

Lignocellulosic Biomass as a Substrate for Oleaginous Microorganisms: A Review

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Abstract

The microorganisms able of accumulating lipids in high percentages, known as oleaginous microorganisms, have been widely studied as an alternative for producing oleochemicals and biofuels. Microbial lipid, so called Single Cell Oil (SCO), production depends on several growth parameters, including the nature of the carbon substrate, which must be efficiently taken up and converted into storage lipid. On the other hand, substrates considered for large scale applications must be abundant and of low acquisition cost. Among others, lignocellulosic biomass is a promising renewable substrate containing high percentages of assimilable sugars (hexoses and pentoses). However, it is also highly recalcitrant and therefore it requires specific pretreatments in order to release its assimilable components. The main drawback of lignocellulose pretreatment is the generation of several by-products that can inhibit the microbial metabolism. In this review, we discuss the main aspects related to the cultivation of oleaginous microorganisms using lignocellulosic biomass as substrate, hoping to contribute to the development of a sustainable process for SCO production in the near future.

Keywords: oleaginous microorganisms; microbial lipids; lignocellulose pretreatment; enzymatic hydrolysis; inhibitors

1. Introduction

The development of new products to meet the needs of the world's population is currently focused on processes that preserve environment healthy. Single Cell Oil (SCO) is one of the new products, which has been recognized in the last decade as an alternative to biofuels, oleochemicals and edible oils [1–9]. SCOs produced from oleaginous microorganisms have similar chemical characteristics to plant lipids. However, one of the greatest advantages of oleaginous microorganisms over vegetable crops is that they require less land and have shorter growth periods [10].

Effective SCO production requires the selection of suitable growth conditions, in which the microorganism's maximum ability to convert the carbon substrate into storage lipid can be expressed. Considering the perspective of commercial applications, special attention should be paid to the substrate acquisition cost because it represents 40 - 80% of the total production cost [11]. The lignocellulosic biomass is a great option because is a renewable and abundant substrate, containing important amounts of assimilable sugars [12]. However, due to its structure and macromolecular composition, lignocellulose is highly recalcitrant and request special chemical, physical or biological pretreatment [13,14], during which, together with assimilable sugars, a number of by-products that may inhibit microbial growth and/or lipogenesis are released [15]. Several approaches to overcome inhibitory effects of the by-products of lignocellulose pretreatment and increase lipid productivities have been proposed. Among them, pretreatment techniques that generate less inhibitory compounds or a detoxification system able to reduce their concentration are considered [16]. Besides, genetic, and

metabolic engineering techniques [17,18], evolutionary adaptation [19,20] and the utilization of specialized microbial consortia [21-24] consist new approaches in lignocellulose biotechnological valorization. However, the technological level achieved so far is still insufficient to support a cost-effective SCO production.

The aim of this review is to discuss recent research dealing with lignocellulosic biomass pretreatment and provide a comprehensive view concerning the growth of oleaginous microorganisms and lipid production on substrates of lignocellulosic origin.

2. Oleaginous microorganisms

2.1. Important oleaginous species

The microorganisms characterized as oleaginous share the common feature of being able to accumulate chemical energy in the form of lipids. The metabolism of these organisms is adapted to convert under specific growth conditions the carbon substrate into storage lipids which are stored in the cytoplasm as lipid bodies with preserved structures in prokaryotes and eukaryotes [25]. Representative oleaginous cells containing lipid bodies are shown in Fig.1. In eukaryotes, and rarely in prokaryotes, lipid bodies are consisted by neutral lipids, mainly triacylglycerols (TAGs) [26].

Oleaginous microorganisms can be found among species of microalgae, fungi (filamentous and yeasts), bacteria and protists. Microalgae strains associated with *Chlorella*, *Scenedesmus*, *Chlamydomonas*, *Nannochloropsis*, *Chlorococcum*, *Isochrysis*, *Cylindrotheca*, *Tetraselmis*, *Auxenochlorella*, *Botryococcus* species are

referenced to have excellent lipid production ability [6,27–33]. Among bacteria the known species are *Rhodococcus*, *Streptomyces*, *Nocardia*, *Mycobacterium*, *Dietzia* or *Gordonia* [34–37]. Representative oleaginous species of filamentous fungi and yeasts belong to *Umbelopsis* (*Mortierella*), *Microsphaeropsis*, *Fusarium*, *Candida*, *Meyerozyma*, *Rhodotorula*, *Rhodosporidium*, *Pichia*, *Cryptococcus*, *Lipomyces*, *Trichosporon* and *Yarrowia* [20,26,33,38–57].

The microbial consortia with the participation of microalgae and bacteria [58–61] or microalgae and yeast species [62–64] have been reported as a strategy to increase lipid production [23,62]. Although studies on consortia have shown that synergism may occur between different species, allowing increased accumulation of lipids, further studies are needed to determine the individual contribution of each partner to lipid production process. Since the physiology of oleaginous microorganisms varies among species [65–68], the ability to accumulate lipids is affected by different factors that are species specific.

2.2. Growth conditions that promote lipid accumulation

The concentration of nutrients, such as nitrogen and carbon, in culture medium is decisive for lipid production [6,39,69–71].

In heterotrophs, usually a high C:N molar ratio is needed to achieve an important lipid accumulation [4,5,47,72–74], while the nature of the nitrogen source plays a critical role in the process [5,75]. Detailed mathematical models have been developed in order to predict growth and lipid accumulation, as well as nutrient (i.e. sugar and nitrogen)

consumption by oleaginous microorganisms [see for instance 74]. In some cases, ammonium nitrogen favors lipid accumulation [76], while in others, organic nitrogen is preferred for lipogenesis [4,5,76,77]. In addition, the limitations of minerals such as magnesium, iron, zinc, phosphorous or the double limitations of minerals including nitrogen and magnesium or nitrogen and phosphorus, induce the production of lipids [5,78,79]. Temperature, pH, dissolved oxygen and culture agitation are other important variables that affect lipid accumulation [72,79]. Studies have shown low biosynthesis of unsaturated fatty acids (FAs) at temperatures above 30°C [47] and increased lipid accumulation under neutral and basic pH conditions [26]. On the other hand, it has been reported that biomass and lipid production are high between 200 and 300 rpm, speeds that allow for high oxygenation. However, lipid production decreases as agitation increases, while at lower agitation speeds the carbon metabolism is diverted to extracellular products such as alcohols (e.g. ethanol, mannitol, arabitol and 2,3-butanediol) [47,80].

On the other hand, the concentration and chemical forms of nitrogen influence the growth and lipid production in autotrophic microorganisms such as microalgae [81]. Studies have shown that many species of microalgae accumulate a greater amount of lipids, especially TAGs, under nitrogen limited conditions, compared to nitrogen excess conditions [82]. Contrary, other studies suggest that nitrogen deficiency adversely affects photosynthesis, thus biomass production and lipid productivity, due to decreased biosynthesis of NADPH, which is the main source of reducing power [83,84]. Furthermore, it is possible that nitrogen limitation affects the lipid profile and several biochemical pathways of the cells [85-87]. Therefore, new approaches, such as

metabolic engineering, may be needed to increase the understanding of the effect of nitrogen on microalgae physiology and on the synthesis and accumulation of TGAs.

In many microalgae species lipid accumulation is favored in phosphate limited conditions [3,88], as well as, at $\text{pH} < 8$. Specifically, the dissociation of NH_4^+ to NH_3 occurs at $\text{pH} > 8$ thus, at lower pH values nitrogen exists as NH_4^+ ions, which is preferred by microalgae over NH_3 [89,90]. Furthermore, studies have demonstrated the lipid content increases with light intensity, CO_2 concentration and oxidative stress caused by salinity [91–93]. On the other hand, growth rate as well as the productivity and lipid composition can be affected by temperature changes [94,95]. The different factors that are involved in the growth and lipid biosynthesis in microalgae can affect in different ways the different species, so their optimum values are species- or even strain-specific and should be experimentally determined.

Recently, the effect of reactive oxygen compounds (ROS) or of free radicals on the synthesis and accumulation of lipids of heterotrophic and autotrophic oleaginous microorganisms has been evaluated. ROS are generated during microbial metabolism as signs of stress and include superoxide (O_2^-), hydroxyl (OH^\cdot), perhydroxyl (HO_2^\cdot) and the alkoxy radical (RO^\cdot), and non-radical forms such as hydrogen peroxide (H_2O_2) and oxygen (O_2). Their accumulation usually results in lipid peroxidation and protein and DNA denaturation. However, it has been demonstrated that, at balanced levels, ROS can promote lipid synthesis [96,97], although the specific mechanisms of ROS participation in lipid synthesis are not yet fully elucidated. Thus, more research work is required to implement stress-based strategies to improve microbial lipid production.

2.3. Sugar conversion into SCO and regulatory mechanisms in sugar assimilation

The conversion of sugars into SCO and other hydrophilic substrates is done through *de novo* biosynthesis, which comprises three physiological phases, including the growth phase occurring under balanced conditions, the oleaginous phase occurring under nitrogen limited conditions, and the reserve lipid turnover phase occurring after the depletion of the carbon source in the growth medium. During growth phase, oleaginous microorganisms convert the carbon source into cell mass, rich in proteins and polysaccharides using both the glycolytic pathway and the pentose phosphate pathway (PPP), while limited quantities of lipids, mainly polar lipids essential for the construction of cell membranes, are synthesized [44]. Then, in the stationary growth phase the depletion of at least one essential nutrient (e.g. nitrogen, sulfate, phosphate or magnesium), induces the beginning of the oil accumulation phase [5,26,70], which extends until the carbon source is exhausted. Finally, during lipid turnover phase, TAGs are degraded to generate energy for cell maintenance and, under specific circumstances, for growth [57].

The metabolism of sugars, including hexoses and pentoses, has been extensively investigated and their theoretical stoichiometric conversion to lipids has been calculated. Oleaginous microorganisms show an efficient capacity to catabolize glucose and other similar sugars to pyruvate, which is used in lipid biosynthesis. 100 g of sugar (about 0.56 mol) yield one mol of pyruvate which is converted into 1.1 mol of acetyl-coA, corresponding to a maximum theoretical value of 0.32 g of lipids per g of glucose. If xylose is considered, a yield of 1.2 mol of acetyl-coA per 100 g of xylose

(0.66 mol) is expected, which corresponds to 0.34 g of lipids per g of substrate [98].

Although the theoretical results offer a good approximation, under real culture conditions, the lipid yield rarely exceeds 0.22 g/g of glucose and 0.23 g/g of xylose [2,99]. On the other hand, the efficient conversion of sugar compounds, such as cellobiose and molasses, into storage lipids, has also been reported [50,73].

The yields obtained from oleaginous microorganisms cultivated on a single sugar are not enough to predict the efficient conversion of lignocellulosic biomass into SCO production. Instead, the simultaneous assimilation of hexoses and pentoses contained in substrates of plant origin is necessary to achieve sustainable SCO production processes [100]. Numerous studies on oleaginous microorganisms (especially yeasts) growing in sugar mixtures have shown that the assimilation of individual sugars is sequential, starting with the easiest to degrade and passing to the most complex, demonstrating diauxic growth [101-106]. Commonly the preferred sugars are hexoses, like glucose [50,107-109], although some species are capable in efficiently metabolizing pentoses like xylose [50,73,101]. Diauxic behavior is attributed to two different mechanisms that may or may not occur simultaneously. The first is catabolic repression, in which the preferred sugar causes repression in the transcription of the enzymes involved in the catabolism of other sugars, and the second is allosteric competition of the transporters, in which the transporters of the preferred sugar inhibit the transporters of the other sugars. Both phenomena result in an inefficient consumption of biomass and low rates of lipid accumulation [100].

Contrary, other studies on the growth of oleaginous microorganisms in mixtures of sugars have shown the capacity of some strains to consume sugars simultaneously

resulting in high lipid production. Lipid yield for oleaginous yeasts and heterotrophically growing microalgae ranges from 0.15 to 0.26 g per g of sugar, when glucose and xylose (or mannose) are used simultaneously as carbon substrates [50,104,110-114]. Furthermore, some strains can consume more than two sugars simultaneously. For instance, strains of *Rhodospiridium* and *Pseudozyma* show a simultaneous consumption of glucose, xylose and fructose [115] and glucose, xylose and arabinose, respectively [116]. Likewise, *Rhodospiridium kratochvilovae* and *Y. lipolytica* showed a simultaneous consumption of different pentoses and hexoses on mixed sugar media [117,118]. In addition, it has been recently documented that strains of *Meyerozyma guilliermondii*, *Scheffersomyces coipomensis* and *Sugiyamaella paludigena* isolated from decaying wood can simultaneously consume glucose, mannose and xylose, the most important sugars in lignocellulosic biomass [119]. In this research, significant simultaneous expression of several key enzymes, such as phosphoglucose isomerase, phosphomannose isomerase and xylulokinase, involved in glucose, mannose, and xylose metabolism, respectively, has been reported proving simultaneous sugar consumption, although a preference for glucose was always observed [119]. Simultaneous sugar consumption can be attributed to the low carrier specialization in yeast [67].

Lipid accumulation is induced by nutrient (usually nitrogen) deficiency which causes a reduction of adenosine monophosphate (AMP) concentration. This reduction inhibits NAD⁺-dependent mitochondrial isocitrate dehydrogenase (NAD⁺-ICDH), which is allosterically activated by AMP [1]. The inhibition of NAD⁺-ICDH causes a deregulation of the Krebs cycle resulting in citric acid accumulation in the mitochondria

that is secreted then in the cytosol in exchange for malate. Subsequently, citric acid is converted to oxaloacetate and acetyl-CoA (the precursor of FA biosynthesis), through the action of ATP-dependent citrate lyase (ACL). It has been reported that a low or null activity of ICDH and a high activity of ACL in the cytoplasm are key factors for the accumulation of lipids [2,5,6,44,119-123].

The process of FA synthesis is carried through the FA synthase complex. First enzyme involved is acetyl-CoA carboxylase (ACC) that converts acetyl-CoA to malonyl-CoA, reaction that frequently takes place in the cytosol of heterotrophic organisms and in the plastid of autotrophic microorganisms, and in some cases in both [3]. Then malonyl elongation is catalyzed by adding 2 carbons to the carbon chain, consuming 2 NADPH molecules per elongation unit in eukaryotes, while in autotrophic bacteria and algae the FAS type II enzyme complex catalytically elongates the lipid chains by two carbon units in an iterative pathway [4,124,125]. FA synthesis requires high reducing power in the form of NADPH. In oleaginous bacteria NADPH is provided by PPP [126], while in oleaginous eukaryotes NADPH is provided by both, the malic enzyme (ME) reaction that converts malate to pyruvate and the PPP [5,6,127-129]. In oleaginous microalgae the main donor of reducing power seems to be the ferredoxin NADP reductase of the photosystem I [6].

Following long chain acyl-CoA synthesis in the cytoplasm, acyl-CoA is transported to the endoplasmic reticulum (ER) and esterified with glycerol-3P (G3P), generating structural (phospholipids, glycolipids) and storage (TAG) lipids through the Kennedy pathway [5,72,130-132]. Glycerol-3-phosphate (G3P) is the second component of TAG and therefore its availability is believed to affect TAG biosynthesis

[133]. Finally, polyunsaturated fatty acids are synthesized by the action of desaturases and elongases located in the ER. In general, the lipids produced by fungi and microalgae are more unsaturated than those of yeasts.

Once the carbon source is depleted in the medium, oleaginous microorganisms use their own storage lipids as an energy source for maintenance purposes or, under certain circumstances, as carbon source for the production of new lipid-free cell material [26,44,52]. In the case of microalgae, lipid turnover can occur in cultures growing under CO₂ starvation [27]. Lipases and hydrolases are the enzymes involved in the degradation of lipids, while the FAs released are catabolized through the process of β -oxidation towards acetyl-CoA with the participation of oxidases [44].

Significant lipid production from sugars is possible only under specific environmental conditions otherwise, carbon metabolism is directed to the production of other compounds, such as low molecular weight metabolites (i.e. organic acids, sugar alcohols, ethanol etc.) that are excreted in the growth environment. This metabolic shift may be due to the response in nutrient insufficiency, pH change, oxygen concentration, among other conditions [50,52,134-139].

The cost of SCO production is critically affected by the productivity of oleaginous microorganisms, especially their ability to accumulate lipids. In this context, studies using genetic engineering in the different stages of de novo synthesis and in different oleaginous microorganisms have been developed [140-141]. It has been shown that overexpression of genes involved in FA and TAG synthesis considerably increases lipid accumulation [1,57,142,143]. Among the over-expressed enzymes that have been

shown to affect lipid accumulation are ACL [122], ACC [131,144-146], ME [147,148], FAS I and FAS II [149], some desaturases [150,151] and G3P [133].

2.4. FA composition of SCOs

SCOs represent a fascinating raw material for product development because they have a chemical profile suitable for the biotechnological production of biodiesel and biochemicals. The FA profile of microbial oils varies according to the genus and species [1], but usually is similar to the oils produced by oleaginous plants such as soybean, rapeseed, sunflower and palm oil [58,152,153].

SCOs produced by oleaginous yeasts and filamentous fungi mainly consist of myristic (C14:0), palmitic (C16:0), palmitoleic (C16:1), stearic (C18:0), oleic (C18:1), linoleic, (C18:2) and α and γ -linoleic C18:3) acids, with C16:0, C18:1 and C18:2 usually being the most abundant FAs [2,50,57,80]. Microalgae species synthesize long-chain FAs with a higher number of double bonds, such as docosahexaenoic acid (C22:6), eicosapentaenoic acid (C20:5) and arachidonic acid (C20:4) [3,28,32,154]. Most bacteria accumulate polyhydroxyalkanoates acids (usually poly-3-hydroxybutyric acid), instead of TGAs [155]. The oleaginous bacteria able to accumulate TAGs are characterized by the presence of more saturated FAs, such as lauric acid (C12:0), C14:0, C16:0 and C18:0, although unsaturated FAs are sometimes present [155,156].

The industrial applications of each oleaginous species are determined by its FA composition. Some microalgae and the most species of yeasts and bacteria, able to synthesize common oils (i.e. having a FA composition similar to plant oils), are intended

to produce biodiesel with similar physical and chemical properties to petroleum diesel [9,28,32,66,71,154,155,157], while other species of microalgae and some fungi are able to synthesize polyunsaturated fatty acids and therefore are intended to produce cosmetics, infant formula additives and animal feed [28,29].

2.5. Importance of lignocellulosic biomass as raw material

The use of lignocellulose as substrate for oleaginous microorganisms promises a production of SCO's economically viable and sustainable [22,158]. Lignocellulosic biomass represents a fascinating raw material for producing valuable compounds because it is a renewable, abundant and inexpensive substrate [159,160]. It is composed of a high percentage of assimilable sugars suitable to produce biofuels or oleochemicals [14,15,22,160]. Most research has been focused on terrestrial lignocellulosic biomass; however, the use of marine lignocellulosic biomass from micro and macro algae has also been considered [161].

2.6. Lignocellulose structure and chemical composition

Lignocellulose provides mechanical support and tolerance to biotic and abiotic stresses in plants. Its structure consists mainly of a network of cellulose, hemicelluloses (which together form the holocellulose) and lignin polymers and in less quantities starch, pectin, extractives, ashes etc. [162–165]. The content of each of the above compounds depends on the species, tissues and age of the cells [161].

Cellulose is the most abundant polymer, representing 34-50% of the dry biomass in softwood species and 41-50% in hardwood species, while in agricultural residues it is approximately 17-42% [161]. It is an amphiphilic and linear homopolymer composed of more than 10,000 glucose molecules linked by $\beta(1-4)$ glycosidic bonds. Specifically, between two glucose molecules the second unit rotates around the C1-C4 axis, forming a dimer known as cellobiose that binds to each other forming linear glucose chains [166].

Hemicelluloses are amorphous, branched heteropolysaccharides formed by a main chain and other lateral ones. The main chain is composed of equal (homopolymer) or different (heteropolymer) sugar units and is shorter in length than cellulose. The side chains are short and linked mainly by $\beta(1-4)$ glycosidic bonds and occasionally by $\beta(1-3)$, which are easily hydrolysable. Sugars can be hexoses (glucose, mannose, and galactose), pentoses (xylose and arabinose), uronic acids and deoxyhexoses (such as rhamnose and fucose) [165]. Hardwoods (i.e. angiosperms) contain mainly glucuronoxylans, while softwoods (i.e. gymnosperms) contain mainly galactoglucomannans, which represent approximately 18-35% of the lignocellulosic biomass [161,167]. In agricultural biomass xylan is the main hemicellulose and represents between 12 and 37% % of the lignocellulosic biomass [161].

Lignin is the most abundant organic polymer after cellulose, representing 19-35% of the lignocellulosic biomass of woods and 3.5-30% of grasses [161,168,169]. It is mainly formed in vascular tissues and provides mechanical resistance to xylem. Lignin is classified into three types of phenylpropane units (or monolignols), guaiacyl (G), syringyl (S) and p-hydroxyphenyl (H), derived from alcohols, coniferyl, sinapyl and p-

coumaryl, respectively. In softwoods, the predominant lignin is guaiacyl, in hardwoods guaiacyl and syringyl in a ratio of 1:1 to 1:3, while all the lignin monomers are present in the grasses [170].

In addition, other biomolecules are also present in the cell wall of plants in smaller quantities. Compounds such as tannins, phenols and lignans are mostly connected to lignin and represent between 1% and 5% of lignocellulosic biomass [166]. It is also possible to find pectins and pectin-like compounds (such as galacturonans, galactans and arabinans), starch, and proteins, although they decrease as plants aged. Free amino acids or alkaloids that contribute to the nitrogen content, inorganic components (e.g. Ca, K, Mg, Mn, Na, P and Cl) and trace elements (e.g. Ba, Al, Fe, Zn, Si, Pb, Ni, V, Co, Ag and Mo) essential for growth are also present [166].

Most of the highly diverse compounds found in the lignocellulosic biomass, can be metabolized by oleaginous microorganisms, but not all of them can lead to an important production of lipids. For this reason, it is essential to analyze the effect of the different lignocellulosic compounds on the metabolism of oleaginous microorganisms in order to design an efficient production process. In this sense, there is still much to be investigated experimentally.

2.7. Recalcitrance of lignocellulosic biomass

Recalcitrance of lignocellulosic biomass is linked to physical and chemical factors involved in the bonds among polymers. First, cellobiose molecules are bound through hydroxyl groups by means of hydrogen bonds to form cellulose microfibrils, with a

hydrophobic interior and a hydrophilic exterior. These, in turn, are joined by Vander Waals forces to form microfibrils with highly recalcitrant regions (crystalline regions) [166,171]. The abundance of crystalline regions changes according to the type of plant, even among species of the same genus [162]. Microfibrils are bind to hemicelluloses and hemicelluloses to lignin forming a stable structure. Lignin at the molecular level controls permeability, improves the mechanical properties of the cells and protects them from microorganisms and chemical degradation, being the main factor which imparts recalcitrance to the biomass.

To reduce/eliminate recalcitrance and obtain assimilable sugars it is necessary to destabilize the cellulose, hemicelluloses and the lignin matrix. The amorphous regions of the cellulose and the branches of the hemicelluloses provide a certain degree of flexibility and susceptibility to decomposition and are the key points to begin deconstructing. This goal is approached through the application of various pretreatments [171,172].

3. Conversion of lignocellulosic biomass into assimilable sugars in nature

In nature, degradation of lignocellulosic material can be mediated mainly by decomposing animals, insects and fungi. Insects such as wasps, ants and termites, animals such as beavers, rats and woodpeckers and mollusks from aquatic environments perform mechanical degradation, while decaying fungi perform enzymatic degradation [170,173]. Wood decay fungi have been extensively studied. They are a diverse group of species belonging mainly to the Basidiomycota and Ascomycota

divisions [71]. They are saprophytes and are capable of penetrating and colonizing the interior of plants through their hyphae, entering through the pores or through the secretion of enzymes that cause the rupture of the cell walls [166,170].

Decomposition of wood by fungi is typically classified into three types: brown rot white rot and soft rot. Brown rot is commonly brown and crumbly and is produced by non-enzymatic and enzymatic systems. Brown rot fungi produce cellulases but not enzymes that degrade lignin. However, they possess a non-enzymatic mechanism that results in the modification of lignin and a slow depletion of lignin from wood in the process of decomposition known as the chelation-mediated Fenton system (CMF). [173,174]. White rot fungi, possessing lignin-degrading enzymes, are the only organisms capable of degrading all wood components. The capacity of these fungi to secrete non-specific ligninolytic and cellulolytic enzymes allows the transformation of a great variety of recalcitrant compounds into assimilable carbon forms, as the extracellular nature of the above enzymes allows fungi to access non-polar and insoluble compounds [175-177]. Soft rot fungi produce cavities and erosion in the cell walls of wood. Under aerobic conditions, these fungi can completely mineralize lignin and polysaccharides (cellulose, hemicelluloses) into CO₂ and H₂O, in addition to causing wood rot [178].

The natural mechanisms usually cause degradation at low rates. However, some technologies based on natural processes, such as biopulping and biodegradation (e.g. used in the degradation of resins and dyes), have been applied to degrade lignocellulosic biomass [177,179,180].

4. Biomass pretreatment to decrease recalcitrance

To obtain assimilable sugars from lignocellulosic biomass, it is necessary to apply previous processes that include mechanical methods, physicochemical pretreatments and enzymatic hydrolysis. First, it is necessary to reduce the size of the particles in order to decrease the degree of polymerization and to increase the surface area and porosity of the biomass to improve the exposure to the action of reagents. This can be done through a mechanical process, considered a fundamental step of the lignocellulosic biorefinery, which includes processes such as cutting or grinding (the size varies from meters to centimeters), coarse grinding (from cm to 500 μm), intermediate micronization (from cm to 100 μm) and fine grinding ($<100 \mu$). These are generally obtained by compression friction or shearing and therefore generate a specific energy requirement (SER) that must be evaluated [71,166,181,182]. SER in mechanical treatment is affected by the moisture content and chemical composition of the substrate and has been demonstrated to increase with increasing moisture and arabinose/xylose content [183].

It has been reported that mechanical processes can increase carbohydrate production, improving yield and enzymatic hydrolysis rate by 5-25% and 23-59%, respectively, compared to untreated biomass [71]. After the mechanical process, a pretreatment is applied that leads to the reduction of the biomass recalcitrance and, in some cases, to the hydrolysis of a significant percentage of polysaccharides. However, mechanical processes are usually intended to increase the accessible surface area of cellulose and hemicelluloses to enzymes to be used in enzymatic hydrolysis [15].

Pretreatments are varied and have been widely studied in productive, technical, economic and environmental terms [184–188]. In this context, chemical pretreatments such as acid, alkaline and acid combined with alkaline have been the most preferred and patented techniques in recent years, compared to other methods. These represent advantages associated with the use of commonly used compounds, flexibility of application at the industrial level and high final yields of assimilable sugars [171,186,187]. Other recommended pretreatments are steam explosion and treatment with organosolv. Steam explosion (or autohydrolysis used as a synonym), is the most widely used physicochemical pretreatment method. It has been described as an economical and environmentally friendly method that reduces the concentration of toxic compounds in hydrolysates compared to other pretreatments, such as acid pretreatment [48,186,189], while organosolv pretreatment, although more expensive than the other processes mentioned, may provide some valuable by-products that allow the sustainability of the process. In a biorefinery, organosolv pretreatment is one of the best options due to very good quality of cellulose obtained, very accessible to enzymes, and lignin residual from which it is possible to produce more than one valuable product (e.g., bioethanol and lignin products) in the same process [163,190].

The selection of the pretreatment method and its operating conditions, are fundamental for a successful enzymatic hydrolysis and subsequent fermentation. The conditions utilized largely depend on the nature and chemical composition of the substrate (hardwood, softwood or herbaceous) and determine the amount of the generated by-products that can interfere with enzymatic hydrolysis and fermentation. Below are a description of the advantages and disadvantages of the most

recommended processes (acid, alkaline, acid-alkaline, steam explosion and organosolv) and a discussion of the yields and effects of these pretreatments on enzymatic hydrolysis. Table 1 shows the most frequent values of the working conditions and yields of the different pretreatments applied to different lignocellulosic substrates.

4.1. Principal pretreatments used

4.1.1. Acid pretreatment

Acid pretreatments are effective in breaking the lignocellulosic matrix at the glycosidic bonds between lignin and hemicelluloses, by solubilizing most of the hemicelluloses (commonly over 90% w/w), as well as reducing some of the cellulose and removing part of lignin (Table 1). The process consists first in the hydrolysis of hemicelluloses to its monomeric sugars, and then in the depolymerization of the cellulose into oligosaccharides, with further release of monomeric sugars. Both steps allow for a significant increase in porosity and a significant lignin removal. However, acid pretreatment is suitable for removing lignin from hardwoods and agricultural residues, but not from softwoods. The difficulty of removing lignin from softwoods is well documented and is due to the structural characteristics of softwood lignin [167,191].

The acids used are diverse and can be both inorganic (e.g. phosphoric, nitric, hydrochloric or sulphuric acid) or organic (e.g. acetic, citric, maleic or oxalic acid) [167,186,187], with sulphuric acid being the most commonly used. Acid pretreatment can be wet acid, using concentrated ($> 30\%$ w/v) or diluted ($<30\%$ w/v) in water acid, or dry diluted acid, which has been recently documented [186,187,192].

Pretreatment using concentrated acid is a process that allows to obtain a high content of assimilable sugars (>50%) with low energy costs since it is carried out at low temperature (< 100 °C), even at room temperature. The disadvantages of using concentrated acids are the requirement of corrosion resistant equipment that increases investment costs and the risk of the reagents, which are highly dangerous and require investment in safety issues. Additionally, concentrated acid causes a partial degradation of hemicelluloses to by-products that accumulate in the liquid waste as organic acids, furfural and 5- hydroxymethylfurfural (HMF) mostly, reporting total values even over 13 g/L [193]. These have been reported as inhibitors of enzymatic hydrolysis and fermentation. Strategies have been developed to reduce the inhibitor concentration, such as the use of two stages acid pretreatment, where a less concentrated acid is first applied to extract hemicelluloses, causing a restricted degradation, following by a more concentrated acid, aiming to destruction cellulose [193,194]. However, the disadvantages have made them less attractive processes to implement and, in this sense, diluted acid pretreatments are preferred.

Diluted acid pretreatment is less aggressive, more environmentally friendly, and less costly, given the lower acid demand [172]. In addition, it allows the recovery of much of the sugar from hemicelluloses at the end of the process, usually with a low production of inhibitory compounds (Table 1). Most pulps obtained from diluted acid are very accessibility to the enzymes therefore it is possible to recover glucose and a cellulose solid fraction that usually has over 70% digestibility (Table 1). The disadvantage of diluted acid pretreatments is that they require higher temperatures than those used in treatments with concentrated acids, thus increasing energy costs.

Glucose release in diluted acid pretreatments has been optimized by using more than one stage, alternating high and low temperatures during short and long retention periods [195,196]. Solid catalysts may also be used in the pretreatment (e.g., carbon-based; zeolites, ion exchange resins) that can be recycled and reused several times. These improve the yields of assimilable sugars and leave a cellulose fraction that is easily hydrolysable, achieving glucose yields of more than 91% after enzymatic hydrolysis [187,197].

Pretreatment with dry diluted acid has been proposed as an alternative to the use of diluted acid pretreatment. In this process, both the raw material and the product are generally solid. The biomass is even used at more than 70% w/w with respect to the diluted acid, which is impregnated and fully absorbed by the biomass [192]. After enzymatic hydrolysis, sugar yields similar to those obtained with diluted acid pretreatment are obtained. One of its advantages is that it produces exceptionally low concentrations of furfural and HMF in the pretreated solid (< 0.1 and up to 0.90%) compared to those formed in other acid pretreatments [187,192]. However, dry diluted acid pretreatment requires special equipment to improve impregnation and more stages in the process, while few studies have been carried out on this topic.

4.1.2. Alkaline pretreatment

Alkaline pretreatment allows a destruction of the lignocellulose and decreases both the degree of polymerization and the crystallinity of the cellulose. It is effective in extracting lignin and solubilizing a part of the hemicelluloses (commonly $>40\%$ w/w), while causing negligible degradation of the cellulose (Table 1). During alkaline

pretreatment, the first reactions are the dissolution and saponification of the intermolecular ester and ionic bonds that cross the hemicelluloses and other components, reactions that increase the porosity of the lignocellulosic biomass through the disintegration of these bonds. In addition, hydrolysis of glycosidic bonds and acetyl groups may occur, breaking down polysaccharides and enhancing subsequent enzymatic hydrolysis [186,198]. The most used bases are sodium, potassium, calcium hydroxide and ammonium hydroxide [185,198]. In general, alkaline pretreatment is more effective on hardwoods, arable crops and agricultural residues with low lignin content than on softwoods with high lignin content [186]. Compared to other pretreatments it is considered of low cost and its main disadvantage is the formation of salts, which are difficult to be removed, and the low yields in monomeric sugar [172,185]. The digestibility in the solid fraction is frequently more than 70% (Table 1).

4.1.3. Sequential acid-alkaline pretreatment

Some researchers have also tested the combination of both acid and alkaline pretreatment processes for significant recovery of reducing sugars. Commonly, the process involves hydrolysis using a dilute acid [15], solid extraction and washing and then treatment with dilute alkaline solution. The acidic stage allows the recovery of most hemicelluloses, that are usually above 70% w/w, and the alkaline stage allows the extraction of a high percentage of lignin frequently >80% w/w (Table 1). The cellulose is recovered at a rate above 75 % and highly hydrolysable. Compared to diluted acid pretreatment, the proposed combined pretreatment minimizes the generation of by-products [199]. The main disadvantage is that more investment in equipment is required

to develop the two stages and more processing time is needed, as the number of stages increases [172].

4.1.4. Steam explosion pretreatment

This pretreatment, being recognized as one of the most efficient processes for lignocellulosic biomass from hardwood and herbaceous, consists of treating the biomass at high pressure using water vapor and at high temperature for a short period of time and then quickly depressurizing, which generates a disruption of the biomass with the partial elimination of the lignin [15,71]. During the process, due to the acidic condition, organic compounds such as acetic acid are generated, causing the formation of acetyl groups, which allow an autohydrolysis of the hemicelluloses and a partial delignification, increasing the exposure of the cellulose to the enzymatic hydrolysis that follows [15,186]. It can also be used in two stages for enhanced recovery of assimilable sugars, first under milder conditions to recover hemicelluloses and then under stronger conditions to destabilize the cellulose and recover higher percentages of glucose [185]. The advantages of steam explosion pretreatment are that it has a lower environmental impact and a lower production of toxic compounds, than those of acid and alkaline processes [186]. On the other hand, this pretreatment is less effective for softwoods, as they have a low content of acetyl groups, making the use of catalysts necessary. E.g. chemical compounds such as SO_2 , H_2SO_4 and CO_2 have been used to impregnate the softwood before pretreatment [71,186]. Nevertheless, this has the disadvantages of requiring more time for impregnation and generating greater formation of inhibitors and

higher degradation of sugars [185,195]. Treatment pressure has a direct effect on reducing sugars yields, with values above 60% w/w [48].

4.1.5. Organosolv pretreatment

Organosolv pretreatment involves the application of an organic solvent to the lignocellulosic biomass in order to separate lignin in the liquid fraction and cellulose in high concentrations in the solid residue. Pretreatment generates excision of lignin bonds, especially of O-aryl ether bonds with carbohydrates, producing a solid phase, which consists mainly of cellulose and hemicelluloses, and causing dissolution of lignin fragments [163]. It is carried out in different organic solvents (ethanol, methanol, acetic acid, formic acid, acetone, glycerol or phenol) whose concentrations generally vary from < 1% w/w to over 80% w/w [163] and is applied with or without catalysts (sulphuric acid, magnesium chloride, or sodium hydroxide). Treatment with ethanol is the most attractive and used method due to the low cost of the solvent and the high yields of extracted lignin [163,190]. The organosolv pretreatment of hardwood and herbaceous in aqueous solutions can generate acetic acid from the acetyl xylan groups, which in turn catalyzes the degradation of hemicelluloses, the dissolution of lignin and stimulates the autohydrolysis of cellulose [190]. Softwoods have reduced xylan content and therefore the alkaline catalyzed organosolv pulping has also received a lot interest [200]. The advantages of this method are that it can be applied to hard and soft woods and the solvents can be easily recovered by more than 90% causing little environmental effect [163]. The main disadvantage is the danger of ignition by concentrated solvents and the generation of various inhibitory residues that may inhibit enzymatic hydrolysis [189]. The

main degradation products are G-type lignin derivatives, such as guaiacol (C6), vanillin (C6C1), vanillic acid (C6C1) and ferulic acid (C6C3), and S-type derivatives, such as syringaldehyde (C6C1) and syringic acid (C6C1) [201].

4.2. Optimization of principal pretreatments

In general, various pretreatments do not allow total recovery of the sugars that are present in the lignocellulosic biomass. On the contrary, these techniques result in yields of 90% or less of the theoretical sugar yield [201]. In this context studies have shown that combined pretreatments improve the yield of sugars after enzymatic hydrolysis [165,172,185,198]. Work has been done for example on combined treatments of alkaline with ionic liquids (IL) and microwaves [202]. IL with steam explosion [189], alkaline with oxidation [113,203], acid with steam explosion [204], among others, improve sugar yield even by more than 100% compared to the application of a single pretreatment. Table 2 presents the main advantages and disadvantages of the alternative treatments that can be used in combination with the above described conventional treatments. It is also possible to use catalytic compounds that are impregnated before or during the pretreatment and improve the destruction of the cellulose, yielding shorter chains, which are easily hydrolyzed, and less degradation products of the cellulose and hemicelluloses monosaccharides [71,168,187,197]. However, these should be used by an appropriate manner, and further studies are needed to avoid negative effects, such as an increase in by-products that inhibit hydrolysis and fermentation.

5. Pretreatment by-products affecting enzymatic hydrolysis and fermentation

By-products generated during the pretreatment of lignocellulosic biomass are to the detriment of sugar yield and also in certain concentrations may reduce the efficiency of enzymatic hydrolysis, as well as the growth and metabolism of most microorganisms used in fermentations. Specifically, several compounds derived from lignocellulose pretreatment, even at low concentrations, can inhibit growth and lipid accumulation in oleaginous microorganisms [15,73,205]. Therefore, it is necessary to study the inhibitory effects, in order to adopt appropriate strategies for the production of SCO from lignocellulosic hydrolysates. The type and concentrations of each compound generated in principal pretreatments depend on the operating conditions and the composition of the biomass used (Table 1).

Among the inhibitory compounds derived from sugars are furan aldehydes, such as furfural and 5-hydroxymethylfurfural (5-HMF), generated in acidic media from the dehydration of pentoses and hexoses, respectively. Both compounds have a significant effect on enzymatic hydrolysis at concentrations of 2.0 g/L for furfural and 4.0 g/L for HMF [206]. In addition, research has shown that furfural and 5-HMF inhibit the metabolism of alcohol-producing yeasts, prolonging the lag phase, inhibiting cell growth and decreasing ethanol productivity. For instance, furfural is found to directly inhibit alcohol dehydrogenase, aldehyde dehydrogenase, pyruvate dehydrogenase and some enzymes involved in glycolysis [207,208]. Also, induce DNA damage or breakdown,

inhibit protein and RNA synthesis [172,209-211], and affect the production of NADH and NADPH, decreasing the uptake rates of specific sugar [211].

Other inhibitory compounds derived from sugars are aliphatic carboxylic acids such as acetic acid, formic acid and levulinic acid. Acetic acid is formed by acid hydrolysis of hemicellulose acetyl groups, levulinic acid is the terminal product of hexose oxidation and formic acid has two pathways of formation, one by the oxidation of pentoses and the other by the oxidation of hexoses [15,212,213]. These acids cause a pH decrease which negatively affects the microbial metabolism. E.g. acetic acid can penetrate the cell membrane in its undissociated form inhibiting product formation, causing pH imbalances at high concentrations and eventually cell growth inhibition or death [172]. These compounds are mainly generated during acid, alkaline and organosolv pretreatment [50,108,214], and are commonly produced at a range of 0.1-5 g/L (Table 1), while seem to be especially toxic to microorganisms at concentrations ranged between 0.3 and 5 g/L (Table 3). Regarding acetic acid, due to the low content of acetyl groups present in softwoods, pretreatments generate lower concentrations of acetic acid, while in hardwoods and agricultural residues with high acetyl group content, the concentration of acetic acid is higher resulting in an important inhibition effect [15]. In contrast, the low concentrations of acetic acid in pretreated softwood stimulate ethanol production due to the lower yeast biomass formation. This is due to the increased ATP demand and/or inefficient ATP production due to uncoupling of the respiratory chain and the oxidative phosphorylation of ADP, which leads to increased ATP-generating glycolytic activity at the expense of cell proliferation [15].

Other sugar derivatives formed during acid pretreatment include polyols generated during the hydrogenation of cellulose and hemicelluloses sugars, such as sorbitol, mannitol, xylitol, galactitol, arabitol, ribitol (adonitol) and erythritol [215,216]. However, these compounds usually have not negative effect. Contrary, it has been suggested that polyols may mimic water and maintain an artificial sphere of hydration around macromolecules and also act as scavengers of reactive oxygen species, thereby preventing lipid peroxidation [215].

Aromatic carboxylic acids derived from lignin are also generated during pretreatment, but in lower amounts. These compounds, represented by cinnamic and benzoic acid derivatives, are commonly produced from herbaceous lignin rather than hardwood and softwood lignin. The common cinnamic acid derivatives include p-coumaric, ferulic and sinapic acids. Benzoic acid derivatives include 4-hydroxybenzoic acid. Also by-products from lignin are three typical aliphatic phenolic aldehydes, namely vanillin, syringaldehyde and 4-hydroxybenzaldehyde, which can also be considered as lignin derivatives of guaiacyl group (G), syringyl group (S) and hydroxyphenyl group (H), respectively [15,73,109]. Aromatic carboxylic compounds derived from lignin are present in hydrolyzed lignocellulosic biomass in relatively low concentrations compared to carbohydrate degradation products, such as aliphatic carboxylic acids and furan aldehydes. However, their inhibitory effect is usually stronger than aliphatic carboxylic acids, causing a loss of integrity of biological membranes, thus affecting their ability to serve as selective barriers and enzyme matrices [211]. Among phenolic compounds vanillin is the most toxic inhibitor for microorganisms [15,211,214]. Phenolic aromatic compounds can also affect enzymatic hydrolysis. Although the treatment of

lignocellulosic hydrolysate with reducing agents, such as bisulfite and dithionite, decreases inhibitory effects due to sulfonation of phenolics, aromatic compounds remain a problem for cellulolytic enzyme activity. It has also been shown that the inhibitory effect of phenolic compounds increases with increasing hydrophobicity [216].

The effect of the pretreatment by-products on microorganisms has been widely studied in the case of ethanol-producing microorganisms. However, since different yeasts have different responses to inhibitors, the effect of the various inhibitory compounds on microbial metabolism deserves further investigation in oleaginous species. It has been shown that most oleaginous microorganisms are sensitive to the inhibitory by-products generated during lignocellulosic biomass pretreatment, although at appropriate concentrations, some of them can assimilate and/or degrade part of the by-products [146,217-220]. Table 3 shows the effect of important inhibitory compounds on the growth of oleaginous microorganisms and their ability to produce lipid.

Among by-products some of them, especially acetic acid, were considered as potential substrates / co-substrates or stimulators for the production of lipids by various oleaginous microorganisms, including *Cutaneotrichosporon curvatum* (*Cryptococcus curvatus*), *Cyberlindnera (Williopsis) saturnus*, *Umbelopsis (Mortierella) isabellina*, *Lipomyces lipofer*, *Rhodotorula (Rhodosporidium) toruloides* and *Yarrowia lipolytica* [49, 104]. For instance, Poontawee et al. showed that the addition of acetic acid in concentrations ranging from 0.1 to 0.25 g/l improved lipid accumulation compared to the control [104].

6. Enzymatic hydrolysis

Enzymatic hydrolysis of lignocellulose after pretreatment is the last step before fermentation. The most commonly used enzymes are cellulases and hemicellulases, which convert cellulose and hemicelluloses into glucose and a mixture of pentoses and hexoses, respectively [221]. Besides, mixtures of cellulases (Celluclast 1.5L, Sigma) and β -glucosidase (Novozyme 188, Sigma) have also been commercialized [199,222]. Cellulases represent a group of at least 15 protein families and some subfamilies that are mainly divided into endo- and exo-glucanases types and β -glucosidases. Endoglucanases attack the amorphous and low crystallinity regions of cellulose leaving a reducing and a non-reducing end, exo-glucanases attack the free ends and release cellobiose molecules and β -glucosidases break the β -1,4-D links of cellobiose, releasing glucose molecules. On the other hand, hemicellulases carry out a complete degradation of hemicelluloses and include a diverse group of enzymes, such as endo- β -1,4-xylanase that produces xylo-oligosaccharides and β -xylanase that breaks down xylan to produce xylose. Other accessory enzymes include α -glucuronidase acetylxyloxyesterase, ferulic acid esterase, α -galactosidase and α -L-arabinofuranosidase which aid in the hydrolysis of hemicelluloses side chains [71]. The synergistic action of cellulases and hemicellulases increases the conversion rate of cellulose and hemicelluloses into free sugars.

Enzymatic hydrolysis may be inefficient due to the numerous factors that negatively affect enzyme activity. Among the factors have been reported are the high concentration of assimilable sugars in the media, the presence of inhibitory compounds

generated during chemical or physical pretreatments [223], and the long residence time, which increases non-specific and irreversible binding of enzymes with residual lignin. In general, the pretreated biomass from softwood presents more non-specific and irreversible binding of the enzymes than hardwood, due to the high residual lignin content, requiring relatively higher enzyme loads for enzymatic hydrolysis.

Increased enzyme specificity and activity along with reduced cost of enzymes is one of the main challenges that must be faced in enzymatic hydrolysis. Currently, work is done to increase the digestibility of cellulose and decrease non-specific functions by adding non-ionic bases or surfactants such as polyethylene glycol and sorbitol ester and polyethoxylated, Tween-80, Tween-20, dodecylbenzenesulfonic acid, Triton X-100 and PEG 4000, which have proven to be highly effective [47,71,186,224].

On the other hand, biotechnological solutions are continuously proposed, e.g. genes encoding for cellulases have been cloned in fungi and yeasts, bacteria, and plants to understand their function and construct new sources for enzyme production [225,226]. Likewise, phytopathogens, having the ability to degrade plant cell walls, such as *Fusarium verticillioides*, *Pycnoporus sanguineus* and *Chrysosporthe cubensis*, seem to have high interest in the perspective of biotechnological production of enzymes [17].

On the other hand, simultaneous enzymatic hydrolysis (saccharification) and fermentation (SSF) seems to be a great alternative in terms of lignocellulosic material conversion that can decisively reduce the processing costs. This approach integrates the release of sugars and the biosynthesis of the microbial metabolite production in a single stage, reducing thus the processing time, the necessary enzymatic load, the occupying equipment and the contamination risk and resulting in a higher product yield,

756 compared to the separate stages [226,227]. Examples of SCO production through SSF
757 include (a) *Cryptococcus curvatus*, cultivated in the presence of cellulase and
758 cellobioses on corn biomass pretreated with ionic liquid, resulting in a lipid yield that
759 reached 112 mg of lipid /g of corn stover [228], (b) *Trichosporon cutaneum* cultivated in
760 the presence of cellulase on pretreated with diluted acid and biodetoxified corn stover,
761 producing 3.2 g/L of lipids [229], (c) *Microsphaeropsis sp.* cultivated in the presence of
762 cellulase in solid state fermentation on a substrate consisting of steam-exploded wheat
763 straw and wheat bran, producing 74 mg of lipid/g of dry substrate [230], (d)
764 *Rhodococcus opacus* grown on diluted acid pretreated residues of pine, poplar and
765 switchgrass producing approximately 15 mg/L of lipids using a mixture of cellulase and
766 β -glucosidase [231].

767 For a satisfactory SSF, it is necessary to optimize several parameters, such as
768 the pH, the percentage of sugars and the dose of enzymes, so as to obtain the higher
769 possible yields at the lower costs. Temperature is another key factor to consider, since
770 saccharification and fermentation are optimal at different temperatures [232,233]. In this
771 context, the use of thermotolerant microorganisms capable of producing significant lipid
772 amounts at elevated temperatures of approximately 40 °C has been proposed, since at
773 this temperature the enzymatic hydrolysis of cellulose is more efficient. However, the
774 accumulation of lipids by the mesophilic microorganisms is usually reduced at such a
775 high temperature [228,234].

776

777 7. SCO production from hydrolyzed lignocellulosic biomass

778

The production of SCO by oleaginous species, principally yeasts, filamentous fungi and bacteria, cultivated on lignocellulosic hydrolysates has been studied by many authors, (selected papers are included in Table 4). Likewise, in recent years, the conversion of lignocellulosic hydrolysates into SCO by heterotrophically growing oleaginous microalgae, such as the green microalgae *Auxenochlorella* (*Chlorella*) *protothecoides* has been studied [235].

In addition to the general conditions required for SCO production by oleaginous microorganisms, their cultivation in lignocellulosic hydrolysates may require additional treatment, e.g. detoxification, due to the presence of inhibitory compounds generated during pretreatment. Nevertheless, some microorganisms are able to growth well even in undetoxified hydrolyzed lignocellulosic media and accumulate satisfactory amounts of lipids. Biomass and lipid production by selected oleaginous microorganisms, cultivated in both detoxified and undetoxified lignocellulosic hydrolysates (DLH and ULH, respectively) derived from different plant biomasses are show in Table 4.

Several investigations have shown that inhibitory compounds generated during lignocellulosic biomass pretreatment negatively affect growth and lipid production (Table 3), making hence often necessary the application of additional treatments to reduce toxicity. A conceptual scheme proposed for SCO production using lignocellulosic hydrolysates as substrate is shown in Fig. 2.

The application of surfactants in ULH has a positive effect on microbial growth and lipid production [236]. Some anionic surfactants were effective in promoting the production of the oleaginous yeast *R. toruloides*, with the most significant impact achieved with the addition of 0.2% (w/v) sodium lignosulfonate [236]. The non-ionic

surfactant polyoxyethylene sorbitan monooleate (Tween-80), added at a rate 1% (w/v) in the hydrolysate, has also been reported to increase cell mass production and lipid content of the marine protist *Thraustochytrium aureum* ATCC 34304 [237]. However, Tween-80 used in *R. toruloides* growing in hydrolysate does not have a positive effect. Surfactants apparently denature the cell wall proteins and structure altering their permeability. However, the exact mechanism of the surfactant requires further investigation in oleaginous microorganisms in order to enhance their growth and lipid accumulation in hydrolyzed lignocellulosic media [236,237].

The reduction of hydrolyzed lignocellulosic biomass toxicity can be achieved by removing inhibitory compounds using different techniques, such as chemical additives, enzymatic treatments, heating and vaporization, liquid-liquid extraction, liquid-solid extraction and microbial treatment [216]. Particularly, the detoxification through the addition of $\text{Ca}(\text{OH})_2$ is commonly used, as a neutralization of the pretreated lignocellulosic biomass using this agent significantly reduces the concentration of 5-HMF, furfural and phenolic compounds by 20-30 % approximately [118,238]. Besides, resin adsorption and electrodialysis or as recently reported biological detoxification by bacteria, such as *Bordetella sp.* and *Bacillus sp.*, have been considered as efficient strategies to remove HMF and furfural [239-242]. However, the additional treatment needed for detoxification increases the production cost and results in a loss of assimilable sugars [240].

Detoxification of pretreated lignocellulosic biomass does not seem to be a very attractive approach as the techniques used result in sugar loss, and also implies an increase in costs due to the application of more stages in the process [19]. On the

contrary, the use of ULH can be a good alternative with lower processing costs, provided that tolerant oleaginous microorganisms, such as strains belongin to *Trichosporon*, *Cryptococcus*, *Lipomyces*, *Rhodotorula*, *Umpelopsis* (*Mortierella*), *Rhodospiridiobolus*, *Rhodosporidium*, *Rhodococcus*, *Meyerozyma*, *Pichia* and *Candida* will be used (Table 4).

ULH obtained from agricultural residues pretreated with weak acids seems to be suitable as a substrate for SCO production by the aforementioned oleaginous microorganisms, supporting lipid accumulation in dry biomass at high rates, even above 60% w/w (Table 4). Likewise, some oleaginous yeasts also accumulate high lipid amounts growing on ULH derived from combined (e.g. acid and other) pretreatments. For example, Poontawee et al. [113] showed that the yeast *Rhodospiridiobolus fluvialis* was able to produce up to 75% w/w of lipids growing in hydrolyzed sugarcane biomass obtained after acid/oxidative pretreatment. The alkaline pretreatment is also an important possibility to obtain high lipids productivities. Chaiyaso et al. [47] have shown an efficient bioconversion of ULH derived from alkaline pretreatment of corncob into biomass and lipids by the oleaginous yeast *Rhodosporidium paludigenum* with lipid accumulation approximately 70% w/w. On the other hand, agricultural residues pretreated using steam explosion are also an interesting option. For instance, significant lipid accumulation (ranging from 22 to 38% w/w) was observed by Ananthi et al. [48] in different conventional oleaginous microorganisms growing on ULH agricultural biomass pretreated with steam explosion.

The physiological response of oleaginous microorganisms to inhibitors generated during pretreatment of lignocellulosic biomass has been studied in various

microorganisms including *Candida*, *Rhodospiridium*, *Cryptococcus*, *Trichosporon*, *Rhodococcus*, *Wickerhamomyces* and *Vanrija*, and interesting results have been obtained regarding tolerance and even degradation of inhibitors [36,41,73,104,113,146,217,243]. For example, *T. cutaneum* can convert 3g/L of furfural and 3g/L of HMF into the corresponding alcohols (furfuryl alcohol and HMF alcohol) and completely degrade 15g/L of formic acid and 10 g/L of acetic acid [146]. In addition, enzymes involved in the degradation of furfural and HMF, including alcohol dehydrogenase, aldehyde reductase and aldehyde dehydrogenase, have been identified in yeasts strains such as *T. cutaneum* ACCC 20271, *R. toruloides* NP11, *Y. lipolytica* CLIB122 and *T. oleaginosus* IBC0246. The number of putative functional genes in the genomes involved in the synthesis of the aforementioned enzymes is higher in *T. cutaneum* ACCC 20271 providing a strong support for high degradation capacity and tolerance to inhibitors [147]. However, more metabolic studies are required to understand the physiology of oleaginous microorganisms against lignocellulose biomass derived inhibitors.

Tolerance to inhibitors is a required but not sufficient property for selecting an oleaginous microorganism to be used in lignocellulosic hydrolysates conversion to SCO; effective growth and lipogenicity are also needed for a sustainable process. However, as shown in Table 3, naturally tolerant microorganisms have usually a restricted capacity to effectively convert sugars into lipid-rich biomass. To overcome these difficulties, recombinant microorganisms could be constructed, simultaneously presenting tolerance and efficient growth and lipogenicity. Genetically modified strains of *Saccharomyces cerevisiae*, yeast widely used in the conversion of lignocellulosic

substrates to ethanol, showing increased tolerance to inhibitors, such as furfural and HMF, have been constructed, and this knowledge could be used for constructing new oleaginous strains. For example, *S. cerevisiae* strains ADH6p and ADH7 overexpressing alcohol dehydrogenase exhibit strong furfural and HMF reducing activities, and in some cases improve growth performance in the presence of aldehyde [211]. On the other hand, the experience of genetic manipulations in the oleaginous yeast *Y. lipolytica* can be used in this context [244]. Both streams of research pave the way for the genetic transformation of oleaginous yeasts, such as the yeast *Candida phangngensis*, the modified strain JQCP04 of which, overexpressed the alcohol dehydrogenase gene of *S. cerevisiae* (ADH6p) under strong control of the TEF constitutive promoter of *Y. lipolytica* [245]. This overexpression allows the reduction of the aldehyde group of the furfural inhibitor to an alcohol, greatly decreasing toxicity, reducing the lag time by 58% and increasing the growth rate compared to wild-type *C. phangngensis*. In a similar study, ADH6 was overexpressed in *Y. lipolytica* YB-392 [246]. The modified strain, although presented a furfural reduction capacity, does not present significant difference in terms of lag time, specific growth rate or biomass yield in the presence of 10 mM furfural, when compared to the wild type.

Some oleaginous red yeasts belonging to the phylum Basidiomycota, such as *Rhodotorula mucilaginosa* BIS11 and *Rhodotorula (Rhodosporidium) toruloides* BIS18, are known to convert hexoses, pentoses, organic acids and aromatic monomers into cell mass rich in lipids, carotenoids, terpenes and precursors of various bioproducts, such as bisabolene [247,248]. The aforementioned yeasts have been genetically modified and the derived strains present an enhanced metabolism and ability to

synthesize bioactive compounds, such as bisabolene, when grow on different ULH [109].

Finally, alternatively or in addition to genetic engineering, laboratory evolution strategies can be developed in order to enhance lipid accumulation ability of oleaginous microorganisms. An adaptive laboratory evolution strategy of *Yarrowia lipolytica* growing in alternative environments which promote growth and encourage the synthesis of storage lipids following by conditions that reward the high-energy containing cells, has been developed. The oleaginous lineages obtained give rise to populations capable of accumulating 30% w/w more lipids than the initial strain. Similar strategies could be used as a robust tool to generate tolerant strains able to grow on ULH and accumulate high amounts of lipids [20]. Independently of the approach used for improving productivity of oleaginous microorganisms, the environmental and economic viability of SCOs can be improved by adopting biorefinery approaches, as the exploitation and commercialization of the various by-products of the SCO production process, such as proteins, amino acids, carbohydrates, carotenoids, glycerol, organic acids, and alcohols [50,135,211,249-251] may be critical in determining the minimum selling price of microbial oil.

8. Outlook

The conversion of lignocellulosic biomass to SCO could be a promising technology, considering the new strategies related to the pretreatment of lignocellulosic biomass, as well as to the improvement of the productivity of oleaginous

microorganisms through genetic engineering in combination with adaptive laboratory evolution. Chemical pretreatments, such as acid, alkaline and acid/alkaline, have proven to be promising technologies for obtaining high yields of assimilable sugars after enzymatic hydrolysis. Steam explosion is considered as an effective, although energy consuming, strategy. Specifically, the acid treatments, especially those using diluted acids at temperature 121° C or higher, are the most popular, allowing after enzymatic hydrolysis a high recovery of pentoses and hexoses. Concerning the inhibition caused on the oleaginous microorganisms by the inhibitory compounds generated during pretreatments, future efforts should concentrate on the optimization of the pretreatment process, so as to reduce by-products and improve sugar yield, as well as to the identification of tolerant to inhibitors microorganisms and capable to efficiently consume lignocellulosic sugars. The application of genetic engineering and/or adaptive evolutionary techniques would greatly reduce limitations in lignocellulosic biomass valorization.

Technological advances in the conversion of lignocellulosic biomass into SCOs can promote sustainable production of SCOs to meet the needs of the population through the production of products such as food, biofuels and fine chemicals.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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945

Table 1. Glucose (Glc), hemicelluloses (H), lignin (L) and inhibitory by-products produced after pretreatments of various lignocellulosic biomasses, as well as biomass digestibility (expressed in Glc and H released) after enzymatic hydrolysis.

							After hydrolysis													After EH				
Reagent							Solid fraction (% w/w, 100g)				Liquid fraction (% w/w, 100g)				By-products (g/L)					Digestibility (%w/w)				
Pretr eatm ent	Substrate		% v/v	S:L ratio	T (°C)	t (min)	Total	Glc	H	L	Total	Glc	H	L	Furf ural	HM F	PC	For mic	Acet ic	Lev ulini c	G	H	Reference	
DA	Sugarcane bagasse	HCl	2.5	1:15	121	45					21	4.0	16		0.12	0.61							[118]	
DA	Defatted rice Bran	H ₂ SO ₄	3	1:8	90	360					50	43	7		0.03	0.3							[56]	
DA	Rice straw	H ₂ SO ₄	1	1:10	180	1		59	1.9	21		5	14		1.6	0.2			1.6		70		[205]	
DA	Rapeseed straw	H ₃ PO ₄	3	1:12	200	15	48	48	0	47		4	10		8.0	2.6		0.6	5.5		83		[252]	
DA	Corncob	H ₂ SO ₄	2.2		170	30	56	34	4.4	14											88		[253]	
DA	Rice straw	C ₂ H ₂ O ₄	5.0		136	31	60	24	22	5											43		[254]	
DA	Oil palm trunk	H ₂ SO ₄	3	1:5	180	40	47	52	ND	37											79		[255]	
DA	Sugar bagasse	C ₂ H ₂ O ₄	3.6	1:20	120	15			3.3			5	93	80							92	96	[256]	
DA	Jerusalem artichoke	H ₂ SO ₄	5	1:10	121	60	60	42	1.9	27		7	83		0.3	0.2	1.1	0.4	3.3		58		[257]	
DA	Jerusalem artichoke	HNO ₃	5	1:10	121	60	66	77	1.3	21		15	97		0.04	0.01	0.5	1.2	3.2		89		[257]	
DA	Cotton gin waste	C ₄ H ₄ O ₄	1.6	1:10	130	45	77	39	2.3	17		1.1	84	88	0.8	0.22	0.1		1.02		68		[258]	
DA	<i>Eucalyptus</i> sp.	H ₂ SO ₄	0.75	1:20	160	10			17	30		13	90		1.4	0.13			2.0		76		[259]	
DA	Poplar	H ₂ SO ₄	0.05		240	10		0		0		50		100									[191]	
DA	Pine	H ₂ SO ₄	0.05		240	10		0		65		70	95	30							70		[191]	
DA	Mixed softwood	C ₂ H ₂ (CO) ₂ O		1:4	180	30				47		16	19		0.9	2.4	5.3		2.3		57		[167]	
DA	Wheat straw	H ₂ SO ₄	2	1:10	121	60						14	82		0.44	0.05			4				[260]	
DA	Corn stover	H ₂ SO ₄	1	1:10	160	10									1.3	2.6	2.9		2.3				[73]	
DA	Wild rice grass	H ₂ SO ₄	2	1:10	121	60	85	38	6	36											45		[261]	
DA	Cassava residue	H ₂ SO ₄	0.01	1:20	180	20		55	17	18		7.6	39		0.05	0.02		0.76	0.44		70		[208]	
TSDA	Cassava residue	H ₂ SO ₄	0.05	1:20	190	10		60	6	21		2.5	58		0.12	0.02		0.13	0.18		73		[206]	
TSDA	<i>Populus tremula</i>	H ₂ SO ₄	65	1:15	35	180						36	19		0.5	0.04		2.7	1.9	1.6			[193]	
TSDA	<i>Pinus sylvestris</i>	H ₂ SO ₄	73	1:15	53	60						44	17		0.2	0.05		6.8	3.5	1.9			[193]	

TSDA	<i>Pinus sp</i>	HCl	3	1:10	65/ 80	108/ 240		38	14	42		38	54						[196]		
DDA	Corn stover	H ₂ SO ₄	2.5	2:1	185	1440		39	21								85		[192]		
Alk	Corn stover	NaOH	2	1:10	121	20								6.4	5.3				[73]		
Alk	Corn stover	NaOH	5	1:10	60	1440	74	28	7.6	3.3		19	65	81			99		[203]		
Alk	Poplar	NaOH	5	1:10	120	1440	88	42	8.1	23		5	46	21			80		[203]		
Alk	Japanese silvergrass	Ca(OH) ₂	10	1:10	25	8 W	72	98	37	77	28	2.4	63	23			60	50	[262]		
Alk	Japanese silvergrass	NH ₃	3	1:10	25	8 W	71	93	53	90	29	6.1	47	9.8			45	10	[262]		
Alk	Napiergrass	Ca(OH) ₂	10	1:10	25	8 W	68	92	32	86	32	8	68	2.8			65	45	[262]		
Alk	Napiergrass	NH ₃	3	1:10	25	8 W	65	91	55	90	35	9	45	10			70	30	[262]		
Alk	Rice straw	Ca(OH) ₂	10	1:10	25	8 W	70	96	30	49	31	4.2	71	51			45	40	[262]		
Alk	Rice straw	NH ₃	3	1:10	25	8 W	66	92	55	54	34	8	45	46			50	10	[262]		
Alk	Hardwoods	NH ₄			140	60	95										100	98	[263]		
A/A	corn stover	HCl/NH ₃	1/13	1:10	120/ 130	40/ 40	42	85	-	14		1	83			0.9	72		[264]		
A/A	Corn stover	HCl/ Ca(OH) ₂	1/0. 1	1:10	120/ 60	40/ 12h	55	92	6	75		8	92	25			78	97	[265]		
A/A	Corncoobs	H ₂ SO ₄ / NaOH	1	1:10	120/ 60	60/ 120	62	75	8	3.2		4	89	88			93		[266]		
A/A	Corn stover	H ₂ SO ₄ / NaOH	0.5/ 2	1:10	180/ 80	1/ 60	62	83	4	5.4		14	71	89	0.9	ND	2.8	98	76	[199]	
SE	Sugarcane bagasse	H ₂ O		1:10	121	120						61							[48]		
SE	rice husk	H ₂ O		1:10	121	120						63							[48]		
SE	<i>Eucalyptus globulus</i>	H ₂ O	-	8:1	200	30	69	37	ND	62					1.3	2.2	0.6	2.4	73	[189]	
SE	<i>Pinus radiata</i>	H ₂ O	-	10:1	200	90	67	50	0.7	47					0.9	2.0	0.4	0.8	10	[189]	
OS	Palm fronds	Ethanol/ H ₂ SO ₄	60/ 1.5	1:10	200	60	85	90	30	57		5	70	43			0.7	4	95	78	[267]
OS	Prairie cordgrass	Ethyl acetat-	37-	1:10	140	20								51		4.0				[267]	
OS	Switchgrass	ethanol- H ₂ O-	25- 38-	1:10	140	20								59		6.0				[267]	
OS	Corn stover	H ₂ SO ₄	0.4	1:10	140	20								68		2.5				[267]	
OS	Yellow poplar	Ethanol/ H ₂ SO ₄	50/ 1	1:10	140	10	61	46		13		7.7		39	0.04	0.06		2.4		[201]	
OS	Yellow poplar	Ethanol/ NaOH	50/ 1	1:10	140	10	73	59		16		0.3		27	<0.0 1	0		4.6		[201]	

Abbreviations: DA, dilute acid; TSDA, two-step dilute acid; DDA, dry dilute acid, Alk, alkaline; A/A, acid/alkaline; SE, steam explosion; OS, organosolv; S:L, solid – liquid ratio; W, weeks; T, temperature; t, time; G, glucose o glucan; H, hemicelluloses; L, lignin; EH, enzymatic hydrolysis; PC phenyl compounds.

Table 2 Features of different pretreatments utilized to improve the efficacy of conventional pretreatment (acid, alkaline, acid/alkaline, steam explosion and organosolv).

Pretreatment	Advantage	Disadvantages	Action mechanism	Work condition	References
Ionic liquids (IL)	Applied with alkaline pretreatment Environmentally friendly Decreases crystallinity and increases porosity Up to 90% assimilable sugars are obtained after enzymatic hydrolysis	Expensive liquids Residual IL interfere with enzymatic hydrolysis	Cleavage of the β -O-4 bonds in lignin followed by dipole-ion formation. Cellulose is destabilized, and hemicelluloses are dissolved. IL are composed by organic cations and small inorganic or organic anions, linked by a strong ionic bond. Commonly IL used are imidazonium salts, AMIMCl (1-Allyl-3-methylimidazonium chloride) and BMIMCl (1-butyl-3-methylimidazolium chloride)	80-160° C 3-50 % solid 30min-8h 60-80 % w/w	[13,165,185,189,202,220]
AFEX	Partial disruption of the fibers leaving short cellulose chains and disrupt lignin Solid 99% recovered Low inhibitor concentration Removes acetyl groups by deacetylation Herbaceous biomass and agricultural residues are high susceptible Lignin removed > 85% Up to 95% assimilable sugars are obtained after enzymatic hydrolysis	Hardwood low susceptible Not suitable for softwoods The dosage of liquid ammonia is 1-2 kg of ammonia/kg of dry biomass, which increases the costs Residual lignin generates unspecific bonds in the enzymatic hydrolysis	Alkaline reagent is impregnated into the biomass, pressure is applied, and it quickly depressurizes Anhydrous liquid or gaseous ammonia	60-200° C 10-50 % solid 5-60 min >100 % w/w	[13,71,165,185,188,195,268]
Ammonia recycled percolation (ARP) and Soaking in aqueous ammonia (SAA)	Significant degree of delignification in hardwood and herbaceous woods Solids 99% recovered Used to preserve most of the glucan and xylan	High cost due to the solvent	Solubilization of hemicelluloses and lignin	140-210° C 10-90 min 5-15 % w/w	[184,188,195]
CO ₂ explosion	Efficient to removing lignin in hard and softwoods and to dissolving cellulose and hemicelluloses No inhibitory compounds have been reported Low-cost pretreatment Acceptable environmental impact More cost-effective treatment than AFEX and less toxic than steam explosion	Lower yield than steam and AFEX explosion	Supercritical fluid, reacting with the moisture in the substrate to form carbonic acid that contributes to the degradation of the biomass	31-250° C 20-60 min 5-15 % w/w	[71,185,186,195]
Hot water	Reduces the size of particles Effective for solubilizing hemicelluloses as oligomers not require catalysts, chemical products or corrosion-resistant materials Lignin removed > 73% Up to 95% assimilable sugars are obtained after enzymatic hydrolysis Inhibitor compounds in low concentrations compared to acid treatments.	Inhibitors can be produced requires a high demand for water and energy	Consists in cooking the lignocellulosic biomass in water at high temperature and pressure	121-240° C 10-20 % solid 4-60 min	[12,71,185,269,270]

Oxidative (Wet oxidation)	Used with alkaline solution (NaOH) reducing inhibiting products Combination with stem exploitation the conversion of cellulose and hemicelluloses is increased Removes hemicelluloses and lignin (between 50-70%). Xylan from hardwoods and herbaceous are affected Lignin removed > 60% Up to 95% assimilable sugars are obtained after enzymatic hydrolysis	Mannans from softwoods are low affected Cellulose is not affected Possibility of non-selective oxidation causing loss of hemicelluloses and cellulose components Large amount of acids and chemical compounds are generated High temperatures and pressure and oxidizing agents are costly	When the biomass is suspended in water, the oxide agents produce electrophilic substitution chain reactions that divide the aromatic lignin nuclei or the bonds between the alkyl and aryl groups Mainly degrades lignin by attacking aromatic ring. Oxide agents such as oxygen (O ₂), hydrogen peroxide (H ₂ O ₂) or peracetic acid, ozone (O ₃)	25-195° C 10-20 min 1-2% w/v	[71,185,264]
Microwave pretreatment	Applied to acids and alkaline and steam exploitation Low cost Short reaction times Change ultra-structure of cellulose by degrading lignin and hemicelluloses Homogeneous heating of the reaction mixture Improve the recovery yields of glucose, xylose, and total sugar by 13-27%, 17-25%, and 20-21%, respectively	Increase the formation of inhibitors	Consists in radiating energy that accelerates the molecules, which begin to friction each other and quickly increasing the medium temperature generating physical, chemical, or biological reactions	150-180° C 3 min 1-2% w/v	[143,189,271]

Table 3. Inhibition of growth and lipid production by oleaginous microorganisms due to the inhibitors generated during the pretreatment of lignocellulosic biomass.

Microorganism	Furan compounds						Phenol compounds						Weak acids						Ref						
	Furfural			5-HMF			Vanillin			Syringaldehyde			4-HB			Formic				Acetic			Levulinic		
	g/L	% RIE (w/w)		g/L	% RIE (w/w)		g/L	% RIE (w/w)		g/L	% RIE (w/w)		g/L	% RIE (w/w)		g/L	% RIE (w/w)			g/L	% RIE (w/w)		g/L	% RIE (w/w)	
<i>C. curvatus</i>	1	-	62	3	-	7.9	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	[260]
<i>T. dermatis</i>	4	-	59	2	-	22	1.2	71	80	1	88	98	1.5	100	100	4	100	-	>9	30	57	10	27	54	[73]
<i>T. cutaneum</i>	1	40	30	2	NH	NH	2	26	21	-	-	-	1.5	42	38	5	38	7	5	25	59	10	NH	NH	[214]
<i>R. toruloides</i>	-	-	-	-	-	-	2	100	-	2.2	16	-	1.2	100	-	4	40	-	-	-	-	-	-	-	[272]
<i>R. toruloides</i>	>1	50	-	-	-	-	>2	50	-	-	-	-	-	-	-	4	50	-	15	50	-	-	-	-	[208]
<i>L. starkeyi</i>	1.4	100	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	3.9	100	-	-	-	-	[273]
<i>T. cutaneum</i>	0.5	65	91	5	35	25	2	40	40	2.5	20	20	2	50	50	6	18	26	25	50	34	10	50	50	[146]
<i>T. mycotoxinivorans</i>	1	47	-	2.5	15	-	-	-	-	-	-	-	-	-	-	-	-	-	2	0	-	-	-	-	[50]
<i>R. fluviale</i>	0.3	75	87	2	75	0	0.5	92	0	-	-	-	-	-	-	0.5	100	100	1	72	97	-	-	-	[104]

Abbreviations: % RIE, reduction due to the inhibitory in respect to yields observed in cultures without inhibitors; S, substrate; X, biomass, L, lipids

Table 4. Growth and lipid production by oleaginous microorganisms cultivated in lignocellulosic hydrolysates.

Microorganism	Strain	biomass	pretreatment	System		ULH/DLH	S(g/L)	X (g/L)	L %(w/w)	L (g/L)	L (g/g)	Reference
<i>Trichosporon dematis</i>	CH007	corncob	DA	batch	flask	DLH	42	17	40	7	0.16	[274]
<i>Cryptococcus curvatus</i>	ATCC 20509	Wheat straw	DA	batch		ULH	29	17	34	5.8		[260]
<i>Cryptococcus curvatus</i>	ATCC 20509	Wheat straw	DA	batch		DLH	21	16	27	4.2		[260]
<i>Lipomyces starkeyi</i>	ATCC 12659	Wheat straw	DA	batch		ULH	29	15	31	4.6		[260]
<i>Lipomyces starkeyi</i>	ATCC 12659	Wheat straw	DA	batch		DLH	21	13	29	3.7		[260]
<i>Rhodospiridium toruloides</i>	ATCC 10788	Wheat straw	DA	batch		DLH	21	9.9	25	2.4		[260]
<i>Rhodotorula glutinis</i>	ATCC 204091	Wheat straw	DA	batch		ULH	29	14	25	3.5		[260]
<i>Rhodotorula glutinis</i>	ATCC 204091	Wheat straw	DA	batch		DLH	21	12	21	2.4		[260]
<i>Trichosporon dematis</i>	32903	Corncob	DA	batch		ULH	71		24	7.5	0.1	[73]
<i>Trichosporon dematis</i>	32903	Corncob	DA	batch		DLH	73		45	11	0.16	[73]
<i>Cryptococcus</i> sp.	SM5S05	Corncob	DA	batch	flask	ULH	40	13	60	7.6	0.13	[275]
<i>Trichosporon cutaneum</i>	Ch002	Corncob	DA	batch	flask	DLH	46	22	36	7.9		[276]
<i>M. isabellina</i>	ATHUM 2935	Rice hull	DA	batch	flask	ULH	26	5.6	64	3.6	0.21	[69]
<i>Trichosporon cutaneum</i>	ACCC 20271	Corncob	DA	batch	flask	ULH	49	38	32	12	0.1	[277]
<i>Cryptococcus curvatus</i>	ATCC 20509	Corn stover	DA	batch	flask	ULH	53	11	61	6.9		[243]
<i>Trichosporon cutaneum</i>	AS 2.571	Corn stover	DA	batch	Bior 3L	DLH	60	19	39	7.6	0.15	[110]
<i>Trichosporon dematis</i>	CH007	Corncob	DA	batch	flask	ULH	60	24	40	9.8	0.16	[278]
<i>Trichosporon fermentans</i>	CICC 1368	Rice straw	DA	batch	flask	DLH	35	29	40	12		[207]
<i>Umbelopsis (Mortierella) isabellina</i>	ATCC42613	Corn stover	DA	batch	flask	ULH	31	14	34	4.8		[38]
<i>Lipomyces tetrasporus</i>	NRRL Y-11562	Cornstover	DA	batch	flask	ULH	123	54	53	29	0.15	[40]
<i>Lipomyces kononenkoae</i>	NRRL Y-7042	Cornstover	DA	batch	flask	ULH	123	48	59	28	0.22	[40]
<i>Rhodospiridium toruloides</i>	NRRL Y-1091	Cornstover	DA	batch	flask	ULH	123	43	61	26	0.19	[40]
<i>Yarrowia lipolytica</i>	Po1g	Sugarcane bagasse	DA	batch	flask	DLH	21	11	59	6.7		[118]
<i>Yarrowia lipolytica</i>	Po1g	Rice bran	DA	batch	flask	DLH	30	11	48	5.2		[56]

<i>Trichosporon cutaneum</i>	ATCC 20271	Corn stover	DA	batch	Bior 20L	DLH	73-130			46-8.1		[146]
<i>Rhodospiridiobolus fluvialis</i>	DMKU-SP314	Sugar cane	DA/OX	batch	flask	ULH	36	21	67	14		[113]
<i>Rhodospiridiobolus fluvialis</i>	DMKU-SP314	Sugar cane	DA/OX	batch	Bior 2L	ULH	36	24	75	18		[113]
<i>Mortierella isabellina</i>	ATCC42613	Corn stover	Alk	batch	flask	ULH	30	11	29	2.5		[38]
<i>Trichosporon mycotoxinivorans</i>	S 2	Paddy straw	Alk			ULH	35	14	35	7.3		[50]
<i>Rhodosporidium paludigenum</i>	KM281510	Corn cob	Alk	batch	flask	ULH	100	23	70	16		[47]
<i>Rhodosporidium paludigenum</i>	KM281510	Corn cob	Alk	batch	Bior 3L	ULH	100	28	70	20	0.21	[47]
<i>Rhodosporidium paludigenum</i>	KM281510	Corn cob	Alk	fed batch	Bior 3L	ULH	100	36	70	25	0.28	[47]
<i>Trichosporon dematis</i>	32903	Corn cob	Alk	batch		ULH	67		28	6.8	0.1	[73]
<i>Trichosporon dematis</i>	32903	Corn cob	Alk	batch		DLH	131		56	20	0.19	[73]
<i>Rhodococcus toruloides</i>	DSMZ 4444	Corn stover	A/A	batch		ULH	110	36	59		0.19	[279]
<i>Rhodococcus toruloides</i>	DSMZ 4445	Corn stover	A/A	Fed batch		ULH	110	54	59		0.29	[279]
<i>Rhodotorula glutinis</i>	CGMCC 2.703	Corn cob	A/A	batch	Bior 5L	ULH	42	15	36	5.5	0.13	[280]
<i>Rhodotorula glutinis</i>	CGMCC 2.703	Corn cob	A/A	fed batch	Bior 5L	ULH	42	75	47	34	0.15	[280]
<i>Meyerozyma guilliermondii</i>	G5-MK414782	Sugarcane bagasse	SE	batch		ULH	60	6.1	38	2.3	0.05	[48]
<i>Meyerozyma guilliermondii</i>	G5-MK414782	Rice husk	SE	batch		ULH	60	6.5	37	2.4	0.04	[48]
<i>Pichia kudriavzevii</i>	G9-MH000699	Sugarcane bagasse	SE	batch		ULH	20	6.2	31	1.9	0.1	[48]
<i>Pichia kudriavzevii</i>	G9-MH000699	Rice husk	SE	batch		ULH	20	8.2	24	1.9	0.1	[48]
<i>Pichia manshurica</i>	G10-MH279643	Sugarcane bagasse	SE	batch		ULH	20	8.2	24	1.9	0.09	[48]

<i>Pichia manshurica</i>	G10-MH279643	Rice husk	SE	batch	ULH	21	6.5	28	1.8	0.09	[48]
<i>Pichia kudriavzevii</i>	SY2-MF926445	Sugarcane bagasse	SE	batch	ULH	60	6.1	30	1.9	0.04	[48]
<i>Pichia kudriavzevii</i>	SY2-MF926445	Rice husk	SE	batch	ULH	51	8.4	29	2.4	0.04	[48]
<i>Candida albicans</i>	SY3-MG996750	Sugarcane bagasse	SE	batch	ULH	20	6.2	31	1.9	0.1	[48]
<i>Candida albicans</i>	SY3-MG996750	Rice husk	SE	batch	ULH	21	8.3	22	1.8	0.09	[48]
<i>Rhodotorula mucilaginosa</i>	SY4-MH279637	Sugarcane bagasse	SE	batch	ULH	20	6.7	30	2	0.1	[48]
<i>Rhodotorula mucilaginosa</i>	SY4-MH279637	Rice husk	SE	batch	ULH	20	8	24	2	0.1	[48]
<i>Rhodococcus opacus</i>	DSM 1069	Loblolly pine	OS	batch	flask			27			[281]

Abbreviations: DA, dilute acid; Alk, alkaline; A/A, acid/alkaline; SE, steam explosion; OX, oxidative; OS, organosolv; S, substrate; X, biomass; L, lipids; ULH, undetoxified lignocellulosic hydrolysates; DLH, detoxified lignocellulosic hydrolysates; Bior, Bioreactor

Fig. 1 Lipid droplets within of yeasts and a filamentous fungi cell. The images above present the lipids as shown through fluorescent filter after Nile red staining of A) *M. guilliermondii*, B) *S. coipomensis*, C) *Mortierella isabellina*, D) *Yarrowia lipolytica* visualized under light microscope (400×). The images below (E, F, G, H) are the same as above respectively, without the fluorescence filter.

Fig. 2 Conceptual scheme of lignocellulosic hydrolysates conversion into SCO.

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Fig. 1

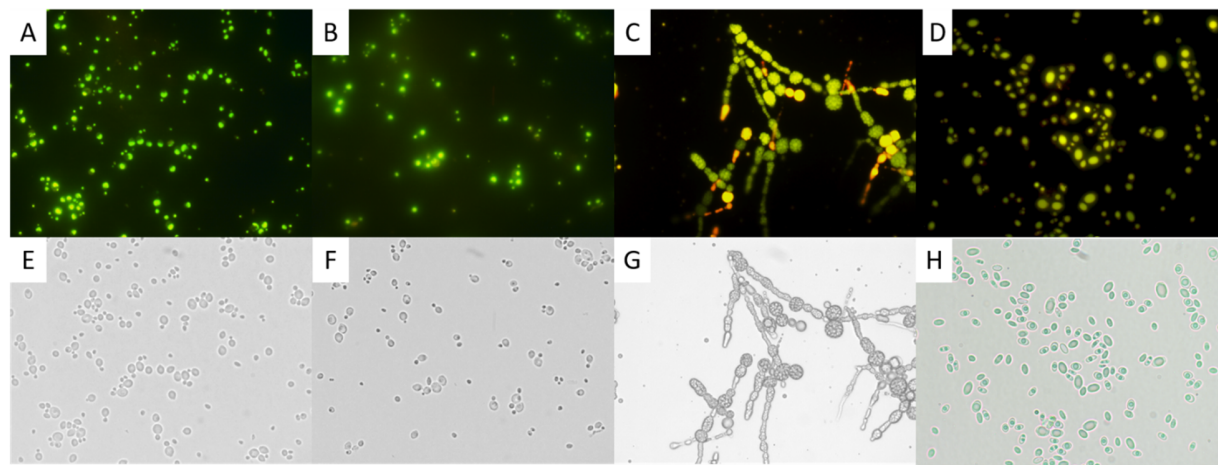


Fig. 2

