

1 **Preparation of renewable bio-polyols from two species of *Colliguaja* for rigid polyurethane**  
2 **foams.**

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28

29 **Abstract**

30

31 In this study we investigated the potential of two non-edible oil extracts from seeds of *Colliguaya*  
32 *Integerrima* (CIO) and *Colliguaja Salicifolia* (CSO) to use as a renewable source for polyols and  
33 eventually polyurethane foams or biodiesel. For this purpose, two novel polyols from the  
34 aforementioned oils were obtained in a one-single step reaction using a mixture of hydrogen peroxide  
35 and acetic acid. The polyol derivatives obtained from the two studied oils were characterized by  
36 spectral (FT-IR,  $^1\text{H}$  NMR and  $^{13}\text{C}$  NMR), physico-chemical (e.g. chromatographic analysis, acid  
37 value, oxidizability values, iodine value, peroxide value, saponification number, kinematic viscosity,  
38 theoretical molecular weights, density, hydroxyl number and hydroxyl functionality) and thermal  
39 (TGA) analyses according to standard methods. Physico-chemical results revealed that all parameters,  
40 with the exception of the iodine value, were higher for bio-polyols (CSP and CIP polyols) compared  
41 to the starting oils. The NMR, TGA and FT-IR analyses demonstrated the formation of polyols.  
42 Finally, the OH functionality values for CIP and CSP polyols were 4.50 and 5.00, respectively. This  
43 result indicated the possible used of CIP and CSP polyols as a raw material for the preparation of  
44 polyurethane rigid foams.

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50 Keywords: *Colliguaya Integerrima*; *Colliguaja Salicifolia*; vegetable oil; bio-polyol; renewable  
51 resources.

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## 53 1. Introduction

54 The high demand for products from petrochemical origin and their negative effects on the  
55 environment, parallel to the growing scarcity of these non-renewable resources, are factors that have  
56 encouraged the chemical industry to look for new sources of renewable resources as raw materials.  
57 These raw materials have contributed in a very positive way to the sustainable development of the  
58 plastics industry due to the great synthetic potential of nature and different principles of green  
59 chemistry [1, 2]. Vegetable oils are one of the most considered alternatives due to abundance, low  
60 toxicity, biodegradability, inherent fluidity and low cost [3-5]. Several vegetable oil molecules must  
61 be chemically transformed to form polyols, and these bio-polyols are used for the obtention of  
62 polyurethanes [6], polyesters [7], and epoxy [8], among others.

63 The synthesis of bio-polyols from fatty acids and vegetable oils has been the focus of many  
64 studies. It's important to note that vegetable oils, with the exception of castor and lesquerella oils do  
65 not contain hydroxyl groups. For that reason, it is necessary to chemically modify the vegetable oils  
66 to introduce hydroxyl groups into their structures to produce polyols. According to the literature, there  
67 are five different pathways for vegetable oil-based bio-polyol production: (1) Epoxidation and  
68 oxirane ring-opening [9]; (2) Hydroformylation and hydrogenation [10, 11]; (3) Ozonolysis [12]; (4)  
69 Thiol-ene coupling [13] and (5) Transesterification/Amidation [14]. In despite of this, the first  
70 methods are the most widely used. Regularly, the researchers use this method in one or two steps.  
71 "The one step reaction consists of the in-situ epoxidation followed by hydroxylation using acetic and  
72 sulfuric acids and hydrogen peroxide. The two-step reaction deals with the triglyceride epoxidation  
73 followed by the ring-opening of oxirane, based on the use of difunctional molecules such as alcohols  
74 or amines" [15, 16]. This multi-step synthesis would unquestionably increase the cost of bio-polyol  
75 production.

76 It is important to mention that various vegetable oils, including palm, soybean, sunflower,  
77 rapeseed, and canola oils are used with slight modifications to produce polyols [17-22]. The great  
78 inconvenience with some of these oils are their use in food, which bring as a consequence a global  
79 imbalance to the food supply and demand in the industrial market [23].

80 Therefore, this study concentrates in the obtention of new bio-polyols from two non-edible oil  
81 extracts from seeds of *Colliguaya Integerrima* and *Colliguaja Salicifolia* by a one-single step reaction  
82 using a mixture of hydrogen peroxide and acetic acid. In addition, we characterized the prepared oils  
83 and polyols using various physico-chemical, spectroscopic, and thermo-analytical methods.

84 *Colliguaja Integerrima* and *Colliguaja Salicifolia* are two varieties of the *Euphorbiaceae*  
85 family. The *Euphorbiaceae* family, with around 300 genera and over 7,000 species, is one of the

86 largest and most diverse families of flowering plants [24]. Both species grow wild in South America,  
87 specifically in the phytogeographical provinces of Patagonia and Monte in Argentina and Chile [25-  
88 27]. The oil extracted from these two species are known for the diuretic activity of their aqueous  
89 extract [28]. To our knowledge, no studies have been previously reported about the production of  
90 polyols from *Colliguaja Integerrima* and *Colliguaja Salicifolia* using a cheap and environmentally  
91 benign method.

92

## 93 2. Experimental Procedures

### 94 2.1. Chemicals and reagents

95 Diethyl ether (C<sub>4</sub>H<sub>10</sub>O), *n*-hexane, glacial acetic acid (AcOH), hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>),  
96 toluene (C<sub>7</sub>H<sub>8</sub>), sulfuric acid (H<sub>2</sub>SO<sub>4</sub>), sodium sulfate (Na<sub>2</sub>SO<sub>4</sub>), sodium carbonate (Na<sub>2</sub>CO<sub>3</sub>), sodium  
97 thiosulfate pentahydrate and potassium hydroxide (KOH) were supplied by Arquimed (Santiago,  
98 Chile). Iodine monochloride solution (Wijs reagent), Starch solution, tetrahydrofuran (THF) and  
99 Phenolphthalein reagent were purchased from Sigma-Aldrich (St. Louis, MO, USA). All used  
100 reagents were of analytical grade with exception of *n*-hexane and tetrahydrofuran (HPLC purity  
101 grade). For GC-MS analysis, Supelco® 37 component fatty acid methyl ester (FAME) mix in  
102 dichlorometane (varied concentrations) was purchased from Sigma-Aldrich.

103

### 104 2.2. *Colliguaya integerrima* and *Colliguaya salicifolia* seeds.

105 The seeds of *Colliguaya Salicifolia* and *Colliguaya Integerrima* were collected in  
106 Cayurranquil, a geographic area in the Cauquenes Province (725468, 6017270) and the Pehuenche  
107 International Pathway, Los Cóncores, at the foothills of Talca (348271, 6026739) Chile, respectively.

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### 109 2.3. Vegetable oil extraction

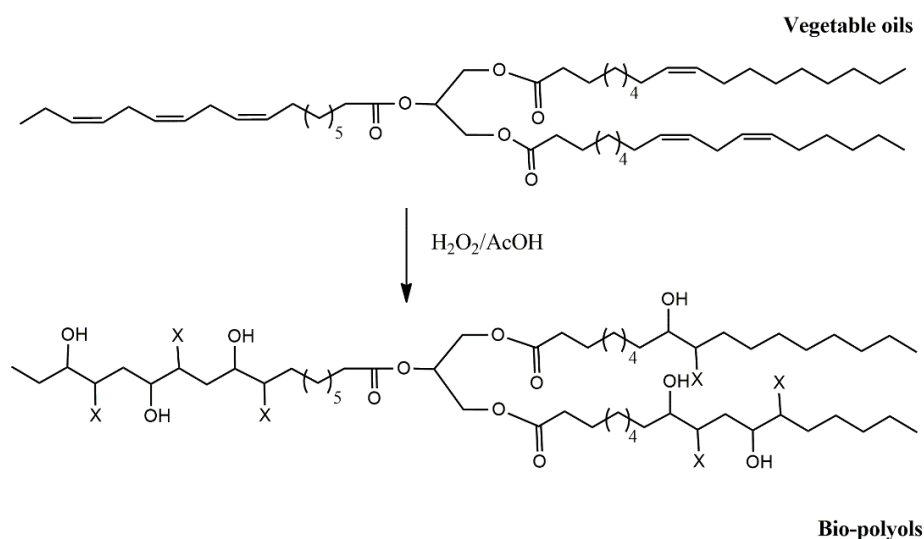
110 Oil extraction was performed according to the AOAC method Am2-93 [29]. About 250 g of  
111 *Colliguaya integerrima* seeds were extracted using *n*-hexane (150 mL) as an extraction solvent in a  
112 Soxhlet apparatus. After 8 hours, the *n*-hexane was removed by distillation under reduced pressure at  
113 40 °C. The *Colliguaya integerrima* orange oil (CIO) obtained was stored at 4 °C under inert  
114 atmosphere until further investigation. The extraction was performed in triplicate for each harvested  
115 sample obtaining a 26% yield. The same procedure was used for the *Colliguaya salicifolia*, but in this  
116 case the oil (CSO) obtained had a yellow coloration with 23% of yield.

117

### 118 2.4. Synthesis of *Colliguaja Integerrima* and *Colliguaja Salicifolia* polyol

119 The synthesis of the polyols was carried out following the methodology described by  
120 Monteavaro et al. [30], with slight modifications (See Scheme 1). As Scheme 1 shows, the idealized  
121 structure of polyols has a saturated hydrocarbon structure with one OH and one acetate group per  
122 double bond. A solution of 5g (5,6 mmol) of *Colliguaja Integerrima* oil and 9.30 mL (0.162 mol) of  
123 glacial acetic acid in 20 mL of toluene with some drops of sulfuric acid were placed into a 3-necked

124 flask equipped with a mechanical stirrer, reflux condenser and isobaric funnel. The mixture was  
 125 mechanically stirred at room temperature until complete homogenization. After that a solution of 30%  
 126 H<sub>2</sub>O<sub>2</sub> (5.30 mL) was slowly added controlling the temperature. When the H<sub>2</sub>O<sub>2</sub> addition was  
 127 completed, the mixture was heated to 60°C for 12 hours. Then the reaction mixture was cooled to  
 128 room temperature and a 10% wt/vol sodium bisulfide solution was added and the mixture was stirred  
 129 for 20 min to eliminate excess peroxide. After that, 50 ml of ethyl ether was added to the mixture,  
 130 and the organic phase was washed several times with 10% wt/vol sodium carbonate solution to neutral  
 131 pH. Finally, the organic phase was dried over sodium sulfate and concentrated under vacuum to  
 132 eliminate the ethyl ether to obtain the *Colliguaja Integerrima* polyol (CIP). The same procedure was  
 133 used for the synthesis of *Colliguaja salicifolia* polyol (CSP).



134 where X = AcO

135 **Scheme 1.** Synthesis of vegetable oil-based polyols without unsaturation.

136

### 137 2.5. Characterization methods used for oils and polyols.

138 The *Colliguaja Integerrima* and *Colliguaja Salicifolia* oils and polyols were characterized  
 139 determining the fatty acid composition, the oxidizability value (Cox), acid value (AV), iodine value  
 140 (IV), saponification number (SN), kinematic viscosity, peroxide value (PV), density, hydroxyl  
 141 number, thermogravimetric analysis (TGA), Fourier-transform infrared (FT-IR), <sup>1</sup>H and <sup>13</sup>C NMR  
 142 spectroscopy. It is important to note, that the fatty acid composition, peroxide value and the  
 143 oxidizability value were performed only for the studied oils, the rest of the characterization techniques  
 144 were done for the *Colliguaja Integerrima* and *Colliguaja Salicifolia* oils and polyols.

145 The fatty acid profile was determined only for the *Colliguaja Integerrima* and *Colliguaja*  
146 *Salicifolia* oils as fatty acid methyl esters by gas chromatography-mass spectrometry. The methyl  
147 esters were prepared using the method described by Morrison and Smith [31]. The separation of the  
148 fatty acid esters was performed using QP 5000 Shimadzu (Kioto, Japan) gas chromatographer with  
149 mass spectrometer and autosampler was used, as well as the 1.2 Classs-5000. A fused-silica column  
150 coated with the DB-5 stationary phase was utilized (30 m X 0.2 mm inner diameter, dry film thickness  
151 of 0.25  $\mu\text{m}$ , J & W Scientific). The initial oven temperature was 60  $^{\circ}\text{C}$ , which was kept for 5 minutes;  
152 a 2  $^{\circ}\text{C min}^{-1}$  temperature increase was programed until it reached 220  $^{\circ}\text{C}$ ; this temperature was kept  
153 for 30 minutes. The injector temperature was 220  $^{\circ}\text{C}$ . Helium was used as a carrier gas with a 1.0 mL  
154  $\text{min}^{-1}$  flow. The injection volume was 1  $\mu\text{L}$  (1% solution in  $\text{CH}_2\text{Cl}_2$ ) with a 1:10 slipt ratio. Column  
155 pressure was 100 kPa. Mass detector conditions were the following: source temperature, 240  $^{\circ}\text{C}$ ;  
156 electron impact mode (EI), 70 eV; scan rate of 1 scan  $\text{s}^{-1}$ , and acquisition range, 29-450 u. Components  
157 were identified by comparing retention times related to a linear standard made with Supelco® 37  
158 Component FAME Mix in dichlorometane (varied concentrations) of an alkane series (C9-C24) and  
159 their mass spectra to those from the Wiley 330000 database and the ones reviewed from the literature.  
160 In addition, with the percentage of unsaturated fatty acids we calculated the oxidizability values (Cox)  
161 of *Colliguaja Integerrima* and *Colliguaja Salicifolia* oils, applying the formula proposed by Fatemi  
162 et al. [32]:

$$163 \quad \text{Cox} = \frac{[1(16:1\%+18:1\%+20:1\%)+10.3(18:2\%+20:2\%)+21.6(18:3\%)]}{100} \quad (1)$$

164 The acid value, iodine value, peroxide value and saponification number of the obtained samples  
165 (*Colliguaja Integerrima* and *Colliguaja Salicifolia* oils and polyols) were determined according to  
166 the AOCS Official Method Cd 3d-63, AOAC Official Method 920.158 (Hanus method), AOAC  
167 Official Method 965.33 and the AOAC Official Method 920.160, respectively [33, 34].

168 The structure of samples (*Colliguaja Integerrima* and *Colliguaja Salicifolia* oils and polyols)  
169 were analyzed by  $^1\text{H}$ ,  $^{13}\text{C}$  NMR and FT-IR spectroscopy combined with hydroxyl number  
170 measurement.  $^1\text{H}$  and  $^{13}\text{C}$  NMR spectra were conducted with a Varian Inova 300 (Varian, Inc., Palo  
171 Alto, CA, USA), 300 MHz, using  $\text{CDCl}_3$  as a solvent and tetramethylsilane as an internal reference.  
172 FT-IR spectra were recorded by using Agilent Cary 360 FTIR in the range of 4000 to 650  $\text{cm}^{-1}$  at a  
173 resolution of 4  $\text{cm}^{-1}$  with 32 scans on ATR (Agilent Technologies, Palo Alto, CA, USA). 2 mL of the  
174 *Colliguaja Integerrima* and *Colliguaja Salicifolia* oil and polyol samples were put directly on the  
175 equipment plate without any previous treatment. The hydroxyl number of the *Colliguaja Integerrima*  
176 and *Colliguaja Salicifolia* polyols was determined according to ASTM 4274-05 [35]. The viscosity  
177 of the *Colliguaja Integerrima* and *Colliguaja Salicifolia* oil and polyol samples were measured by

178 Brookfield viscometer (LVDV-II, Brookfield Engineering Laboratories, Inc., Stoughton,  
179 Massachusetts) at  $25 \pm 0.5$  °C. The density of the *Colliguaja Integerrima* and *Colliguaja Salicifolia*  
180 oil and polyol samples were measured by means of a pycnometer at  $25 \pm 0.5$  °C. Finally, thermal  
181 stability of the oils and polyols were performed in a thermogravimetric analyzer NETZSCH TG 209F1  
182 Iris (NETZSCH Company, Germany) with  $10$  °C  $\text{min}^{-1}$  constant heating rate. The heating was from  
183  $30$  °C to  $500$  °C in inert atmosphere with a flow rate of  $60$  mL  $\text{min}^{-1}$ .

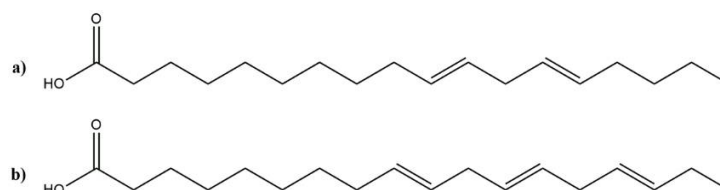
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### 185 3. Results and Discussion

#### 186 3.1. Physico-chemical characteristics of vegetable oils

187 The chemical composition and characteristics of the precursor of polyols (*Colliguaja*  
188 *Integerrima* and *Colliguaja Salicifolia* oils) used in this study are shown in Table 1. In addition, we  
189 determined the acid value, cox value, iodine value, peroxide value, saponification number, kinematic  
190 viscosity, theoretical molecular weights and density of these oils.

191 As can we see, the saturated fatty acids (SFA) of the oils differ very little, because the  
192 percentage of palmitic acid, which is the main SFA, is similar in the two studied oils. On the other  
193 hand, the percentages of unsaturated fatty acids (UFA), were 87.36 and 88.23% for CIO and CSO,  
194 respectively. Specifically, the dominant constituents (over 80%) of both studied oils are C18 fatty  
195 acids in despite of there also being about 7 % of C20 fatty acids. The percentage value of linoleic acid  
196 (C 18:2) was observed in 31.11% and 20.40% for CIO and CSO, respectively. The main differences  
197 between CIO and CSO oils are derived from the percentage of linolenic acid (C 18:3), observed in  
198 26.39 and 46.60, respectively. Figure 1 shows the chemical structures of linoleic and linolenic acids  
199 found in CIO and CSO oils. It is important to note, that this difference in the distribution of the double  
200 bonds in the fatty acid chains are fundamental for knowing the possibilities of increasing OH groups  
201 in the polyols synthesized using these oils and directly proportional to their potential as a future  
202 polyurethane foam.



204 **Figure 1.** Chemical structures of linoleic (a) and linolenic (b) acids found in CIO and CSO oils.

205

206 Taking into account the above mentioned and using the measured composition (lipid profile),  
207 we measured the degree of unsaturation by the iodine value (IV), which is directly related to the Cox



208 value for CIO and CSO oils. The results for CIO and CSO oils indicated values of IV (143.8 and  
209 179.3 g I<sub>2</sub>/100 g, respectively) and Cox (9.35 and 12.46, respectively), providing it a particular  
210 resistance to oxidation. The saponification value (SN), which is a parameter related with the  
211 molecular mass of the fatty acids found in the oil, was also studied. The SN values for CIO and CSO  
212 oils were 196 and 194 mg KOH/g oil, respectively, which are in the average SN range of 175-250  
213 mg/g reported for common vegetable oils [36]. It should be noted that these values don't show  
214 significant differences, which means that the fatty acid composition of the studied oils are similar in  
215 molecular weight. It is known that acid value (AV) measures the number of carboxylic acid groups  
216 present in fat or oil; this value must not be too high, because it is a result of the hydrolysis of  
217 triglycerides. The highest acid value was found for CSO (0.25 mg KOH/g oil), however, the AV for  
218 both studied oils was less than 1.0 mg KOH/g oil (See Table 1), indicating that oils did not undergo  
219 hydrolytic processes. Additionally, the peroxide value (PV) of CIO and CSO were similar and less  
220 than 20 meq/kg, respectively, indicating that these oils were unoxidized and of high initial quality.

221 Table 1 also gives the approximate average molecular weights ( $M_w$ ) for CIO and CSO. The  $M_w$   
222 of oils were calculated averaging the individual molecular weights of each constituent triglyceride,  
223 according to Stavarache et al. [37]. The results showed values of 873.7 and 872.9 g/mol for CIO and  
224 CSO, respectively. It is important to highlight that the calculated theoretical molecular weight is based  
225 on the assumption that no dimers and trimers were formed.

226 Finally, we also measured the kinematic viscosity and density for CIO and CSO oils. Generally,  
227 the kinematic viscosity is related to a measure of the internal friction or resistance of an oil to flow.  
228 According to Krisnangkura et al. [38], viscosity may be considered the interaction forces of  
229 molecules. The viscosity values shown in Table 1 were 58.6 and 48.8 mm<sup>2</sup>/s for CIO and CSO oils,  
230 respectively. The difference in these values is due to the degree of unsaturation presented in both  
231 studied oils and are in concordance with the results reported by Rodrigues Jr et al. [39]. In this  
232 research, Rodrigues Jr reported that one double bond increased the viscosity, whereas, two or three  
233 double bonds caused a decrease in the viscosity of the systems. On the other hand, density is an  
234 important physical characteristic of any substance and is the weight of a unit volume of fluid [40]. In  
235 this case, the values reported in Table 1 are 0.884 and 0.896 g/cm<sup>3</sup> for CIO and CSO oils, respectively.  
236 It is important to know that all reported values shown in Table 1 (physical characteristics) of CIO and  
237 CSO oils had a drastic change in their numerical values when the oils became their respective polyols.

238

239 **Table 1.**

240 Chemical composition and characteristics of *Colliguaja Integerrima* (CIO) and *Colliguaja Salicifolia*  
241 (CSO) oils.

Parameters	Oils	
	CIO	CSO
<b>Fatty acid (%)</b>		
<b>Myristic, C<sub>14:0</sub></b>	0.06	0.04
<b>Palmitic, C<sub>16:0</sub></b>	10.54	8.46
<b>Palmitoleic, C<sub>16:1</sub></b>	0.05	0.08
<b>Margaric, C<sub>17:0</sub></b>	0.00	0.00
<b>Stearic, C<sub>18:0</sub></b>	2.03	2.06
<b>Oleic, C<sub>18:1</sub></b>	23.50	15.08
<b>Linoleic, C<sub>18:2</sub></b>	31.11	20.40
<b>Gamma- linolenic's, C<sub>18:3</sub></b>	0.48	0.00
<b>Alpha-linolenic's, C<sub>18:3</sub></b>	26.39	46.60
<b>Gondoic, C<sub>20:1</sub></b>	5.35	6.34
<b>Eicosadienoic C<sub>20:2</sub></b>	0.48	0.73
<b>Cox value</b>	9.35	12.24
<b>AV [mg KOH/g oil]</b>	0.17	0.25
<b>IV [g I<sub>2</sub>/100 g oil]</b>	143.8	179.3
<b>PV [meq O<sub>2</sub>/kg oil]</b>	19	18
<b>SN [mg KOH/g oil]</b>	196	194
<b>Kinematic Viscosity [mm<sup>2</sup>/s]</b>	58.6	48.8
<b>Density [g/cm<sup>3</sup>]</b>	0.884	0.896
<b>Molar Mass [g/mol]</b>	873.7	872.9

242

243 *3.2. Synthesis and characterization of Colliguaja Integerrima and Colliguaja Salicifolia polyols*  
 244 *prepared by a one-step synthesis*

245 The main goal of our research was to prepare polyols from CIO and CSO oils, respectively.  
 246 *Colliguaja Integerrima* and *Colliguaja Salicifolia* polyols (CIP and CSP, respectively) were prepared  
 247 by a one-step synthesis using the acetic acid/H<sub>2</sub>O<sub>2</sub> system. The results reveal a wide difference of  
 248 physicochemical characteristics among both obtained polyols and its starting oils. The measures of  
 249 OH functionality was given an idea of the characteristics of the polyol obtained. For example, if the  
 250 reaction was complete we obtained a polyol with high OH functionality. On the contrary, if the  
 251 reaction was partial we obtained a polyol with remaining epoxy groups. These two results will be  
 252 depending on the reaction conditions. As previously mentioned, we obtained CIP and CSP polyols

253 with OH numbers of 225.0 and 240.8 mg KOH/g (See Table 2), respectively. According to these  
254 values, it is evident that both hydroxylation reactions to obtain the CIP and CSP polyols were  
255 complete, which are coherent with the NMR and FT-IR results.

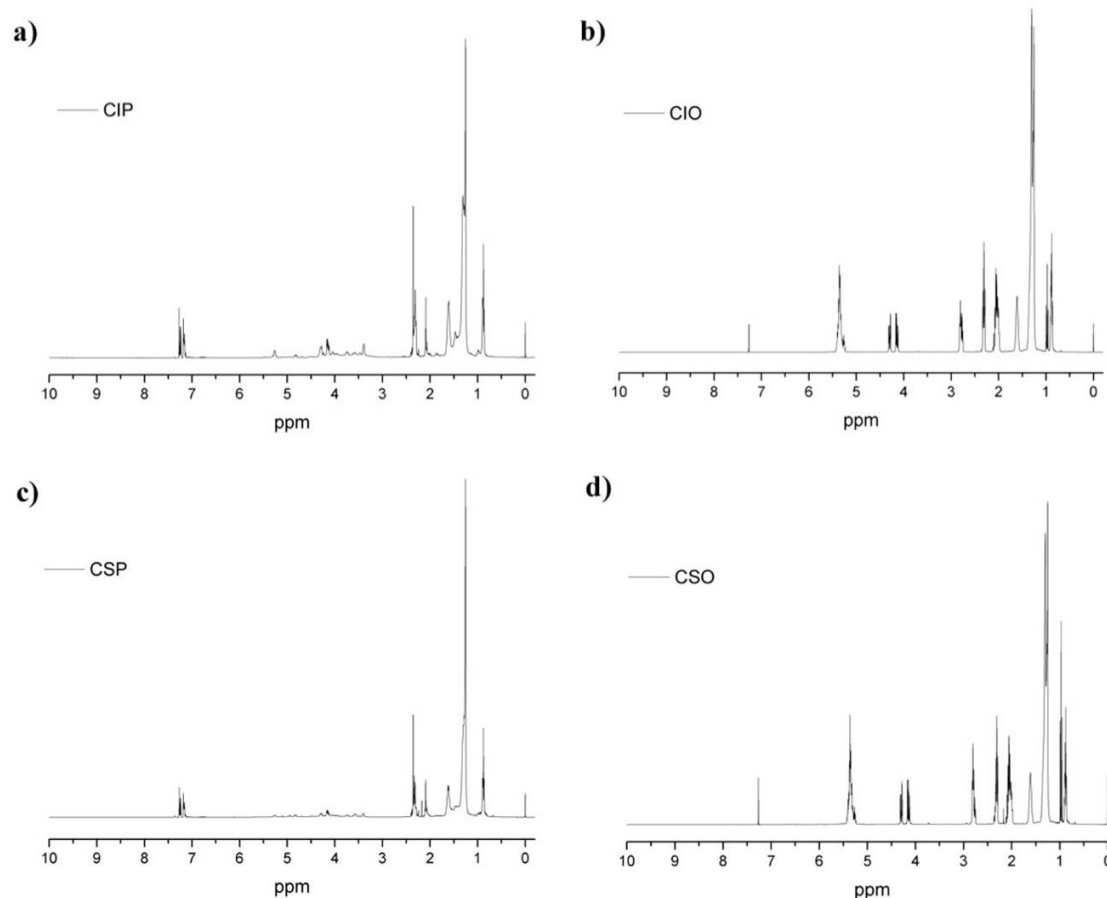
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### 257 3.2.1. $^1\text{H}$ and $^{13}\text{C}$ NMR Analysis

258 The functional group present in the CIP and CSP polyols with their respective starting oils were  
259 confirmed by  $^1\text{H}$  NMR and FT-IR analysis and the results are shown in Figure 2 and 3, respectively.  
260 Due to the large quantity of obtained results, we reported in Figure S1 (See supporting information)  
261 the  $^{13}\text{C}$  NMR spectra of the studied samples (CIP CSP CIO and CSO). It is known that polyols are a  
262 complex blend of products. For that reason, the NMR spectra analysis was performed by zone because  
263 each zone gives indications about the average structure of polyols.

264 Figure 2a and c shows the  $^1\text{H}$  NMR spectra of CIP and CSP polyols, respectively. The main  
265 difference between polyols and their corresponding oils (Figure 2b and d) in the  $^1\text{H}$  NMR spectra  
266 were the appearance of new peaks in the zone between 3.27 - 3.83 ppm, which are assigned to the  
267 presence of methylene protons attached to the hydroxyl group (-CH-OH). In addition, the signal  
268 corresponding to the olefinic hydrogen (-CH=CH-) that appeared in the zone between 5.32 - 5.44  
269 ppm disappeared, suggesting that polyol structures were practically without unsaturation. Finally, the  
270 absence of signals in the zone between 2.8 and 3.2 ppm, relative to the epoxide groups (-CH(O)CH-  
271 ), confirmed the occurrence of the hydroxylation reaction to obtain the CIP and CSP polyols.

272 On the other hand, the  $^{13}\text{C}$  NMR spectra of CIP and CSP polyols with their respective starting  
273 oils offers similar information. These spectra were characterized by the almost disappearance of the  
274 ethenic double bond signs of both starting oils and the appearance of a new sign in 75.32 ppm, which  
275 corresponds to -CH-OH groups formed during the epoxy opened ring. In agreement with the results  
276 obtained by the  $^1\text{H}$  NMR spectra, the signals centered in 54.38 ppm, relative to the epoxide groups  
277 nonappearance, proved the formation of polyols. Finally, the signal found at 173-175 ppm, relative  
278 to the carbonyl ester, showed a peak present in both oils and polyols.



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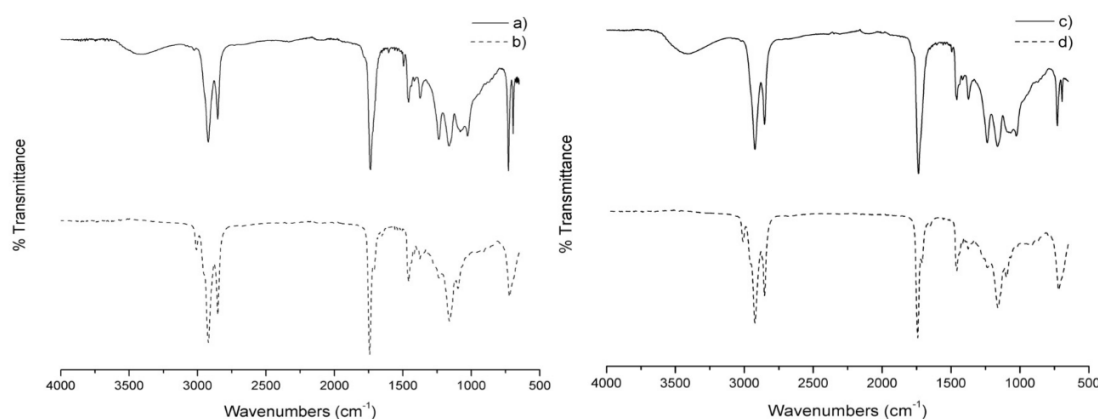
280 **Figure 2.**  $^1\text{H}$  NMR spectra of CIP (a), CSP (c) polyols with their respective CIO (b) and CSO (d)  
 281 oils.

282

### 283 3.2.2. FT-IR Analysis

284 In order to complement the NMR analysis, the successful conversion of CIO and CSO oils into  
 285 polyols was confirmed qualitatively by FTIR spectroscopy. These spectra are compared in Figure 3a-  
 286 d, respectively. Figure 3a and c shows the FT-IR spectra of CIP and CSP polyols, respectively. Both  
 287 polyols FT-IR spectra exhibited a broad peak centered approximately at  $3400\text{ cm}^{-1}$ , which were  
 288 assigned to the presence of hydroxyl (-OH) stretching vibration. Another difference between CIP and  
 289 CSP polyols with their respective oils was the most intensive band (C=O, carbonyl stretching),  
 290 attributed to the presence of the ester linkage. It slightly shifted from  $1748.0$  to  $1738.8\text{ cm}^{-1}$  for CIO  
 291 oils and CIP polyol, respectively. The same behavior was found for CSO oils and the CSP polyol, in  
 292 this case the band slightly shifted from  $1743.7$  to  $1734.3\text{ cm}^{-1}$ , respectively. Another important  
 293 asymmetrical stretching band present in both FTIR spectra polyols corresponded to C-O-C groups at  
 294  $1158\text{ cm}^{-1}$ . It is important to mention that the absence of the bands at around  $870$  and  $920\text{ cm}^{-1}$ ,

295 assigned to the epoxy groups in both spectra polyols, corroborate that the hydroxylation reaction of  
296 the oils was complete. Finally, the bands at 2919.6 and 2846.1  $\text{cm}^{-1}$  and 2924.3 and 2850  $\text{cm}^{-1}$   
297 assigned to asymmetrical and symmetrical stretching CH groups, for CIP and CSP polyols,  
298 respectively, were also detected. This evidence from FTIR analysis confirmed the formation of  
299 polyols and the results obtained by  $^1\text{H}$  and  $^{13}\text{C}$  NMR.



300

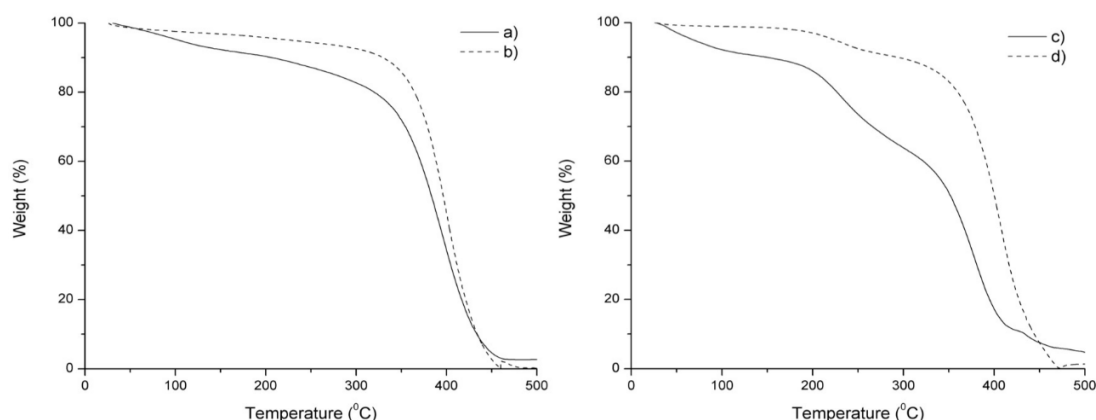
301 **Figure 3.** FT-IR spectra of CIP (a), CSP (c) polyols whit their respective CIO (b) and CSO (d) oils.

302

### 303 3.2.3. TGA Analysis

304 In order to investigate the influence of the structure and composition on thermal stability of the  
305 oils and polyols, thermogravimetric analysis was performed in the interval from 30 to 600  $^{\circ}\text{C}$ . The  
306 TGA (TG) curves and their calculated derivatives (DTG) are shown in Figures 4 and S2 (See  
307 supporting information), respectively. Following the same analysis used for NMR and FTIR  
308 discussion, we compare the thermograms obtained for polyols and their respective oils. As seen in  
309 Figure 3a and c, the weight loss curves for the thermal degradation of both polyols closely resembles  
310 the TG and DTG curves of their starting oils. Specifically, CIP and CSP polyols exhibited slightly  
311 minor thermal stability compared to its oil. In addition, the initial weight loss observed under 100 $^{\circ}\text{C}$   
312 in the TG curve in both polyols could be attributed to the loss of the residual water molecules. In the  
313 oils at 100 $^{\circ}\text{C}$  this weight loss was not observed. The total weight loss for both polyols was about 95%,  
314 meanwhile oils degrade completely [41]. We suggest that these results could be due to the presence  
315 of hydroxyl groups in the polyol.

316 The TG curve of CIP polyol indicates another degradation stage (Figure 4a), which is reflected  
317 as a single peak in the DTG curve (Figure S2a) at 400.24 $^{\circ}\text{C}$ . On the other hand, a quite different  
318 decomposition was observed for the CSP polyol; its major decomposition occurred in three steps  
319 starting at 196  $^{\circ}\text{C}$ , 390 $^{\circ}\text{C}$  and 428 $^{\circ}\text{C}$ , respectively.



320

321 **Figure 4.** TGA curve of CIP (a), CSP (c) polyols with their respective CIO (b) and CSO (d) oils.

322

323 *3.2.3.4. Physico-chemical characteristics of vegetable polyols*

324 Moreover, we determined the acid value (AV), iodine value (IV), saponification number (SN),  
325 kinematic viscosity ( $\nu$ ), theoretical molecular weights ( $M_w$ ), density ( $\rho$ ), and OH numbers of the polyols  
326 and the results are also included in Table 2.

327 The AV and SN for the polyol samples were higher when compared to the starting oils. It is  
328 important to mention that the CIP and CSP polyol samples did not contain free acids other than fatty  
329 acids; then, the acid value may be directly converted to percent free fatty acids. Hence, the slight  
330 increase in the AV and SN could be associated with the possible deterioration of the studied oils at  
331 the moment of producing polyols, such as rancidity. Dileesh et al. reported that the cause for rancidity  
332 is the hydrolytic or oxidative cleavage of triglycerides causing the formation of free fatty acids in oils  
333 or fats [42]. The same behavior occurred with the values of kinematic viscosity and density, both  
334 values are major as expected. In the case of the viscosity, the values for CIP and CSP polyols were  
335 3638.48 and 5748.86 mm<sup>2</sup>/s, respectively. The big difference in these values were due to the hydrogen  
336 bonding, which was directly proportional to the major amount of OH groups present in the CSP polyol  
337 (see OH functionality in Table 2). The obtained results showed a similarity tendency with the results  
338 reported by Knothe and Steidly [43]. In this study the authors mentioned that free fatty acids or  
339 compounds with hydroxy groups possessed significantly higher viscosity than the starting material  
340 without hydroxy groups. Additional proof that the hydrolysis reaction of CIO and CSO had occurred  
341 was reflected in the iodine values of their respective polyols. While examining the iodine values for  
342 the CIP and CSP polyols and their respective oils, the values decreased dramatically, which was  
343 evident since the unsaturation (C=C bonds) in the CIO and CSO oils were replaced by hydroxyl  
344 groups.

345 Furthermore, we determined the OH functionality, which is an important indicator of the  
 346 crosslinking that can be obtained in future polyurethane foams. To calculate this parameter, we used  
 347 the OH number obtained by a procedure described in section 2.5, and the formula proposed by  
 348 Zlatanić et al. [44].

349 The OH numbers of the CIP and CSP polyols were 225.0 and 240.8 mg KOH/g, respectively.  
 350 The theoretical molecular weight ( $M_w$ ) shown in Table 2 for CIP and CSP polyols (1122.4 and 1166.1  
 351 g/mol, respectively) were calculated from the composition of polyols based on assumption that no  
 352 oligomers were formed and considering that one OH group was formed per double bond. The OH  
 353 functionality results showed values of 4.50 and 5.00 for CIP and CSP polyols, respectively. It's  
 354 important to note that these differences between the OH values were due to the fatty composition of  
 355 the starting oils. According to these values, we can expect the preparation of rigid foams [45]. Rigid  
 356 polyurethane foams are widely used in engineering applications such as thermal insulation, building  
 357 materials, chemical pipelines, space filling, among others [46].

358

359 **Table 2.**

360 Chemical composition and characteristics of *Colliguaja Integerrima* (CIP) and *Colliguaja Salicifolia*  
 361 (CSP) polyols.

Parameters	Polyols	
	CIP	CSP
AV [mg KOH/g]	4.50	12.95
IV [g I <sub>2</sub> /100 g]	0.2	0.5
SN [mg KOH/g]	227	235
Kinematic Viscosity [mm <sup>2</sup> /s]	3638.48	5748.86
Density [g/cm <sup>3</sup> ]	1.012	0.921
Molar Mass [g/mol]	1122.4	1166.1
OH numbers [mg KOH/g]	225.0	240.8
OH functionality	4.50	5.00

362

363

#### 364 4. Conclusion

365 Two novel polyols were successfully synthesized from two non-edible vegetable oils,  
366 *Colliguaja Integerrima* and *Colliguaja Salicifolia*, by in situ epoxidation and hydroxylation of oils in  
367 a one single step. The physico-chemical and spectroscopic analysis presented above successfully  
368 characterized the reaction of polyols formation. Specifically, the FTIR, TGA and NMR spectroscopic  
369 results confirmed complete disappearance of the signature of the double bonds present in the  
370 vegetable oils and the incorporation of hydroxyl groups to form their respective polyols. In addition,  
371 the iodine value, acid value, hydroxyl number, hydroxyl functionality, density and viscosity of the  
372 synthesized polyols were also successfully determined. All these values were higher for CIP and CSP  
373 polyols when compared to starting oils, with the exception of the iodine value which decreased near  
374 to 0. Finally, the data collected in this study have established an essential starting point for the  
375 obtention of new materials. Specifically, we plan for a future study to examine the obtention of a new  
376 class of rigid polyurethane foams that could be used in engineering applications.

377

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379

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