

Determination of Size Distribution of Precipitation Aggregates Using Non-Invasive Microscopy and Semiautomated Image Processing and Analysis

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Abstract

Precipitation processes are technologies commonly used in hydrometallurgical plants to recover metals or to treat wastewaters. Moreover, solid-liquid separation technologies, such as thickening or filtering, are relevant unit operations, included in the precipitation technologies. These methods are strongly dependent on the characteristics of the solid precipitates formed during the specific precipitation reaction. One of these characteristics is the particle size distribution (PSD) of the solid precipitates which are fed into a solid-liquid separation process. Therefore, PSD determination is a typical practice for the characterization of the slurries generated in a precipitation plant. Furthermore, the precipitates generated in these processes have a colloidal or aggregation behavior, depending on the operational conditions. Nevertheless, the conventional methods used to estimate PSD (e.g., laser diffraction and/or cicloizer) have not been designed to measure particles that tend to aggregate or disaggregate, since they include external forces (e.g., centrifugal, agitation, pumping and sonication). These forces affect the true size of the aggregates formed in a unit operation, thereby losing representativity in terms of aggregates particle size. This study presents an alternative method of measuring the size distribution of particles with aggregation behavior, particularly, by using non-invasive microscopy and image processing and analysis. The samples used have been obtained from an experimental precipitation process by applying sulfidization to treat the cyanide-copper complexes contained in a cyanidation solution. This method has been validated with statistical tools and compared with a conventional analysis based on laser diffraction. Our results show significant differences between the methods analyzed, demonstrating that image processing and analysis by microscopy is an excellent and non-invasive alternative to obtaining size distribution of aggregates in precipitation processes.

Keywords: SART process; precipitation aggregates; image analysis; microscopy; particle size distribution

1. Introduction

1.1 Background

The precipitation process is one of the technological options available for treating solutions in hydrometallurgical plants, with the purpose of recovering or removing metals, among others compounds [1]. Typical applications are found in gold cementation, using zinc powder [2]; copper cementation, using scrap iron [1]; acid mine drainage (AMD) treatment, using milk of lime [3]; copper sulfide precipitation from acid mine drainage, using hydrogen sulfide [4]; and copper sulfide precipitation from cyanide solutions in gold mining [5]. These processes must accommodate a subsequent solid-liquid separation stage (i.e., thickeners and/or filters) to remove the solids generated from the solution. The characteristics of these precipitates (colloidal behavior and fine particles) determine the thickeners, large filter size, and rigorous operational control required in order to prevent a high content of suspended solids in the recovered solutions [6-9]. Particularly, the copper sulfide precipitation process from acid mine drainage and cyanide solutions is very attractive, owing to its capacity to recover valuable by-products from wastewaters (in the case of AMD) and gold mining (in the case of cyanide solutions). An appropriate characterization of the precipitate size is crucial for the selection and design of an adequate separation process. In this context, there are some studies that characterize the precipitates formed in sulfidization processes for treating AMD [6,7] and cyanide solutions [9]. These studies determined the aggregate characteristics from metal sulfide precipitates and the dependence of pH and sulfide dosage (chemical solution characteristics) on aggregate size. Thus, settling rate results determined

by operational conditions related to pH and sulfide dosage. These results indicate the relevance of the aggregate size to operational conditions when operating and designing solid-liquid separation equipment. For this reason, the experimental technique used to quantify particle size and particle size distribution could play a critical role in the interpretation of data, which may underestimate or overestimate set-points for chosen operational conditions when operating solid-liquid separation equipment. Unfortunately, the methodologies currently used to measure particle size and particle size distribution (PSD) of fine particles (0.1 - 100 μm), such as Malvern Mastersizer (MMS) or cyclosizer (CS), have been designed to quantify PSD, but not to measure aggregate size distribution (ASD). This quantification is crucial when defining optimal operational conditions for thickening process. The two methods mentioned above (MMS and CS) involve external forces (e.g., agitation, pumping and centrifugal in the case of CS) which can affect the physical integrity of the aggregates, and consequently alter their size distribution. A previous study shows the impact of CS on the mineral's surface, owing to the external forces applied to separate particles of different sizes [10]. However, the Focused Beam Reflectance Measurement (FBRM) allows the aggregate size distribution to be determined, although this technique is still very expensive for experimental and research purposes. Hence, it is necessary to quantify the ASD using non-invasive and less expensive techniques than FBRM. In this context, this study proposes a new non-invasive method to quantify size distribution of aggregates using microscopy and semiautomated image processing and analysis.

1.2 Particle size distribution using microscopy and image processing and analysis

The measurement of particle or aggregate size distribution is not a simple task, because it depends on a series of factors which affect the measurement. As mentioned above, these

factors include the heterogeneity of the sample itself as well as the strategy employed to make the results representative of the sample's characteristics. In this regard, microscopy is a technique that has not only been used as a powerful tool when morphological information is required to understand the behavior of a material (such as civil engineering materials) [11,12] or in the electronics industry [13], but also to quantify the particle size distribution successfully in various fields, such as food, pharmaceuticals, and mineral processing. For example, microscopy has been employed to quantify microstructures and correlate them with rheological properties in apple tissue [14]. Also, microscopy has been applied to determine the bubble size distribution in aerated whey protein gels [15]. Moreover, successful applications have also been reported regarding the measurement of soil grain-size distribution, in which no significant differences were found in comparison with the traditional mechanical (sieve) analysis [11,16] or the use of reflected light microscopy (RLM) for the recognition of hematite grains in materials engineering [17]. In addition, interesting applications have been reported in batch solution crystallization processes, where images captured by microscopy enabled the estimation of the time-varying particle size distribution of particles in suspension, through crystallization experiments [18]. After using image processing and analysis, it was also possible to determine simultaneous occurrence of particulate events such as nucleation, breakage, and aggregation, in order to monitor and control the properties of crystalline products [18]. In this sense, the application of confocal microscopy and multiple sensors for dynamic measurements of crystal properties, such as size, shape, and polymorph, allows relevant attributes to be determined, related not only to downstream processes (filtration, washing, granulation, drying, grinding, transportation, storage, and tableting), but also to end-use properties, such as bulk density, mechanical strength of a tablet, catalytic activity, stability, wettability, and flowability [19].

Consequently, the application of image processing and analysis for aggregate size and shape determinations could be beneficial for the mining , comminution, and materials handling industries. In particular, the efficiency of these technologies is located in their capacity to make measurements without disrupting production streams, as traditional sieving methods do. Additionally, measurements can be made in real time, so that appropriate adjustments to the comminution and screening processes can be made in real time, before large quantities of out-of-specification materials are produced [20].

Among the advantages of microscopy over other techniques, is the fact that it is less expensive than the others – in terms of capital costs -and in particular the fact that it makes the particle size and shape visible, without any intervention during the analysis. Its disadvantages, however, mainly relate to the reliability of its measurements, that is, for selecting the representative number of particles measured [14,21,22]. Furthermore, in some cases it is difficult to determine whether two or more particles are “touching” or if they are permanently stuck together and, therefore, must be considered to be one bigger particle [19].

In addition, some authors emphasize that the sampling preparation, acquisition, and nature of images, image processing, such as linear filters, rank filters, and morphological filters, play a key role [12]. All of the considerations mentioned are essential in the variability of the measurement. However, there are several statistical tools that one may use to address the disadvantages mentioned above and to validate that the microscopic measurement is representative. In this regard, analysis of the variability between the images per sample and between samples will allow it to be determined whether there are significant differences between the distribution of particles or aggregates size that were measured. Depending on the data distribution (normal distribution or not), parametric and non-parametric statistics can be used to compare the population group (data within images or between images).

The aim of this study was to apply a non-invasive method to quantify the size distribution of aggregates using optical microscopy and semiautomated image processing and analysis. This valuable information can be a useful tool for measuring, in a more realistic manner, the aggregate size distribution and the critical parameter when designing optimal operational conditions for the solid-liquid separation processes.

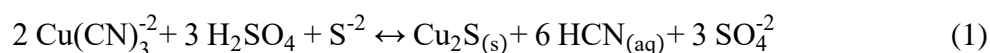
2. Methodology

2.1 Reagents

The reagents used in this study (NaCN, CuCN, NaHS, NaOH, and H₂SO₄) were analytical grade chemicals obtained from Merck and Sigma Aldrich. All solutions were made using demineralized water (<1 µS). The pH electrode (Methrom, Model 913) was calibrated using pH buffer solutions (Hanna).

2.2 Generation of precipitation aggregates

The precipitation aggregates generated were sulfide copper, which was produced from synthetic cyanide solutions, simulating the typical operational conditions of the SART (Sulfidization, Acidification, Recycling, and Thickening) process. This technology has been designed to recover copper and cyanide from cyanide solutions in gold mining [5,23], according to the following general chemical reaction:



The synthetic cyanide solution was made by mixing NaCN, CuCN, and NaOH to adjust the pH value at 12, avoiding HCN volatilization. The copper and total cyanide concentration were fixed at 1800 mg/L and 2460 mg/L, respectively. The copper concentration was chosen

based on the copper concentrations found in gold mining, which have high cyanide-soluble copper content in the ore [5,24-26]. Moreover, the cyanide concentration was defined according to the cyanide associated to copper, in order to keep a free cyanide concentration of 100 mg/L; a typical value set in gold mining operations to ensure gold dissolution [2,27]. This value was estimated from the thermodynamic equilibrium of the copper-cyanide complexes by using the software Hydra/Medusa from the KTH Royal Institute of Sweden [28]. The sulfidization reaction (Equation 1) was carried out in a glass reactor of 650 mL capacity over a period of 15 minutes, setting the pH at 4.0 and sulfide dosage at 120% stoichiometric, using 1 M sulfuric acid and NaHS dosage, respectively. These conditions were selected with the aim of ensuring the maximum precipitate generation according to literature [5].

2.2 Size distribution analysis techniques

2.2.1 Laser diffraction analysis

A 600 mL sample of a suspension which resulted from the sulfide precipitation was analyzed by the laser diffraction technique, using a Malvern Mastersizer 2000 (MM2000). The aim was to measure the particle size distribution (PSD) of the suspended solids (i.e., copper sulfide precipitates). The Mastersizer equipment uses an agitated tank which operates at 1000 rpm. The sample is recirculated by a centrifugal pump (2500 rpm), in order to keep the solids suspended and homogenized in the suspension. Additionally, the supplier of the Mastersizer 2000 (MM2000) recommends the use of an additional pre-treatment of ultrasound at 20 KHz during 1 minute, during which suspended particles form aggregates [29].

2.2.2 Microscopy and semiautomated image processing and analysis

The particle size distribution (PSD) of aggregates was measured using an optical microscope (Leica DM 750) connected to a digital camera HD 5 MGPXL WI-FI (Leica ICC50W), which captured the images. The size distribution estimate was determined using two software for image processing. The Leica Application Suite V4 12 was used to measure the equivalent diameter of the aggregates up to 320 μm , whereas aggregates with an equivalent diameter larger than 320 μm were analyzed using the software Image Pro Plus 6. After these analyses, the complete PSD was estimated by mixing the distribution curves obtained from both software. The image-processing and analysis was carried out using two software, in order to ensure the precision of the measurements in a wide range of diameter sizes.

It is crucial that samples are representative, in order to give reliable information for process-control purposes. Taking this issue into account and adding the fact that copper sulfide precipitates tend to form aggregates rapidly, the suspension sampling and the image-capture must be carried out in a short time span. Hence, when the sulfidization reaction was completed (after 15 min), the suspension sampling and image-capture were performed in a maximum time period of two minutes. Samples were taken at the same level of the agitated reactor, using a siringe connected to a 7 mm tubing to avoid the destruction of aggregates. In this time, it was possible to capture nine images (M1 to M9 images), which were obtained from 70 μL of suspension collected from the reactor. These samples were placed on three zones of the microscope slide in order to be analyzed by the optical microscope.

2.3 Measurement of copper content in the sulfide precipitate

The copper sulfide precipitate obtained during the sulfidization reaction was characterized by a scan by an electron microscope coupled with an energy-dispersive X-ray (SEM-EDX),

JEOL model IT300 LV. With this analysis, the copper content in the precipitate generated was quantified.

2.4 Copper sulfide conversion

A sample of the suspension was taken from the sulfidization reactor during each 15-min reaction interval. This sample was filtered using a syringe filter of 0.22 μm pore size. The solution collected was neutralized at pH 12 with a 1M NaOH solution. The dissolved copper was measured using an atomic absorption spectrometer (AAS), GBC model SensAA dual. The copper concentration measured in the sample was used to estimate the conversion of sulfide copper precipitate (copper recovery), considering the initial copper concentration in the cyanide solution. Moreover, the total suspended solids (TSS) was estimated using the following equation.

$$\text{TSS} = \frac{\text{Initial copper concentration} \times \text{Copper conversion}}{\text{Copper content}} \quad (2)$$

2.5 Statistical analysis

For the PSD estimation, data obtained from images captured using optical microscopy (MC) comprised nine images (M1...M9), from which 192 objects were randomly chosen (particles were measured by a proper methodology according to their size, as previously described). Furthermore, the PSD measurements made using the laser diffraction technique (MM2000) were divided into two groups: (i) samples without pre-treatment (MS1) and (ii) samples pre-treated by the use of sonication (MS2). Thus, 556 and 377 objects formed the population of MS1 and MS2, respectively. Then, the first step was to analyze the data distribution (test normal distribution) for the PSD obtained by optical microscopy and laser diffraction technique, for the samples with and without pre-treatment. The exploratory data analysis,

which determines whether the data has a normal distribution, is crucial for adequately selecting the parametric or non-parametric statistics. This is because many statistical procedures, including correlation, regression, t test and the analysis of variance ANOVA (parametric tests), are based on the assumption that the data follows a normal distribution. In the case of abnormally distributed data, the use of parametric statistics does not allow accurate and reliable conclusions to be drawn [30]. In this regard, the normality was evaluated by two common and robust non-parametric statistics for this purpose:: modified Kolmogorov-Smirnov (K-S) and Shapiro-Wilk (S-W). After determining the data distribution, multiple comparison tests were conducted in order to determine whether there were significant differences between the data obtained by optical microscopy and those obtained by the laser diffraction technique for PSD. From a statistical point of view, these are crucial for guaranteeing that optical microscopy can be used as a valid technique for PSD analysis. In the case of images obtained by microscopy (M1...M9), the comparison was carried out by the analysis of variance ANOVA (parametric test) and Kruskal Wallis, which is the equivalent non-parametric statistic for one-way ANOVA [31]. In cases where ANOVA and Kruskal Wallis reject the null hypothesis, this means that there are significant differences between the PSD on the microscopy images. It is then necessary to perform additional analysis (post-hoc test) to clarify the differences between particular pairs of experimental groups. Tukey's HSD (honestly significant difference) procedure was used as a post-hoc test because it allows multiple comparisons of the mean to be performed, in order to evaluate whether there are significant differences between the means at 95% of confidence level. The same procedure was performed for the data comparison between microscopy and laser diffraction technique, with and without pre-treatment as well as for the validation test using non-agglomerated material as CuCN.

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261 ***2.6 Validation of method using an unbiased sample***

262 Considering the aggregation behavior of copper precipitates and the effect of time
263 measurement on the PSD, a validation procedure was performed, in order to estimate the
264 error of the method proposed in this study with respect to the MM2000, using an unbiased
265 sample. For this purpose, a sample of an insoluble salt in water without aggregation behavior
266 (CuCN, the same used for synthetic solutions) was used to validate the measure of PSD by
267 microscopy. In this sense, a suspension of 1 g/L of CuCN was prepared using demineralized
268 water. The method of data acquisition by microscopy employed was the same as the method
269 described in section 2.2.2. The statistical procedure employed was the same as the procedure
270 described in section 2.5.

271

272 **3. Results and discussion**273 ***3.1 Generation of precipitation aggregates***

274 The results of the reaction conversion and the copper content obtained from the sulfidization
275 reaction are shown in Table 1. A maximum precipitate generation of 99.97% was reached for
276 the operational conditions assessed, and it was possible to obtain a precipitate quality with
277 67.69 % w/w of copper content, as found in other SART studies or industrial plants [5]. After
278 determining the copper content and conversion, this data was used to estimate the TSS
279 generated in the reaction, which reached a value of 2,658 mg/L.

280

281 ***3.2 Size distribution analysis***

282 From the distribution curves, the particle size was estimated at 50% distribution (P50) and
283 90% (P90) for all conditions studied (see Table 2). Size data were obtained by laser

diffraction using the MM2000 for samples with and without pre-treatment, and by image processing and analysis obtained from samples studied by optical microscopy. The samples pre-treated with sonication (20 kHz), as suggested by the supplier, showed the lowest particle sizes prior to particle size measurement using the MM2000 (6.9 and 17.4 μm for P50 and P90, respectively), in comparison with the samples analyzed by optical microscopy (119 and 307 μm , respectively) and the samples analyzed by laser diffraction without sonication (25.7 and 59.6 μm , respectively). It is important to mention that the use of sonication is indeed a pre-treatment, as recommended by the supplier. This pre-treatment is carried out with the aim of ensuring good particle size measurements, thereby avoiding aggregation effects in the results. However, the differences observed in the values of particle sizes among the three methods can be explained by the influence of external forces on the samples prior to measuring the particle size, particularly in both cases of MM2000 (agitation, pumping, and sonication). In fact, the sonicated samples presented smaller particle sizes due to disaggregation effects promoted by the sonication, generating fine particles. This methodology can be useful as an informative backup. However, it can yield impractical results for equipment design and process control purposes, since the particles with aggregation behavior will form new aggregates when sonication or other external forces (agitation, pumping) are stopped. Therefore, the results obtained from image analysis captured by optical microscopy are non-invasive. These results can thereby determine more realistic particle sizes of the aggregates. Thus, the P50 size determined by microscopy is around 17 times higher than the MM2000 analysis with pre-treatment, and almost 5 times higher than the MM2000 results without pre-treatment. Figure 1 shows the cumulative size distribution curves obtained with the three methods (MC, MS1 And MS2), where the size distribution resulting from image analysis obtained by microscopy reached values higher

than 400 μm , presenting a curve with reduced slope between values 100 and 400 μm . Also, 40% of aggregates are smaller than 30 μm in size. Moreover, the disaggregation effect that occurs when using the MM2000 determines a PSD with a high quantity of fine particles. The method of measurement for particle size by optical microscopy was also useful for observing the aggregation evolution over time, specifically when fine particles agglomerate to form new, larger aggregates. In the case of copper sulfide precipitates, the attraction forces promote rapid aggregation among particles. Therefore, the image capture must be very fast. Figure 2 shows the optical micrographs captured by the camera for M1 and M9 samples. In this case, M9 had a higher quantity of aggregates with fewer fine particles around the large aggregates. Figure 3 shows the D50 with respect to the time, from M1 to M9 (at 2 min). The particle size increases drastically from M7, indicating the increase of aggregates, although the behavior in samples M1 to M6 is parabolic, demonstrating a variable behavior. In this context, the validation of the method proposed for measuring particle size distribution is fundamental to support the representativity of the samples taken from a process.

3.3 Statistical analysis of the particle size distribution for copper aggregates

The analysis of size distribution for samples studied by optical microscopy and laser diffraction technique is shown in Table 3. It is appreciated that none of the techniques used for PSD characterization have shown a normal distribution. This is an indication of the complexity of the aggregates and the variability that can be found in the distribution. Figure 4 shows the distribution of all the images (M1...M9) in a Box-and-Whisker plot. In this figure not only is it confirmed that the distribution is not normal, but also it is shown that two of the images (M1 and M8) have 50% of the data located in the range of 160-340 μm in comparison with the rest of the images in which 50% of the data are located in a PSD lower

than 160 μm . This can be explained by the fact mentioned above, namely, that the precipitates obtained in the sulfidization process tend to aggregate over time. Therefore fewer small particles are quantified by the image analysis during the image capture. The aggregates grow over time, changing the size distribution.

According to the non-parametric Kruskal-Wallis, there are significant differences between the images (F-ratio=27.35; p-value=0.0006). Additionally, ANOVA analysis showed that there are significant differences (F-ratio=4.12; p-value=0.0002) between the images (M1....M9) obtained by optical microscopy. However, those differences do not appear in all the images. Figure 5 shows the Tukey's HSD plot for the PSD by optical microscopy, in which it is observed that images M1 and M8 exhibited differences from the other images. The differences observed in these images with respect to the other images can be attributed to the aggregation behavior of precipitates over time. In this case, the M1 image was measured first and M8 was captured closer to the defined time-limit for taking the picture (2 min). Therefore, the size of the aggregates is greater than in the other samples. (The 2 min time could be variable for different particles. This will depend on the aggregation characteristics.)

Considering that M1 and M8 showed a different distribution, these images were removed from the analysis, since the time that elapsed affected the representativity of these samples, maximizing the size of aggregates with respect to the real-time expended in the reactor. ANOVA and Kruskal-Wallis results without M1 and M8 showed that there are no significant differences between the images for the ANOVA (F-ratio=1.87; p-value=0.0903) and the Kruskal-Wallis test (F-ratio=1.7266; p-value=0.1163). This means that the distribution obtained is representative from a statistical point of view. Additionally, Levene's statistic was calculated in order to determine whether there are significant differences between the

standard deviation of the seven images. Results obtained for this statistic showed that there are no significant differences ($F\text{-ratio}=1.7266$; $p\text{-value}=0.1188$) within the standard deviation. Thus, the standard deviation obtained from the seven images is representative at 95% of confidence level.

The validated PSD obtained by optical microscopy was compared with the analysis of the laser diffraction technique with and without pre-treatment. ANOVA and Kruskal-wallis analysis showed significant differences between the PSD ($p\leq 0.05$). Figure 6 shows the Tukey's HSD plot in which significant differences between optical microscopy and laser diffraction technique with and without pre-treatment can be observed. It is particularly interesting that the pre-treatment applied to the sample has a significant impact on the PSD. The sample in which a previous sonication (MS2) was applied showed the lower mean of $16.2449\text{ }\mu\text{m}$ with a standard deviation of $3.699\text{ }\mu\text{m}$, whereas the sample without sonication has a mean of $60.226\text{ }\mu\text{m}$ and a standard deviation of $3.046\text{ }\mu\text{m}$. Considering that PSD plays a crucial role in the solid-liquid separation processes, the type of analysis must be carefully considered, because the pre-treatment and the type of analysis themselves generate variability in the PSD characterization.

Furthermore, images obtained by optical microscopy (seven images) showed higher values in the mean ($119.721\text{ }\mu\text{m}$) in comparison with the laser diffraction technique. This result can be explained by the fact that the optical microscopy is not an invasive measurement technique. Therefore, the PSD obtained by optical microscopy represents reality effectively. This is crucial in the selection and design of solid-liquid separation processes. Finally, Figure 7 shows the definitive PSD obtained for the six first images ($P50=70\text{ }\mu\text{m}$; $P90=190\text{ }\mu\text{m}$), comparing it with the MM2000 PSD results. The curve obtained with optical microscopy presents two main zones of particles or aggregates, one representing the fine particles (<70

μm) and another one representing the larger aggregates (>70 μm). The limit of these two zones and their values of P50 should be the relevant information for use in solid-liquid separation process of precipitates.

3.4 Validation of method using an unbiased sample

Results of the comparative analysis for the CuCN sample are shown in Figure 8, where a Tukey's HSD plot for the nine images obtained for CuCN sample is compared with laser diffraction technique measurement (MS). In that Figure, it is observed that there are no significant differences ($p=0.11699$ in ANOVA) between the images (M1...M9) and between them and the laser diffraction technique measurement (MS), as well. This means that microscopy is a validated statistical technique as a non-invasive method for the PSD determination.

4. Conclusions

Image processing and analysis using optical microscopy, coupled with statistical methods to validate the results, is a non-invasive and reliable alternative to conventional methods for quantifying the PSD of slurries containing solids with aggregation behavior, generated from precipitation processes. Furthermore, the method presented in this study is easy to implement for research and industrial purposes in a standard laboratory. Additionally, this methodology could also be used to determine PSD for different fine particles (ranging between 1 and 500 μm), as an alternative to conventional methods. Therefore, this methodology could be the basis for the application of image processing and analysis to measure PSD in different processes online, in order to improve the control and performance of solid-liquid separation equipment.

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Figure Captions

Figure 1. Cumulative particle size distribution curve for different methods of particle size measurement. In the case of MC, it considers 9 original samples.

Figure 2. Optical micrographs of samples analyzed at different times, M1 at 10 seconds (left), M9 at 2 minutes (right).

Figure 3. Results of D50 particle size of copper precipitates with respect to the capture time of image in the microscope.

Figure 4. Box-and-Whisker plot for the PSD of nine images obtained by optical microscopy.

Figure 5. Tukey's HDS plot for PSD by optical microscopy.

Figure 6. Tukey's HDS plot for comparison of PSD between optical microscopy and laser diffraction technique with and without pre-treatment.

Figure 7. Cumulative particle size distribution curves for three methods of particle size measurement. In this case, the PSD obtained from image analysis by optical microscopy includes only M1 to M6.

Figure 8. Tukey's HDS plot for comparison of PSD between optical microscopy (M1...M9) and laser diffraction technique (MS) for the CuCN sample.

528 **List of tables**

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530 **Table 1.** Sulfidization results.

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532 **Table 2.** Particle size estimated by optical microscopy and laser diffraction technique.

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534 **Table 3.** Analysis of normal distribution for samples analyzed by optical microscopy and
535 laser diffraction technique.

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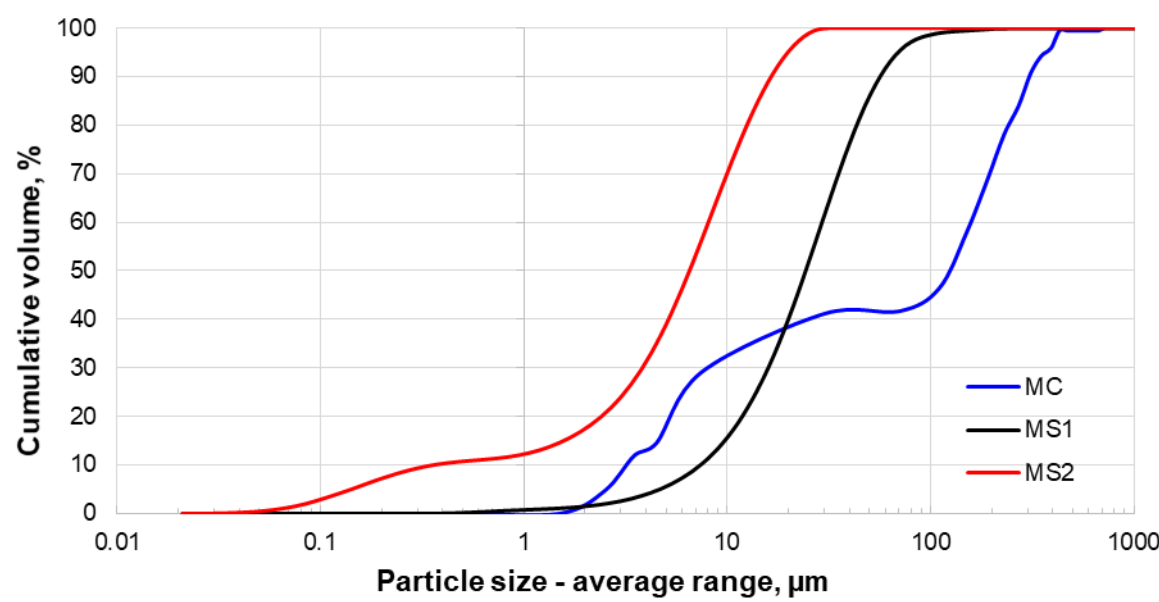


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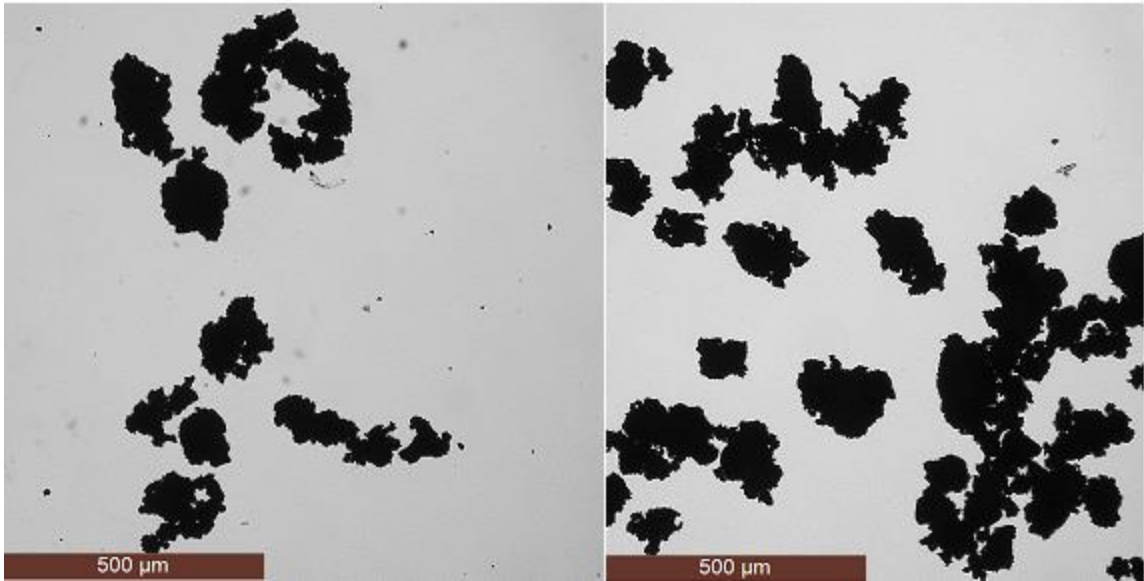


Figure 2. Optical micrographs of samples analyzed at different times, M1 at 10 seconds (left), M9 at 2 minutes (right).

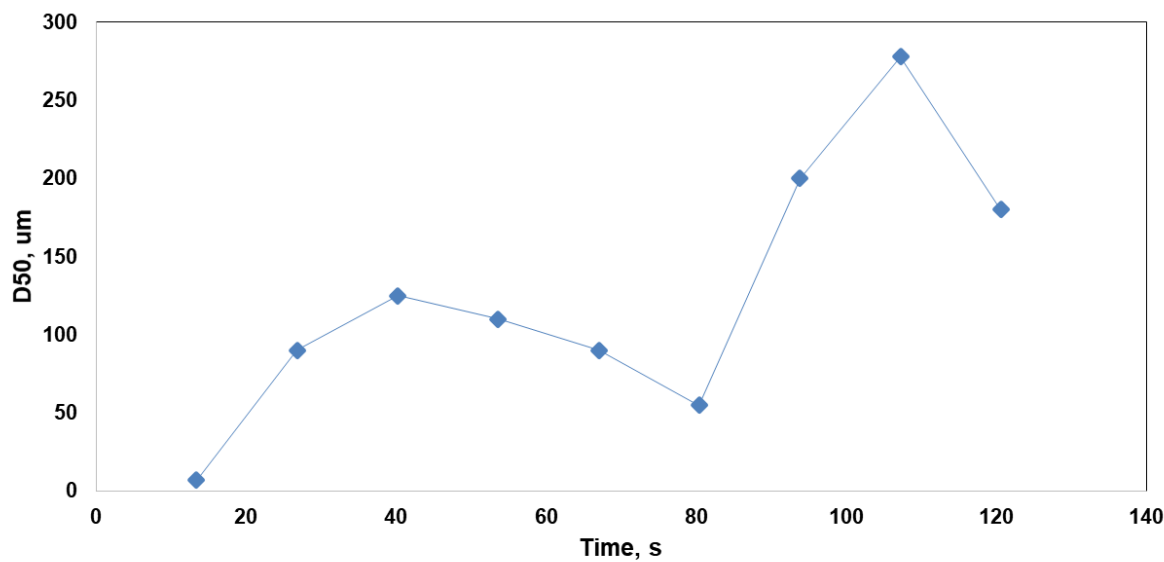
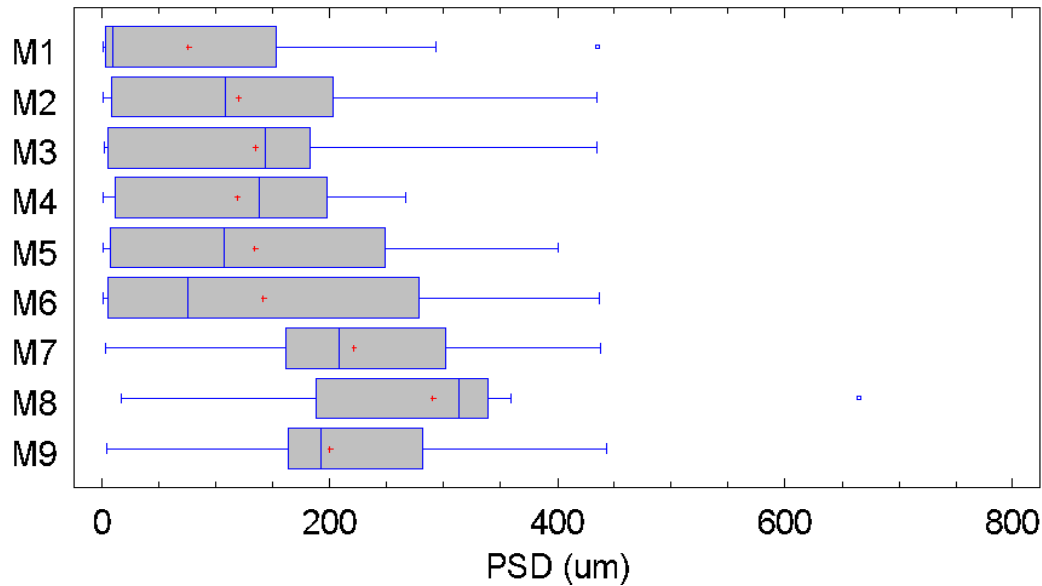


Figure 3. Results of D50 particle size of copper precipitates with respect to the capture time of image in the microscope.

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554 **Figure 4.** Box-and-Whisker plot for the PSD of nine images obtained by optical microscopy.

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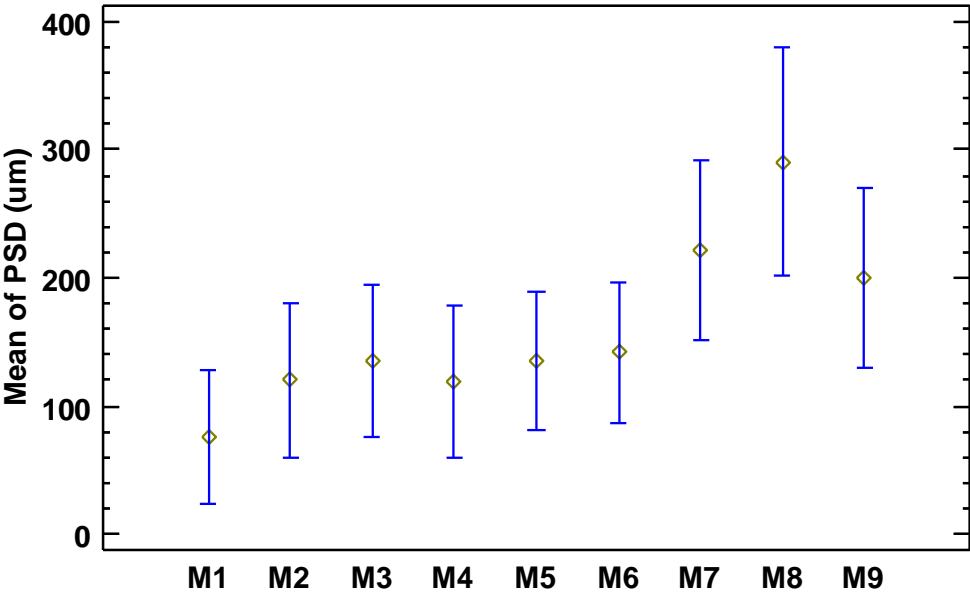


Figure 5. Tukey’s HSD plot for PSD by optical microscopy.

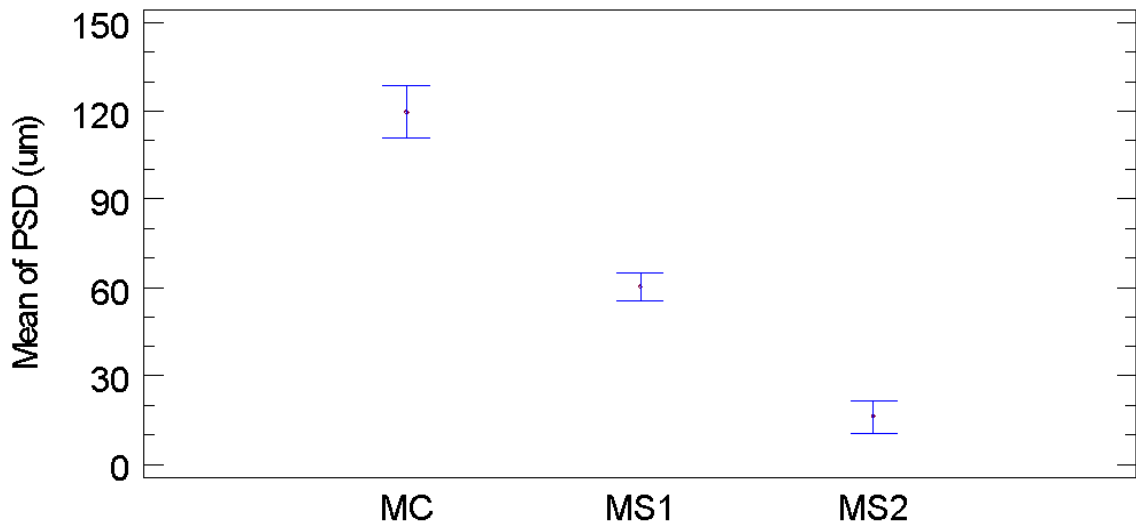


Figure 6. Tukey’s HSD plot for comparison of PSD between optical microscopy and laser diffraction technique with and without pre-treatment.

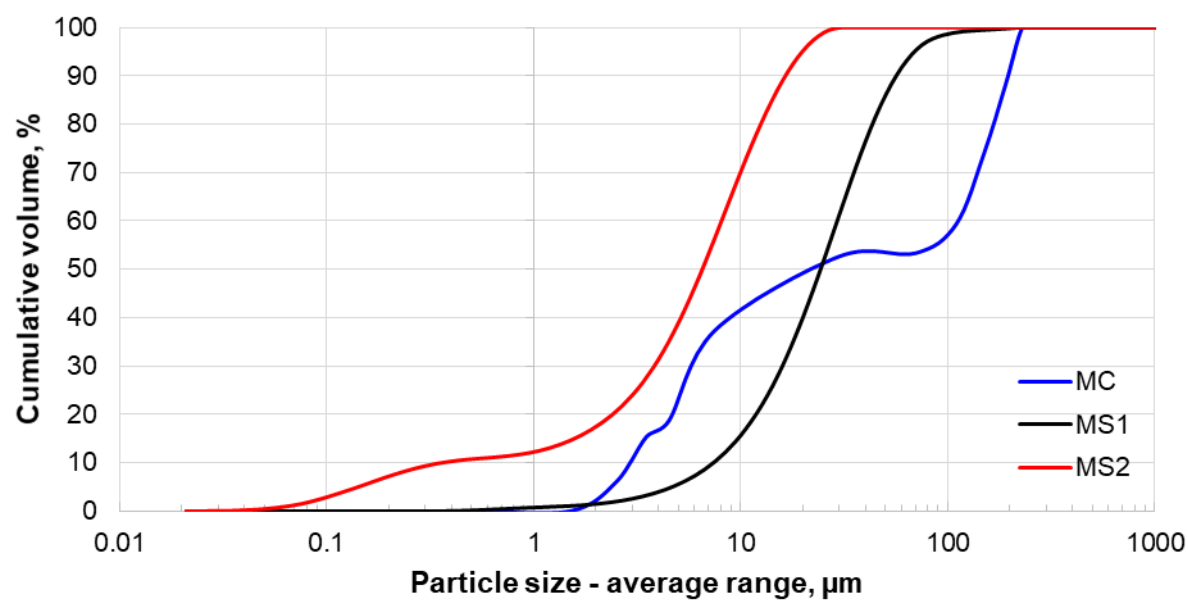


Figure 7. Cumulative particle size distribution curves for three methods of particle size measurement. In this case, the PSD obtained from image analysis by optical microscopy includes only M1 to M6.

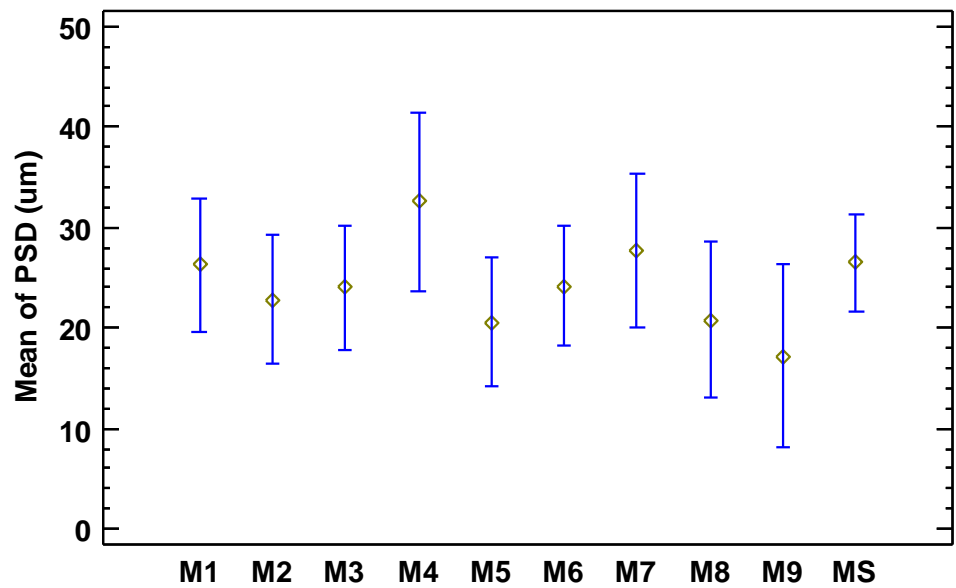


Figure 8. Tukey’s HSD plot for comparison of PSD between optical microscopy (M1...M9) and laser diffraction technique (MS) for the CuCN sample.

Description	Value
Copper content, % w/w	67.69
Copper sulfide conversion, %	99.97
Total suspended solids, mg/L	2,658

32

Table 2. Particle size estimated by optical microscopy and laser diffraction technique.

Particle size, μm	MC	MS1	MS2
P50	119	25.7	6.9
P90	307	59.6	17.4

P50: Particle size at 50% distribution; P90: Particle size at 90% distribution.
MC: Optical microscopy; MS1: Laser diffraction without pre-treatment;
MS2: Laser diffraction with pre-treatment.

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