

Modeling and Efficiency Optimization of Steam Boilers by Employing Neural Networks and Response-Surface Method (RSM)

Heydar Maddah¹, Milad Sadeghzadeh², Mohammad Hossein Ahmadi³, Ravinder Kumar⁴,

Shahaboddin Shamshirband^{5,6}

¹Department of Chemistry, Payame Noor University (PNU), P.O. Box, 19395-3697 Tehran, Iran.

²Department of Renewable Energy and Environmental Engineering, University of Tehran, Tehran, Iran.

³Faculty of Mechanical Engineering, Shahrood University of Technology, Shahrood, Iran.

⁴School of Mechanical Engineering, Lovely Professional University, Phagwara-144411 Punjab, India

⁵ Department for Management of Science and Technology Development, Ton Duc Thang University, Ho Chi Minh City, Viet Nam

⁶Faculty of Information Technology, Ton Duc Thang University, Ho Chi Minh City, Viet Nam

E-mail addresses of the corresponding author:

Shahaboddin.shamshirband@tdtu.edu.vn

Abstract

Boiler efficiency is called to some extent of total thermal energy which can be recovered from the fuel. Boiler efficiency losses are due to four major factors: the dry gas flux, the latent heat of steam in the flue gas, the combustion loss or the loss of unburned fuel, radiation and convection losses. In this research, the thermal behavior of boilers in gas refinery facilities is studied and their efficiency and their losses are calculated. The main part of this research is comprised of analyzing the effect of various parameters on efficiency such as excess air, fuel moisture, air humidity, fuel and air temperature, the temperature of combustion gases, and thermal value of the fuel. Based on the obtained results, it is possible to analyze and

make recommendations for optimizing boilers in the gas refinery complex using response-surface method (RSM).

Keywords: Modeling; Optimization; Steam Boiler; Neural Network; Response-Surface

1. Introduction

Steam boilers are designed to supply steam for heat transfer purposes due to considerable latent heat value [1,2]. Steam is the main feed of several industries in case of direct or indirect utilization since the heat transfer coefficient of steam is two times more than water. Therefore, it can be utilized effectively in power production plants in order to generate electricity [3,4]. Thus, the boiler considered as the most significant component in power plants, refineries, and so forth [5,6]. The working conditions of a boiler should be always monitored. It must be highlighted that boilers are working under high temperature and pressurized status, hence explosion is a serious risk, which is threatening in boilers operation [7,8]. In the design procedure of the boilers, several aspects, including financial, fuel cost, and maintenance factors should be covered and noticed. The complexity of steam boiler makes it challenging to perform common measurements since several factors affect the performance of the boiler. Traditional evaluation methods of boiler performance are neither cost-effective nor time-saving [9,10]. Besides, to carry out a comprehensive, accurate analysis, the fuel composition should be analyzed before and after the combustion process in detail [11,12].

The earlier studies on heat transfer and boiling were carried out by researchers such as Gongur and Winterton [13] and Kandlikar [14]. The researchers collected a large amount of laboratory data by conducting several experiments. They achieved to present some correlations that could be employed to estimate the boiling behavior with little error. In the current time, computational fluid dynamic (CFD) methods have been used extensively to investigate the boiling regime and its associated involved mechanisms. Judd and Hwang [15] proposed a model for the prediction of boiling heat, which includes evaporation and natural heat transfer mechanisms. They found that the evaporation heat transfer is a significant proportion of the total heat transfer. The application of various CFD models for forced boiling simulation studied by several researchers [16–20]. Various two-phase models with different simulation approaches employed. In these studies, the conservation equations for mass, momentum, and energy for each

dissolved phase have been used. Also, a series of empirical auxiliary relationships utilized in the simulation procedure. Krepper et al. [21] provided a model for the evaluation of the boiling mechanism. They investigated boiling in critical thermal flux conditions. In their research, essential parameters such as rotation, cross-flow between adjacent channels and bubble concentration regions were determined. By calculating the temperature of the bar surface, critical areas were identified, and different geometries were evaluated through CFD modeling. Rivera and Xicale [22] performed experimental evaluation and analytical assessment on an upstream flow of water-lithium bromide in a uniform vertical heated tube and provided valuable laboratory data for the saturated nucleate boiling heat transfer coefficients. Owhaib et al. [23] experimentally and analytically investigated a flow of R-134a fluid in a quartz vertical circular tube which was uniformly heated by a heater. Their primary purpose was to simulate the saturated and sub-cooled boiling of the rising refrigerant in the vertical pipe through the pressurized steam that was flowed out of the pipe. Stevanovic et al. [24] provided a single-dimensional multi-fluid model to predict two-phase flow patterns in vertical pipes. The presented model was based on the conservation of mass, energy and momentum and was applicable to any fluid flow that has two-phase flow patterns. Yang et al. [25] presented numerical simulations and practical experiments for modeling the behavior of the R-141b refrigerant in a horizontal coil based on the fluid volume method and considering the multiphase flow model. There was a good agreement between the numerical predictions of phase change with their laboratory data. Kouhikamali [26] developed a numerical simulation for condensation in a vertical cylinder under the forced convection regime. Condensation simulations were carried out using fluid volume model and the effects of parameters such as hydraulic diameter, fluid velocity, Reynolds number, wall temperature difference, and fluid saturation temperature on heat transfer coefficient were investigated. Ozawa et al. [27] examined a range of thermal behaviors, including boiling patterns, heat transfer, pressure drop, and critical thermal flux during high-pressure carbon dioxide boiling for a horizontal microwave channel. The studied variables were tube diameter changes, mass flux, wall thermal flux, and saturation temperature and pressure of the fluid. Saisorn et al. [28] examined the R-134a refrigerant evaporation flow through horizontal and vertical mini channels in order to obtain heat transfer data and also simulation and determination of fluid flow patterns. Dimensions of the fixed tube were considered to be constant, and the parameters of the thermal flux, mass flux and the saturation pressure of the inlet fluid were analyzed to determine the flow of fluid in two horizontal and upward flow conditions. Shen et al. [29] studied a downward fluid flow in a vertical tube for a wide range

of parameters such as pressure, mass flux, and thermal flux. Water considered as the working fluid, and the thermal distribution diagram was plotted near the tube wall. In the following, the effect of the thermal flux of the wall on the heat transfer coefficient and wall temperature investigated, new experimental correlations presented, and the heat transfer coefficient compared in a downstream current with a rising flow.

Chen et al. [30] investigated the engineering applications of constructal theory in China. Xie et al. [31] applied constructal theory to optimize heat transfer performance and pressure drop of an evaporator boiler. Behbahaninia et al. [32] presented a novel auditing approach to monitoring the performance of steam boilers based on exergy approach. This method was proposed based on ASME ptc 4.1 to calculate the exergy loss and exergy efficiency. Some significant factors such as exergy destruction inside the boiler, exergy loss in the wall of the boiler, exergy destruction in the gas-air heater, exergy loss in the flue gas. It concluded that the major irreversibility of the boiler is due to inside exergy destruction, i.e. more than 38%. In addition, the total exergy efficiency of the boiler was calculated by 53.7%. Li et al. [33] investigated the performance of a boiler in a biomass energy production plant and used the exergy method. It was reported that the most irreversibilities was originated from the combustion process. It was found that the total exergy efficiency of the boiler could be increased by decreasing the excess air and by augmenting the superheater temperature. Li et al. [34] compared various scenarios in order to prevent the inefficient working of a boiler in a 660 MW coal power plant. The authors recommended that the approach of closing part of the 2nd air nozzle was the most beneficial approach among other studied methods. In another study, Li et al. [35] analyzed the effect of increasing primary air ratio on the performance of a boiler in a coal-fired power plant. It was monitored that increasing the primary air temperature was more practical and also improved the thermal performance of the boiler instead of rising the air ratio. Javan et al. [36] performed an exergoeconomic optimization of a gas-fired steam power plant by applying a genetic algorithm. Based on the results, the boiler was the most exergy destructive source in the power plant. Therefore, two approaches presented and compared to decrease the amount of exergy destruction in the boiler in order to improve the total efficiency of the power plant: reducing the amount of excess air and decreasing the outlet temperature of the boiler's exhaust gas through heat recovery approaches. It was stated that this optimization technique was able to lower the total cost rate by 20% and decreased the dangerous environmental impact by 88%. Pattanayak et al. [37] optimized the sootblowing frequency of a boiler in a coal-fired power plant in order to lower the hazardous combustion emission and increase the boiler's efficiency. Sobota [38] proposed an on-line monitoring method to improve

the efficiency of a steam boiler. Nikula et al. [39] proposed a data-driven model to estimate and monitor the thermal performance of the boiler in order to achieve a higher efficiency boiler with a reduction in emission pollutants. Vandani et al. [40] used a genetic algorithm and partial swarm optimization techniques to improve the exergetic efficiency of boiler blowdown. It was stated that outlet pressure and outlet temperature of the boiler played a significant role in improving the exergy efficiency.

In this research, the modeling of boiler efficiency will be performed based on experimental data and response-surface method (RSM). Steam flow rate and output temperature selected as independent variables. The dependent variable is considered as the boiler efficiency.

2. Modeling Fundamentals

The neural network model is a data-driven model, so it requires experimental data to build the model. In this study, with the help of the neural network modeling, the target output is predicted through two input data sets. Figure 1 illustrates the upper and lower limit of input and output data. The utilized input data in the neural network modeling process is listed in Table 1. Where, \dot{m} represents the mass flow rate (kg/s), T is the temperature (°C), and η states the boiler efficiency.

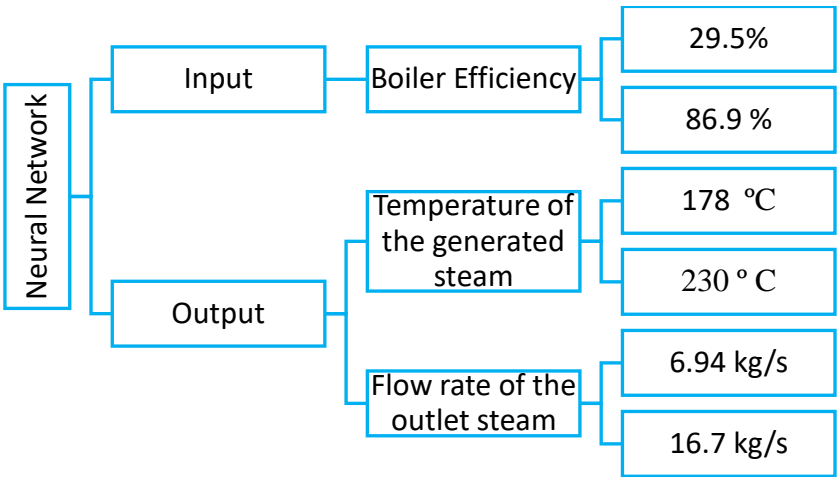


Figure 1. The upper and lower limit of input and output data for construction of a neural network model

Table 1. The experimental data used to form the neural network model

		$\dot{m}(\text{kg/s})$	$T(^{\circ}\text{C})$	η	$\dot{m}(\text{kg/s})$	$T(^{\circ}\text{C})$	η		
data	Input in neural divided categories validating as it is	15.06277	179.8114	68.8229	10.3826	202.5607	68.3157	and output artificial network are into 3 of training, and testing	
		11.50799	217.4076	68.10162	8.112843	195.3354	66.59289		
		10.96721	227.7698	66.7485	12.47747	228.7439	66.83186		
		11.83226	195.8293	69.17249	15.45171	206.8831	69.76082		
		8.164	211.1887	66.49393	10.33337	222.0078	66.69333		
		8.230552	195.8363	67.13933	7.35201	199.2193	66.00094		
		15.4074	189.2565	69.76787	8.328303	202.0249	67.16067		
		12.80646	218.8824	68.03788	7.689097	220.9679	65.33974		
		9.523767	215.6007	67.21874	14.14401	229.5426	67.54719		
		15.35225	192.4996	69.97655	11.38288	205.2453	68.95443		
		7.509398	208.2864	66.27828	13.44131	226.1227	67.40915		
		11.39483	199.8923	68.57542	13.74267	216.4291	68.86722		
		13.96593	182.7876	68.82806	12.49931	207.5064	68.88944		
		10.24027	179.2494	67.70906	13.05674	228.3764	67.44843		
		10.84519	203.5396	68.7183	15.47826	220.874	68.30319		
		12.06786	192.4699	69.16695	13.38398	227.8997	67.56851		
		15.6384	195.6674	69.49326	15.45541	211.61	69.13087		
		14.51184	192.9422	69.69088	11.48975	197.7378	69.29713		
		7.618852	186.887	66.61787	8.318545	202.7819	66.87618		
		9.65485	198.7617	68.26366	7.606863	225.4183	64.83067		
		10.63276	214.2778	67.86751	13.88847	178.7724	69.11839		
		15.35098	188.5912	69.38854	9.938753	186.1481	67.56152		
		11.02739	212.649	68.18121	13.46965	202.5215	69.66543		
		9.276587	201.0394	67.34079	13.28742	206.2356	69.53684		
		12.75497	200.5314	69.42711	12.10742	181.1039	68.71523		
		11.60532	187.1125	68.66235	13.89687	212.2176	68.83852		
		15.68032	188.0465	69.69601	11.85233	224.261	67.02746		
		16.0319	210.0539	69.16832	11.68888	183.7009	68.7909		
		14.89612	191.9886	69.48701	11.78454	200.7642	69.38998		
		13.83662	207.1033	69.35699	16.04421	192.572	69.86828		
		14.1702	227.1288	67.70859	10.72913	229.2328	66.56324		
		15.69162	215.1525	68.53946	8.083356	209.6555	66.52948		
		7.57872	213.3194	65.88433	9.281896	191.195	67.60546		
		10.21025	227.8878	65.96942	13.60328	184.896	68.9027		
		6.986591	218.3174	65.18013	15.10385	206.3403	69.70184		
		14.99537	209.6018	69.78638	16.37641	221.0458	68.45829		
		11.87784	227.2961	66.81758	9.036371	221.5243	66.38769		
		10.50436	181.1014	67.63481	14.33667	221.3341	68.1886		
		9.147886	191.973	67.25517	12.62322	188.5932	69.35013		
		12.1442	229.3074	67.04037	10.86203	206.3097	68.49007		
		9.758881	218.1548	67.08144	11.90317	223.497	67.82707		
		7.609162	202.7184	66.5345	11.76321	184.292	68.53394		
		7.770549	213.4068	65.85192	13.27719	222.5302	67.67154		
		7.608856	199.6806	66.64859	14.17492	224.7884	67.86074		
		10.92877	197.7678	68.71765	9.880103	189.329	67.77672		
		8.143986	189.0901	66.894	7.815672	182.0029	66.12302		
		11.25155	197.9128	69.15146	14.97466	202.6592	69.45441		
		15.68414	179.5427	68.899					

demonstrated in Figure 2. Training data is used to create a model. The validation data is used to check the quality and correctness of the training stage. Test data is not used in the training phase and is used only for performance evaluation and examining the neural network modeling.

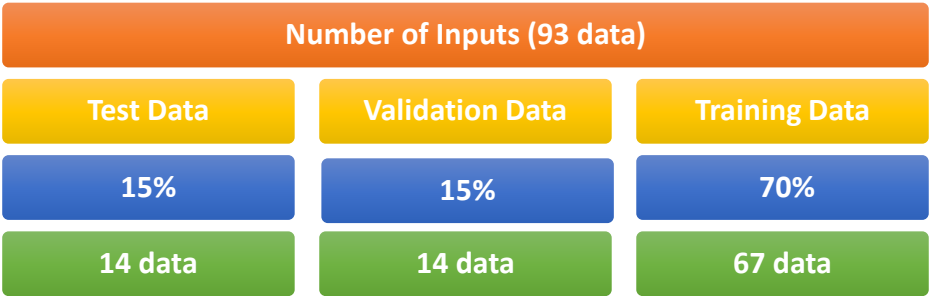


Figure 2. Randomized classification of empirical data in order to construct a neural network model

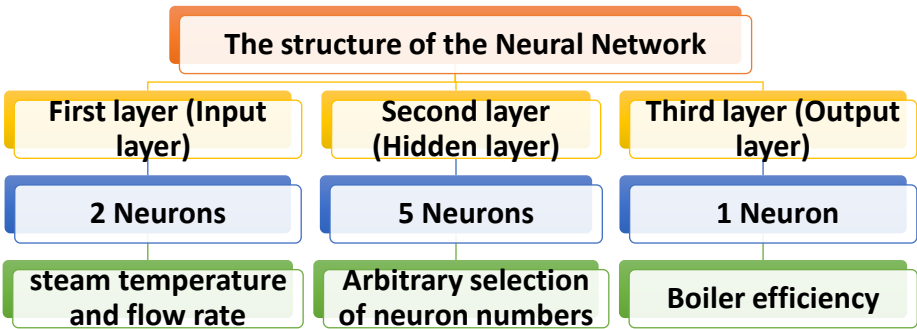


Figure 3. Triple layer neural network structure

The neural network is expressed on the basis of a particular topology. The topology is referred to the structure of the network. In this investigation, a triple layer neural network, Figure 3, is used to predict the output variable, the boiler efficiency. A sample 2-5-1 structure is depicted in Figure 4. As can be seen, the number of neurons in the first, second and third layers is 2, 5, and 1, respectively. The number of neurons in the second layer, known as the hidden layer, is arbitrary. In this research, 5 neurons are determined to be placed in the hidden layer. The selection the neurons' number in the first and third layers is not arbitrary and is selected based on the number of input data to the model. According to Figure 4, the neurons in each layer are connected by the edges to the neurons in the adjacent layer. These edges determine the relationship between the input and output variables by the weight coefficients assigned to them. This mathematical relation is discussed in the following.

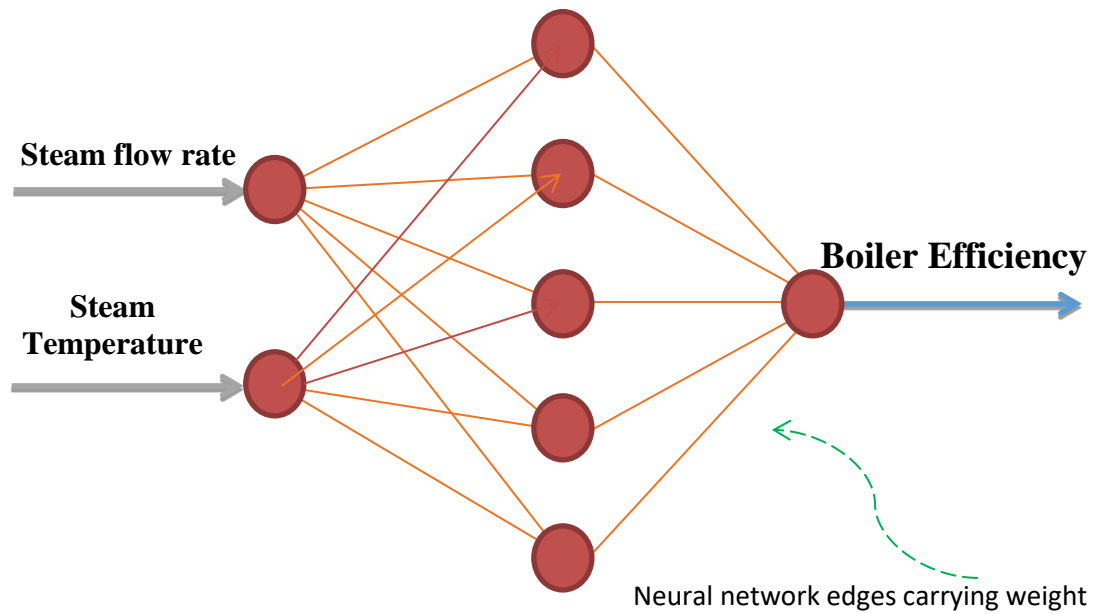


Figure 4. Sample schematic structure of a 2-5-1 neural network model: 2 neurons in the input layer, 5 neurons in the hidden layer, and a neuron in the output layer

The connection between input data and output data is determined by a network of linked nodes as shown in Figure 4.

Input and output data are correlated with a series of weighted coefficients. There are 10 ($2 \times 5 = 10$) edges between the first layer and the second layer. There are 5 ($5 \times 1 = 5$) edges between the second layer and the third layer. Each edge is assigned a weight. The weights of these edges are presented as a 5×2 matrix and a 5×1 matrix. The relationship between output and input data is expressed as follows:

$$\eta = [LW]_{1 \times 5} \times \tanh \left([IW]_{5 \times 2} \times \begin{bmatrix} m \\ T \end{bmatrix}_{2 \times 1} + [b_1]_{5 \times 1} \right) + [b_2]_{1 \times 1} \quad (1)$$

The employed variables in the Eq. (1) are listed and defined in Table 2.

Table 2. Definition of required variables in modeling using neural network

Variable	Definition	Description
η_{NN}	Output of the neural network model	Boiler efficiency, the final output of the neural network model
\dot{m}	1 st input variable	Steam mass flow rate, Kg/s
T	2 nd input variable	Temperature, °C
$[IW]_{5 \times 2}$	Edge matrix between 1 st and 2 nd layers	Each of the edges between layer 1 and 2 is assigned a weight
$[LW]_{1 \times 5}$	Edge matrix between 2 nd and 3 rd layers	Each of the edges between layer 2 and 3 is assigned a weight
$[b_1]_{5 \times 1}$	Bias matrix of the 2 nd layer	After multiplying the weight matrix in the input signal, the results are summed with the bias.
$[b_2]_{1 \times 1}$	Bias matrix of the 3 rd layer	After multiplying the weight matrix in the input signal, the results are summed with the bias.

3. Modeling Results of Boiler Efficiency Using Neural Network

In this section, the obtained results from the modeling by means of neural network are compared with the actual results. The total number of data used in modeling is 95. Of these, 70% are for training, 15% for validating, and the rest for testing the network. Figure 5 illustrates the graph error of the modeling results. The graph error is the difference between the output of the network and the actual output.

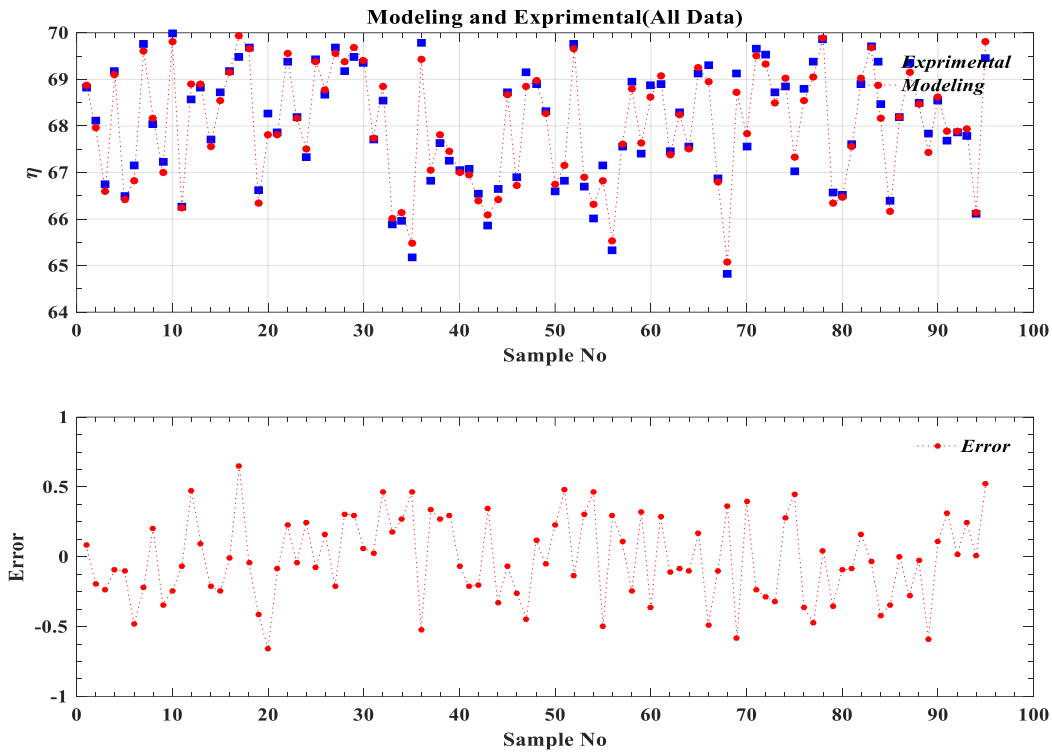


Figure 5. Comparison of model estimations with actual efficiency measurements (95 Data)

As it is monitored, the prediction error is approximately 1% in the positive and negative range with the help of the neural network. In the following figures, the actual data (experimental) and modeling data are presented separately for each of the three categories, i.e. categories of training, validating, and testing.

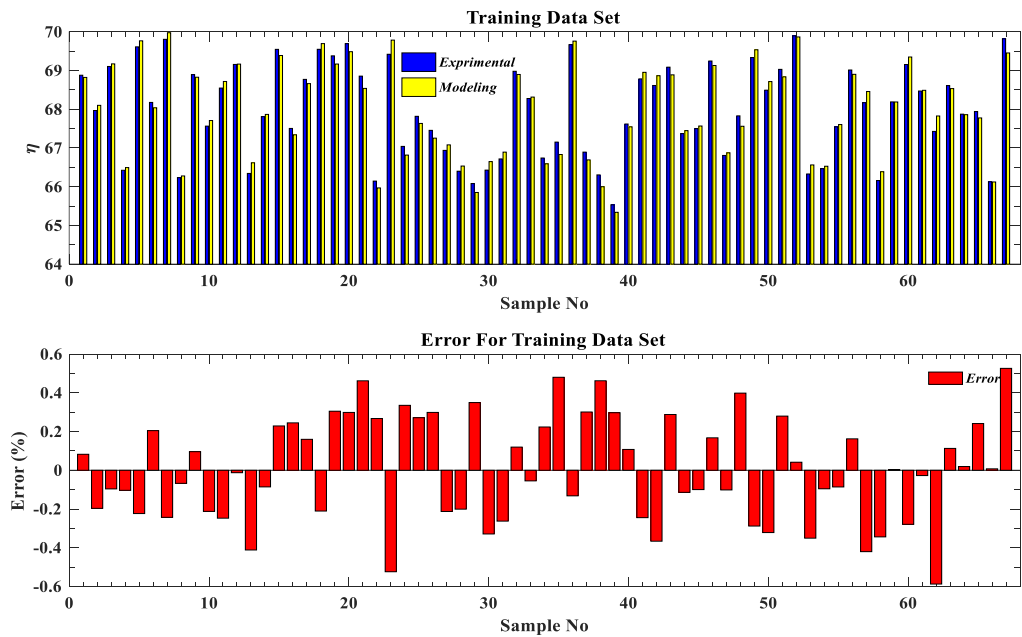


Figure 6. Comparison of experimental data and modeling for training stage (75 data)

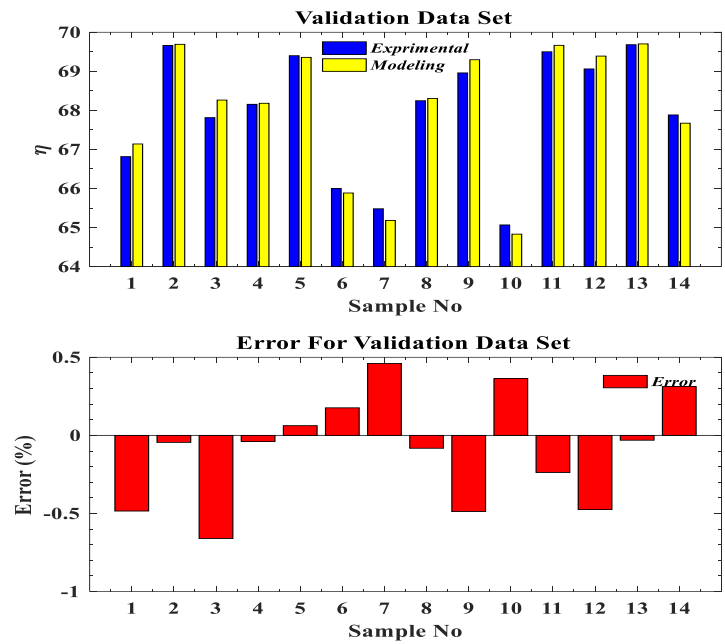


Figure 7. Comparison of experimental data and modeling for validation (14 data)

Figures 6-8 demonstrate the error in the modeling data in percent for the three classes of train, validation, and test, respectively. Based on these figures, the error data for training, validating, and testing phases are obtained by 0.6, 0.5, and 1, respectively. Test data are not involved in the training stage. Therefore, test data error is more than training and validation.

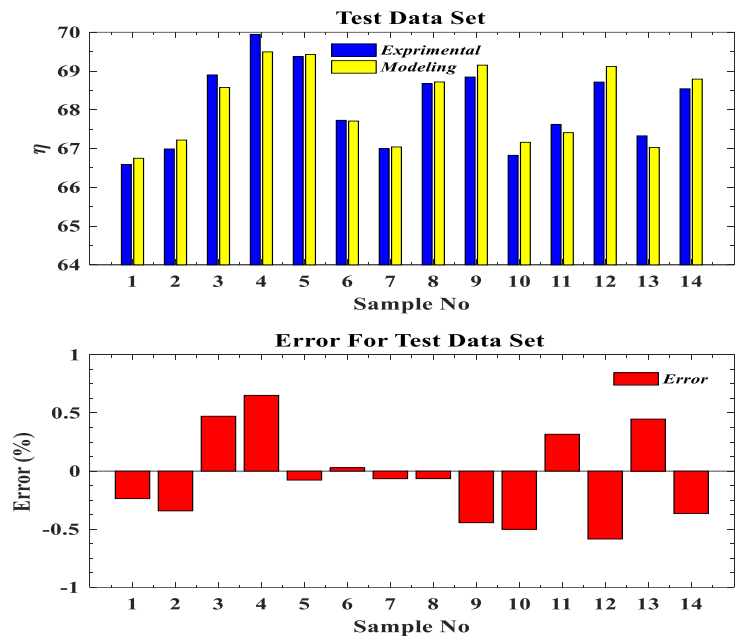


Figure 8. Comparison of experimental data and modeling for test stage (14 data)

The regression line diagram along with the mean squared error (MSE) and correlation coefficient for each of categories of training, validation, and test are shown in Figures 9-11. As it is expected, the low error rate and high correlation coefficient indicate the proper performance of the neural network in prediction of the boiler efficiency. In the Figures 9-11, horizontal axis is real efficiency and vertical axis demonstrates the modeling efficiency. Ideally, when the model error is zero, all points are located on the line $Y = T$ (First bisector quadrant line). In reality there is a small amount of error that causes the points to be scattered up and down the line. The best-passing equation from the points in this graph along with the correlation coefficient as well as the MSE error are given in the following figures for the train, validation, and test stages.

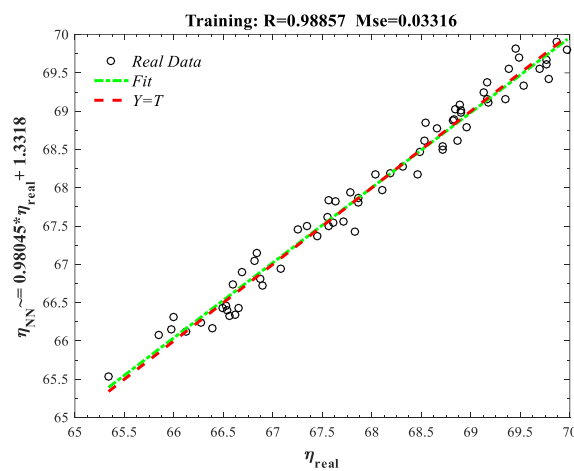


Figure 9. The regression line diagram for training data

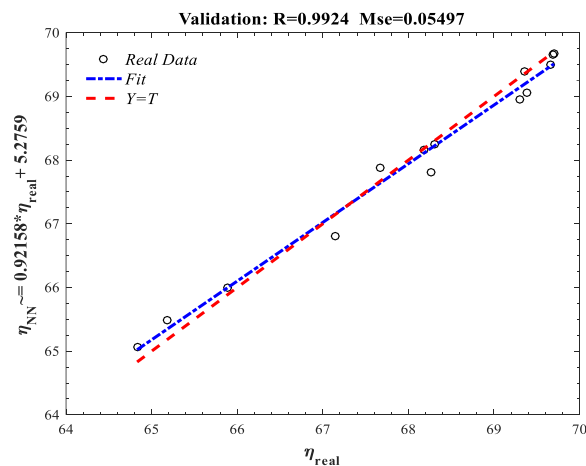


Figure 10. The regression line diagram for validation data

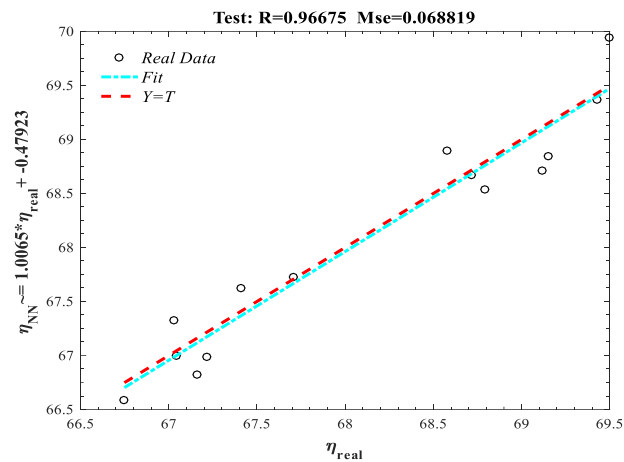


Figure 11. The regression line diagram for test data

The network performance in respect to modeling error and regression coefficient R2 are obtained according to Table 3.

Table 3. The performance of the neural network in predicting efficiency

	Train (70%)	Validation (15%)	Test (15%)
Number of data	67	14	14
Mean Squared Error (MSE)	0.033	0.055	0.069
Regression coefficient (R ²)	0.998	0.994	0.966

The performance values (error and correlation coefficient) of the network are graphically depicted in Figure 12 and Figure 13, respectively, as follows:

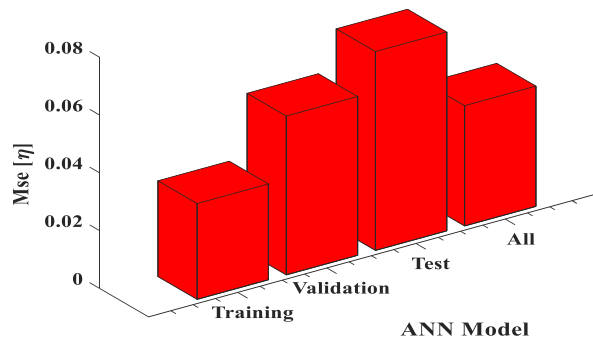


Figure 12. Values of mean squared error (MSE) of training, validation, test, and all.

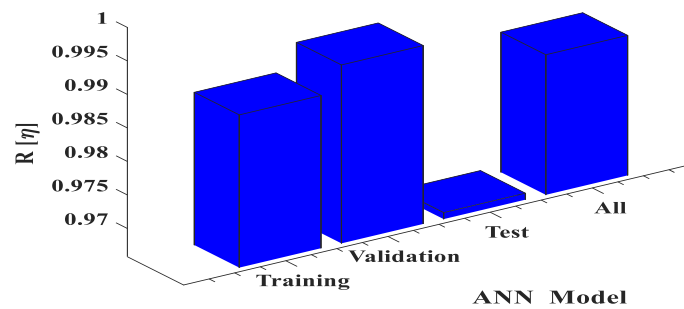


Figure 13. Correlation coefficient of training, validation, test, and all.

Most of the stopping training criteria are based on the mean square error control. Therefore, the MSE curve is plotted as a function of the repetition of the training algorithm in Figure 14.

Monitoring MSE for test data and validation data is performed in the same way as training data in various repetitions, and when the validation data error begins to increase, the training should be stopped. The most generalization is occurred at the 11th epoch.

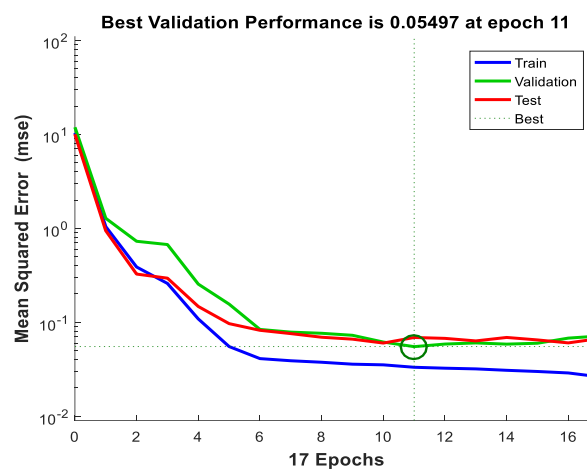


Figure 14. Mean Squared Error Diagram in Different epochs of Training Process for estimating the Boiler Efficiency.

The mean square error (MSE) during the training process is demonstrated in the Figure 14. Obviously, increasing the frequency is led to gradually decrease in error of all three categories. With the progress of the algorithm in each repetition, the mean square error for the validation data is calculated. The algorithm will not stop until the validation error decreases, and training continues. When the validation error is not decreasing in 6 consecutive repetitions, the training stops. The number 6 is the stop training indicator, which

is adjustable in the software. This number is known as the validation check and is assumed 6 by default in the software.

The point where the validation error reaches its minimum is considered as the output of the model. For instance, in the Figure 14 before the 11th epoch, the network error trend for the training, validation, and testing data is decreasing and from repetition 11, the verification error is increasing, while the training data error continues to decline. From Repeat 11 to Repeat 17 (6 consecutive repetitions), the validation error has an increasing trend, so the training algorithm ends and Repeat No. 11 is considered as an output. In other words, the training is stopped if the evaluation set error is raised in 6 consecutive repetitions. This stop occurred at repeat No. 11. It should be noted that the algorithm calculates the mean squared error as follows:

$$MSE = \sum_{i=1}^n \frac{(\eta_{NN} - \eta_{Real})^2}{Ne} \quad (2)$$

In Eq. (2), η_{NN} denotes the obtained modeling efficiency, η_{Real} indicates the real measured boiler efficiency, and Ne represents the total number of samples.

4. Optimization with the Help of the Response-Surface Method

Response-surface method or RSM is a collection of statistical techniques and applied mathematics for creating empirical models. The purpose of response-surface is to optimize the response (output variable), which is influenced by several independent variables (input variables). In this study, two independent variables of flow rate and output steam temperature of the boiler, and dependent variable of efficiency are discussed.

In Figure 15, the fitted response surface on the boiler experimental data is presented, and as can be seen, this surface is well suited with the experimental data. The constant coefficients obtained from the RSM optimization for Eq. (3) are presented in the Table 4.

$$\eta(\dot{m}, T) = c_0 + c_1\dot{m} + c_2T + c_{12}\dot{m}T + c_{11}\dot{m}^2 + c_{22}T^2 \quad (3)$$

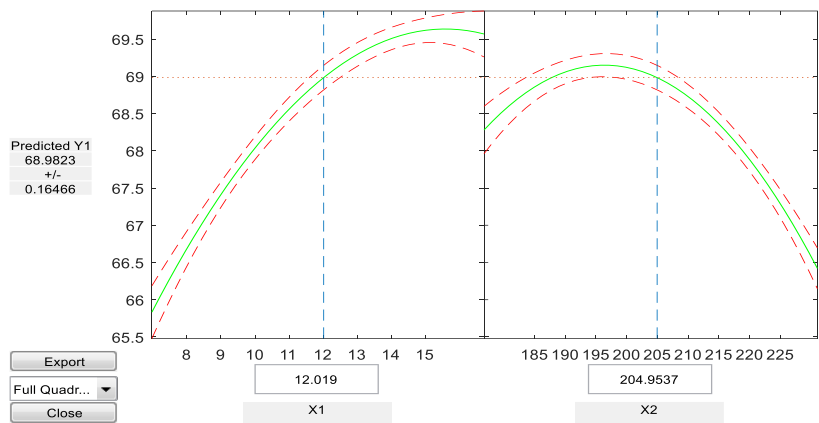


Figure 15. RSM analysis (inputs: flow rate and temperature)

Table 4. The optimal values of the constants which are obtained by RSM optimization

Constants	C0	C1	C2	C12	C11	C22
Optimized Value	-31.372	1.690	0.8977	-0.00047	-0.05112	-0.00227

In Figure 16, the response surface along with the experimental data is presented in a 3-D graph.

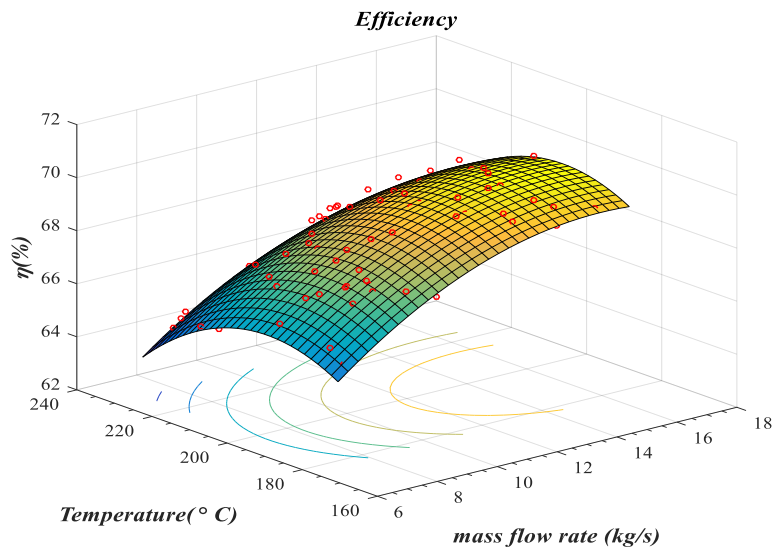


Figure 16. The fitted surface on the empirical data obtained from the boiler

The efficiency surface has an optimal point, which is presented in Table 5 for its optimal value.

Table 5. The optimal boiler efficiency (obtained from the RSM)

Variable	Objective function	1 st independent variable	2 nd independent variable
Unit	Efficiency (%)	Flow rate (kg/s)	Temperature (°C)
Optimal value from RSM	69.8	15.7	195.9

5. Sensitivity Analysis of Effecting Variables

With the aid of sensitivity analysis, the effect of each independent variable can be obtained on dependent variables (boiler efficiency). In the sensitivity analysis, all variables are assumed to be constant and only one variable within its permitted range is changed. In Figure 17, sensitivity analysis is performed for the temperature variable. As can be monitored, the magnitude of the efficiency at 196 °C results to its maximum value for almost all flow rates. As the flow rate increases and becomes close to the designed flow rate of the boiler changes, the rate of change in efficiency will be slower in terms of temperature.

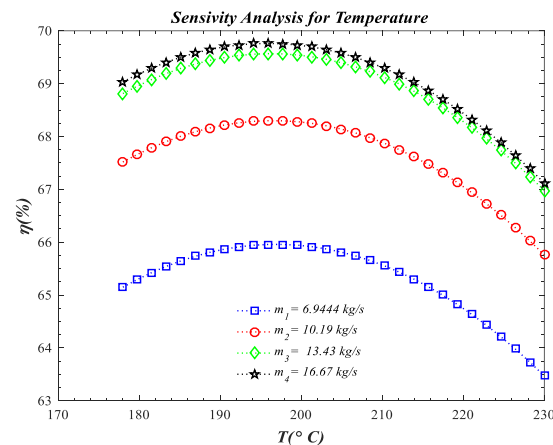


Figure 17. Temperature sensitivity analysis at four different flow rates

Figure 18 shows the sensitivity analysis for the flow rate independent variable. As can be seen, in the flow rate of 15.7 Kg /s, the amount of efficiency yields to its maximum. With increasing temperature, first, the efficiency increases and then decreases.

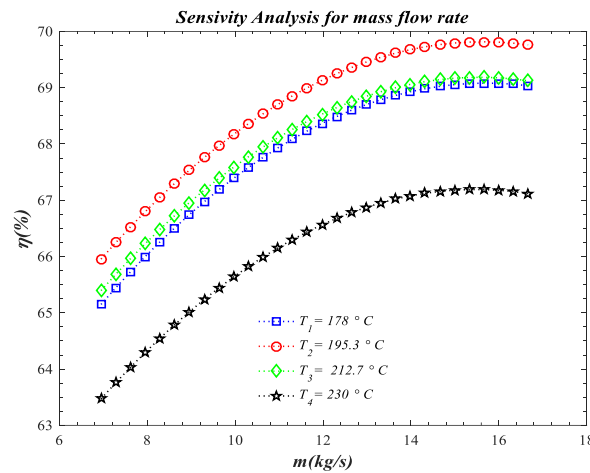


Figure 18. Flow rate sensitivity analysis at four different temperatures

7. Conclusion

The plant's steam production and distribution unit is designed and installed by Iranian Energy Engineering Company "Garmagostar" in order to provide steam and heating loads of reboilers, heaters, flares, sweetening packages, seawater treatment plant and other steam utilities. The total number of data used in the modeling process is 95 which are categorized as 70% for training, 15% for validation, and the rest for test procedure of the network. Modeling by means of neural network yields to the prediction error in the range of ± 1 . The associated error of the training stage, validation stage, and test stage were obtained less than 0.6%, 0.5%, and 1%, respectively. As expected, the data test error is higher than training and validation due to the lack of participation of the test data at the training and learning stage of the neural network. In the ideal mode, when the model error is zero, all points are placed on the line of $Y = T$ (Bisection of 1st and 3rd coordination sections). In practice there is a small amount of error that causes the points to be scattered up and down of the line. The best-passing equation of the points along with the correlation coefficient as well as the mean square error are calculated for validation and test phases of the total data. Response-surface method (RSM) is a set of statistical techniques and applied mathematics for constructing empirical models. The target goal of the RSM is to optimize the response (output variable), which is influenced by several independent variables (inputs). In this study, two independent variables of steam flow rate and temperature of the generated steam and dependent variable of efficiency are discussed. The amount of efficiency at

temperatures of 196 ° C results in maximum efficiency for almost all flow rates. As the flow rate increases and approaches to the specific boiler design flow rate, the trend of variations of efficiency in term of temperature is getting slower. Also, sensitivity analysis for the flow rate variable was performed and it is monitored that the maximum amount of efficiency is yielded at flow rate of 15.7 Kg/s. With increasing temperature, first, the efficiency increases and then decreases.

References

- [1] Echi S, Bouabidi A, Driss Z, Abid MS. CFD simulation and optimization of industrial boiler. *Energy* 2019;169:105–14. doi:10.1016/J.ENERGY.2018.12.006.
- [2] Ahmadi MH, Alhuyi Nazari M, Sadeghzadeh M, Pourfayaz F, Ghazvini M, Ming T, et al. Thermodynamic and economic analysis of performance evaluation of all the thermal power plants: A review. *Energy Sci Eng* 2019;7:30–65. doi:10.1002/ese3.223.
- [3] Szega M, Czyż T. Problems of calculation the energy efficiency of a dual-fuel steam boiler fired with industrial waste gases. *Energy* 2019;178:134–44. doi:10.1016/J.ENERGY.2019.04.068.
- [4] Mohammadi A, Ashouri M, Ahmadi MH, Bidi M, Sadeghzadeh M, Ming T. Thermo-economic analysis and multiobjective optimization of a combined gas turbine, steam, and organic Rankine cycle. *Energy Sci Eng* 2018;506–22. doi:10.1002/ese3.227.
- [5] Hajebzadeh H, Ansari ANM, Niazi S. Mathematical modeling and validation of a 320 MW tangentially fired boiler: A case study. *Appl Therm Eng* 2019;146:232–42. doi:10.1016/J.APPLTHERMALENG.2018.09.102.
- [6] Shams Ghoreishi SM, Akbari Vakilabadi M, Bidi M, Khoeini Poorfar A, Sadeghzadeh M, Ahmadi MH, et al. Analysis, economical and technical enhancement of an organic Rankine cycle recovering waste heat from an exhaust gas stream. *Energy Sci Eng* 2019;1–25. doi:10.1002/ese3.274.
- [7] El Hefni B, Bouskela D. Boiler (Steam Generator) Modeling. *Model. Simul. Therm. Power Plants with ThermoSysPro A Theor. Introd. a Pract. Guid.*, Cham: Springer International Publishing; 2019, p. 153–64. doi:10.1007/978-3-030-05105-1_7.
- [8] Sankar G, Kumar DS, Balasubramanian KR. Computational modeling of pulverized coal fired boilers – A review on the current position. *Fuel* 2019;236:643–65. doi:10.1016/J.FUEL.2018.08.154.

- [9] Trojan M. Modeling of a steam boiler operation using the boiler nonlinear mathematical model. *Energy* 2019;175:1194–208. doi:10.1016/J.ENERGY.2019.03.160.
- [10] Naeimi A, Bidi M, Ahmadi MH, Kumar R, Sadeghzadeh M, Alhuyi Nazari M. Design and exergy analysis of waste heat recovery system and gas engine for power generation in Tehran cement factory. *Therm Sci Eng Prog* 2019;9:299–307. doi:10.1016/j.tsep.2018.12.007.
- [11] Barroso J, Barreras F, Amaveda H, Lozano A. On the optimization of boiler efficiency using bagasse as fuel☆. *Fuel* 2003;82:1451–63. doi:10.1016/S0016-2361(03)00061-9.
- [12] Said SM, Hamouda AS, Mahmaoud H, Abd-Elwahab S. Computer-based boiler efficiency improvement. *Environ Prog Sustain Energy* 2019;1–9. doi:10.1002/ep.13161.
- [13] Gungor KE, Winterton RHS. A general correlation for flow boiling in tubes and annuli. *Int J Heat Mass Transf* 1986;29:351–8. doi:10.1016/0017-9310(86)90205-X.
- [14] Kandlikar SG. A General Correlation for Saturated Two-Phase Flow Boiling Heat Transfer Inside Horizontal and Vertical Tubes. *J Heat Transfer* 1990;112:219–28.
- [15] Judd RL, Hwang KS. A Comprehensive Model for Nucleate Pool Boiling Heat Transfer Including Microlayer Evaporation. *J Heat Transfer* 1976;98:623–9.
- [16] Krepper E, Rzehak R. CFD for subcooled flow boiling: Simulation of DEBORA experiments. *Nucl Eng Des* 2011;241:3851–66. doi:10.1016/J.NUCENGDES.2011.07.003.
- [17] Kunkelmann C, Stephan P. CFD simulation of boiling flows using the volume-of-fluid method within OpenFOAM. *Numer Heat Transf Part A Appl* 2009;56:631–46. doi:10.1080/10407780903423908.
- [18] Zhang X, Yu T, Cong T, Peng M. Effects of interaction models on upward subcooled boiling flow in annulus. *Prog Nucl Energy* 2018;105:61–75. doi:10.1016/J.PNUCENE.2017.12.004.
- [19] Promtong M, Cheung SCP, Yeoh GH, Vahaji S, Tu J. CFD investigation of sub-cooled boiling flow using a mechanistic wall heat partitioning approach with Wet-Steam properties. *J Comput Multiph Flows* 2018;10:239–58. doi:10.1177/1757482X18791900.
- [20] Pothukuchi H, Kelm S, Patnaik BSV, Prasad BVSSS, Allelein H-J. Numerical investigation of subcooled flow boiling in an annulus under the influence of eccentricity. *Appl Therm Eng*

- 2018;129:1604–17. doi:10.1016/J.APPLTHERMALENG.2017.10.105.
- [21] Krepper E, Končar B, Egorov Y. CFD modelling of subcooled boiling—Concept, validation and application to fuel assembly design. *Nucl Eng Des* 2007;237:716–31.
doi:10.1016/J.NUCENGDES.2006.10.023.
- [22] Rivera W, Xicale A. Heat transfer coefficients in two phase flow for the water/lithium bromide mixture used in solar absorption refrigeration systems. *Sol Energy Mater Sol Cells* 2001;70:309–20.
doi:10.1016/S0927-0248(01)00073-3.
- [23] Owhaib W, Palm B, Martín-Callizo C. Flow boiling visualization in a vertical circular minichannel at high vapor quality. *Exp Therm Fluid Sci* 2006;30:755–63.
doi:10.1016/J.EXPTHERMFLUSCI.2006.03.005.
- [24] Stevanovic V, Prica S, Maslovacic B. Multi-Fluid Model Predictions of Gas- Liquid Two-Phase Flows in Vertical Tubes. *FME Trans* 2007;35:173–81.
- [25] Yang Z, Peng XF, Ye P. Numerical and experimental investigation of two phase flow during boiling in a coiled tube. *Int J Heat Mass Transf* 2008;51:1003–16.
doi:10.1016/J.IJHEATMASSTRANSFER.2007.05.025.
- [26] Kouhikamali R. Numerical simulation and parametric study of forced convective condensation in cylindrical vertical channels in multiple effect desalination systems. *Desalination* 2010;254:49–57.
doi:10.1016/J.DESAL.2009.12.015.
- [27] Ozawa M, Ami T, Umekawa H, Matsumoto R, Hara T. Forced flow boiling of carbon dioxide in horizontal mini-channel. *Int J Therm Sci* 2011;50:296–308.
doi:10.1016/J.IJTHERMALSCI.2010.04.017.
- [28] Saisorn S, Kaew-On J, Wongwises S. An experimental investigation of flow boiling heat transfer of R-134a in horizontal and vertical mini-channels. *Exp Therm Fluid Sci* 2013;46:232–44.
doi:10.1016/J.EXPTHERMFLUSCI.2012.12.015.
- [29] Shen Z, Yang D, Chen G, Xiao F. Experimental investigation on heat transfer characteristics of smooth tube with downward flow. *Int J Heat Mass Transf* 2014;68:669–76.
doi:10.1016/J.IJHEATMASSTRANSFER.2013.09.045.

- [30] Chen L, Feng H, Xie Z, Sun F. Progress of constructal theory in China over the past decade. *Int J Heat Mass Transf* 2019;130:393–419. doi:10.1016/J.IJHEATMASSTRANSFER.2018.10.064.
- [31] Xie Z, Feng H, Chen L, Wu Z. Constructal design for supercharged boiler evaporator. *Int J Heat Mass Transf* 2019;138:571–9. doi:10.1016/J.IJHEATMASSTRANSFER.2019.04.078.
- [32] Behbahaninia A, Ramezani S, Lotfi Hejrandoost M. A loss method for exergy auditing of steam boilers. *Energy* 2017;140:253–60. doi:10.1016/J.ENERGY.2017.08.090.
- [33] Li C, Gillum C, Toupin K, Donaldson B. Biomass boiler energy conversion system analysis with the aid of exergy-based methods. *Energy Convers Manag* 2015;103:665–73. doi:10.1016/J.ENCONMAN.2015.07.014.
- [34] Li Z, Miao Z, Shen X, Li J. Prevention of boiler performance degradation under large primary air ratio scenario in a 660 MW brown coal boiler. *Energy* 2018;155:474–83. doi:10.1016/J.ENERGY.2018.05.008.
- [35] Li Z, Miao Z, Zhou Y, Wen S, Li J. Influence of increased primary air ratio on boiler performance in a 660 MW brown coal boiler. *Energy* 2018;152:804–17. doi:10.1016/J.ENERGY.2018.04.001.
- [36] Javan S, Ahmadi P, Mansoubi H, Jaafar MNM. Exergoeconomic Based Optimization of a Gas Fired Steam Power Plant Using Genetic Algorithm. *Heat Transf Res* 2015;44:533–51. doi:10.1002/htj.21135.
- [37] Pattanayak L, Ayyagari SPK, Sahu JN. Optimization of sootblowing frequency to improve boiler performance and reduce combustion pollution. *Clean Technol Environ Policy* 2015;17:1897–906. doi:10.1007/s10098-015-0906-0.
- [38] Sobota T. Improving Steam Boiler Operation by On-Line Monitoring of the Strength and Thermal Performance. *Heat Transf Eng* 2018;39:1260–71. doi:10.1080/01457632.2017.1363641.
- [39] Nikula R-P, Ruusunen M, Leiviskä K. Data-driven framework for boiler performance monitoring. *Appl Energy* 2016;183:1374–88. doi:10.1016/J.APENERGY.2016.09.072.
- [40] Vandani AMK, Bidi M, Ahmadi F. Exergy analysis and evolutionary optimization of boiler blowdown heat recovery in steam power plants. *Energy Convers Manag* 2015;106:1–9. doi:10.1016/J.ENCONMAN.2015.09.018.

