
Article

Copper, Iron and Aluminium Electrochemical Corrosion Rates and Intrinsic Diffusivities Dependence on Temperature Investigations

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Abstract: Our investigations show that electrochemical corrosion of copper is faster than electrochemical corrosion of aluminium at temperatures below 100°C. Literature data analysis shows that the Al atoms diffuse faster than the Cu atoms at temperatures higher than 475°C, Al rich intermetallic compounds (IMCs) are formed faster in the Cu-Al system, and the Kirkendall plane shifts toward Al side. Electrochemical corrosion occurs due to electric current and due to diffusion. An electronic device working time, for example, depends on initial copper cover thickness on aluminium wire, connected to the electronic device, temperature, and volume and dislocation pipe diffusion coefficients, so copper, iron, and aluminium electrochemical corrosion rates are investigated experimentally at room temperature and at temperature 100°C. Intrinsic diffusivities ratios of copper and aluminium at different temperatures and diffusion activation energies in the Cu-Al system are calculated by proposed here methods using literature experimental data. Dislocation pipe and volume diffusion activation energies of pure iron are calculated separately by earlier proposed method using literature experimental data. Aluminium dissolved into NaCl solution as the Al^{3+} ions at room temperature and at temperature 100°C, iron dissolved into NaCl solution as the Fe^{2+} (not Fe^{3+}) ions at room temperature and at temperature 100°C, copper dissolved into NaCl solution as the Cu^+ ions at room temperature and as the Cu^+ and the Cu^{2+} ions at temperature 100°C. It is founded experimentally that copper corrosion is higher than aluminium corrosion, and ratio of electrochemical corrosion rates, $k_{Cu}/k_{Al}>1$, decreases with temperature increasing, although iron electrochemical corrosion rate doesn't depend on temperature below 100°C. It is obvious, because melting point of iron is more higher than melting point of copper or aluminium. It is calculated that copper electrochemical corrosion rate is approximately equal to aluminium electrochemical corrosion at temperature about 300°C, so copper can dissolve into NaCl solution mostly as the Cu^{2+} ions at temperature about 300°C. Ratio of intrinsic diffusivities, $D_{Cu}/D_{Al}<1$, increases with temperature increasing, and intrinsic diffusivity of aluminium could be approximately equal to intrinsic diffusivity of copper at temperature about 460°C.

Keywords: electrochemical corrosion, metallic coatings, electrolysis, diffusion, intermetallic compounds, phases formation kinetics, copper, aluminium, iron, Kirkendall-Frenkel porosity, Kirkendall shift, activation energy

1. Introduction

An Al wire coated with thin Cu cover ($\approx 15\mu m$ thickness), utilized near an automobile motor, is heated to temperatures about 373-473K (100-200°C). Intermetallics (IMCs) can formed at the Cu/Al interface and grow gradually during heating at such temperatures. The IMC layers are brittle and have high resistivity. Therefore, for assurance of the reliability of the product, information on the growth behaviour of the IMC layers during heating is essentially important [1]. Figure 1 shows the problem: an electronic device working time, t_0 , depends on initial Cu cover thickness, X_{Cu} , and temperature. Electric

conductivity of copper is higher than electric conductivity of aluminium in approximately two times, but the formation of intermetallic phases induce significant increase in contact resistance which is found to increase linearly with the thickness of the intermetallics formed [20]. The temperature range used to produce the intermetallic phases was from 250 to 515°C. Moreover, the presence of an electrical field greatly accelerated the kinetics of formation of intermetallic phases and altered significantly their morphology, and the impaired mechanical integrity of the Al-Cu bimetallic joints treated by an electrical current was clearly demonstrated by an extensive cracking not only across the whole intermetallic bandwidth but also within different phases and at a neighbouring interface [20]. Three phases thickness, X_{123} , can be estimated in such a way. The mass conservation law gives:

$$X_{Cu}(t=0) \cdot 1 = \frac{9}{9+4} X_3(t_0) + \frac{1}{1+1} X_2(t_0) + \frac{1}{1+2} X_3(t_0) \approx \frac{1.526 X_{123}}{3} \approx 0.509 X_{123}, \text{ and } X_{123} \approx 2 X_{Cu}, \quad (1)$$

so three phases general thickness is approximately greater in two times than initial Cu cover thickness.

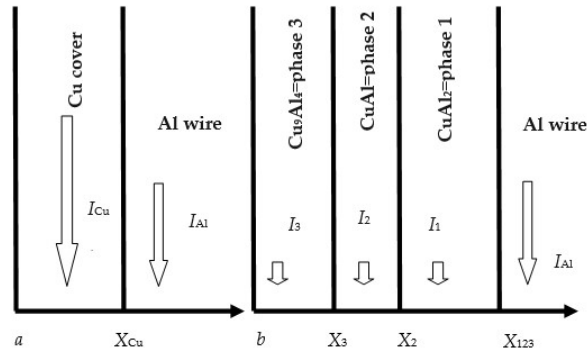


Figure 1. (a) Initial stage ($t=0$): an electronic device is working, since the electric current, $I=I_{Cu}+I_{Al}$, has optimal value; (b) final stage ($t=t_0$): the electronic device isn't working, because the electric current, $I=I_3+I_2+I_1+I_{Al}$, has too small value, since pure Cu cover has disappeared.

Otherwise, it was proved experimentally that thin Al pad ($\approx 1 \mu\text{m}$ thickness) can prevent gold and copper corrosion, because intermetallics formation rate in Au-Al system is much more higher than intermetallics formation rate in Cu-Al system, so it is possible to use Cu instead of Au for wire bonding in microelectronics packaging, and Cu has higher electric conductivity, higher thermal conduction, and lower material cost than Au [2]. Corrosion and intermetallics rate formation in gold and copper wire bonding in microelectronics packaging were investigated in [2] at temperatures $T_1=175 \text{ }^\circ\text{C}$, $T_2=200 \text{ }^\circ\text{C}$, and $T_3=225 \text{ }^\circ\text{C}$ during 120, 240, 360, and 480 h. The authors have reported that cross-sectional analysis of the Cu ball on Al pad confirmed that corrosion occurred at temperatures about $T=200^\circ\text{C}$ primarily beneath the Cu balls and did not initiate from the Al pad, formation of CuCl_2 didn't allow self-passivation of Cu to occur, so rate of copper corrosion increased, and the rate of Cu-Al intermetallics formation was found to be three to five times slower than Au-Al intermetallics formation at all three annealing temperatures. So, copper dissolved into NaCl solution as Cu^{2+} ions at temperatures about $T=200^\circ\text{C}$, as we expected. They didn't investigate corrosion rates dependence of copper and aluminium on temperature. Moreover, phase layers general thicknesses for Cu-Al system were calculated [2]:

$$X_{123}^2 = K_{123}t + K_{01} = K_0 e^{-\frac{Q}{RT}} + K_{01} = 3.52 \cdot 10^{-4} \frac{\mu\text{m}^2}{\text{s}} \cdot e^{-\frac{25500 \text{ Jmol}^{-1}}{RT}} t + 0.44 \mu\text{m}^2, \quad (2)$$

where $R \approx 8.314 \text{ JK}^{-1}$ is the gas constant, K_{01} is constant related to initial IMC thickness. General reaction rates of IMC formation were calculated: $K_{123}(T_1) = 3.57 \cdot 10^{-7} \text{ } \mu\text{m}^2/\text{s}$, $K_{123}(T_2) = 6.26 \cdot 10^{-7} \text{ } \mu\text{m}^2/\text{s}$, and $K_{123}(T_3) = 7.15 \cdot 10^{-7} \text{ } \mu\text{m}^2/\text{s}$. The pre-exponential factor and IMC formation activation energy were calculated: $K_0 \approx 3.52 \cdot 10^{-4} \text{ } \mu\text{m}^2/\text{s}$, $Q \approx 25.5 \text{ kJ/mol}$. We can use these results to calculate the electronic device working time by equation (11) in [3] at different temperatures:

$$t_0 \approx \frac{X_{Cu}^2}{C_3^2 K_{123}} = \frac{169}{81} \frac{X_{Cu}^2}{K_{123}} \approx \frac{2X_{Cu}^2}{K_0} e^{Q/(RT)} \approx 5900 \cdot X_{Cu}^2 [\mu\text{m}^2] \cdot e^{25.5 \text{ kJ/mol} / (RT)} \text{ s} \quad (3)$$

$$t_0(T_1 = 175^\circ \text{C} = 448 \text{ K}) \approx 5900 \cdot 225 \cdot e^{25500 / (8.314 \cdot 448)} \text{ s} \approx 40 \text{ years} ; \quad t_0(T_2 = 200^\circ \text{C}) \approx 28 \text{ years} ;$$

$$t_0(T_3 = 225^\circ \text{C}) \approx 21 \text{ years} ; \quad t_0(T_4 = 300^\circ \text{C}) \approx 9 \text{ years} ; \quad t_0(T_5 = 350^\circ \text{C}) \approx 6 \text{ years} .$$

Other researchers have obtained [15]: $K_{123}(T_4=300^\circ\text{C})=4.2 \cdot 10^{-4} \text{ } \mu\text{m}^2/\text{s}$, $K_{123}(T_5=350^\circ\text{C})=3.4 \cdot 10^{-3} \text{ } \mu\text{m}^2/\text{s}$. Equation (3) gives:

$$t_0(T_4 = 300^\circ \text{C}) \approx \frac{2X_{Cu}^2}{K_{123}} \approx 12 \text{ days} ; \quad t_0(T_5 = 350^\circ \text{C}) \approx \frac{2X_{Cu}^2}{K_{123}} \approx 1.5 \text{ days}$$

We can calculate: $Q \approx 124 \text{ kJ/mol}$; $K_0 \approx 8.5 \cdot 10^{-5} \text{ m}^2/\text{s} = 8.5 \cdot 10^7 \text{ } \mu\text{m}^2/\text{s}$;

$$t_0(T = 175^\circ \text{C}) \approx 5.3 \cdot 10^{-6} \cdot e^{124 \text{ J/mol} / (448 \text{ R})} \text{ s} \approx 49 \text{ years} ; \quad t_0(T = 200^\circ \text{C}) \approx 8.4 \text{ years} ;$$

$$t_0(T = 225^\circ \text{C}) \approx \frac{2X_{Cu}^2}{K_0} e^{Q/(RT)} \approx 5.3 \cdot 10^{-6} \cdot e^{124 \text{ J/mol} / (498 \text{ R})} \text{ s} \approx 1.7 \text{ years}$$

It was reported in [1] that the growth of layer 1 is controlled predominantly by boundary diffusion, but that of layers 2 and 3 are governed mainly by volume diffusion at temperatures $T=483\text{-}543\text{K}$ ($210\text{-}270^\circ\text{C}$) for various periods up to 3.456Ms (960h). The authors obtained: $K_{01} \approx 5.3 \cdot 10^{-7} \text{ m}^2/\text{s}$, $Q_1 \approx 86 \text{ kJ/mol}$, $K_{023} \approx 4.2 \cdot 10^{-5} \text{ m}^2/\text{s}$, $Q_{23} \approx 146 \text{ kJ/mol}$. We can calculate: $K_{123}(T_6=210^\circ\text{C})=1.5 \cdot 10^{-6} \text{ } \mu\text{m}^2/\text{s}$,

$$t_0(T = 210^\circ \text{C}) \approx \frac{2X_{Cu}^2}{K_{123}} \approx 9.6 \text{ years}$$

The less temperature is, the higher contribution of grain-boundary diffusion and dislocation pipe diffusion to the layers growth is, so models of grain-boundary diffusion and dislocation pipe diffusion involving outflow into volume should be taken into account [11,17,19].

Diffusion activation energy of Al is less than diffusion activation energy of Cu ($Q_{Al} < Q_{Cu}$) at temperatures from 160°C to 250°C for mutual diffusion in copper–aluminium thin film double layers, but the pre-exponential factors are different in tens times [14]:

$$D_{Al}^* = 4 \cdot 10^{-5} e^{-121 \text{ kJ/mol} / (RT)} \text{ m}^2 / \text{s} , \quad D_{Cu}^* = 9.5 \cdot 10^{-4} e^{-135 \text{ kJ/mol} / (RT)} \text{ m}^2 / \text{s} , \quad (4)$$

in θ -phase (phase 1) CuAl_2 , $C_{Al} = 2/3 \approx 0.67$, $C_{Cu} = 1/3 \approx 0.33$;

$$D_{Al}^* = 1.5 \cdot 10^{-11} e^{-68 \text{ kJ/mol} / (RT)} \text{ m}^2 / \text{s} , \quad D_{Cu}^* = 1 \cdot 10^{-6} e^{-106 \text{ kJ/mol} / (RT)} \text{ m}^2 / \text{s} , \quad (5)$$

in η_2 -phase (phase 2) CuAl, $C_{Al}=C_{Cu}=1/2=0.5$;

$$D_{Al}^* = 1.7 \cdot 10^{-7} e^{-116 \text{ kJmol}^{-1}/(RT)} m^2/s, \quad D_{Cu}^* = 2.4 \cdot 10^{-6} e^{-125 \text{ kJmol}^{-1}/(RT)} m^2/s, \quad (6)$$

in γ_2 -phase (phase 3) Cu₉Al₄, $C_{Al}=4/13 \approx 0.31$, $C_{Cu}=9/13 \approx 0.69$.

We can calculate mutual diffusion coefficient for each phase at temperature 160°C by the Darken equation [21,19] and taking into account Eqs. (4)-(6):

$$D_i^* = C_{Al} D_{Cu}^* + C_{Cu} D_{Al}^*; i = 1,2,3; \quad D_1^* = 6.64 \cdot 10^{-20} m^2/s; \quad D_2^* = 1.3 \cdot 10^{-19} m^2/s; \quad D_3^* = 1.8 \cdot 10^{-21} m^2/s.$$

We can calculate using the methods described in [3,4]: $K_{123}(T=160^\circ\text{C}) \approx 2.8 \cdot 10^{-6} \mu\text{m}^2/\text{s}$,

$$t_0(T = 160^\circ\text{C}) \approx \frac{2X_{Cu}^2}{K_{123}} \approx 5 \text{ years}, \text{ so the problem remains unsolved.}$$

It was founded experimentally, that copper electrochemical corrosion is higher than aluminium electrochemical corrosion in approximately two times at room temperature [3,4], so thin Al layer can prevent copper electrochemical corrosion. It was reported also about influence of hydrogen and absence of passive layer on corrosive properties of aluminium alloys [5].

Besides, the soldered copper/tin based contacts are the weakest part of the chip that can be related to intermetallics and the Kirkendall-Frenkel porosity formation in the contact zone [6]. One of the most common reasons for chip failure is the soldered. The typical range of packaging and operation of the integrated circuits is from room temperature to 250°C [7].

Hydrostatic pressure of Argon gas (≈ 10 MPa) can decrease Kirkendall-Frenkel porosity formation, but practically can't decrease mutual diffusion coefficients, but hot isostatic pressing ($p \approx 100$ MPa, Argon) removes porosity due to homogenisation heat treatment in alloy CMSX4 and superalloy CMSX10 [8].

It was clarified also that carbon steel-stainless steel with the environment of flowing sodium chloride does indeed produce synergetic corrosion instead of antagonistic corrosion [9].

Electric current can destruct wire bonding in microelectronics packaging, so we planned to investigate copper, iron, and aluminium electrochemical corrosion at room temperature and at temperature 100°C. Direct current can dissolve metal anode into electrolyte, and we planned to do experiments under the same conditions: initial radii of Cu, Fe, and Al anodes should be approximately equal, electrolyte concentration should be the same, anodes lengths immersed into electrolyte should be equal, graphite cathodes should be the same, direct electric current value should be practically the same. Aluminium can dissolve into electrolyte only as the Al³⁺ ions, so the charge of aluminium ions should be exactly equal to 3, but copper can dissolve into electrolyte as the Cu⁺ ions and the Cu²⁺ ions, and the charge of copper ions could be equal to 1 or 2, and iron can dissolve into electrolyte as the Fe²⁺ ions and the Fe³⁺ ions, and the charge of iron ions could be equal to 2 or 3. We need to find appropriate mathematical equations to calculate the charges of copper, iron, and aluminium ions dissolved into NaCl solution.

2. Experimental results of copper, iron, and aluminium electrochemical corrosion

2.1. Investigation at room temperature

Cylindrical anodes (99.99 % Cu, 99.96 % Fe, and 99.99 % Al) were used for copper and aluminium [3,4], and also iron electrochemical corrosion investigation. Sodium chloride (NaCl) solution was used as electrolyte (Figure 2).

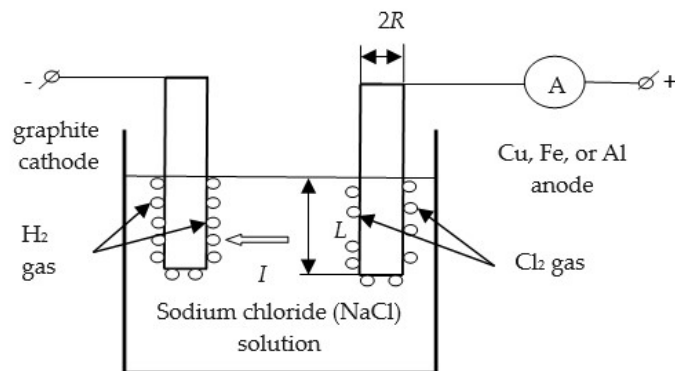


Figure 2. Scheme of experimental equipment at room temperature. Cu, Fe, and Al anodes dissolve into NaCl solution as Cu^+ , Fe^{2+} , and Al^{3+} ions.

Direct electric current and anodes mass decreasing were measured. First of all, we need to be assured that the Cu^+ ions (or the Cu^{2+}), the Fe^{2+} (or the Fe^{3+}), and the Al^{3+} were present in NaCl solution. Rate of anode dissolving into electrolyte can be calculated using Faraday's law of electrolysis:

$$\frac{dm}{dt} = \frac{MI}{zF}, \quad dm = \rho \cdot L \cdot \pi \cdot d(R^2(t)). \quad (4)$$

Here m is anode mass dissolved into electrolyte, t is time of experiment, M is molar mass, I is direct electric current value, F is the Faraday constant ($F \approx 96500 \text{ C mol}^{-1}$), z is charge of ions, R is anode radius, L is anode length immersed into electrolyte. Electric current value did not change, so one can calculate:

$$z = \frac{MI t}{F \pi \rho L (R^2(t=0) - R^2(t))}, \quad (5)$$

where ρ is anode density. Charges of copper, iron, and aluminium ions were calculated:

$$z_{\text{Cu}} = \frac{63.55 \cdot 10^{-3} \text{ kg/mol} \cdot 2.8 \text{ A} \cdot 1.2 \cdot 10^3 \text{ s}}{F \cdot \pi \cdot 8.9 \cdot 10^3 \text{ kg/m}^3 \cdot L_{\text{Cu}} \cdot (R_{\text{Cu}}^2(t=0) - R_{\text{Cu}}^2(t_4))} \approx 0.995 \approx 1, \quad (6)$$

$$z_{\text{Al}} = \frac{27 \cdot 10^{-3} \text{ kg/mol} \cdot 3.1 \text{ A} \cdot 1.2 \cdot 10^3 \text{ s}}{F \cdot \pi \cdot 2.7 \cdot 10^3 \text{ kg/m}^3 \cdot L_{\text{Al}} \cdot (R_{\text{Al}}^2(t=0) - R_{\text{Al}}^2(t_4))} \approx 2.954 \approx 3, \quad (7)$$

$$z_{\text{Fe}} = \frac{55.847 \cdot 10^{-3} \text{ kg/mol} \cdot 3.15 \text{ A} \cdot 1.2 \cdot 10^3 \text{ s}}{F \cdot \pi \cdot 7.86 \cdot 10^3 \text{ kg/m}^3 \cdot L_{\text{Fe}} \cdot (R_{\text{Fe}}^2(t=0) - R_{\text{Fe}}^2(t_4))} \approx 2.03 \approx 2, \quad (8)$$

where $L_{\text{Cu}} \approx L_{\text{Al}} \approx L_{\text{Fe}}$; $L_{\text{Cu}} = L_{\text{Fe}} = 5 \cdot 10^{-2} \text{ m}$, $L_{\text{Al}} = 4.5 \cdot 10^{-2} \text{ m}$; $R_{0\text{Cu}} = R_{0\text{Al}} = 2.8 \text{ mm}$, $R_{0\text{Fe}} = 2.98 \text{ mm}$; $I_{\text{Al}} \approx I_{\text{Cu}} \approx I_{\text{Fe}}$; $I_{\text{Fe}} = 3.15 \text{ A}$, $I_{\text{Al}} = 3.1 \text{ A}$, $I_{\text{Cu}} = 2.8 \text{ A}$, so copper dissolved into NaCl solution as the Cu^+ ions, iron dissolved into NaCl solution as the Fe^{2+} ions, and aluminium dissolved into NaCl solution as the Al^{3+} ions. Anodes radii decreasing kinetics is shown on Figure 2. Experiments were carried during $t_1=5 \text{ min}$, $t_2=10 \text{ min}$, $t_3=15 \text{ min}$, and $t_4=20 \text{ min}$.

Experimental results are as follows: $R_{1Cu}=2.74$ mm, $R_{2Cu}=2.67$ mm, $R_{3Cu}=2.59$ mm, $R_{4Cu}=2.5$ mm; $R_{1Al}=2.77$ mm, $R_{2Al}=2.73$ mm, $R_{3Al}=2.68$ mm, $R_{4Al}=2.62$ mm, $R_{1Fe}=2.95$ mm, $R_{2Fe}=2.92$ mm, $R_{3Fe}=2.88$ mm, $R_{4Fe}=2.83$ mm. Measurement precision was 0.01 mm or 10 micrometers.

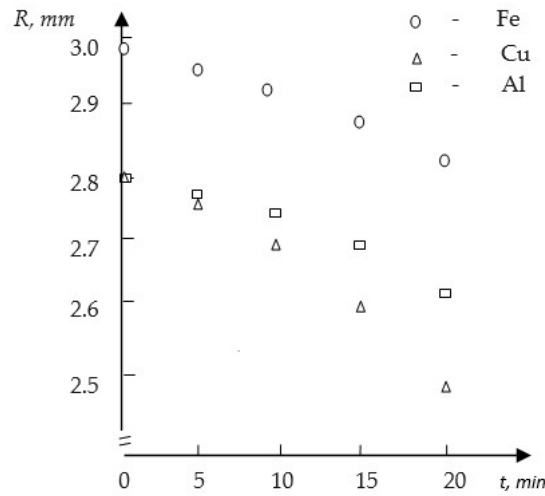
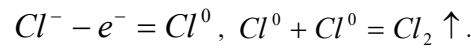
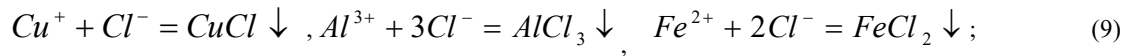
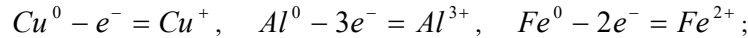


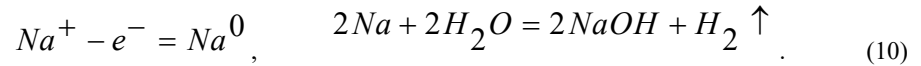
Figure 3. Cu, Fe, and Al anodes radii decreasing kinetics at room temperature.

Chemical reactions took place near positive electrode (anode):



Chlorine gas was formed near anode.

Chemical reactions took place near negative electrode (cathode):



Hydrogen gas was formed near cathode.

Anodes radii decreasing rate constants can be calculated as average value of four experiments to increase calculation precise:

$$k_{Cu} = \frac{4R_0^2 - \sum_{i=1}^4 R_i^2}{\sum_{i=1}^4 t_i} \approx 1.25 \cdot 10^{-9} \text{ m}^2/\text{s}, \quad k_{Al} = \frac{4R_0^2 - \sum_{i=1}^4 R_i^2}{\sum_{i=1}^4 t_i} \approx 7.29 \cdot 10^{-10} \text{ m}^2/\text{s}, \quad (11)$$

$$k_{Fe} = \frac{4R_{0Fe}^2 - \sum_{i=1}^4 R_{iFe}^2}{\sum_{i=1}^4 t_i} \approx 7.26 \cdot 10^{-10} \text{ m}^2/\text{s}, \quad k_{Cu} \approx 1.71k_{Al}; k_{Al} \approx k_{Fe},$$

so copper electrochemical corrosion is much more higher than aluminium and iron electrochemical corrosion, despite of $I_{Fe} \approx I_{Al} \geq I_{Cu}$; $I_{Fe} \approx I_{Al} \approx 1.1I_{Cu}$. It is need to point out that k_{Cu} , k_{Fe} , and k_{Al} have dimensionalities as diffusion coefficients [m^2/s], because electrochemical corrosion occurs through anodes' surface.

2.2 Investigation at temperature 100 °C

Experiments were carried also at temperature 100°C. Cylindrical anodes (99.99 % Cu, 99.99 % Al, and 99.96 % Fe) were used for copper and aluminium [10], and also iron electric corrosion investigation. Sodium chloride (NaCl) solution was used as electrolyte (Figure 4). Direct electric current and anodes' mass decreasing rate were measured (Figure 5).

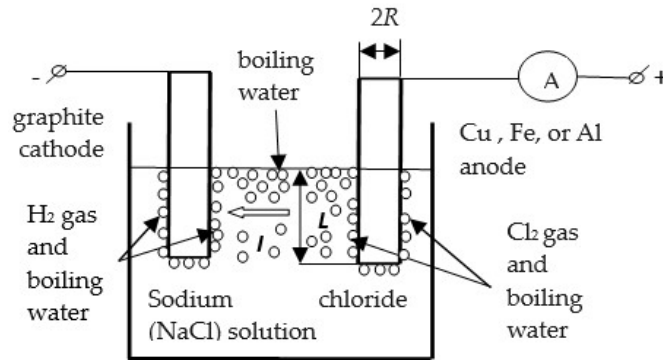


Figure 4. Scheme of experimental equipment at $T=100^{\circ}\text{C}$. Cu, Fe, and Al anodes dissolve into NaCl solution as Cu^+ , Cu^{2+} , Fe^{2+} , and Al^{3+} ions.

Electric current value did not change, so one can calculate:

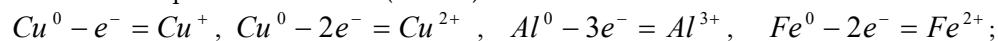
$$z_{\text{Cu}} = \frac{63.55 \cdot 10^{-3} \text{ kg/mol} \cdot 3.05 \text{ A} \cdot 1.2 \cdot 10^3 \text{ s}}{F \cdot \pi \cdot 8.9 \cdot 10^3 \text{ kg/m}^3 L_{\text{Cu}} \cdot (R_{\text{Cu}}^2(t=0) - R_{\text{Cu}}^2(t_4))} \approx 1.47 \approx \frac{1+2}{2}, \quad (12)$$

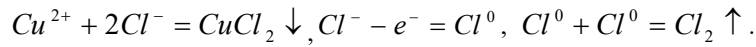
$$z_{\text{Al}} = \frac{27 \cdot 10^{-3} \text{ kg/mol} \cdot 3.15 \text{ A} \cdot 1.2 \cdot 10^3 \text{ s}}{F \cdot \pi \cdot 2.7 \cdot 10^3 \text{ kg/m}^3 L_{\text{Al}} \cdot (R_{\text{Al}}^2(t=0) - R_{\text{Al}}^2(t_4))} \approx 2.85 \approx 3, \quad (13)$$

$$z_{\text{Fe}} = \frac{55.847 \cdot 10^{-3} \text{ kg/mol} \cdot 3.15 \text{ A} \cdot 1.2 \cdot 10^3 \text{ s}}{F \cdot \pi \cdot 7.86 \cdot 10^3 \text{ kg/m}^3 L_{\text{Fe}} \cdot (R_{\text{Fe}}^2(t=0) - R_{\text{Fe}}^2(t_4))} \approx 2.01 \approx 2, \quad (14)$$

where $L_{\text{Cu}}=L_{\text{Al}}=4 \cdot 10^{-2} \text{ m}$, $L_{\text{Fe}}=5 \cdot 10^{-2} \text{ m}$, $R_{0\text{Cu}}=2.27 \text{ mm}$, $R_{0\text{Al}}=2.6 \text{ mm}$, $R_{0\text{Fe}}=2.83 \text{ mm}$, $I_{\text{Al}}=3.15 \text{ A}$, $I_{\text{Fe}}=3.13 \text{ A}$, $I_{\text{Cu}}=3.05 \text{ A}$, so copper dissolved into NaCl solution as Cu^+ and Cu^{2+} ions (copper dissolved into NaCl solution as Cu^+ ions at room temperature), iron dissolved into NaCl solution as the Fe^{2+} ions (as at room temperature), and aluminium dissolved into NaCl solution as Al^{3+} ions (as at room temperature). Anodes radii decreasing kinetics is shown on Figure 5. Experiments were carried during $t_1=5 \text{ min}$, $t_2=10 \text{ min}$, $t_3=15 \text{ min}$, and $t_4=20 \text{ min}$. Experimental results are as follows: $R_{1\text{Cu}}=2.2 \text{ mm}$, $R_{2\text{Cu}}=2.12 \text{ mm}$, $R_{3\text{Cu}}=2.03 \text{ mm}$, $R_{4\text{Cu}}=1.92 \text{ mm}$; $R_{1\text{Al}}=2.56 \text{ mm}$, $R_{2\text{Al}}=2.51 \text{ mm}$, $R_{3\text{Al}}=2.45 \text{ mm}$, $R_{4\text{Al}}=2.38 \text{ mm}$; $R_{1\text{Fe}}=2.80 \text{ mm}$, $R_{2\text{Fe}}=2.76 \text{ mm}$, $R_{3\text{Fe}}=2.72 \text{ mm}$, $R_{4\text{Fe}}=2.67 \text{ mm}$. Measurement precision was 0.01 mm or 10 micrometers. We carried additional experiments, but result was the same.

Chemical reactions are more complicated at 100°C than at room temperature near positive electrodes (anodes):





Chlorine gas and boiling water were formed near anodes.

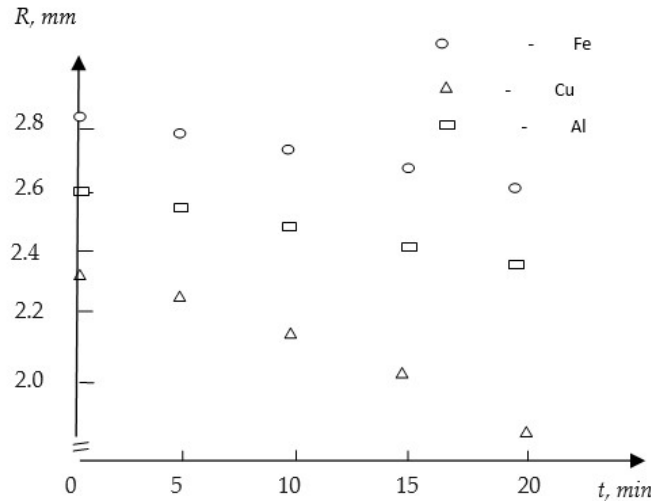
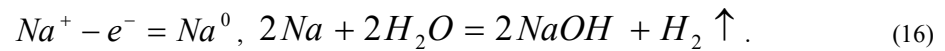


Figure 5. Cu, Fe, and Al anodes radii decreasing kinetics at $T=100^\circ\text{C}$.

Chemical reactions took place near negative electrodes (cathodes):



Hydrogen gas and boiling water were formed near cathodes.

Anodes radii decreasing rate constants can be calculated as average value of four experiments to increase calculation precise:

$$k_{\text{Cu}} = \frac{4R_{0\text{Cu}}^2 - \sum_{i=1}^4 R_{i\text{Cu}}^2}{\sum_{i=1}^4 t_i} \approx 1.154 \cdot 10^{-9} \text{ m}^2 / \text{s}, \{1.25 \cdot 10^{-9} \text{ at room temperature}\},$$

$$k_{\text{Al}} = \frac{4R_{0\text{Al}}^2 - \sum_{i=1}^4 R_{i\text{Al}}^2}{\sum_{i=1}^4 t_i} \approx 8.42 \cdot 10^{-10} \text{ m}^2 / \text{s}, \{7.29 \cdot 10^{-10} \text{ at room temperature}\} \quad (17)$$

$$k_{\text{Fe}} = \frac{4R_{0\text{Fe}}^2 - \sum_{i=1}^4 R_{i\text{Fe}}^2}{\sum_{i=1}^4 t_i} \approx 6.83 \cdot 10^{-10} \text{ m}^2 / \text{s}, \{7.23 \cdot 10^{-10} \text{ at room temperature}\}, k_{\text{Cu}} \approx 1.37 k_{\text{Al}}, \{1.72 \text{ at room temperature}$$

$$T_1 \approx 27^\circ\text{C}\},$$

so copper electrochemical corrosion is higher at room temperature $T_1 \approx 27^\circ\text{C}$, aluminium electrochemical corrosion is higher at temperature $T_2 = 100^\circ\text{C}$, and ratio of electrochemical corrosion rates, $k_{\text{Cu}}/k_{\text{Al}}$, decreases with temperature increasing, although iron electrochemical corrosion rate practically doesn't depend on temperature below 100°C . It is obvious, because of higher melting point of iron than melting point of copper or aluminium. We

can conclude that the Cu^{2+} ions are less mobile than Cu^+ ions. It is need to point out that k_{Cu} , k_{Al} , and k_{Fe} have dimensionalities as diffusion coefficients, D^*_{Cu} , D^*_{Al} , D^*_{Fe} [m^2/s], because electrochemical corrosion occurs through anodes' surface.

Dislocation pipe and volume diffusion activation energies can be calculated in such a way. The Arrhenius law is valid for dislocation pipe diffusion and volume diffusion in ultra high purity samples [11,19]:

$$D_d^* = D_{0d} e^{-Q_d/(RT)} \quad \text{or} \quad D_d^* = D_{0d} e^{-E_d/(k_B T)}, \quad \text{and} \quad D_V^* = D_{0V} e^{-Q_V/(RT)} \quad \text{or} \quad D_V^* = D_{0V} e^{-E_V/(k_B T)}, \quad (18)$$

$$Q[J/mol] = F \cdot E[eV]. \quad (19)$$

Here $R \approx 8.314 \text{ JK}^{-1}$ is the gas constant, k_B is the Boltzmann constant, $Q_d(E_d)$ is the dislocation pipe diffusion activation energy ($Q_d = FE_d$), $F \approx 96500 \text{ Cmol}^{-1}$ is the Faraday constant, $Q_V(E_V)$ is the volume diffusion activation energy ($Q_V = FE_V$), D_{0d} and D_{0V} are the pre-exponential factors, T is absolute temperature.

Our experimental results allow to calculate:

$$\frac{k_{\text{Cu}}}{k_{\text{Al}}}(T) \approx \frac{D_{\text{Cu}}^*}{D_{\text{Al}}^*}(T) = \frac{D_{0\text{Cu}}^*}{D_{0\text{Al}}^*} e^{(Q_{\text{Al}} - Q_{\text{Cu}})/(RT)}; \ln\left(\frac{D_{0\text{Cu}}^*}{D_{0\text{Al}}^*}\right) = -0.6; Q_{\text{Al}} - Q_{\text{Cu}} = 2.9 \text{ kJ/mol} \quad (20)$$

$$\frac{D_{0\text{Cu}}^*}{D_{0\text{Al}}^*} = 0.55, \quad \frac{D_{\text{Cu}}^*}{D_{\text{Al}}^*}(T_3) = 1 \Rightarrow T_3 = \frac{2900 \text{ J/mol}}{0.6R} \approx 583 \text{ K} \approx 310^\circ \text{C} \quad (21)$$

so diffusion activation energy of Al, Q_{Al} , is higher than diffusion activation energy of Cu, Q_{Cu} , ($Q_{\text{Al}} > Q_{\text{Cu}}$, $Q_{\text{Al}} - Q_{\text{Cu}} = 2.9 \text{ kJ/mol}$), at temperatures from 20°C to 100°C , because the Cu^+ ions have higher mobilities than the Al^{3+} ions, and copper electrochemical corrosion rate can be approximately equal to aluminium electrochemical corrosion at temperature about $T_3 \approx 300^\circ\text{C}$ due to the Cu^{2+} ions are less mobile than the Cu^+ ions. Moreover, the pre-exponential factors are approximately the same: $D_{0\text{Al}}^* \approx 2D_{0\text{Cu}}^*$.

3. Intrinsic diffusivities ratio and diffusion activation energy calculations

3.1. Intrinsic diffusivities ratio of Cu and Al analysis

We can analyse described experimental results in the Al-Cu system for bulk samples [12], since the ratio $D_{\text{Al}}^*/D_{\text{Cu}}^*$ didn't calculated in [12]:

$$\frac{D_{\text{Cu}}^*}{D_{\text{Al}}^*} \approx \frac{\sum_{j=1}^N X_j - X_K(1 - C_i)\sqrt{\pi}}{\sum_{j=1}^N X_j + C_i X_K \sqrt{\pi}} < 1, \quad C_i = C_{\text{Al}}, \quad (22)$$

where N is formed phases quantity, X_j is phase j 's thickness, C_i is the average concentration of aluminium in phase i , X_K is the Kirkendall shift length.

Five phases are formed in the Al-Cu system at temperatures from 400°C to 535°C in bulk samples [12]: θ -phase (phase 1) CuAl_2 ($C_i = 2/3$), η_2 -phase (phase 2) CuAl ($C_i = 1/2$), ζ_2 -phase (phase 3b) Cu_4Al_3 ($C_{3b} = 3/7$), δ -phase (phase 3a) Cu_3Al_2 ($C_{3a} = 2/5$), and γ_2 -phase (phase 3) Cu_9Al_4 ($C_3 = 4/13 \approx 0.31 \approx 1/3$, $C = C_{\text{Al}}$). Inert markers were in δ -phase (phase 3a) Cu_3Al_2 ($C_{3a} = 2/5 = 0.4$) and moved to Al side during mutual diffusion. In general, inert markers move to faster diffusivity component side. We can calculate ($C_{3a} = 0.4$):

$$\frac{D_{\text{Cu}}^*}{D_{\text{Al}}^*}(T_1 = 535^\circ\text{C}) \approx \frac{X_1 + X_2 + X_{3b} + X_{3a} + X_3 - X_K 0.6\sqrt{\pi}}{X_1 + X_2 + X_{3b} + X_{3a} + X_3 + 0.4 X_K \sqrt{\pi}} \approx 0.814; y_1 = \frac{D_{\text{Al}}^*}{D_{\text{Cu}}^*} = \frac{1}{0.814} \approx 1.228, \quad (23)$$

$$T_1 = 535^\circ\text{C} = 808\text{K}, t = 40\text{h}, X_K \approx 20.5\mu\text{m}, X_1 + X_2 + X_{3b} + X_{3a} + X_3 \approx 180\mu\text{m};$$

$$\frac{D_{\text{Cu}}^*}{D_{\text{Al}}^*}(T_2 = 515^\circ\text{C}) \approx \frac{X_1 + X_2 + X_{3b} + X_{3a} + X_3 - X_K(1 - C_{3a})\sqrt{\pi}}{X_1 + X_2 + X_{3b} + X_{3a} + X_3 + C_{3a} X_K \sqrt{\pi}} \approx 0.856; y_2 = \frac{D_{\text{Al}}^*}{D_{\text{Cu}}^*} \approx 1.168, \quad (24)$$

$T_2=515^\circ\text{C}=788\text{K}$, $t=40\text{h}$, $X_K\approx 11\mu\text{m}$, $X_1+X_2+X_{3b}+X_{3a}+X_3\approx 127\mu\text{m}$;

$$\frac{D_{Cu}^*}{D_{Al}^*}(T_3 = 495^\circ\text{C}) \approx \frac{X_1 + X_2 + X_{3b} + X_{3a} + X_3 - X_K 0.6\sqrt{\pi}}{X_1 + X_2 + X_{3b} + X_{3a} + X_3 + 0.4X_K\sqrt{\pi}} \approx 0.916; y_3 = \frac{1}{0.916} \approx 1.092, \quad (25)$$

$T_3=495^\circ\text{C}=768\text{K}$, $t=40\text{h}$, $X_K\approx 5\mu\text{m}$, $X_1+X_2+X_{3b}+X_{3a}+X_3\approx 101\mu\text{m}$;

$$\frac{D_{Cu}^*}{D_{Al}^*}(T_4 = 475^\circ\text{C}) \approx \frac{X_1 + X_2 + X_{3b} + X_{3a} + X_3 - X_K(1-0.4)\sqrt{\pi}}{X_1 + X_2 + X_{3b} + X_{3a} + X_3 + 0.4CX_K\sqrt{\pi}} \approx 0.969; y_4 = \frac{D_{Al}^*}{D_{Cu}^*} \approx 1.032, \quad (26)$$

$T_4=475^\circ\text{C}=748\text{K}$, $t=90\text{h}$, $X_K\approx 2\mu\text{m}$, $X_1+X_2+X_{3b}+X_{3a}+X_3\approx 113\mu\text{m}$.

We can use these four points to calculate by the least square method to increase calculation precise:

$$\Delta Q = Q_{Al} - Q_{Cu} = \frac{4 \sum_{j=1}^4 \left(\frac{1000}{RT_j} \ln y_j \right) - \sum_{j=1}^4 \ln y_j \sum_{j=1}^4 \frac{1000}{RT_j}}{4 \sum_{j=1}^4 \left(\frac{1000}{RT_j} \right)^2 - \left(\sum_{j=1}^4 \frac{1000}{RT_j} \right)^2} \approx -13.4 \text{ kJ/mol} \quad (27)$$

$$y_0 = \exp \frac{\sum_{j=1}^4 \left(\frac{1000}{RT_j} \right)^2 \sum_{j=1}^4 \ln y_j - \sum_{j=1}^4 \frac{1000}{RT_j} \sum_{j=1}^4 \left(\frac{1000}{RT_j} \ln y_j \right)}{4 \sum_{j=1}^4 \left(\frac{1000}{RT_j} \right)^2 - \left(\sum_{j=1}^4 \frac{1000}{RT_j} \right)^2} \approx \exp(2.2) \approx 9 \quad (28)$$

$$\frac{D_{Al}^*}{D_{Cu}^*}(T) = \frac{D_{0Al}^*}{D_{0Cu}^*} e^{(Q_{Al}-Q_{Cu})/(RT)} \approx 9e^{-13.4 \text{ kJmol}^{-1}/(RT)}, \quad (29)$$

$$\frac{D_{Al}^*}{D_{Cu}^*}(T_5) = y_5 = 1 \Rightarrow T_5 = \frac{13400 \text{ J/mol}}{R \ln 9} \approx 733 \text{ K} \approx 460^\circ\text{C} \quad (30)$$

so $Q_{Al} < Q_{Cu}$ ($Q_{Al}-Q_{Cu}=-13.4\text{kJ/mol}$) because the Cu^{2+} ions have less mobilities than the Al^{3+} ions, and we can conclude that the Kirkendall displacement changes sign at temperature about $T_5\approx 460^\circ\text{C}$ for bulk samples. The pre-exponential factors are different in nine times: $D_{0Al}^*\approx 9D_{0Cu}^*$.

Diffusion activation energy of Al is less than diffusion activation energy of Cu ($Q_{Al} < Q_{Cu}$) at temperatures from 160°C to 250°C for mutual diffusion in copper–aluminium thin film double layers, but the pre-exponential factors are different in tens times [14]. Isolated W islands, 150 \AA in diameter, have been deposited between Cu and Al thin film double layers to serve as inert diffusion markers. Marker displacements have been measured. We can calculate ratio D_{Al}^*/D_{Cu}^* for each phase at different temperatures:

$$\frac{D_{Cu}^*}{D_{Al}^*}(T) = \frac{D_{0Cu}^*}{D_{0Al}^*} e^{(Q_{Al}-Q_{Cu})/(RT)} = 24e^{-14 \text{ kJmol}^{-1}/(RT)} \text{ in } \theta\text{-phase (phase 1) CuAl}_2, C_{Al}=2/3\approx 0.67,$$

$$\frac{D_{1Cu}^*}{D_{1Al}^*}(T = 250^\circ\text{C} = 523 \text{ K}) = 24e^{-14000 \text{ Jmol}^{-1}/(8.314 \times 523)} \approx 24e^{-3.22} \approx 0.96,$$

$$\frac{D_{1Cu}^*}{D_{1Al}^*}(T = 160^\circ\text{C} = 433 \text{ K}) \approx 24e^{-3.89} \approx 0.49,$$

so the Al atoms diffuse faster than the Cu atoms in θ -phase at temperatures from 160°C to 250°C;

$$\frac{D_{Cu}^*}{D_{Al}^*}(T) = \frac{D_{0Cu}^*}{D_{0Al}^*} e^{(Q_{Al}-Q_{Cu})/(RT)} = 7 \cdot 10^4 e^{-38kJmol^{-1}/(RT)} \text{ in } \eta_2\text{-phase (phase 2) CuAl, } C_{Al}=1/2=0.5,$$

$$\frac{D_{2Cu}^*}{D_{2Al}^*}(T = 250^\circ C) = 7 \cdot 10^4 e^{-38000 Jmol^{-1}/(RT)} \approx 11.2, \quad \frac{D_{2Cu}^*}{D_{2Al}^*}(T = 160^\circ C) \approx 1.8,$$

so the Cu atoms diffuse faster than the Al atoms in η_2 -phase at temperatures from 160°C to 250°C;

$$\frac{D_{Cu}^*}{D_{Al}^*}(T) = \frac{D_{0Cu}^*}{D_{0Al}^*} e^{(Q_{Al}-Q_{Cu})/(RT)} = 14 e^{-9kJmol^{-1}/(RT)} \text{ in } \gamma_2\text{-phase (phase 3) Cu}_9\text{Al}_4, C_{Al}=4/13 \approx 0.31,$$

$$\frac{D_{3Cu}^*}{D_{3Al}^*}(T = 250^\circ C) = 14 e^{-9000 Jmol^{-1}/(RT)} \approx 1.77, \quad \frac{D_{3Cu}^*}{D_{3Al}^*}(T = 160^\circ C) = 14 e^{-9kJmol^{-1}/(RT)} \approx 1.15,$$

so the Cu atoms diffuse faster than the Al atoms in γ_2 -phase at temperatures from 160°C to 250°C.

The Cu rich phases can be formed faster than the Al rich phases at temperatures from 160°C to 250°C, and the Cu atoms can diffuse faster than the Al atoms in the Al-Cu system at temperatures from 160°C to 250°C. The Al rich phases can be formed faster than the Cu rich phases at temperatures from 400°C to 535°C, and the Al atoms can diffuse faster than the Cu atoms in the Al-Cu system at temperatures from 400°C to 535°C. It depends on the crystal structure of each phase, but, in general, it could depends on conclusions that the Cu^{2+} ions are less mobile than the Cu^+ ions, and the ratio D_{Al}^*/D_{Cu}^* depends on temperature.

3.2. Diffusion activation energy calculation

3.2.1 Diffusion activation energy calculation in the Cu-Al system

Mutual diffusion coefficients were calculated for all five phases [12]:

$$\tilde{D}_1^* = 5.6 \cdot 10^{-5} e^{-127.6kJmol^{-1}/(RT)} m^2 / s; \quad \tilde{D}_2^* = 2.2 \cdot 10^{-4} e^{-148.5kJmol^{-1}/(RT)} m^2 / s; \quad (31)$$

$$\tilde{D}_{3b}^* = 1.6 \cdot 10^2 e^{-230.5kJmol^{-1}/(RT)} m^2 / s, \quad \tilde{D}_{3a}^* = 2.1 \cdot 10^{-4} e^{-138.1kJmol^{-1}/(RT)} m^2 / s, \quad \tilde{D}_3^* = 8.5 \cdot 10^{-5} e^{-136kJmol^{-1}/(RT)} m^2 / s.$$

We can see that $Q_1 < Q_2$, $Q_1 < Q_3$, and $Q_3 < Q_2$ because of $K_1 > K_2$, $K_1 > K_3$, and $K_3 > K_2$, and $D_{01} \approx D_{02} \approx D_{03}$. Phase j 's rate formation is K_j . Three phases are formed in the Al-Cu system at temperatures 300°C and 350°C [15]: $CuAl_2$, $CuAl$, and Cu_9Al_4 . Phases formation rates were experimentally measured: $K_1=860 \times 10^{-18} m^2/s$, $K_2=100 \times 10^{-18} m^2/s$, and $K_3=360 \times 10^{-18} m^2/s$ at temperature 350°C; $K_1=77 \times 10^{-18} m^2/s$, $K_2=18 \times 10^{-18} m^2/s$, and $K_3=35 \times 10^{-18} m^2/s$ at temperature 300°C, so $K_1 > K_2$, $K_1 > K_3$, and $K_3 > K_2$. We can calculate assuming $C_1=2/3$, $C_2=1/2$, $C_3=1/3$, $C=C_{Al}$ [4]:

$$D_1 \approx \frac{1}{2} (C_1(1-C_1)K_1 + C_2(1-C_1)\sqrt{K_1K_2} + C_3(1-C_1)\sqrt{K_1K_3}); \quad (32)$$

$$D_2 \approx \frac{1}{2} (C_2(1-C_2)K_2 + C_2(1-C_1)\sqrt{K_1K_2} + C_3(1-C_2)\sqrt{K_2K_3}); \quad (33)$$

$$D_3 \approx \frac{1}{2} (C_3(1-C_3)K_3 + C_3(1-C_1)\sqrt{K_1K_3} + C_3(1-C_2)\sqrt{K_2K_3}); \quad (34)$$

$$D_1(T_2 = 350^\circ C) \approx \frac{1}{9}K_1 + \frac{1}{12}\sqrt{K_1K_2} + \frac{1}{18}\sqrt{K_1K_3} \approx 150 \cdot 10^{-18} m^2 / s, D_1(T_1 = 300^\circ C) \approx 15 \cdot 10^{-18} m^2 / s; \quad (35)$$

$$D_2(T_2 = 350^\circ C) \approx \frac{1}{8}K_2 + \frac{1}{12}\sqrt{K_1K_2} + \frac{1}{12}\sqrt{K_2K_3} \approx 50 \cdot 10^{-18} m^2 / s, D_2(T_1 = 300^\circ C) \approx 8 \cdot 10^{-18} m^2 / s; \quad (36)$$

$$D_3(T_2 = 350^\circ C) \approx \frac{1}{9}K_3 + \frac{1}{18}\sqrt{K_1K_3} + \frac{1}{12}\sqrt{K_2K_3} \approx 90 \cdot 10^{-18} m^2 / s, D_3(T_1 = 300^\circ C) \approx 12 \cdot 10^{-18} m^2 / s. \quad (37)$$

Authors [15] didn't calculate diffusion activation energies and the pre-exponential factors, so we can do it:

$$Q_i = \frac{RT_1T_2}{T_2 - T_1} \ln \left(\frac{D_i(T_2)}{D_i(T_1)} \right), \quad D_{0i} = D_i(T_1)e^{Q_i/(RT_1)} = D_i(T_2)e^{Q_i/(RT_2)}; \quad (38)$$

$$\tilde{D}_1 = 4.3 \cdot 10^{-5} e^{-136.7 kJ/mol \cdot 1/(RT)} m^2 / s, \quad \tilde{D}_2 = 6.6 \cdot 10^{-8} e^{-108.8 kJ/mol \cdot 1/(RT)} m^2 / s, \quad (39)$$

$$\tilde{D}_3 = 9.6 \cdot 10^{-7} e^{-119.6 kJ/mol \cdot 1/(RT)} m^2 / s.$$

Equations (39) correspond to Equations (31). We can use several, N , points to calculate by the least square method to increase calculation precise:

$$Q_i = - \frac{N \sum_{j=1}^N \left(\frac{1000}{RT_j} \ln D_i(T_j) \right) - \sum_{j=1}^N \ln D_i(T_j) \sum_{j=1}^N \frac{1000}{RT_j}}{N \sum_{j=1}^N \left(\frac{1000}{RT_j} \right)^2 - \left(\sum_{j=1}^N \frac{1000}{RT_j} \right)^2} [kJ / mol] \quad (40)$$

$$D_{0i} = \exp \frac{\sum_{j=1}^5 \left(\frac{1000}{RT_j} \right)^2 \sum_{j=1}^5 \ln D_i(T_j) - \sum_{j=1}^5 \frac{1000}{RT_j} \sum_{j=1}^4 \left(\frac{1000}{RT_j} \ln D_i(T_j) \right)}{5 \sum_{j=1}^5 \left(\frac{1000}{RT_j} \right)^2 - \left(\sum_{j=1}^5 \frac{1000}{RT_j} \right)^2} [m^2 / s] \quad (41)$$

Equations (40) and (41) give Equations (38) for only two points ($N=2$).

3.2.2. Diffusion activation energy calculation in pure iron

A method of dislocation pipe diffusion parameters determination during the type B diffusion kinetics was suggested by model of dislocation pipe diffusion involving outflow [11]. The method involves diffusion dislocation pipe kinetics for two different annealing times at the same temperature during the type B kinetics and dislocation pipe kinetics for one annealing time at other lower temperature during the type C kinetics. Transition time for type B kinetics to type A kinetics (volume diffusion) and kinetics law $t^{1/6}$ [17] for cone top rate are used in this method.

Bulk diffusion coefficients, D_V , for the diffusion of ^{59}Fe in the high purity iron were calculated in [16] using type B→A kinetics: $D_V=1.5 \cdot 10^{-18} m^2 s^{-1}$ at $T_1=973\text{K}$ for $t_{B \rightarrow A}=67.5\text{ks}$ ($T_m/T_1=1.86$, T_m is melting point of iron). Only one experiment was carried out at the same

temperature for two annealing times t_1 and t_2 ($t_1 \ll t_2$, $t_2 = 40 t_1$). Dislocation diffusion coefficients for the diffusion of ^{59}Fe in the iron were calculated in [16] using type C kinetics:

$$D_d = 3 \cdot 10^{-16} \text{ m}^2 \text{ s}^{-1} \text{ at } T_2 = 753 \text{ K for } t_c = 2.4 \text{ ks } (T_m/T_2 = 2.4). \text{ One can find ratio } D_d/D_v: y(t_{c \rightarrow b}) = \sqrt{\frac{D_d}{6D}} \delta$$

, where $\delta = 1 \text{ nm}$, $\frac{D_d}{D} = 4.3 \times 10^6$. Ratio D_d/D_v increases remarkably for lower temperature. Dislocation pipe and volume diffusion activation energies and pre-exponential factors

$$\text{didn't were calculated in [16]. It is possible to calculate } E_d \text{ and } D_0: E_d = \ln \left(\frac{D_d(T_1)}{D_d(T_2)} \right) k_B \frac{T_1 T_2}{T_1 - T_2}$$

$D_0 = D_d(T_1) \exp \left(\frac{E_d}{k_B T_1} \right)$, $E_d = 1.1 \text{ eV}$; $Q_d = 106 \text{ kJ/mol}$, $D_0 = 6.85 \cdot 10^{-9} \text{ m}^2 \text{ s}^{-1}$. One can calculate dislocation pipe diffusion coefficient for temperature 973 K directly ($T_1 = 753 \text{ K}$ and $T_2 = 693 \text{ K}$ (type C kinetics)): $D_d \approx 10^{-14} \text{ m}^2 \text{ s}^{-1}$. Such value corresponds to value calculated using proposed method. The Fisher law ($t^{1/4}$) gives: $D_d \approx 10^{-16} \div 10^{-15} \text{ m}^2 \text{ s}^{-1}$. Such value is in two orders lower than experimentally obtained in [16]. The volume diffusion activation energy E_v can be calculated: $E_v = \ln \left(\frac{D_0}{D_v(T_1)} \right) k_B T_1$, $E_v = 1.85 \text{ eV}$; $Q_v \approx 179 \text{ kJ/mol}$. Ratio $\frac{E_d}{E_v} = 0.6$ as described in [19].

4. Conclusions

The Al atoms diffuse faster than the Cu atoms at temperature higher than 475°C, but the Cu atoms diffuse faster than the Al atoms at temperature lower than 100°C. Diffusion activation energy of Al is less than diffusion activation energy of Cu at temperature higher than 475°C, but diffusion activation energy of Cu is less than diffusion activation energy of Al at temperature lower than 100°C. Our investigations show that it is possible, because the Cu^{2+} ions are less mobile than Cu^+ ions.

Volume diffusion activation energy of Fe is higher than volume diffusion activation energy of Cu or Al, but dislocation pipe diffusion activation energy of Fe is smaller than volume diffusion activation energy of Cu or Al, so the Fe atoms diffuse faster along dislocation line, but the Cu or Al atoms diffuse faster in volume.

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