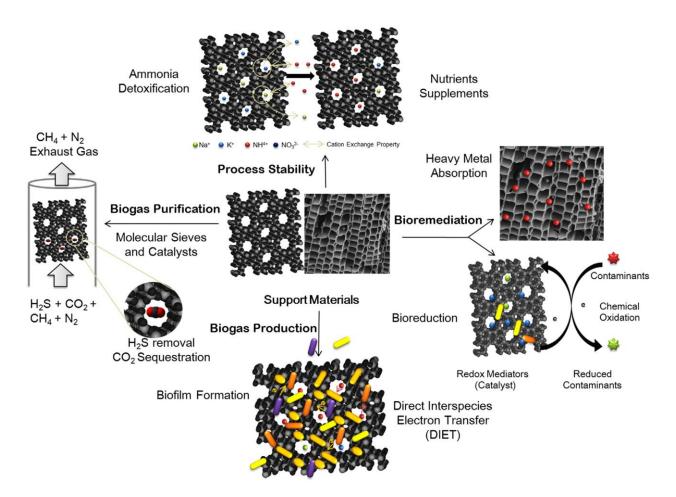


Figure 3: Benefits of Additive materials in Anaerobic Digestion Process - Adapted from Arif et al. 2018 (Arif et al., 2018)

This research is categorized into five areas, each of which covers a unique prospect of iron-based additions in anaerobic digestion. Before digging into the details of iron-based additions and their effects on the A-D process, an overview of the world population and its consequences, the demand for renewable energy, the importance of biofuels, and their environmental effects were investigated. The A-D process and its enhancement methods were also investigated. Finally, the significance of iron as an addition, as well as its influence on A-D process performance, is discussed.

Figure 4 depicts the approach and methods used in conducting this review. The global energy dilemma was initially discussed, followed by biomass energy prospects as a substitute for fossil fuels, biodegradation of biomasses challenges, and prospective intensification approaches for biogas production. On one hand, as shown in Table 1, reviews of the most often used iron-based additives for anaerobic digestion improvement were identified and classified into iron scraps and wastes, iron powders, iron nanoparticles, and the Fenton process. The impact of iron supplementation on biogas generation and methane content, solid reduction, pathogen reduction, and other topics were discussed. Finally, the development of iron precipitates and their fate following digestate disposal were discussed. It was suggested that future research into suitable additives for preventing iron complexes be conducted.

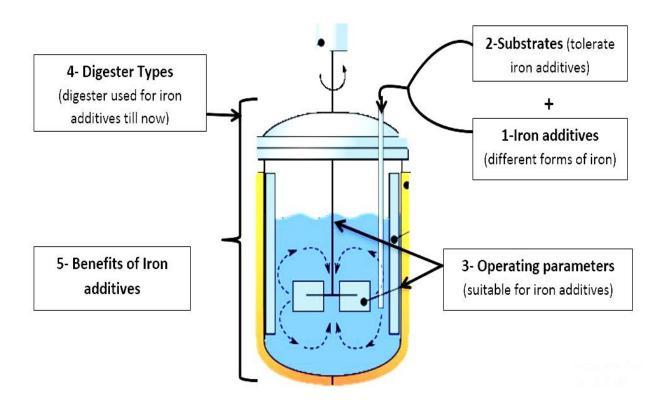


Figure 4: Major Focused Areas of this Study

#### 3- IRON AND IRON-BASED ADDITIVES: -

Because of its conductive qualities and inexpensive cost, iron has become one of the most popular additions for improving anaerobic digestion efficacy. The ability of iron to lower the oxidative–reductive potential (ORP) of anaerobic digestion media and thus provide a more favorable environment for anaerobic digestion; and (ii) its role as a cofactor of several key enzymatic activities, such as pyruvate–ferrodoxin oxidoreductase, which contains Fe–S clusters and plays a key role in fermentation Anaerobic digestion has been reported to be stimulated by various iron types. On the one hand, Fe (III) reduction is a good way to oxidize organics directly into simple molecules. Nonetheless, because Fe (III) reduction is more thermodynamically advantageous than methanogenesis, it can limit the conversion of organics to methane. Due to its ability to operate as an electron donor, Fe<sup>0</sup> (also known as zero valent iron (ZVI)) has been discovered to speed up the hydrolysis and fermentation processes.

Previous studies show that different types of iron additives can be used in the A-D process for efficiency enhancement, nutrients supplement, and to improve substrate digestibility. Iron-based additives can be prepared by adopting different methods before using them into the A-D process. Most commonly used iron-based additives are Waste iron scraps (Wiss), Iron Nanoparticles (Fe NPs), Iron chlorides (FeCl<sub>2</sub>,FeCl<sub>3</sub>), Zero Valent Scrap Iron (ZVSI), Iron oxides (Fe<sub>2</sub>O<sub>3</sub>,Fe<sub>3</sub>O<sub>4</sub>), Iron powder (Fe powder), Zero Valent Iron (ZVI), Iron sulfate (FeSO<sub>4</sub>) and NanoZero Valent Iron (NZVI). Table.1 depicts various types of iron-based additives reported until now and their preparation method.

Table 1: iron-based additives and their preparation method

Type	Color	Source	Source Size Method of Preparation		Ref
WIS	Brown	The byproduct of	0.5-8 mm	WIS is soaked in 0.1mol/L of	(Hao et
(Rusted)		manufacturing industries		NaOH solution for 1 day before	al., 2017)
				use	
ZVSI	Grey	Scrap from ironwork	2 mm	WIS is soaked in 4% solution	(Wang et
	powder		width, 0.35	of CuCl <sub>2</sub> prepared in ethanol	al., 2018)
			mm	for 24 hours and wash with	
			thickness	distilled water	
Fe	Ash Grey	Commercially available	0.2 mm in	commercially prepared by	(Suanon
powder			diameter	industries	et al.,
					2017)
Fe <sub>2</sub> O <sub>3</sub>	Red	the by-product of bauxite	50 to 300	Method not defined	(Ye et
	powder	ore from refining	mm in		al., 2018)
			diameter		
Fe <sub>3</sub> O <sub>4</sub>	Black	Commercially available	0.2 mm in	commercially prepared by	(Chen et
	powder		diameter	industries	al., 2018)
NZVI	Black	Synthesized using Iron and	0.1 to 25	NaHB4 and FeSO <sub>4</sub> via liquid-	(Suanon
	powder	NaHB4	nm	phase reduction method in	et al.,
				anaerobic conditions	2017)
Fe <sub>2</sub> O <sub>3</sub>	Dark Red	Granular FeCl <sub>3</sub> .6H <sub>2</sub> O and	0.1 to 100	Co-precipitation method	(Noonari
NPs		25% ammonia solution	nm		et al.,
					2019)
Fe <sub>3</sub> O <sub>4</sub>	Black	FeCl2.4H2O and	10-35nm	Hydrothermal Method	(Ali et
NPs	powder	FeCl3.6H2O			al., 2017)

 $Fe_3O_4$  additive to the A-D process reported having a significant effect on biogas yield followed by its nanoparticles ( $Fe_3O_4$  NPs), Iron powder, and Iron nanoparticles. These additives also help to improve substrate digestibility by decomposition of lignocellulosic biomass into a simple structure (Zhao et al., 2017). It is also reported that  $Fe_3O_4$  NPs produces higher biogas yield as compared to NZVI (Abdelsalam et al., 2017). The highest biogas yield ever reported from the A-D process is also achieved using  $Fe_3O_4$  NPs additives (Casals et al., 2014). Studies show that  $FeSO_4$ , Fe(OH),  $Fe_2O_3$ , and  $Fe(NO)_3$  additives have no significant effect to increase biogas yield and substrate digestibility (S N Ugwu et al., 2020).

### 4 - SUBSTRATES:-

Various substrates can be used in the A-D process for biogas production. Lots of studies have been done that show that iron additives can increase the biogas yield and improve the process stability by utilizing different substrates. Ali et al. (2017) reported the use of Municipal Solid Waste (MSW) as a substrate for the A-D process with Fe<sub>3</sub>O<sub>4</sub>

nanoparticles additive. He suggested that 75mg/L concentration of iron-based additive had a 72.09% improvement in methane generation. Abdelsalam et al. (2017) investigated the effect of iron nanoparticles and iron oxide nanoparticles on biogas and methane production using cattle dung slurry and found that Fe<sub>3</sub>O<sub>4</sub> NPs having 20mg/L concentration result in 65.6% increase in biogas production.

Wei et al. (2018) reported the use of ZVI to enhance the methane generation using wastewater sludge as a substrate for the A-D process. He found that there was a 26.9% relative increase in methane yield using ZVI as an additive because it improved the hydrolysis rate of reaction. Noonari et al. (2019) tested the use of canola straws and banana plant waste as Co-Digestion with buffalo dung as inoculum with Fe<sub>3</sub>O<sub>4</sub> nanoparticles additive and found that methane generation from canola straw and buffalo dung was increased by 39.1% with 0.81 mg dosage of iron-based additive.

Farghali et al. (2020) reported the use of waste iron powder and iron oxide nanoparticles with cattle manure substrate (F/I ratio 2:1) and found that methane yield from cattle manure increased by 57% and H<sub>2</sub>S production rate also reduced by 77.2% using waste iron powder additive with a concentration of 1000 mg/L. Cheng et al. (2020) investigated the effect of rusted iron shavings on a mixture of food wastes and municipal sludge and noted that rusted iron shavings increase the removal rate of volatile suspended solids by 18% and methane yield by 64.4% compared with the case in which no iron shavings added. It also produces a reductive environment which leads to an increase in methane yield.

Previous studies have proved that Fe<sub>3</sub>O<sub>4</sub> and its nanoparticles additives have a significant effect in the enhancement of methane and biogas generation using various substrates like cattle dung, municipal solid waste, wastewater sludge, canola straws and banana plant waste with buffalo dung inoculum, food wastes and municipal sludge waste used in different anaerobic digesters and varying operating parameters.

### 4 - OPERATING PARAMETERS & DIGESTER TYPE:-

Previous studies have proven to be very effective in improving the methane generation, process stability, and digestion rate. All these improvements are subjected to the optimum selection of the anaerobic digester and operating parameters of the A-D Process. The batch reactor is the preferable mode for the anaerobic digestion process.

Table 2 presents suitable operating parameters for the A-D process and their effects on biogas and methane yield for all the previous studies mentioned above.

Table 2: Iron based additives, operating parameters, digester type and impact on biogas and methane production

Additive	Substrat	Size	Digester	HRT	RPM	pН	Dosag	Effects	Ref
	e		type and	(Days			e		
			Temp.	)					
Fe <sub>3</sub> O <sub>4</sub>	MSW	10-	Batch	60		6.74	50mg/	65.4% increase in	(Ali et
NPs		35	Anaerobic				L	methane	al.,
		nm	Digester					generation	2017)
			37±0.5°C			6.99	75mg/	72.1% increase in	-
			57 <u>=</u> 0.6				L	methane	
								generation	
						7.01	100mg	44.2% increase in	-
							/L	methane	
								generation	
						7.11	125mg	42.5% increase in	
							/L	methane	
								generation	
Fe NPs	Cattle Dung	9±0. 3 nm	2-L wide neck culture	50	20 for 1min	6.13 (man	5mg/L	43.7% increase in biogas generation	(Abdel alam e
	Dung		neck culture		1min				alam e
	Slurry		vessel flask		per	ure)	10mg/	45.1% increase in	al.,
			(batch		hour	and	L	biogas generation	2017)
			mode)			5.85	20mg/	45.4% increase in	
						(slurr	L	biogas generation	
Fe <sub>3</sub> O <sub>4</sub>		7±0.	37±0.3°C			y)	5mg/L	63.1% increase in	
NPs		3 nm						biogas generation	
							10mg/	64.5% increase in	
							L	biogas generation	
							20mg/	65.6% increase in	
							L	biogas generation	
ZVI	Waste	0.2	Batch	50		5.9	1g/L	12.4% increase in	(Wei e
	Water	mm	Anaerobic			(subst		methane	al.,
	Sludge		Digester			rate)		production	2018)
						7.4	4g/L	26.9% increase in	-
			35±1 °C			(inoc		methane	

						ulum)		production	
							20g/L	21.7 % increase in	-
								methane	
								production	
Fe <sub>3</sub> O <sub>4</sub>		1µm		40		6.9	0.4mg/	26.1% increase in	(Noona
NPs							L	methane	i et al.
	Banana		Continuous		70 for			production	2019)
	Plant		stirred tank		1min	7.1	0.5mg/	49.3% increase in	
	Waste		reactor		after		L	methane	
	With				every			production	
	Buffalo		37±1 °C		30	7.2	0.82m	33.9% increase in	-
	Dung				min		g/L	methane	
								production	
						7.5	1.22m	20.1% increase in	
							g/L	methane	
								production	
						7.6	1.63m	17.7% increase in	
							g/L	methane	
								production	
Waste	Dairy	20	Batch	30		7.2-	100mg	37% increase in	(Fargha
iron	Manure	μm	Anaerobic			7.4	/L	methane yield	i et al.
Powder			Bio-Digester			7.2-	500mg	39.4% increase in	2020)
			with			7.5	/L	methane yield	
			Thermo-			7.2-	1000m	56.9% increase in	•
			cooled bath			7.5	g/L	methane yield	
Iron	-	20-				7.2-	100mg	19.7% increase in	-
oxide		40	38 °C			7.4	/L	methane yield	
NPs		nm				7.3-	500mg	18.1% increase in	-
						7.5	/L	methane yield	
						7.3-	1000m	21.1% increase in	-
						7.5	g/L	methane yield	
Rusted	Mixed	10m	2.5 L lab-	36	A	5.6-7	25g/L	64.4% increase in	(Cheng
Iron	Food	$m\times2$	scale		sampl			methane	et al.,
Shaving	Wastes &	mm	Anaerobic		e			production	2020)
s	Municipa	× 0.5	Digester		mixed				
	1 Sludge	mm	35±1 °C		by				
					6500				

					rpm				
					for 15				
					min				
ZVI	Dewatere	50	3-L	100	Samp	6.8-	0.5g/L	18.7% increase in	(Xiang
	d sludge	nm	Continuous		le	7.6		biogas yield	et al.,
			stirred tank		agitat		1g/L	21.7% increase in	2019)
			reactor		ed by			biogas yield	
			35 °C		5000		2g/L	16.8% increase in	
					rpm			biogas yield	
					for 10		4g/L	14.3% increase in	
					min			biogas yield	

#### 5 - BENEFITS OF IRON BASE ADDITIVES:-

Iron can act as an electron acceptor as well as an electron donor in the redox reaction of the A-D process that's why iron-based additives can be used for the improvement of methane generation. Iron-based additives have lots of advantages like improvement of methane yield, control of  $H_2S$  inhibition, supplementation of nutrients, and much more. This section highlights the impact of iron-based additives on Volatile Fatty Acids (VFAs), reduction of Volatile Suspended Solids (VSS), and biogas content.

### 5.1- METHANE CONTENT & BIOGAS OUTPUT: -

Iron based additives can promote the total methane generation because iron based additives promote the production of acetate which is an essential input to produce methane through methanogenesis process. Iron based additives can also act as donor of electrons directly, which causes the reduction of carbon dioxide into methane through hydrogenotrophic methanogenesis triggering the enhancement of methane generation (Abdelsalam et al., 2017). Amen et al. (Amen & Eljamal, 2017) examined the effects of a pure nZVI, nZVI coated (ICZ), and nZVI mixed with zeolite (IMZ) augmented anaerobic response to a control bioreaction. The addition of 1000 mg/L iron-based nanoparticles to ICZ helped achieve the largest cumulative methane volume. The inclusion of nZVI and IMZ, on the other hand, resulted in upward stimulation of greatest methane level of 88 percent and 74 percent, respectively. Similarly, the excess hydrogen released by nZVI (30 mol/L) oxidation enhanced hydrogenotrophic methanogenesis, resulting in a 30% increase in biogas output (He et al., 2017). The addition of a larger dose of nZVI/CUo (>1500 mg/L) on the other hand, decreased biogas generation (Amen et al., 2018).

Previous studies show that iron-based additives have a very significant impact on enhanced biogas production and the improvement of methane content. Ali et al. (2017) reported 72.1% escalation in methane content, Abdelsalam et al. (2017) reported 65.6 % increase in biogas production, Farghali et al. (2020) reported 56.9% rise in methane

generation and Cheng et al. (2020) reported 64.4 % increase in methane generation using various iron base additives.

### 5.2- AVOIDING VFAS:-

Excess VFAs are produced when substrates are hydrolyzed; this may lead to a lowering of pH and finally inhibition of methanogens process. This problem can be solved using iron-based additives in the A-D process (Zhang et al., 2016). Feng et al. (2014) stated the reduction in the quantity of VFAs from 530 mg-COD/L to 19.8 mg-COD/L by using ZVI in the A-D process. Similarly, Hao et al. (2017) noted a sharp drop in the quantity of VFAs by using waste iron scrap additives. He reported a decline of 700 mg-COD/L. Intermediate products such as volatile fatty acids (VFAs) are critical in the biogas production process during anaerobic digestion. They are carboxylic short-chain fatty acids (C2-C6) generated by syntrophic bacteria following biomass hydrolysis. In an anaerobic digestion process, several parameters like as pH and the inclusion of iron-based supplements might impact VFAs. At a pH below 2, propionic acid and butyric acid, the two primary VFA products in the acidification step, decompose exclusively into acetate. Propionate accumulation and disruption of pH balance between acidogenesis and methanogenesis are caused by the high rate of propionate production and low decomposition rate (much lower than other VFAs), but according to Zhang, Zhang, and Li (2015), the addition of trace iron could stabilise anaerobic digestion processes.

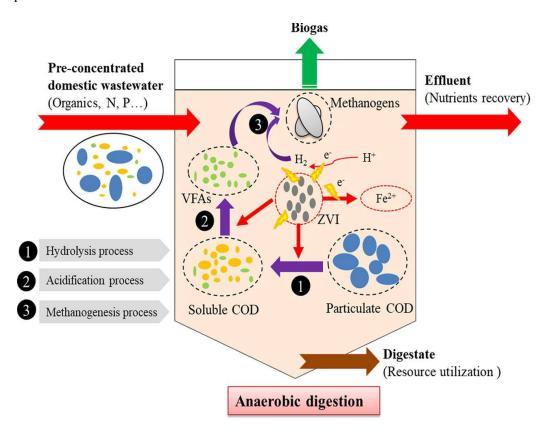


Figure 5: ZVI effects on three anaerobic digestion process- Adapted from Feng et al. 2015

### 5.3- VSS REDUCTION:-

Substrate degradation by microorganisms results in a decrease in the amount of total VSS. This is also known as Chemical Oxygen Demand (COD) (Samson Nnaemeka Ugwu & Enweremadu, 2020). In the studies of Hao et al. (2017), it was examined that the addition of iron scrap (waste) can improve the VSS reduction rate by 14%. Zhang et al. (2016) stated the use of clean iron scrap in the A-D process which resulted in the maximum VSS rate of reduction 49%. However, in the Fenton peroxidation process, the usage of H2O2 catalysed by iron salts dissolved sludges and broke down cellular elements, resulting in higher sCOD concentrations (Salihu and Alam 2016). Throughout the digestion phase, Uman et al. (2018) showed a rather low sCOD content of around 250 mg/L. Maamir et al. (2017) found that when the concentration of H2O2 grew from 125 to 1000 mM, the COD of Fenton-treated substrate increased from 1133 to 5594 mg/O2 (56%) when compared to the control COD value of 1123 mgO2/L until optimal working conditions were reached. The ideal Fenton procedure processed olive mill solid waste obtained an 82 percent sCOD rise under these working conditions (pH 3, 120 minutes, H2O2/[Fe2 +] = 1000 and [Fe2+] = 1.5 mM) (Rezaei & Vione, 2018).

In tests done by Hao (Hao et al., 2017), the addition of WIS enhanced the elimination of VSS by 4.5 percent and 14.0 percent of the additional raw substrate VSS, respectively, at both the acidogenic and methanogenic stages of anaerobic digestion. A comparable study found that removing solids with iron shavings resulted in carbohydrate ingestion of 75 to 98 percent. According to Zhang et al. (2014), the iron-enhanced reactors using rusty scraps, Fe powder, and clean scrap had the maximum VSS reduction rate of 48.27 percent. According to Amen et al. (2017), the addition of nZVI, IMZ, and ICZ to the substrate digestion of volatile solid fraction resulted in a volatile solid reduction of up to 23.8 percent, and that for up-scaling, 1 g of volatile solids will require 2.67 g of ICZ particles to achieve maximum solid removal and methane yield (Amen & Eljamal, 2017).

### 4- CONCLUSIONS:-

The addition of iron-based additives to an anaerobic digester can have significant effects like enhancement of biogas generation, increased VSS rate of reduction, improvement of process stability, and reduction of VFAs. A detailed literature analysis has been conducted for a better understanding of recent advancements in this field. Previous studies related to iron-based additives in the A-D process have been studied and are presented in this study. This study has discussed the following topics in detail:

- types of iron-based additives, their source, preparation method, color, and size.
- Substrates reported in previous studies to check the effect of iron-based additives
- Optimal operating parameters using iron-based additives
- preferred type and mode of anaerobic digester.
- Benefits of using iron-based additives include methane content, VFA limitation, and VSS reduction rate.

This study examined all these issues and concluded that Fe3O4 and Fe3O4 NPs additives had a considerable effect on biogas yield augmentation when compared to other iron-based additives. Most studies choose a mesophilic temperature range for the A-D process, mixing of the substrate at varying rpm to homogenize the substrate and inoculum, batch-mode anaerobic digesters for research reasons, and HRT ranging from 40 to 100 days depending on the nature of the study. Finally, it has been established that iron-based additions considerably improve the rate of biogas generation and increase the rate of VSS reduction. Since no essential research work has been done in these areas, it is recommended that future researchers investigate the effects of variations in organic load rating (OLR) and thermophilic operating temperature on the anaerobic digestion process utilizing iron-based additions.

## 5-STATEMENT AND DECLARATION:-

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