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Article

Fibrinolytic Enzyme from Green Microalgae: A New Potential Drug for Thrombolytic Therapy?

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Abstract: Thrombosis is characterized by the pathological formation of fibrin clots within a blood vessel, leading to the obstruction of blood flow. Fibrinolytic enzymes from microorganisms have exhibited promising effects to dissolve clots in a more efficient and safe way. Then, the aim of this study was to evaluate the biomass and fibrinolytic enzyme production of *Tetradesmus obliquus* under autotrophic and mixotrophic conditions using different concentration of corn steep liquor (CSL). Different extraction and precipitating methods were tested, and the enzyme was purified by ion exchange chromatography. More advantageous culture condition was mixotrophic using 0.25% CSL, showing the highest values of biomass productivity ($P_x = 169.3 \pm 44.36 \text{ mg} \cdot \text{L}^{-1} \text{ day}^{-1}$) and specific growth rate ($\mu_{\text{max}} = 0.17 \pm 0.00 \text{ day}^{-1}$), and significant fibrinolytic production ($391.34 \pm 40.03 \text{ U} \cdot \text{mg}^{-1}$). Moreover, fibrinolytic activity was higher when extracted by homogenization and precipitated using acetone, which exhibited clear zone of fibrin degradation in the fibrinolytic plate assay. Additionally, the purified enzyme showed specific activity of $1176.90 \pm 140.37 \text{ U} \cdot \text{mg}^{-1}$ and molecular weight around 97 kDa. Finally, the enzyme has higher enzymatic activity than various fibrinolytic enzymes, and the obtained enzyme has potential to be developed as a therapeutic agent in thrombosis treatment. Additional studies are need to investigate the biochemical properties and biological profile of this enzyme.

Keywords: thrombosis; kinetic parameters; cell growth; protein purification; biomass production; Chlorophyceae; agro-industrial sub-product; extraction methods; molecular weight; chromatography

1. Introduction

Cardiovascular diseases (CVDs) are main cause of death worldwide and are responsible for about 32% of all global deaths [1]. Thrombosis is a severe CVD complication characterized by the pathological formation of fibrin clots that cause obstruction of blood flow, leading to intense clinical manifestations such as acute ischemic stroke, myocardial infarction, and venous thromboembolism [2,3].

In general, conventional thrombosis treatment are based on antiplatelet or anticoagulant agents, which can cause severe bleeding leading to hemorrhage [4,5]. Alternatively, fibrinolytic enzymes such as tissue plasminogen activator (t-PA), urokinase (u-PA), and streptokinase have been widely used for thrombosis therapy. However, these drugs have some limitations including short half-life, low specificity to fibrin, high cost, and excessive bleeding [6]. Thus, finding more effective and safe fibrinolytic enzymes have become the key to thrombosis treatment.

In this sense, studies have reported the promising antithrombotic effects of fibrinolytic agents from photosynthetic microorganisms such as *Chlorella vulgaris* and *Arthrosphaera platensis* [7,8]. In addition, some bioactive such as lectin, linoleic acid, and flavonoids extracted from

microalgae *Tetraedesmus obliquus* showed anticancer and antimicrobial activities [9–11]; however, there is no report on the fibrinolytic potential of this genus.

The production of microalgae has tripled in the last 5 years and it has attracted interest in research and industrial fields worldwide due to some characteristics such as high photosynthetic efficiency, fast growth rate, resistance to various contaminants, capacity to grow on non-arable lands, and be cultured using different metabolic pathways (autotrophic, heterotrophic, and mixotrophic growth modes) [12–14]. Specifically, previous studies have shown that mixotrophic conditions using different organic carbon substrates provide higher production of enzymes and increase biomass yields from *T. obliquus* [15,16].

Organic wastes and by-products are frequently used as substrates for mixotrophic growth and are advantageous for sustainable resource recycling and cost reduction of microalgal production [17]. Corn steep liquor (CSL) is a by-product from the corn wet milling industries and has high amounts of carbohydrates, amino acids, vitamins, organic acids and minerals, being a nitrogen-rich source used for microalgal cultivation [18]. By the way, this by-product has been successful to production of fibrinolytic enzymes from *C. vulgaris* and *A. platensis* [7,8]; but not yet on *T. obliquus* cultivation. So, this study aims to evaluate and compare the biomass and fibrinolytic enzymes productions from *Tetraedesmus obliquus* cultivated under autotrophic and mixotrophic (using CSL) growth conditions.

2. Materials and Methods

2.1. Culture media and growth conditions

Tetraedesmus obliquus (SISGEN A5F5402) was isolated from Açude of Apipucos (Recife, Pernambuco, Brazil, coordinates 8° 1' 13.08" S; 34° 55' 56.51" W) and cultivated under autotrophic condition in 1000 mL Erlenmeyer flasks containing 400 mL of BG-11 medium [19] with an initial concentration of 50 mg·L⁻¹, temperature of 30 ± 1 °C, continuous light intensity of 40 μmol photons m⁻²·s⁻¹, under constant aeration [20]. Mixotrophic condition was defined by the addition of different concentrations of corn steep liquor (0.25, 0.50, 0.75, 1.00, 2.00, and 4.00% (v/v) into BG-11 medium. CSL (Corn Products Brazil, Cabo de Santo Agostinho, PE, Brazil) was previously treated according to Liggett and Koffler [21].

Cell growth was measured daily until to reach the end of the exponential growth phase. Cell biomass was harvested by centrifugation (5,000 rpm for 5 min), washed three times with distilled water, freeze-dried and stored at 4 °C.

Biomass concentration was determined by measuring the optical density (OD) at λ665 nm by a UV/Visible spectrophotometer using an appropriate calibration curve correlating OD665 to biomass concentration (Equation 1, R² = 0.99).

$$\text{Biomass concentration} = 0.0041 \text{ OD}_{665} + 0.0486 \quad (1)$$

2.2. Kinetic parameters

Biomass productivity (P_x) at the end of cultivation was calculated by Equation 2:

$$P_x = \frac{(X_t - X_0)}{t_c} \quad (2)$$

where X_t is the final cell concentration (mg·L⁻¹), X₀ the initial cell concentration (mg·L⁻¹) and t_c time in culture final cell concentration (days).

Maximum specific growth rate (μ_{max}), expressed in day⁻¹, was calculated by the following equation:

$$\mu_{max} = \frac{1}{\Delta t} \ln \frac{X_j}{X_{j-1}} \quad (3)$$

where X_j and X_{j-1} are cell concentrations at the end and the beginning of each time interval (Δt = 1 day).

2.3. Fibrinolytic enzyme extraction

Cell biomass (100 mg·mL⁻¹) was resuspended in 0.02M Tris-HCl buffer pH 7.0 and submitted to two different extraction methods: (1) homogenization by constant stirring for 30 minutes in ice bath (MATSUBARA et al., 2000); (2) sonication using a sonicator (Bandelin Sonoplus HD 2070, Microtip MS 72, Germany) with 20 pulses for 1 minute with intervals of 1 min between each pulse on ice bath (ROMÁN et al., 2022). Both cell extract was centrifuged at 15,000 rpm for 10 minutes at 4 °C and the supernatant used to further analysis.

2.4. Precipitation methods

Cell extract was precipitated using two different solvents: (1) acetone (80%) was added to the cell extract slowly at 4 °C. The precipitated was collected by centrifugation (8,000 rpm for 10 min), after which the pellet was freeze-dried, and stored; (2) ammonium sulfate was added to the cell extract with gentle stirring at 4 °C until the solution was saturated at concentration of 0–40% and 40–70% (w/v). Then, the protein precipitated by centrifugation (8,000 rpm for 10 min) was dissolved in 0.02M Tris-HCl buffer pH 7.4 and dialyzed against the same buffer for 6 h at 25 °C. After dialysis, protease and fibrinolytic activities, and protein content were determined.

2.5. Protein purification

Fibrinolytic enzyme was purified through two-step chromatography using ion exchange and gel filtration. Protein redissolved was loaded on to ion-exchange chromatography using DEAE Sephadex column (1.6 X 50 cm) pre-equilibrated with 0.02M Tris-HCl buffer pH 7.4 at a flow rate of 1 mL·min⁻¹, and the absorbance measured at λ 280 nm. Fractions showing fibrinolytic activity were pooled and concentrated. Weight determination was achieved using Gel Filtration Markers Kit for protein molecular weights 6,500-66,000 Da from Sigma-Aldrich.

2.6. Sodium dodecyl sulfate-polyacrylamide gel electrophoresis

Sodium dodecyl sulfate-polyacrylamide gel electrophoresis (SDS-PAGE) was carried out using a 12% polyacrylamide gel as described by Laemmli [22]. The molecular weight was calibrated using Gel Filtration Markers Kit (6,500-66,000 Da, Sigma-Aldrich). Protein bands were detected by staining with silver.

2.7. Protein concentration analysis

Protein concentration was obtained using the BCA Protein Assay Reagent Kit (BCATM Protein Assay Kit, Thermo SCIENTIFIC). Bovine serum albumin was used as standard.

2.8. Protease activity assay

Protease activity was assayed using azocasein as a substrate. The reaction mixture contained 30 μ L of 0.08 mM azocasein, 140 μ L of 0.02M Tris-HCl pH 7.4, and 30 μ L of the cell-free extract. After 15 min, the reaction was stopped and the absorbance was measured at λ 450 nm using a microplate reader. One unit of azocasein activity was defined as the amount of enzyme required to increase the absorbance by 0.001 per minute, and the protease activity was expressed as activity units [23].

2.9. Determination of fibrinolytic enzyme

2.9.1. Fibrinolytic plate assay

Fibrinolytic activity of the cell extracts was determined on a fibrin plate [24] with adaptations. Typically, the fibrin plate was prepared by mixing 0.45 bovine fibrinogen and 0.02M Tris-HCl buffer pH 7.4 with 2% agarose dissolved in 0.02 M Tris-HCl buffer pH 7.4 and 200 μ L of CaCl₂. The prepared solution was poured into a Petri plate (90 x 15 mm) containing 200 μ L of a thrombin suspension. The fibrinolytic activity of the cell extracts was obtained by creating wells of 5 mm, which were

impregnated with 20 μ L of *T. obliquus* extracts and incubated at 37 °C for 20h. The zone of clearance was defined as the fibrinolytic activity of cell extracts.

2.9.2. Fibrinolytic assay using spectrophotometry

The fibrinolytic activity was evaluated according spectrophotometric method described by Wang [25]. A solution of fibrinogen (0.72%) and 0.02 M Tris-HCl buffer pH 7.4 was placed in a test tube and incubated at 37 °C for 5 minutes. After addition of thrombin (20 U·mL⁻¹) solution, the resulting mixture was incubated at 37 °C for 10 minutes, enzyme solution was added, and incubation continued at 37 °C. The solution was mixed after 20 and 40 minutes. At 60 minutes, reaction was stopped by adding 0.2 M trichloroacetic acid (TCA). Finally, the solution was centrifugated (8,000 rpm for 10 minutes) and the supernatant was measured at λ 275 nm. One unit (U) of fibrinolytic activity was defined as the amount of enzyme required to increase 0.01 units of absorbance per minute.

2.10. Determination of fibrinolytic enzyme

All the experiments were in duplicates and data are presented as the mean \pm standard deviation (SD). The statistical analyses were performed using the t-test and all results are expressed as average error bars showing SD. P values < 0.05 were considered statistically significant.

3. Results and discussion

3.1. Cell growth profile and kinetic parameters of *T. obliquus* cultivation under different growth conditions

Cell growth profiles of *T. obliquus* in autotrophic and mixotrophic growth conditions using different CSL concentrations are shown in Figure 1. No lag phase and exponential phase of 16 days was observed in autotrophic growth (Figure 1), showing the highest X_m values (1970 ± 231 mg·L⁻¹), which can be explained by previously adaptation of *T. obliquus* cells in medium culture constituted by inorganic nitrogen sources such as NaNO_3 and $(\text{NH}_4)_5[\text{Fe}(\text{C}_6\text{H}_4\text{O}_7)_2]$. On the other hand, in mixotrophic cultivation using 0.25% CSL, the exponential growth phase started after 8 days of cultivation obtaining a X_m of 1611 ± 206 mg·L⁻¹. Increasing CSL concentration to 0.50%, *T. obliquus* showed a short two-days lag phase and started the exponential phase on the third day of cultivation (Figure 1), reaching the lowest value of maximum cell concentration ($X_m = 932.68 \pm 82.78$ mg·L⁻¹) on the fifteenth day. This shows that concentrations of CSL higher than 0.50% inhibited *T. obliquus* cells growth. This was also observed in the mixotrophic cultivation of *Arthrosphaera platensis* using CSL concentration above 0.6% which inhibited cell growth [8].

CSL concentration also influenced the cell growth kinetic parameters. As shown in Table 1, the mixotrophic culture using 0.25% CSL showed significantly higher values of biomass productivity ($P_x = 169.3 \pm 44.36$ mg·L⁻¹·day⁻¹) and specific growth rate ($\mu_{max} = 0.17 \pm 0.00$ day⁻¹) than mixotrophic culture using 0.50% CSL ($P_x = 95.72 \pm 10.63$ mg·L⁻¹·day⁻¹; $\mu_{max} = 0.12 \pm 0.00$ day⁻¹). These results show that the high CSL concentration ($>0.50\%$) in mixotrophic cultivation of *T. obliquus* decrease P_x and μ_{max} values probably due to a stress provoked by the excess of nitrogen [26,27]. CSL is rich in protein content (420 mg·g⁻¹) and the mains amino acids available are arginine (44.30 mg·g⁻¹), alanine (35.70 mg·g⁻¹), and glutamic acid (42.00 mg·g⁻¹), showing that CSL is a potential organic N-source [28,29]. By the way, CSL has been considered as a low-cost material for the microbial production of enzymes [17,30,31] and its effects on fibrinolytic enzymes production of *T. obliquus* has not yet been studied. The highest biomass productivity (169.28 ± 44.36 mg·L⁻¹·day⁻¹) was obtained in cultivation using 0.25% CSL which was selected for further steps.

Table 1. Cultivation parameters and enzymatic activities of *T. obliquus* cultivated in different growth conditions.

Growth conditions	X_m (mg·L ⁻¹)	P_x (mg·L ⁻¹ ·di ⁻¹)	μ_{max} (day ⁻¹)	Methods	Total protein (mg·mL ⁻¹)	Protease activity (U·mg ⁻¹)	Fibrinolytic activity (U·mg ⁻¹)
Autotrophic	1970.24 ± 231.10 ^a	112.35 ± 13.51 ^{a,b}	0.19 ± 0.03 ^a	Homogenization	0.93 ± 0.00 ^a	12.48 ± 1.35 ^a	430.46 ± 40.19 ^a
				Sonication	2.99 ± 0.50 ^b	4.50 ± 0.4 ^b	149.44 ± 3.82 ^b
Mixotrophic (CSL 0.25%)	1611.71 ± 206.95 ^a	130.90 ± 12.77 ^a	0.17 ± 0.00 ^a	Homogenization	0.86 ± 0.00 ^c	12.50 ± 2.94 ^a	391.34 ± 40.03 ^a
				Sonication	3.32 ± 0.22 ^b	84.75 ± 3.51 ^c	243.38 ± 11.47 ^c
Mixotrophic (CSL 0.50%)	932.68 ± 82.78 ^b	93.38 ± 10.95 ^b	0.12 ± 0.00 ^b	Homogenization	2.90 ± 0.09 ^b	4.64 ± 3.06 ^b	130.95 ± 0.99 ^b
				Sonication	2.76 ± 0.14 ^b	5.85 ± 3.68 ^b	135.63 ± 6.98 ^b

Maximum cell concentration (X_m), biomass productivity (P_x), specific growth rate (μ_{max}). Data expressed as means ± standard deviations of duplicate experiments. ^{a,b,c,d} Different superscript letters indicate statistically significant differences ($p < 0.05$).

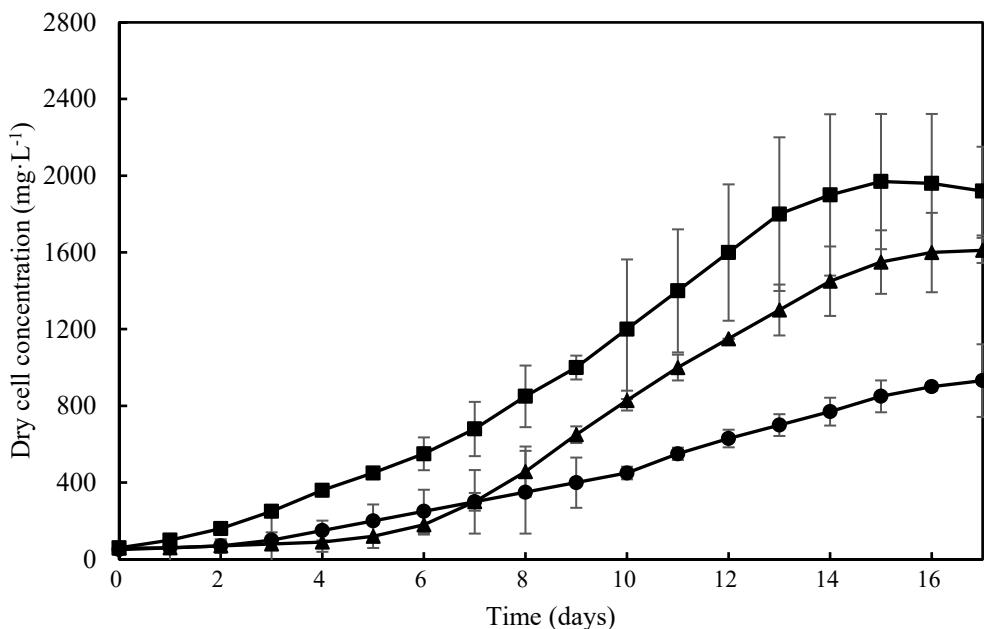


Figure 1. Growth profiles of *Tetraselmus obliquus* cultivated autotrophically and mixotrophically under different concentrations of corn steep liquor: Autotrophic (■), mixotrophic 0.25% (▲), and mixotrophic 0.50% (●).

3.2. Protease and fibrinolytic productions

The choice of growth condition has an important influence on the production of microbial enzymes. As shown in Table 1, *T. obliquus* produced a high amount of protease enzyme when cultivated on mixotrophic condition using 0.25% CSL (84.75 U·mg⁻¹), followed by autotrophic (12.48 U·mg⁻¹) and mixotrophic 0.50% CSL (5.85 U·mg⁻¹) conditions. Moreover, protease activity of *T. obliquus* cultivated on 0.25% CSL is higher than those produced by different marine algae, such as *Ulva lactuca* (6.55 – 7.33 U·mg⁻¹), *Ulva fasciata* (8.00 U·mg⁻¹), *Enteromorpha* sp. (6.74 – 9.60 U·mg⁻¹), and *Chaetomorpha antenna* (9.40 U·mg⁻¹) [32].

No significant difference in fibrinolytic activities was observed between autotrophic ($430.46 \pm 40.19 \text{ U}\cdot\text{mg}^{-1}$) and 0.25% CSL ($391.34 \pm 40.03 \text{ U}\cdot\text{mg}^{-1}$) cultivations, which were higher than 0.50% CSL ($135.63 \pm 6.98 \text{ U}\cdot\text{mg}^{-1}$). In addition, fibrinolytic enzyme production from autotrophic and mixotrophic 0.25% CSL were higher than other photosynthetic microorganisms, including *Arthospira platensis* ($268.14 \pm 10.71 \text{ U}\cdot\text{mg}^{-1}$) and *Chlorella vulgaris* ($302.29 \pm 37.53 \text{ U}\cdot\text{mg}^{-1}$) [7,8]. The results showed that protease and fibrinolytic enzymes productions were higher in cultures with lower CSL concentration. As well known, the biochemical composition of microalgae biomass, e.g., enzyme production, depends on the culture conditions such as the medium composition [33]. Then, the highest enzymes activities were obtained using 0.25% CSL, which also enhanced enzyme production by *Arthospira platensis* [8]. On the other hand, cultivation with higher CSL concentration ($\geq 0.50\%$), decrease the enzymes productions, since high concentration of some nutrients, such as nitrogen, might affect the biomass composition [34].

3.3. Effect of extraction methods on the enzymatic activities

Extraction methods influenced on enzyme activity. Homogenization and sonication extraction methods were evaluated to obtain protease and fibrinolytic extracts. Homogenization was the most efficient method to extract protease ($12.48 \pm 1.35 \text{ U}\cdot\text{mg}^{-1}$) and fibrinolytic enzymes ($430.46 \pm 40.19 \text{ U}\cdot\text{mg}^{-1}$) from autotrophic cultivation, while sonication methods decreased enzymes activities to 4.50 ± 0.42 and $149.44 \pm 3.82 \text{ U}\cdot\text{mg}^{-1}$, respectively (Table 1). Similar results were observed in cell extracts from mixotrophic cultures using 0.25% CSL, which also showed higher protease ($12.50 \pm 2.94 \text{ U}\cdot\text{mg}^{-1}$) and fibrinolytic ($391.34 \pm 40.03 \text{ U}\cdot\text{mg}^{-1}$) activities using homogenization method when compared to sonication methods. This can be explained by possible enzyme denaturation caused by prolonged sonication time, high temperature, or elevated frequency as reported by Sukor et al., [35] and Ranjha et al., [36]. Then, these results showed that homogenization is more effective to extraction of protease and fibrinolytic enzyme from *T. obliquus*.

3.4. Effect of precipitation methods on the enzymatic activities

T. obliquus extract rich protein was precipitated using acetone or ammonium sulfate in two fractions of saturation (0–40% and 40–70%). Both 0–40% and 40–70% ammonium sulfate fractions showed similar protease activity (614.06 ± 64.95 and $614.60 \pm 13.65 \text{ U}\cdot\text{mg}^{-1}$, respectively), which was higher compared to acetone precipitation ($182.85 \pm 7.03 \text{ U}\cdot\text{mg}^{-1}$). Then, ammonium sulfate fractions are more advantageous for protease activity applications. However, although the 40–70% ammonium sulfate fraction exhibited the highest fibrinolytic activity ($569.52 \pm 23.20 \text{ U}\cdot\text{mg}^{-1}$), the acetone fraction showed better performance due to its potential fibrinolytic activity ($503.41 \pm 22.35 \text{ U}\cdot\text{mg}^{-1}$) and the highest enzyme yield of 32.98%. These results are similar to those reported by Barros et al., [8], which precipitated a fibrinolytic enzyme from *Arthospira platensis* using acetone and showed fibrinolytic activity of $256.02 \pm 23.45 \text{ U}\cdot\text{mg}^{-1}$ and protein yield of 53.81%.

Taking into account that the fibrinolytic activity measures the enzyme capacity of degrading fibrin specifically, and the acetone fraction showed the highest recovery yield, this fraction was considered more advantageous to be studied for thrombosis therapy purposes. Acetone is listed among the Generally Recognized as Safe (GRAS) by Food and Drug Administration (FDA), since toxicological and medical studies show no adverse effects on human health [37]. Additionally, use acetone for precipitation includes some advantages such as simple-step extraction, less cost, and less time-consuming [38,39]. Therefore, acetone was selected as the most advantageous precipitating agent to obtain fibrinolytic enzyme from *T. obliquus*.

Table 2. Comparation of different precipitating agents for precipitation of the homogenized cell extract from *T. obliquus* cultivated in 0.25% CSL.

Precipitating agents	Total protease activity (U·mL ⁻¹)	Yield (%)	Specific protease activity (U·mg ⁻¹) ¹⁾	P.F	Total fibrinolytic activity (U·mL ⁻¹)	Yield (%)	Specific fibrinolytic activity (U·mg ⁻¹) ¹⁾	P.F
Cell extract	94.80 ± 20.78	100.00	175.74 ± 0.00		338.01 ± 34.78	100.00	391.34 ± 40.03	
Ammonium sulfate (0-40%)	78.60 ± 8.31 ^a	82.91	614.06 ± 64.95 ^a	3.49	36.45 ± 2.96 ^a	10.78	569.52 ± 23.20 ^a	1.45
Ammonium sulfate (40-70%)	81.00 ± 1.80 ^a	85.44	614.60 ± 13.65 ^a	3.49	30.60 ± 0.06 ^b	9.05	464.37 ± 0.00 ^b	1.18
Acetone	81.00 ± 3.11 ^a	85.44	182.85 ± 7.03 ^b	1.04	111.50 ± 9.90 ^c	32.98	503.41 ± 22.35 ^b	1.28

Data expressed as means ± standard deviations of duplicate experiments.

3.5. Fibrinolytic activity in fibrin plate

Figure 2 shows a qualitative assessment of the fibrinolytic activity from *T. obliquus* by the fibrin plate method. The cell extract from *T. obliquus* cultivated in 0.25% CSL showed a high clear zone (82 mm²) when compared to cell extract obtained from cell cultivated autotrophically (69 mm²) or mixotrophically with 0.50% CSL (69 mm²) (Table 3; Figure 2A). These values are high than that of fibrinolytic enzymes from *Bionectria* sp. strains, which ranged from 21.9 to 66.7 mm² [40].

Table 3. Fibrinolysis process of *T. obliquus* extracts obtained by homogenization.

Growth conditions	Fibrinolysis area (mm ²)
Autotrophic	69
Mixotrophic (0.25% CSL)	82
Mixotrophic (0.50% CSL)	69

Fibrinolytic activities of protein precipitated by different precipitating agents are shown in Figure 2B. Both 0–40% ammonium sulfate and acetone fractions exhibited clear zone of fibrin degradation around the well after 48h. On the other hand, 40–70% ammonium sulfate fraction did not show clear zone area of hydrolysis.

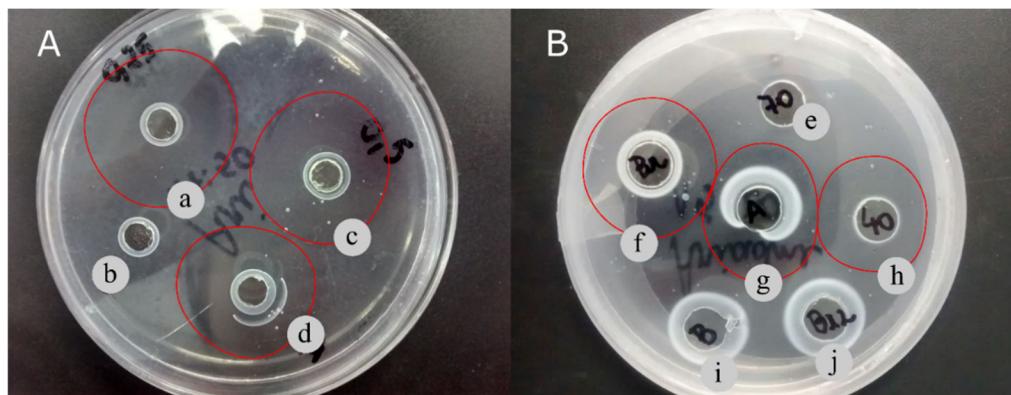


Figure 2. Fibrinolytic activity of *Tetradesmus obliquus* by fibrin plate method. (A) Fibrinolytic activity of homogenized extracts obtained by 0.25% CSL mixotrophic cultivation (a), Tris-HCl buffer control (b), 0.5% CSL mixotrophic cultivation (c), and autotrophic cultivation (d). (B) Fibrinolytic activity of 40-70% ammonium sulfate precipitate (e), cell extract (f), acetone precipitate (g), 0-40% ammonium sulfate (h), Tris-HCl buffer control (i), and cell extract extracted twice (j) after 48h.

3.6. Enzyme purification

Fibrinolytic enzyme from *T. obliquus* was purified using a combination of acetone precipitation and DEAE-sephadex ion exchange column. The chromatogram shown in Figure 3 exhibit a single peak with fibrinolytic activity of $1176.90 \pm 140.37 \text{ U}\cdot\text{mg}^{-1}$, and after purification by DEAE-sephadex, the fibrinolytic enzyme was 3.00-fold purified with a yield of 67.45% relative to that of the cell extract (Table 4). In general, the activity of the purified fibrinolytic enzyme from *T. obliquus* was higher than those obtained from *Costaria costata* ($915.5 \text{ U}\cdot\text{mg}^{-1}$), *Codium divaricatum* ($6.3 \text{ U}\cdot\text{mg}^{-1}$), *Codium fragile* ($61.50 \text{ U}\cdot\text{mg}^{-1}$), and *Ulva pertusa* ($295.18 \text{ U}\cdot\text{mg}^{-1}$) algae and various bacterial species such as *Bacillus flexus* ($315.20 \text{ U}\cdot\text{mg}^{-1}$), *Bacillus velezensis* BS2 ($131.15 \text{ U}\cdot\text{mg}^{-1}$), *Bacillus subtilis* HQS-3 ($30.00 \text{ U}\cdot\text{mg}^{-1}$), and *Bacillus subtilis* ICTF-1 ($280.00 \text{ U}\cdot\text{mg}^{-1}$) [41–45].

Table 4. – Steps of purification of fibrinolytic enzyme from *Tetradesmus obliquus*.

Purification step	Total protein (mg·mL ⁻¹)	Protease activity (U·mg ⁻¹)	P.F	Total activity (U·mL ⁻¹)	Yield (%)	Fibrinolytic activity (U·mg ⁻¹)	P.F	Total activity (U·mL ⁻¹)	Yield (%)
Cell extract	0.47 ± 0.02	175.74 ± 0.00	1.00	94.80 ± 20.78	100.00	391.34 ± 40.03	1.00	338.01 ± 34.78	100.00
Acetone precipitation	0.44 ± 0.02	182.85 ± 7.03	1.04	81.00 ± 3.11	85.44	503.41 ± 22.35	1.28	232.80 ± 9.90	68.87
DEAE-Sephadex	0.21 ± 0.00	311.95 ± 4.91	1.77	66.00 ± 1.03	69.62	1176.90 ± 140.37	3.00	228.00 ± 29.69	67.45

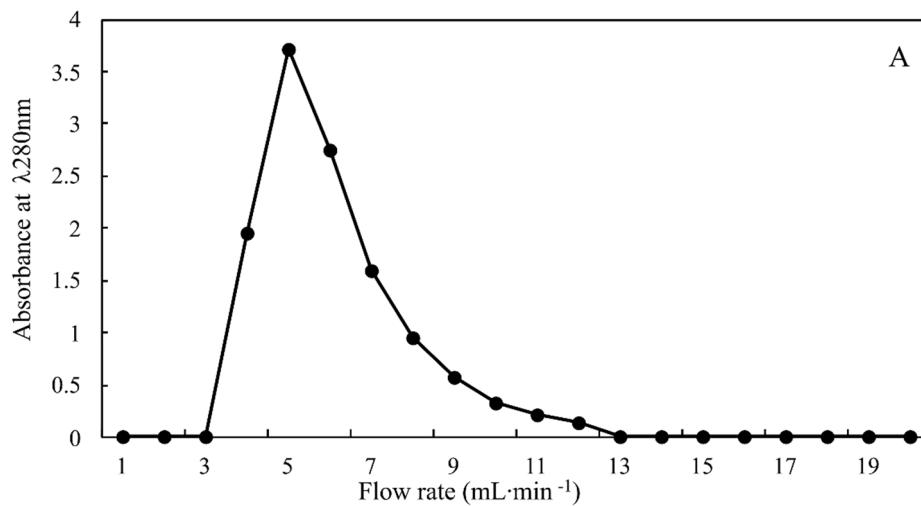


Figure 3. Chromatogram of fibrinolytic enzyme from *Tetradesmus obliquus* on the DEAE-Sephadex column.

SDS-PAGE showed one protein band with the molecular mass of about 97 kDa (Figure 4). This is higher than that exhibited by other *T. obliquus* proteins reported by Silva et al., [20] and Heide et al., [46] that have a molecular weight of 78 and 12 kDa, respectively. Additionally, the molecular weight of fibrinolytic enzymes obtained from other microalgae species, including *Arthrosira*

platensis (72 kDa) and *Chlorella vulgaris* (45 kDa) are also lower than the fibrinolytic enzyme from *T. obliquus* [7,8]. These results show that this is a different protein from those reported previously.

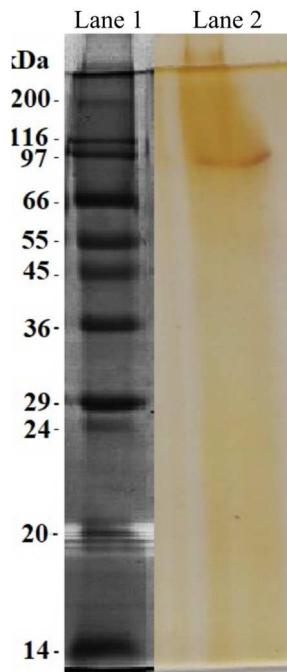


Figure 4. Fibrin zymography of fibrinolytic enzyme purified by filtration gel column chromatography (Sephadex G-75). Lane 1, Molecular weight marker; Lane 2, purified enzyme.

5. Conclusions

In the present study was possible to produce and purify an enzyme from *Tetraedesmus obliquus* microalgae with specific activity of $1176.90 \pm 140.37 \text{ U}\cdot\text{mg}^{-1}$. Mixotrophic cultivation using an inexpensive and advantageous agro-industrial by-product (0.25% CSL) showed higher growth kinetic parameters and fibrinolytic production. Additionally, cell extraction by homogenization had highest fibrinolytic activity, while the protein precipitation with acetone exhibited the highest recovery yield. In general, these methods are considered as simple, efficient, less cost, less time-consuming, and recognized as safe for human health, which can facilitate this enzyme production as well as its purification. Therefore, these results can conclude that the fibrinolytic enzyme from *T. obliquus* has wide potential to industrial application besides its promising effects as an alternative for thrombolytic therapy.

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