

Article

Assessment of K-struvite precipitation as a means of nutrient recovery from source separated human urine

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Abstract: The impact of nutrients on the environment, particularly on water bodies, has led to extensive studies for nutrient control. Within this context, studies have been focused on source separation of human urine from domestic wastewater to recover nutrients. Potassium is one of the most important components of human urine. However, data on potassium removal or recovery are quite limited except for some indirect information through use of zeolites for mostly ammonia removal. Potassium struvite or K-struvite ($\text{MgKPO}_4 \cdot 6\text{H}_2\text{O}$) is a sparingly soluble salt belonging to struvite and has the potential of being used as a means of potassium and phosphate recovery from segregated human urine. This study aimed to assess the potential of K-struvite precipitation for control and recovery of nutrients. Within this context, K-struvite precipitation experiments were performed on both synthetically prepared samples and synthetic human urine solution to determine effect of operation parameters i.e. pH, stoichiometry, and temperature on potassium recovery performance. Results indicated that process performance as well as type of solid phases co-precipitated with K-struvite were closely related to initial potassium concentration, pH and reaction stoichiometry. At pH 10, the potassium recovery efficiency was maximized up to 87% by application of 100% excess dose of Mg and P for both synthetic samples and synthetic human urine solution. On the other hand, application of excess dose of K did not provide any improvement in K recovery efficiency. The effect of temperature on solubility of K-struvite was insignificant at the temperature of 24-90°C. Solid phase analyses confirmed that K-struvite was co-precipitated with either $\text{Mg}_3(\text{PO}_4)_2$, $\text{MgNaPO}_4 \cdot 7\text{H}_2\text{O}$, or $\text{MgHPO}_4 \cdot 7\text{H}_2\text{O}$ depending on pH and stoichiometry instead of a pure compound.

Keywords: human urine; K-struvite precipitation; nutrient recovery; operation parameters; solid phases

1. Introduction

Magnesium ammonium phosphate ($\text{MgNH}_4\text{PO}_4 \cdot 6\text{H}_2\text{O}$; MAP), a member of struvite family, has been used with success for nitrogen removal and as a means of nutrient recovery. MAP precipitation has a wide area of application such as source separated urine [1-4], anaerobic treatment discharge [5], as well as a number of industrial wastewaters among them are leather tanning [6-10], slaughterhouse [11], animal husbandries [12], textile printing [13], landfill leachate [14-16], even membrane process concentrates [17]. This has led to the scientists to the other recoverable nutrient, potassium which is also abundant in source-separated urine. The struvite family of compounds also includes magnesium potassium phosphate (K-struvite), a sparingly soluble salt, which has been considered as a potential method for potassium removal and recovery. Potassium is also a valuable nutrient and can be recovered from the source separated urine [18-20]. MAP precipitation is relatively easy to conduct due to two reasons. The first reason is its low solubility with respect to K-struvite and the second is the two major co-precipitating solids; $\text{Mg}(\text{OH})_2$ and $\text{Mg}_3(\text{PO}_4)_2$ can be avoided at the optimum pH of around 9.5 of MAP [21]. K-

struvite precipitation suffers from both higher solubility and unavoidable co-precipitates which make the process a less efficient one with respect to MAP precipitation. Theoretical assessment of the process is not easy, and determination of thermodynamic constants is still on the way. Struvite type of compounds has the general formula of $M^{2+}N^+xO_4 \cdot nH_2O$, where M^{2+} : Mg or Ca; N^+ : K, Rb, Cs, Tl, or Na, NH_4^+ ; x : P or As, and $n=6-8$. Additional information about these compounds can be found elsewhere [22-24]. K-struvite ($MgKPO_4 \cdot 6H_2O$; MPP) is a member of this family. MPP is also a sparingly soluble salt, but its dissolution is not congruent. Because it cannot be precipitated as a pure compound, but rather as a mixture of other sparingly soluble solids in urine and other sodium containing solutions. For the case of source separated urine co-precipitating solids are MPP and magnesium sodium phosphate ($MgNaPO_4 \cdot 7H_2O$; MSP). The exact solubilities of both co-precipitates are not known. For MPP, pK_{sp} values are given as 10.6 [25], 11.7 [26], and 12.2 ± 0.253 [27]. These figures exhibit a wide range. For MSP, Xu and co-workers [27] calculated the pK_{sp} as 11.6 ± 0.253 which is within the range of pK_{sp} values of MPP indicating close K_{sp} values for MPP and MSP. So, they inevitably precipitate together. As the pK_{sp} of MAP 13.26 [28,29], existence of ammonia inhibits the MPP precipitation. Therefore, studies in the literature were conducted on synthetically prepared urine that does not contain ammonia or real urine pre-treated to remove ammonia [24,27,30,31]. Warmadewanthi and Lui [32] claimed that magnesium phosphates (Bobierrite, $Mg_3(PO_4)_2 \cdot 8H_2O$, $pK_{sp}= 25.2$ and tri magnesium phosphate $Mg_3(PO_4)_2 \cdot 22H_2O$, $pK_{sp}= 23.1$) were also co-precipitated with MPP. The pH values over which these solid phases begin to precipitate reported as 12 and 9 for bobierrite and tri magnesium phosphate, respectively. Xu et al. [24] pointed out $Mg_3(PO_4)_2 \cdot 8H_2O$ may precipitate after pH 10 and 11 depending on P:K ratio in MAP precipitation. A similar evaluation was made by Lee et al. [21] and Zhang et al. [33] for MAP precipitation. On the other hand, Taylor et al. [25] reported experimental results of MPP precipitation conducted pH between 10.42 – 10.87 where both bobierrite and tri magnesium phosphate co-precipitated. However, no other study of MPP precipitation cited in this paper has shown any evidence of magnesium phosphate precipitation including crystal identification means such as X-ray diffraction (XRD). Thermodynamic models have not included these compounds as well.

So far MPP precipitations have been conducted in mostly in source separated urine, synthetic urine solution except for a study using 1/5 diluted urine, but in a draft tube and baffle reactor [30]. The present study attempts to evaluate K-struvite precipitation using a wide range of initial potassium concentration (10 - 250 mM) in batch systems with synthetic solutions. The effects of pH, reaction stoichiometry, time and temperature on K recovery performance were investigated. The applicability of K-struvite precipitation to the synthetic human urine was explored in terms of process performance. Solid phase analyses were also realized.

2. Materials and Methods

2.1. Samples

Synthetic samples were prepared using KH_2PO_4 and $MgCl_2 \cdot 6H_2O$ and KOH, NaH_2PO_4 , and $MgCl_2 \cdot 6H_2O$ for K-struvite precipitation experiments with stoichiometric and excess doses, respectively. While synthetic human urine prepared, urea was excluded from the original recipe given elsewhere [27,30,34]. The recipe used in the present study is given in Table S1 (see Supplementary Material). All reagents were of analytical grade and purchased from Sigma–Aldrich Chemicals (USA).

2.2. Analytical Procedure and Instruments

Synthetic samples were prepared using CO_2 -free deionized water as explained in our previous study [35]. All analyses were accomplished as defined in Standard Methods for the Examination of Water and Wastewater [36]. pH was measured with Orion 920A model pH meter. PFP7/C Research Flame Photometer (Jenway™) was used for potassium measurement. Solid phase analyses were made using X-ray diffractometer (XRD; Rigaku Dmax

2200, Japan) and scanning electron microscopy (SEM; Philips XL30 SFEG). The deionized water was produced by Sartorius Arium 611 - UV Water Purification System (with conductivity of $0.055 \mu\text{S cm}^{-1}$).

2.3. Precipitation Experiments

500-mL Erlenmeyer flasks with stopper which were equipped with magnetic stirrer to ensure homogenous mixing, were used as precipitation vessels. After reagent addition to CO_2 -free deionized water, if required, initial pH values were adjusted under flash-mixing conditions using NaOH solution (0.1-1 N). During the course of slow-mixing, solution pH was measured once a day and adjusted when necessary. At the end of MPP precipitation, all samples were filtrated through Sartorius 0.45 mm membrane filters before analysing.

2.4. Equilibrium Time and Temperature

In order to determine the duration (time) needed to reach the equilibrium, the 7-day precipitation and a long duration of one-month equilibrium time results were compared for 250 mM initial concentration at pH 9.0 (Table S2, see Supplementary Material). The differences between two durations were slight indicating that the 7-day equilibrium duration was considered adequate for experimental evaluations. This finding is consistent with the result of Xu et al. [27]. After one week storage, maximum relative tolerances were measured as 3.2% and 5.2% for P and K, respectively, in their experiments. Based on these data, they assumed that the reaction time required to reach equilibrium was selected as 60 min.

The effect of temperature on solubility of K-struvite and potentially precipitating other solids was also explored through a MPP precipitation conducted at pH 9.0 by employing 333 mM initial dosage of a stoichiometric K/Mg/P solution. This experiment was realized at room temperature (24°C), 30°C , and 90°C . The results are displayed in Table S3 (see Supplementary Material). As seen from the table, solubilities, or supernatant concentrations after precipitation were almost identical indicating that the effect of temperature was negligible in the range studied. The temperature dependency of magnesium ammonium phosphate (magnesium struvite) has been assessed in the literature and similar results have been found [29]. Based on these data all precipitation experiments were performed in a temperature-controlled laboratory section at $25 \pm 0.1^\circ\text{C}$ for a week ensuring equilibrium condition.

3. Results and discussion

3.1. Effect of pH

pH is one of the key parameters in precipitation processes which involve acid-base reactions. The first experimental evaluation was made using a 250 mM initial concentration with a K/Mg/P molar ratio of 1/1/1 to ensure high level of saturation for a wide pH range of 6 to 11. The results of MPP precipitation performed using KH_2PO_4 and $\text{MgCl}_2 \cdot 6\text{H}_2\text{O}$ as precipitating agents are presented in Table 1.

The results indicated that K concentration together with P and Mg decreased in all experiments with pH values between 7.03 and 11.00. At pH 6.06, however, K concentration remained unchanged, while P and Mg concentration significantly reduced from 250 mM to 16 mM. Considering that the formation of MSP was impossible since no pH adjustment was made using NaOH during this run, the significant reduction of both Mg and P might be attributed to the precipitation of MgHPO_4 . At pH 7.03, K removal with precipitation is evident and only K salt precipitating is MPP. The precipitate was assumed to be a mixture of MgHPO_4 and MPP because K removal was 20% and NaOH addition for pH adjustment was extremely low. Results of precipitation at pH 7.99 could be interpreted in a similar manner as that of 7.03 while MPP precipitation becoming significantly higher as K removal was 44%. The precipitation conducted at pH 9.14 yielded slightly higher K removal than that of pH 7.99 indicating almost the same extent of MPP precipitation.

MgHPO₄ even Mg(OH)₂ were not likely to precipitate leaving only possibility of MSP. Results of pH 10.01 and pH 11.00 were quite similar with one another and seemed to have similar mechanism with that of pH 9.14, with a small reduction in K recovery efficiency. Although, residual K concentrations differed, the mechanism depicted above was in accordance with the experimental results of Taylor et al. [25]. Xu et al. [24] in their experimental study with synthetic urine found that K removal efficiencies decreased after pH 12, pH 10 and 11 yielded efficiencies very close to each other and represented optimum pH for K removal. They explained the K removal efficiency drop at pH 12 with formation of Mg(OH)₂ and Mg₃(PO₄)₂. Huang et al [31] tested low grade MgO as a means of K removal from urine that was pre-treated to remove ammonia. Their experimental data indicated that K precipitation remained practically unchanged after pH of approximately 10.7.

Table 1. Effect of pH on K-struvite precipitation (K/Mg/P: 250/250/250 mM)

pH	Unit	Initial			Final		
		K	P	Mg	K	P	Mg
6.06	mM	250	250	250	248	16	16
	mg/L	9775	7750	6076	9714	520	390
7.03	mM	250	250	250	198	16	5
	mg/L	9775	7750	6076	7772	553	134
7.99	mM	250	250	250	138	7.5	8
	mg/L	9775	7750	6076	5399	232	200
9.14	mM	250	250	250	132	5	1.5
	mg/L	9775	7750	6076	5366	148	34
10.01	mM	250	250	250	144	6	1.5
	mg/L	9775	7750	6076	5645	189	27
11.00	mM	250	250	250	147	6	0.9
	mg/L	9775	7750	6076	5763	97	24

In the light of the above evaluations, forthcoming MPP precipitation experiments were run within the range of 8-10. In the present paper, we also intentionally avoided to use the term “optimum pH” since it does not seem meaningful for a system where more than one solid phase precipitating. Instead, the term “maximum removal or recovery” could be used which is relative to system composition and aim of the work.

To assess the effect of pH on K recovery performance another set of precipitation experiments was run at pH 9 and 10 with an initial concentration of 100 mM equimolar Mg, K, and P, which represented upper concentration of K in human urine. The results are outlined in Table 2. As seen from the table, while residual P and Mg concentrations were similar with those of the experiments with 250 mM initial concentration, resulting K concentration was lower, K recovery efficiency was also reduced (at pH 9 dropped from 47% to 25%).

Table 2. Effect of pH on K-struvite recovery (K/Mg/P: 100/100/100 mM)

pH	Unit	Initial			Final		
		K	P	Mg	K	P	Mg
9.03	mM	100	100	100	75	1.3	1.3
	mg/L	3910	3100	2431	2937	41	32
10.05	mM	100	100	100	72	0.2	6
	mg/L	3910	3100	2431	2812	7	16

Table 3 displays the results of precipitation experiments initiated at 10 mM stoichiometric dose. As seen in the table, K recovery efficiencies were maximum 7% and did not change by pH. Data given in this subsection, altogether indicated that K recovery efficiencies constantly decreased as initial K concentration reduced and became practically inapplicable for 10 mM (390 mgK L⁻¹).

Table 3. Effect of pH on K-struvite recovery (K/Mg/P: 10/10/10 mM)

pH	Unit	Initial			Final		
		K	P	Mg	K	P	Mg
8.08	mM	10	10	10	9.5	4.9	0.3
	mg/L	391	310	243	373	154	0.8
9.10	mM	10	10	10	9.3	3.4	3
	mg/L	391	310	243	367	106	0.7
10.00	mM	10	10	10	9.3	2.8	2
	mg/L	391	310	243	363	88	0.5

3.2. Precipitation with Different Stoichiometry

To investigate the effect of the reaction stoichiometry on the process performance, MPP precipitation experiments with over-stoichiometric dose were planned and realized. KOH, NaH₂PO₄, and MgCl₂·6H₂O were utilized as reagents in these experiments. In the first step, K was dosed over stoichiometric to Mg and P at the excess K ratios 20, 34 and 44%. The results are outlined in Table 4.

Table 4. Effect of excess K dose on process performance

pH	Unit	Initial			Final		
		K	P	Mg	K	P	Mg
9.02	mM	180	150	150	121	1.65	1.6
	mg/L	7038	4650	3646	4731	50	40
9.02	mM	180	125	125	112	2.4	1.3
	mg/L	7038	3875	3038	4379	74	32
8.99	mM	250	187	187	190	2.2	0.9
	mg/L	9775	5797	4545	7429	68	22

As seen in Table 4, for 125 and 150 mM doses of Mg and P, application of 180 mM K resulted in very low residual P and Mg levels. K removals were limited to 32 and 37% for 150 and 125 mM doses, respectively, exhibiting much less than KMgPO₄ stoichiometry. For a K dose of 250 mM, P and Mg levels were again low, but K removal was at 24% and the residual amount at 190 mM, whereas it was 132 mM for 250 mM stoichiometric (K/Mg/P: 1/1/1) dosing at pH 9.14 (Table 1). These results indicate that overdose of K was ineffective in controlling and improving the K recovery performance.

In the second step, the effect of overdoses of Mg and P on K recovery efficiency was explored at pH values of 9 and/or 10. Table 5 shows the results of these experiments. For 180 mM K concentration, increasing both Mg and P doses from 187.5 to 250 mM improved K recovery efficiency from 24% to 50%. The improvement in K recovery efficiency was also evident at 100 % overdoses of P and Mg for a wide range of initial K concentration from 6.25 to 125 mM. The maximum K recovery was obtained as 85 % with 100 mM K concentration at pH 10.02. Comparison K recovery efficiencies obtained at pH 9 with those of pH 10 showed that using pH 10 seemed more effective to enhance K recovery. Furthermore, in all experiments, residual Mg and P values were very low indicating simultaneous

precipitation of magnesium phosphate solids. Therefore, over stoichiometric Mg and P application would help K recovery without an increase in residual Mg and P.

Table 5. Results of precipitation experiments at overdoses of Mg and P

pH		Initial			Final		
		K	P	Mg	K	P	Mg
9.09	mM	180	187.5	187.5	135	1.9	1.4
	mg/L	7038	5813	4557	5278	59	34
9.07	mM	180	250	250	90	0.4	4
	mg/L	7038	7750	6076	3519	12	97
9.07	mM	125	250	250	41	0.9	3
	mg/L	4887	7750	6076	1603	28	73
9.00	mM	50	100	100	17	1.9	2
	mg/L	1955	3100	2431	686	59	51
10.03	mM	125	250	250	38	3	0.6
	mg/L	4887	7750	6076	1486	93	15
10.02	mM	100	200	200	15	0.2	1.5
	mg/L	3901	6200	4861	578	8	36
10.02	mM	50	100	100	11	0.2	1.4
	mg/L	1955	3100	2431	441	6	34
10.11	mM	25	50	50	7	0.8	1.3
	mg/L	977	1550	1215	276	24	32
10.08	mM	12.5	25	25	6	1	1.2
	mg/L	489	775	608	254	31	29
10.12	mM	6.25	12.5	12.5	5	1.9	1.2
	mg/L	244	387	303	176	57	30

3.3. Dissolution of Precipitate

To determine the components and their composition of the precipitate produced in the experiments, a selected solid phase (obtained from the experiment run at 250 mM stoichiometric doses of K/Mg/P and pH 9.0) was completely dissolved in acid. The amount of solid dissolved was 8 gL⁻¹. The composition of the obtained solution was found as shown in Table 6.

Table 6. Composition of precipitate

	K	PO ₄	Mg	Na
mM	6.5	19	19	7

The results clearly showed that amount of P and Mg were several folds greater than K indicating high amount of magnesium phosphate contributed to the solid. Existence of sodium was almost equal amount of K suggested the presence of a sodium containing solid which was likely to be MSP [37]. The obtained solid phase stoichiometry is Mg/K/Na/P: 2.9/1/1.01/2.9 and the stoichiometry of both MSP and MPP is 2/1/1/2. This finding gives the impression as if the solid phase comprised a mixture of MSP, MPP and some magnesium phosphates.

3.4. Potassium Recovery from Human Urine

Human urine is the principal source for potassium recovery using K-struvite precipitation. Therefore, we also conducted precipitation experiments on synthetic human urine (SHU) defined in the Materials and Methods section. Considering the findings in the relevant literature [24,27,30,38] that ammonia removal by a suitable process, such as stripping, prior to K-struvite precipitation is an essential step so as to enhance K recovery from SHU solutions, urea was not added to the SHU solution to avoid MAP precipitation. So, the main reactive species of SHU were K, Mg and P. The results obtained from our experimental study and their interpretation strongly suggested that in a such system the solid phase would be composed of a mixture of different substances. Therefore, different stoichiometric doses were employed in these precipitation experiments. The obtained results are given in Table 7.

Table 7. Results of K-struvite precipitation for SHU solution

pH	K:Mg:P		Initial			Final	
			K	P	Mg	K	P
9.40	3/1/0.5	mM	31.82	10.32	5.16	23	3.44
		mg/L	1244	319	125	920	106
9.42	3/1/1	mM	31.82	10.32	10.32	24	0,99
		mg/L	1244	319	251	954	29
9.39	3/1/1.3	mM	31.82	10.32	13.41	24	0.36
		mg/L	1244	319	326	953	11
9.44	3/1/1.5	mM	31.82	10.32	15.48	25	0.14
		mg/L	1244	319	376	988	4
9.48	1/1/1	mM	31.82	31.82	31.82	25	0.01
		mg/L	1244	986	773	989	1
9.44	1/2/2	mM	31.82	63.64	63.64	11	9.67
		mg/L	1244	1972	1547	441	300
10.04	1/2/2	mM	31.82	63.64	63.64	4	4.78
		mg/L	1244	1972	1547	167	147

As seen in Table 7, the best result, through the experiments conducted using SHU solution with initial K concentration of 31.82 mM, was obtained as 87% K recovery with K/Mg/P ratio of 1/2/2 and at pH 10.04. With the same stoichiometry, but at pH 9.44, K recovery (67%) as well as P removal decreased. These K recovery efficiencies are comparable with data published in the literature. For example, ammonium, K, and P removals were reported as 73%, 76%, and 68%, respectively, in Xu et al. [30] study performed on ammonia stripped-diluted (1/5) real human urine in a laboratory-scale draft tube and baffle reactor. In another study, conducted in a pilot-scale fluidized bed reactor using SHU (recipe: 30.9 mM KH_2PO_4 , 21 mM KCl, 0.7 mM $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$, 78.7 mM NaCl, 16.2 mM Na_2SO_4 , and 2.86 mM NH_4Cl), for optimized operation conditions of pH of 10.5, Mg:P molar ratio of 1:1, super saturation ratio of 3.0, and superficial velocity of 350 cm min^{-1} , K and P removal efficiencies were reported as 20–35% and 80–90%, respectively [38]. This K removal efficiency is the same level with that of the precipitation experiment conducted at pH 9.48 with the K/Mg/P stoichiometry of 1/1/1.

3.5. Solid phase analyses

Further studies were conducted to assess the solid phases that were formed through the K-struvite precipitation. Within the context, three selected solid phases were analysed using x-ray diffraction (XRD) method (Fig. S1-S3, see Supplementary Material). The first solid phase was the one obtained from the precipitation at pH 10.05 with stoichiometric dose (K/Mg/P: 1/1/1) for an initial K concentration of 100 mM. The result indicated the existence of magnesium phosphate and consistent with the discussion of this experiment as well as with the experimental evaluation given by Taylor et al. [25]. Other solid phases analysed using XRD were the precipitates that resulted from the experiments at the pH 10 with the applications of over-stoichiometric (K/Mg/P: 125/250/250 mM) and stoichiometric (250/250/250 mM) Mg and P doses. Examination of these results showed that the existence of sodium in the solid rather than magnesium phosphate implying the structure of MSP as pointed out in the relevant literature [24,27,30] .

Scanning electron microscope (SEM) photographs of solid phases obtained through the experiments were used to evaluate the morphology of the precipitates (Figure 1)

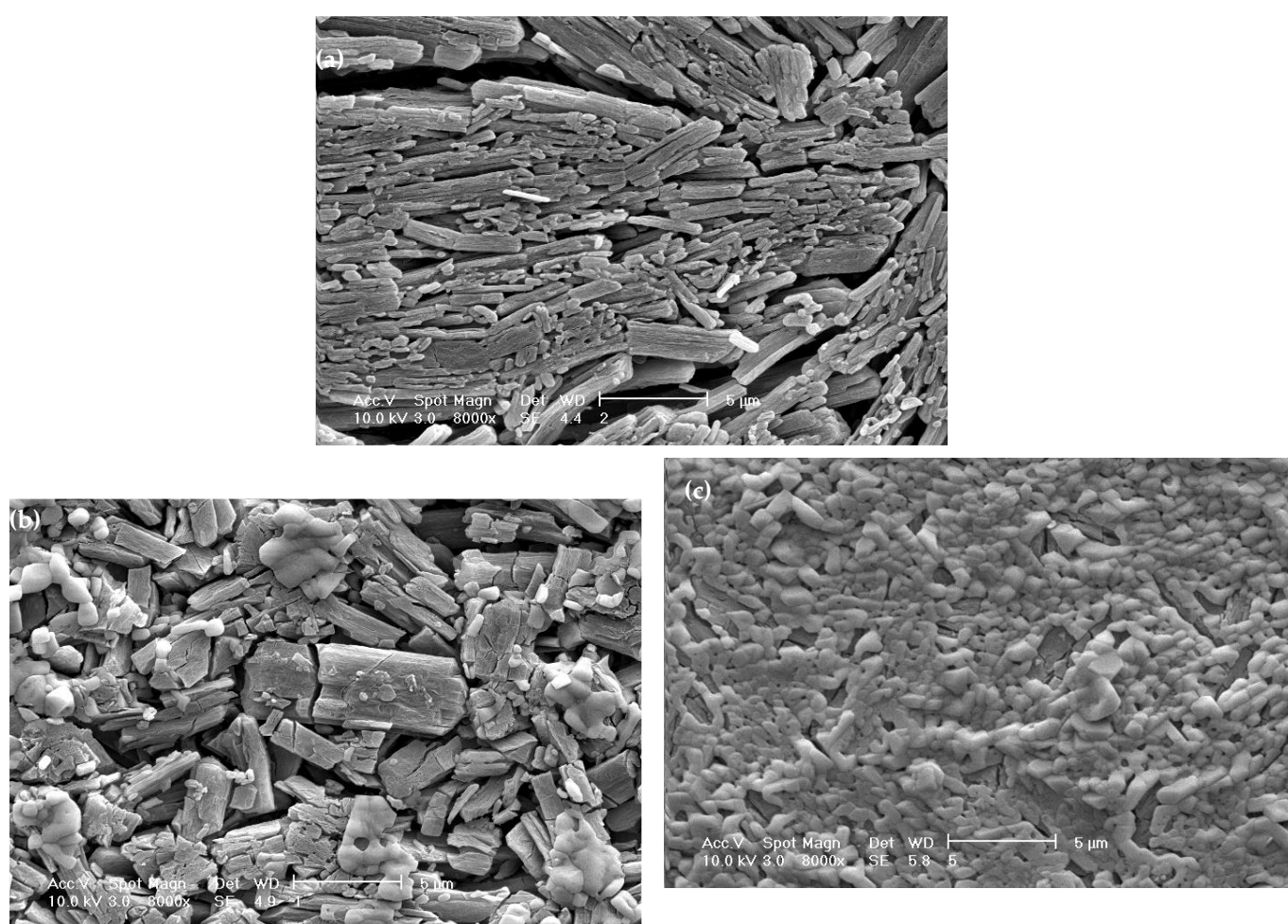


Figure 1. SEM analyses of solid products obtained from precipitation experiments performed at (a) pH 9.14 and K/Mg/P: 250/250/250 mM, (b) pH 10.05 and K/Mg/P: 100/100/100 mM, and (c) pH 10.03 and K/Mg/P: 125/250/250 mM.

In Figure 1 (a) K-struvite crystals can be clearly seen as a similar structure with that of MAP having long needle like shape. In Figure 1 (b) magnesium phosphate crystals with their spherical shape and together with K-struvite can be observed. Their size was irregular. In the case of overdose of Mg and P a mixture of crystals each having different structure was noticed (Figure 1(c)).

4. Conclusions

The following conclusions could be drawn from the present study.

- ✓ In the case of synthetic samples, K recovery efficiency found to be dependent on initial K concentration, reaction stoichiometry and pH.
- ✓ K recovery efficiencies reduced while initial K concentration decreased. The lowest K recovery efficiency (7%) was obtained for initial K concentration of 390 mg K L⁻¹ at stoichiometric dose. For a wide range of initial K concentration of 6.25 to 125 mM, K recovery efficiency improved when applied 100% excess doses of P and Mg to K. On the other hand, excess dose of K found to be incapable of improving K recovery performance.
- ✓ 100% excess dose of Mg and P (K/Mg/P:100/200/200 Mm) yielded K recovery efficiency of 85% corresponding to a maximum one for synthetic samples at pH 10.02. Almost equal K recovery efficiency (87%) was also obtained for synthetic human urine at pH 10.04 and 100% excess dose of Mg and P.
- ✓ In all these precipitation experiments performed using synthetically prepared samples, P and Mg were almost completely precipitated, resulting the effluents with low Mg and P contents.
- ✓ The results indicated that K-struvite never precipitated alone, but its precipitation was accompanied by other solids which, as evidenced by XRD results as well as stoichiometric evaluation of the composition of dissolution of solids, were Mg₃(PO₄)₂, MgNaPO₄·7H₂O, and MgHPO₄·7H₂O.

Supplementary Materials: The following are available online at www.mdpi.com/xxx/s1, Table S1: Recipe of synthetic human urine used in this study [34], Table S2: Effect of duration on K-struvite precipitation performance, Table S3: Effect of temperature on K-struvite precipitation performance, Figure S1: XRD analysis (K/Mg/P: 250/250/250 mM, pH 10.01), Figure S2: XRD analysis (K/Mg/P: 125/250/250 mM, pH 10.03), Figure S3: XRD analysis (K/Mg/P: 100/100/100 mM, pH 10.05).

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References

1. Kabdasli, I.; Tunay, O.; Islek, C.; Erdinc, E.; Huskalar, S.; Tatli, M.B. Nitrogen recovery by urea hydrolysis and struvite precipitation from anthropogenic urine. *Water Science and Technology* **2006**, *53*, 305-312, doi:10.2166/wst.2006.433.
2. Kabdasli, I.; Tunay, O.; Udert, K.M. Transfer into the solid phase. *Source Separation and Decentralization for Wastewater Management* **2013**, 351-365.
3. Kabdasli, I.; Tunay, O.; Tatli, B.M.; Topcuoglu, S. Nitrogen recovery by struvite precipitation from anthropogenic nutrient solution. *Fresenius Environmental Bulletin* **2006**, *15*, 1146-1149.
4. Tünay, O., Kabdaşlı, I.; Tatlı M.B. Nitrogen removal and recovery from human urine by struvite precipitation. *Int. J. Environment and Waste Management* **2009**, *3*, 382-392.
5. Lorick, D.; Macura, B.; Ahlstrom, M.; Grimvall, A.; Harder, R. Effectiveness of struvite precipitation and ammonia stripping for recovery of phosphorus and nitrogen from anaerobic digestate: a systematic review. *Environmental Evidence* **2020**, *9*, doi:10.1186/s13750-020-00211-x.

6. Kabdasli, I.; Tunay, O.; Cetin, M.S.; Olmez, T. Assessment of magnesium ammonium phosphate precipitation for the treatment of leather tanning industry wastewaters. *Water Science and Technology* **2002**, *46*, 231-239.
7. Tunay, O.; Kabdasli, I.; Orhon, D.; Kolcak, S. Ammonia removal by magnesium ammonium phosphate precipitation in industrial wastewaters. *Water Science and Technology* **1997**, *36*, 225-228, doi:10.1016/s0273-1223(97)00391-0.
8. Zengin, G.; Olmez, T.; Dogruel, S.; Kabdasli, I.; Tunay, O. Assessment of source-based nitrogen removal alternatives in leather tanning industry wastewater. *Water Science and Technology* **2002**, *45*, 205-215, doi:10.2166/wst.2002.0428.
9. Tunay, O.; Yelmez, Z.B.; Olmez, T.; Kabdasli, I. Residual COD reduction in biologically treated leather tanning effluents by advanced treatment processes. *Journal of the American Leather Chemists Association* **2006**, *101*, 123-131.
10. Kabdasli, I.; Olmez, T.; Tunay, O. Nitrogen removal from tannery wastewater by protein recovery. *Water Science and Technology* **2003**, *48*, 215-223, doi:10.2166/wst.2003.0058.
11. Kabdasli, I.; Tunay, O.; Ozcan, P. Application of struvite precipitation coupled with biological treatment to slaughterhouse wastewaters. *Environmental Technology* **2009**, *30*, 1095-1101, doi:10.1080/09593330903136856.
12. Huang, H.M.; Xiao, D.A.; Liu, J.H.; Hou, L.; Ding, L. Recovery and removal of nutrients from swine wastewater by using a novel integrated reactor for struvite decomposition and recycling. *Scientific Reports* **2015**, *5*, doi:10.1038/srep10183.
13. Kabdaşlı, I.; Gürel, M.; Tünay, O. Characterization and treatment of textile printing wastewaters. *Environmental Technology* **2000**, *21*, 1147-1155, doi:10.1080/09593330.2000.9619001.
14. Kabdasli, I.; Safak, A.; Tunay, O. Bench-scale evaluation of treatment schemes incorporating struvite precipitation for young landfill leachate. *Waste Management* **2008**, *28*, 2386-2392, doi:10.1016/j.wasman.2007.10.020.
15. Zhang, T.; Ding, L.L.; Ren, H.Q. Pretreatment of ammonium removal from landfill leachate by chemical precipitation. *Journal of Hazardous Materials* **2009**, *166*, 911-915, doi:10.1016/j.jhazmat.2008.11.101.
16. Kabdasli, I.; Tunay, O.; Ozturk, I.; Yilmaz, S.; Arıkan, O. Ammonia removal from young landfill leachate by magnesium ammonium phosphate precipitation and air stripping. *Water Science and Technology* **2000**, *41*, 237-240, doi:10.2166/wst.2000.0034.
17. Arola, K.; Van der Bruggen, B.; Manttari, M.; Kallioinen, M. Treatment options for nanofiltration and reverse osmosis concentrates from municipal wastewater treatment: A review. *Critical Reviews in Environmental Science and Technology* **2019**, *49*, 2049-2116, doi:10.1080/10643389.2019.1594519.
18. Kabdaşlı, I.; Sertaç, B.; Tünay, O. Nutrient removal from human urine by chemical precipitation. *Fresenius Environmental Bulletin* **2019**, *28*, 852-856.
19. Kuşcuoğlu, S. Determination of K-struvite Application Bases. İstanbul Technical University, İstanbul, 2008.
20. Sertaç, B. Recovery of Nitrogen and Phosphorous Removal from Source-Separated Human Urine by Chemical Precipitation. İstanbul Technical University, İstanbul, 2012.
21. Lee, S.I.; Weon, S.Y.; Lee, C.W.; Koopman, B. Removal of nitrogen and phosphate from wastewater by addition of bittern. *Chemosphere* **2003**, *51*, 265-271, doi:10.1016/s0045-6535(02)00807-x.

22. Siciliano, A.; Limonti, C.; Curcio, G.M.; Molinari, R. Advances in Struvite Precipitation Technologies for Nutrients Removal and Recovery from Aqueous Waste and Wastewater. *Sustainability* **2020**, *12*, doi:10.3390/su12187538.
23. Tansel, B.; Lunn, G.; Monje, O. Struvite formation and decomposition characteristics for ammonia and phosphorus recovery: A review of magnesium-ammonia-phosphate interactions. *Chemosphere* **2018**, *194*, 504-514, doi:10.1016/j.chemosphere.2017.12.004.
24. Xu, K.N.; Wang, C.W.; Liu, H.Y.; Qian, Y. Simultaneous removal of phosphorus and potassium from synthetic urine through the precipitation of magnesium potassium phosphate hexahydrate. *Chemosphere* **2011**, *84*, 207-212, doi:10.1016/j.chemosphere.2011.04.057.
25. Taylor, A.W.; Frazier, A.W.; Gurney, E.L. Solubility products of magnesium ammonium and magnesium potassium phosphates. **1963**, *59*, 1580-1584.
26. Luff, B.B.; Reed, R.B. THERMODYNAMIC PROPERTIES OF MAGNESIUM POTASSIUM ORTHO-PHOSPHATE HEXAHYDRATE. *Journal of Chemical and Engineering Data* **1980**, *25*, 310-312, doi:10.1021/jc60087a028.
27. Xu, K.N.; Li, J.Y.; Zheng, M.; Zhang, C.; Xie, T.; Wang, C.W. The precipitation of magnesium potassium phosphate hexahydrate for P and K recovery from synthetic urine. *Water Research* **2015**, *80*, 71-79, doi:10.1016/j.watres.2015.05.026.
28. Ohlinger, K.N.; Young, T.M.; Schroeder, E.D. Predicting struvite formation in digestion. *Water Research* **1998**, *32*, 3607-3614, doi:10.1016/s0043-1354(98)00123-7.
29. Kabdaşlı, I.; Tünay, O. Nutrient recovery by struvite precipitation, ion exchange and adsorption from source-separated human urine – a review. **2018**, *7*, 106-138, doi:10.1080/21622515.2018.1473504.
30. Xu, K.N.; Wang, C.W.; Wang, X.X.; Qian, Y. Laboratory experiments on simultaneous removal of K and P from synthetic and real urine for nutrient recycle by crystallization of magnesium-potassium-phosphate-hexahydrate in a draft tube and baffle reactor. *Chemosphere* **2012**, *88*, 219-223, doi:10.1016/j.chemosphere.2012.02.061.
31. Huang, H.M.; Li, J.; Li, B.; Zhang, D.D.; Zhao, N.; Tang, S.F. Comparison of different K-struvite crystallization processes for simultaneous potassium and phosphate recovery from source-separated urine. *Science of the Total Environment* **2019**, *651*, 787-795, doi:10.1016/j.scitotenv.2018.09.232.
32. Warmadewanthi; Liu, J.C. Recovery of phosphate and ammonium as struvite from semiconductor wastewater. *Separation and Purification Technology* **2009**, *64*, 368-373, doi:10.1016/j.seppur.2008.10.040.
33. Zhang, C.; Chen, Y.G. Simultaneous Nitrogen and Phosphorus Recovery from Sludge-Fermentation Liquid Mixture and Application of the Fermentation Liquid To Enhance Municipal Wastewater Biological Nutrient Removal. *Environmental Science & Technology* **2009**, *43*, 6164-6170, doi:10.1021/es9005948.
34. Wilsenach, J.A.; Schuurbiens, C.A.H.; van Loosdrecht, M.C.M. Phosphate and potassium recovery from source separated urine through struvite precipitation. *Water Research* **2007**, *41*, 458-466, doi:10.1016/j.watres.2006.10.014.
35. Kabdasli, I.; Atalay, Z.; Tunay, O. Effect of solution composition on struvite crystallization. *Journal of Chemical Technology and Biotechnology* **2017**, *92*, 2921-2928, doi:10.1002/jctb.5310.
36. APHA. *Standard Methods for Examination of Water and Wastewater*, 21 st ed.; American Public Health Association: USA, 2005.
37. Yang, H.X.; Sun, H.J. Crystal structure of a new phosphate compound, $\text{Mg}_2\text{KNa}(\text{PO}_4)_2 \cdot 14\text{H}_2\text{O}$. *Journal of Solid State Chemistry* **2004**, *177*, 2991-2997, doi:10.1016/j.jssc.2004.05.008.

38. Zhang, C.; Xu, K.N.; Li, J.Y.; Wang, C.W.; Zheng, M. Recovery of Phosphorus and Potassium from Source-Separated Urine Using a Fluidized Bed Reactor: Optimization Operation and Mechanism Modeling. *Industrial & Engineering Chemistry Research* **2017**, *56*, 3033-3039, doi:10.1021/acs.iecr.6b04819.