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## Article

# A Green Chemistry and Energy Cost-Effective Approach in Innovative Advanced Oxidation Processes Through Photoactive Microgels for Sustainable Applications

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**Abstract:** Sustainability challenges faced by the chemical industry today include the increasing prevalence of persistent Contaminants of Emerging Concern in wastewater, which requires the development of advanced treatment technologies. Additionally, transitioning from petroleum-derived raw materials to renewable biomass is essential for achieving more sustainable chemical processes. PNIPAM microgels with covalently integrated Rose Bengal as a photosensitizer has been synthesized and characterized in this study. The micellar-like structure of the colloidal microgels enhances substrate adsorption and overall efficiency. Designed in alignment with Green Chemistry principles, these materials support sustainable applications such as the green synthesis of 5-hydroxy-2(5H)-furanone, a C4 building block intermediate, and the removal of Diclofenac from wastewater. These photoactive microgels act as efficient photocatalysts, capable of generating singlet oxygen ( $O_2(^1\Delta_g)$ ) under visible light, with full recoverability and reusability over multiple cycles. By employing direct solar-driven photocatalysis, the approach offers a cost-effective, eco-friendly solution to address economic and environmental challenges in water treatment processes, as demonstrated by scale-up economic simulations. Additionally, it allows the synthesis of 5-hydroxy-2(5H)-furanone in aqueous media, a sustainable key-factor enabled by the enhanced adsorption capabilities of the microgels.

**Keywords:** Green Chemistry; Sunlight-driven Photocatalysis; Wastewater Disinfection; C4-chemicals Sustainable Synthesis; Colloidal Microgels; Rose Bengal; Singlet Oxygen

## 1. Introduction

At the end of the 20th century, Green Chemistry emerged as a discipline aimed at integrating sustainability into chemical process design, focusing on both environmental and economic aspects. Defined by P. T. Anastas and J. C. Warner through 12 guiding principles [1], it advocates for the efficient use of resources and the minimization of waste. While its principles emphasize energy and material optimization, they often overlook whether the end-use of the resulting products aligns with sustainability goals. Over time, this movement has evolved to address new challenges, such as the persistence of chemical products in the natural environment, highlighting the need for continued innovation in sustainable chemistry [1-4]. A relevant example is the increasing detection of Contaminants of Emerging Concern (CECs) in aquatic environments, including pharmaceuticals, personal care products, endocrine-disrupting chemicals, pesticides, and their metabolic byproducts. To date, more than a thousand of these compounds have been identified, and their presence in wastewater has become more prevalent in recent years. Alarmingly, many CECs persist even after

tertiary treatments in wastewater treatment plants (WWTPs), creating significant challenges for the safe reuse of treated water in agriculture and domestic applications. This persistence poses a serious public health concern, prompting extensive research into advanced technologies to effectively eliminate these pollutants. Efforts are now focused on integrating such innovative solutions into WWTPs to mitigate this growing problem and ensure the safety and sustainability of water resources [5-9].

Another critical aspect of environmental sustainability is the selection of raw materials for chemical processes, as this choice plays a pivotal role in determining both the sustainability of the process and its overall environmental impact. Therefore, it is crucial to evaluate the origin of the raw material. Currently, 90% of organic compounds synthesized rely on raw materials derived from petroleum, a limited resource. The most plausible alternative is biomass, which is easily accessible, abundant, and has historically provided raw materials for humanity until the advent of fossil resources [10, 11]. Returning to biomass would represent a step towards closing the sustainability loop. Lignocellulosic biomass, composed predominantly of carbohydrate polymers (cellulose and hemicellulose) and aromatic polymers (lignin), represents over 90% of plant biomass and serves as the most abundant renewable carbon source without competing with food supplies. Its conversion into value-added fuels and chemicals offers a sustainable pathway to energy production and carbon neutrality [10, 12, 13]. Among its derivatives, furfural and furoic acid are key platform chemicals obtained through hydrolysis and oxidation processes, respectively [14, 15]. Furfural was recognized by the U.S. Department of Energy as a top value-added chemical [16]. Furoic acid, readily obtained from furfural via biological oxidation, is a well-known compound in green chemistry, serving as a C4 building block intermediate for the synthesis of various industrially significant substances, including plastics, manufacturing fibers, lubricants, and resins [17-19].

On the other hand, hydrogels are extensively used in biochemistry due to their biocompatible physicochemical properties, which closely resemble those of living tissues. This resemblance provides them with valuable roles in both biomedical sciences and environmental applications, particularly in water treatment and biodiversity conservation. Colloidal microgels, a subclass of hydrogels, are stabilized within a continuous medium, forming stable dispersions [20-22]. Poly(*N*-isopropylacrylamide) (PNIPAM) is one of the most widely used microgel particles due to its stimuli-responsive properties, allowing it to adapt its physical and chemical characteristics to external environmental changes. This adaptability has made it highly appealing for diverse of the above-mentioned applications. PNIPAM is a temperature-sensitive polymer, hydrophilic at room temperature, and widely used for fabricating sustainable stimuli-responsive materials with defined size, functionalized surfaces, and enhanced colloidal stability. Additional stimuli, such as pH responsiveness, can be introduced through copolymerization with ionic monomers. The swelling behavior is influenced by polymer/polymer and polymer/water interactions, as well as factors like temperature, pH, and ionic strength. PNIPAM microgels are particularly suited for light-responsive designs, which are further enhanced by the incorporation of photosensitizers, and are ideal for pH-sensing applications in wastewater monitoring [23, 24].

Innovative strategies are essential to drive reactions aimed at achieving biological and environmental sustainability. Within this framework, the development of polymers incorporating photosensitizing units has emerged as a topic of considerable interest. Among photocatalytic processes, oxidation remains one of the most extensively investigated. In recent years, methodologies utilizing photosensitizers have gained recognition as promising green alternatives [25-28]. Notably, singlet oxygen has demonstrated significant potential in oxidation reactions of environmental relevance, such as the synthesis of natural products and pharmaceuticals [29], as well as in pioneering applications within sustainable organic chemistry [30]. In this line, our research group has developed heterogeneous photocatalysts in the form of hydrophilic, photoactive polymeric microparticles derived from styrene resins, functionalized covalently with Rose Bengal (RB) as a photosensitizer. These materials have proven effective in the photochemical oxidation of 2-furoic acid for the green synthesis of 5-hydroxy-2(5H)-furanone [17]. Moreover, they have demonstrated significant potential

in removing emerging pollutants (EPs) from water through advanced oxidation processes [31, 32]. The present study focuses on the covalent incorporation of RB into the PNIPAM matrix to develop a supported photosensitizer. A key advantage over previous approaches lies in the colloidal structure of the microgel, which promotes substrate adsorption within micellar-like configurations formed under specific stimuli, such as pH and temperature, thereby enhancing the efficiency of the heterogeneous catalyst. The literature documents several instances of photosensitizers covalently bound to PNIPAM-based polymeric matrices [33-35], with Rose Bengal being utilized in some of these cases [36-41], but none of these have been applied to the specific objectives described in this article, such as the removal of Diclofenac from water and the green synthesis of raw materials from lignocellulosic biomass.

Photocatalysis, a key principle of green chemistry, is a sustainable process that uses light and a photosensitizer to drive chemical transformations. Recently, the design of polymers with photosensitizing units has gained attention. Stimuli-responsive polymers like PNIPAM, with covalently attached photosensitizing groups, allow for controlled photoreactions. This approach has been shown to effectively remove phenol from polluted water through singlet oxygen oxidation [42] and could be extended to pollutants with similar chemical structures, like Diclofenac, as demonstrated in recent studies using silica-based RB-supported photocatalysts [43, 44]. To further advance the sustainable design of the photocatalytic process, another key resource is the use of renewable energy. Sunlight can be directly harnessed to induce photochemical transformations of chemical structures [45]. The sun offers immense photochemical potential, and numerous studies in the literature report the successful use of direct solar irradiation for water decontamination [46-49]. Additionally, sunlight could also be employed for the synthesis of raw materials derived from furfural [10, 18].

This study introduces an innovative method for synthesizing colloidal PNIPAM microgels with covalently integrated Rose Bengal as a photosensitizer. The microgel structure enhances the photochemical efficiency of the photosensitizer by adsorbing substrates into the polymeric matrix, thereby increasing process performance. This makes the materials particularly effective for advanced oxidation processes driven by singlet oxygen generated under direct solar irradiation, targeting applications in biological and environmental oxidations. The polymers design, align with Green Chemistry principles, intended uses include sustainable goals such as synthesizing 5-hydroxy-2(5H)-furanone as a renewable raw material and removing CECs, such as Diclofenac, from wastewater. The approach integrates cost-effective and sustainable strategies, including light-driven photocatalysis using solar energy, recyclability with straightforward material separation (heterogeneous catalysis), non-use of organic solvents, minimal energy requirements (solar light and ambient temperature reactions), and reduced byproduct generation. This makes the microgels an eco-friendly and efficient solution for environmental challenges.

## 2. Materials and Methods

### 2.1. Reagents, Solvents and Polymeric Precursors

The reagents used in the present work are listed below: N-isopropylacrylamide (NIPAM, Fisher, purified by recrystallization with hexane/toluene), aminoethyl methacrylate (AEMA, Aldrich, 90%), N,N'-methylenebisacrylamide (MBAM, Fisher, purified by recrystallization from ethanol), 2,2'-azobis[2-(methylamidinopropane)] dichloride (V50, Aldrich, 97%), hydrochloric acid (HCl, Scharlau, extra pure, 37%), Rose Bengal sodium salt (RB, Fluka), chloroform (CHCl<sub>3</sub>, Scharlau, stabilized with ethanol, multisolvent grade for HPLC), 1-[3-(dimethylamino)propyl]-3-ethylcarbodiimide (EDC, Aldrich), methanol (MeOH, Scharlau, multisolvent grade for HPLC), 9,10-anthracenedipropionic acid (ADPA, Aldrich, ≥98.0%), diclofenac (Sigma Aldrich), and furoic acid (Sigma Aldrich). The water used in all cases was of Millipore-Q quality (Milli-Q, ultrapure, double-deionized).



## 2.2. Synthesis of the Photoactive Colloidal Microgels

### Step 1. Synthesis of NIPAM-co-AEMA polymeric microgel

The synthesis of NIPAM-co-AEMA microgels was performed via single-step emulsion polymerization in a 100 mL reaction vessel equipped with a reflux condenser, magnetic stirrer, thermometer, and an argon gas inlet. NIPAM (0.99 g, 99 wt.% of the total monomer), AEMA (0.01 g, 1 wt.%), and MBAM (0.10 g, 10 wt.% as the crosslinker) were dissolved in 100 mL of Milli-Q water and added to the reaction vessel. The mixture was heated in an oil bath maintained at 70 °C and purged with argon gas for 20 minutes to remove oxygen. After the system reached the target temperature, a solution of the initiator (0.04 g of V50, 4 wt.% of the total monomer weight) in 5 mL of Milli-Q water was introduced into the vessel. The polymerization was carried out for 24 hours under constant stirring. Upon completion, the reaction mixture was cooled to room temperature, and the resulting microgel dispersion was dialyzed against Milli-Q water for a week to remove unreacted monomers and other impurities, with the dialysate replaced daily.

### Step 2. Rose Bengal anchorage via carbodiimide coupling reaction: synthesis of NIPAM-co-AEMA-RB

Rose Bengal sodium salt was dissolved in water and acidified to pH=2 using 1 M HCl. The resulting solution was extracted with chloroform, and the organic phase was washed three times with water to remove impurities. The product was then concentrated under reduced pressure. In a 100 mL round-bottom flask, NIPAM-co-AEMA polymer (1.412 g,  $8.52 \times 10^{-5}$  mol AEMA), acidified Rose Bengal (83 mg,  $8.52 \times 10^{-5}$  mol), and 1-ethyl-3-(3-dimethylaminopropyl)carbodiimide (EDC) (1.6 mg,  $8.52 \times 10^{-6}$  mol) were combined. Methanol was added as the solvent to a final volume of 100 mL. The flask was sealed with a septum and the mixture was stirred at room temperature for 48 hours to allow the covalent attachment of Rose Bengal to the polymer. After the reaction, the microgel particles were separated by centrifugation at 10,000 rpm for 20 minutes using a Sorvall RC 5b Plus centrifuge. The particles were washed sequentially with methanol, a 1:1 methanol-water solution, and finally with water to ensure removal of unreacted reagents. The supernatant from the washing steps was collected to quantify the Rose Bengal loading via UV-Vis spectroscopy. Finally, the purified microgel particles were dispersed and stored in 100 mL of Milli-Q water.

## 2.3. Characterization of the Colloidal Microgels

The characterization process of the colloidal polymeric microgels was performed using acid-base titration experiments, dynamic light scattering (DLS) and UV-Vis absorption spectroscopy. Acid-base titration via potentiometry was conducted with a Crison Titromatic potentiometric titration instrument. When required, the pH was adjusted by adding small quantities of 0.01 M HCl or 0.01 M NaOH. These experiments enabled the quantification of the AEMA percentage in the NIPAM-co-AEMA microgel particles (by analyzing the  $\text{NH}_2$  group of this monomer, which protonates in an acidic medium). Additionally, the yield of the overall reaction was determined by acid-base titration, quantifying the amount of RB anchored to the polymer NIPAM-co-AEMA-RB. The natural pH of each microgel was also measured.

Dynamic light scattering (DLS) analysis was performed to study the colloidal properties of the polymers. These studies were conducted using a Brookhaven Zeta-Plus (laser 15 mW,  $\lambda_{\text{em}}=678$  nm, detector 90°). This technique allows for determining the diffusion coefficients of the colloidal microgels and their electrophoretic mobility. All samples were prepared at a particle concentration of 0.1% by weight in Milli-Q water and placed in a 3 mL quartz cuvette. The diffusion coefficients of the microgel particles were used to calculate their hydrodynamic diameter using the Stokes–Einstein equation. UV-Vis absorption spectroscopy studies were carried out using a Hewlett-Packard Agilent 8453 UV-Vis spectrophotometer. The calculation of RB loading after the covalent attachment of Rose Bengal to the NIPAM-co-AEMA polymer was performed by two methods: acid-base titration (as described previously) and UV-Vis spectroscopy ( $\lambda = 549$  nm), analyzing the unreacted RB in the supernatant and comparing both results.

The adsorption capacity of the microgels were characterized through experiments with different substrates. The chosen substrates were those intended for subsequent photochemical studies in this work (ADPA, Diclofenac, and Furoic Acid). These experiments also served to determine the optimal ratio between substrate concentration and hydrogel weight for each reaction. To achieve this, several solutions containing a fixed amount of microgel particles were mixed with a known and variable amount of substrate in Milli-Q water, and the system was left to equilibrate for 24 hours. The particles were then separated from the solution by centrifugation (10,000 rpm for 20 minutes, using a Sorvall RC 5B Plus centrifuge). The experiment was performed at the natural pH of the microgel. In cases where deviations occurred after the substrate was added, the pH was adjusted by adding small quantities of 0.01 M HCl or 0.01 M NaOH. UV-Vis spectroscopy measurements were performed in order to evaluate the adsorption of the substrates ADPA (UV-Vis Hewlett-Packard Agilent 8453 at 398 nm) and Furoic Acid (246 nm) into the microgel. For Diclofenac, the measurements were performed using HPLC (Agilent 1260 with 4-nitrobenzoic acid  $10^{-4}$  M). For each case, curves of  $\mu\text{mol}$  substrate per gram of microgel as a function of the equilibrium substrate concentration were plotted.

#### *2.4. Evaluation the Photo-Oxidation Kinetics of the Photoactive Colloidal Microgels*

The singlet oxygen production efficiency of the polymeric microgel photosensitizers was evaluated using the standard photooxidation reaction of anthracene-9,10-dipropionic acid (ADPA), a method previously reported in the literature [17, 31, 50]. The experiments were conducted in aqueous media within a 500 mL jacketed Pyrex reactor containing ADPA at a concentration of  $1.2 \times 10^{-4}$  M in Milli-Q water. The required amount of microgel solution was added based on the adsorption data obtained in adsorption experiments. The pH of the solution was measured, and if it deviated from the natural pH of the microgel, it was adjusted using small volumes of 0.01 M HCl or 0.01 M NaOH.

In the first experimental phase, the air-equilibrated solution was irradiated at 25°C using a 50 W halogen lamp, with continuous stirring throughout the process. The jacketed part of the reactor was filled with an aqueous  $\text{FeCl}_3$  solution (0.1 M), serving as a filter for wavelengths below 450 nm. The temperature was monitored to ensure it remained within the range of 23–25°C. The jacketed  $\text{FeCl}_3$  solution was connected to a water flow system linked to a small heater/cooler to regulate the temperature if needed. At regular intervals, a 3 mL aliquot was withdrawn using a  $1 \times 1$  cm quartz spectrophotometer cuvette to monitor the decreasing absorbance of ADPA. Reaction kinetics were calculated using the Kinetics mode of a Hewlett-Packard Agilent 8453 UV-Vis spectrophotometer at 398 nm, employing the same reaction cuvette. In order to compare the effect of the microgel, similar experiments were conducted without the microgel, using only a RB solution at a concentration equivalent to that of the RB covalently anchored to the microgel. Control experiments without irradiation were also performed.

The second phase of experiments was conducted under direct natural solar irradiation. The reaction reactor was set up following the same protocol as in the previous experiment, with the only modification being the change in the irradiation source from artificial to natural sunlight. The irradiation at the surface of the reaction medium was measured using a Fluke IRR1-SOL meter, the temperature was monitored to ensure it remained within range, and the ADPA concentration was measured using UV-Vis spectroscopy.

#### *2.5. Studies of Diclofenac Pollutant Photo-Degradation*

To evaluate the degradation of Diclofenac pollutant, experiments were conducted following the same protocol as before for irradiation with both simulated solar light (50 W halogen lamp) and natural sunlight. In both cases, a 500 mL jacketed reactor system surrounded by an  $\text{FeCl}_3$  solution was used. The appropriate amount of microgel, determined from adsorption studies, was added to a 5 ppm ( $1.69 \times 10^{-5}$  M) Diclofenac solution in Milli-Q water. The pH was also adjusted to the natural pH of the microgel, and under continuous stirring, the temperature was maintained at 25°C using the previously described system. The photo-oxidation reaction of the pollutant Diclofenac was

monitored by analyzing 200  $\mu\text{L}$  aliquots taken at known time intervals using Agilent 1260 reversed-phase HPLC chromatography. A  $10^{-4}$  M solution of 4-nitrobenzoic acid was used as an internal standard, with the temperature maintained at  $30^{\circ}\text{C}$ .

Control experiments were also conducted under identical conditions without a photosensitizer, as well as with a Rose Bengal solution at a concentration equivalent to the amount of RB anchored to the microgel, serving as the photosensitizer. The impact of solar irradiation was evaluated using both simulated sunlight (50 W halogen lamp) and natural sunlight. For the natural sunlight experiments, the setup was exposed to direct sunlight on sunny days in Murcia during midday hours at various times of the year to account for seasonal variations in solar irradiation. In all experiments, the solar irradiation at the surface of the reaction medium was measured using a Fluke IRR1-SOL meter, and the temperature was carefully monitored to ensure it remained between 23 and  $25^{\circ}\text{C}$ .

The recyclability of NIPAM-co-AEMA-RB photosensitizer was assessed through a series of photo-catalytic experiments. The procedure followed was identical to the previously described method, with the Diclofenac solution being renewed for each cycle. Each reaction cycle was conducted for 180 minutes, with cycle 2 performed without irradiation as a control. At the end of each cycle, the microgel photocatalysts were recovered from the solution by centrifugation at 10,000 rpm for 20 minutes using a Sorvall RC 5B Plus centrifuge.

#### 2.6. Photo-Oxidation of Furoic Acid and Green Synthesis 5-Hydroxy-2(5H)-Furanone

The oxidation of 2-furoic acid to 5-hydroxy-2(5H)-furanone via singlet oxygen was studied in an aqueous reaction medium (Milli-Q water with methanol 95:5 v/v). The appropriate amount of microgel photosensitizer was added to 500 mL of a 2-furoic acid solution ( $10^{-3}$  M) in a jacketed Pyrex reactor. The heterogeneous mixture was maintained under stirring and in equilibrium with air. Subsequently, the experiments were conducted following the same protocol as previously described for irradiation with both simulated sunlight (50 W halogen lamp) and natural sunlight (at different times of the year), while monitoring the incident irradiation. The pH was adjusted to the natural pH of the microgel, and the temperature was kept between 23 and  $25^{\circ}\text{C}$  under stirring, using the previously described procedure. Control experiments were conducted under identical conditions in the dark, with free Rose Bengal in solution as the photosensitizer (at the same concentration as the RB anchored in the microgel). The decreasing absorbance of 2-furoic acid was monitored by UV-Vis spectroscopy at 246 nm. For each measurement, 3 mL aliquots were withdrawn from the reaction mixture and analyzed using a quartz spectrophotometer cuvette, following the same procedure as with ADPA. After the reaction was completed, the photocatalyst was recovered by centrifugation (10,000 rpm for 12 minutes, using a Sorvall RC 5B Plus centrifuge), and the product was analyzed by HPLC to confirm the successful synthesis of 5-hydroxy-2(5H)-furanone and the absence of reactants or byproducts, such as additional oxidation to maleic acid or others. The catalyst was then reused to evaluate its catalytic efficiency across multiple reaction cycles.

### 3. Results and Discussion

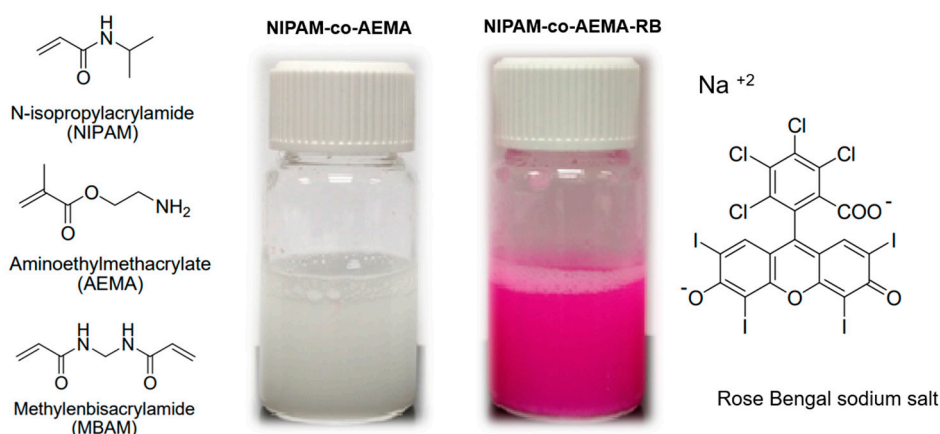
#### 3.1. Synthesis and Characterization of the Photoactive Colloidal Microgels

The microgels were designed following green chemistry principles and in order to incorporate energy efficiency into their future functional use. The polymeric matrix was formulated with 90% of N-isopropylacrylamide (NIPAM), 1% of aminoethylmethacrylate (AEMA) -a total of 91% monomer- and 9% of methylenbisacrylamide (MBAM) as a crosslinker, leveraging the pH- and temperature-responsive properties of NIPAM for controlled swelling with enhanced substrate adsorption and increased reaction efficiency. This design enables reactions to occur in water without organic solvents, aligning with green chemistry goals. Additionally, the microgels' natural pH matches that of wastewater treatment plant effluents, making them suitable for quaternary water treatment to remove CECs. Furthermore, PNIPAM microgels are non-toxic per Regulation (EC) No. 1272/2008, ensuring environmental and human safety. As discussed in the introduction, previous studies have

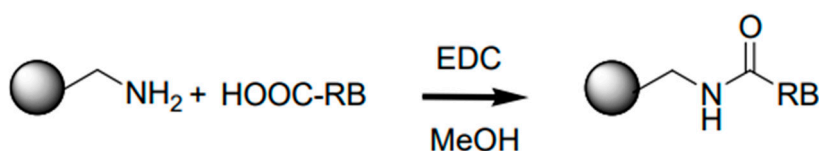
synthesized copolymers with other monomers anchored to PNIPAM [23, 36]. In this design, AEMA was selected as the co-monomer and included in a small proportion (90:1 ratio relative to NIPAM) to avoid an excess of free amine groups ( $-NH_2$ ), which could interfere with the micellar properties of the resulting microgel. The amount of AEMA also determines the RB loading, and the chosen proportion is sufficient to ensure the anchoring of RB [17, 31], while keeping costs manageable, given the higher price of RB compared to the monomers. Moreover, this design incorporates sufficient RB anchoring to ensure effective sunlight-driven photocatalysis [32].

The 9% MBAM crosslinker enhances the microgel's substrate adsorption capacity by providing porosity, flexibility, and permeability to the polymeric structure, with this proportion optimized based on previous studies [51-54]. Furthermore, the green design of the microgels includes a PNIPAM-based matrix with near 100% polymerization efficiency, minimizing waste during synthesis. Its functional applications include photocatalysis under sunlight, water as the reaction solvent, and the ability to be reused across multiple reaction cycles, all aligning with green chemistry principles.

The colloidal aqueous microgels were synthesized in two steps. The polymer synthesis involved an initial polymerization step, as previously described in the literature [55, 56], in which NIPAM-co-AEMA microgels were synthesized by copolymerizing NIPAM and AEMA with MBAM as the crosslinker. As shown in Figure 1, the polymer resulting from the first reaction step, NIPAM-co-AEMA (without RB attached), exhibits a white color. In a second step, the photosensitizer Rose Bengal is covalently attached within the polymeric matrix through a carbodiimide coupling reaction (Figure 2) [57]. polymer NIPAM-co-AEMA-RB has the appearance of colloidal solution and displays a pink hue due to the covalently attached RB.



**Figure 1.** Left: Chemical structure of NIPAM, AEMA and MBAM. Centre: Illustration of colloidal microgels without RB (left vial, NIPAM-co-AEMA) and with covalently anchored Rose Bengal (NIPAM-co-AEMA-RB). Right: Chemical structure of Rose Bengal in basic media  $RB^{-2}$ .



**Figure 2.** Scheme of the carbodiimide coupling reaction in MeOH medium, using EDC and Rose Bengal with the carboxylate group protonated ( $HOOC-RB$ , previously adjusted to  $pH = 2$ ).

The new microgels have been characterized, and the colloidal properties of the polymers have been studied. These studies included acid-base titration experiments, diffusion coefficients, electrophoretic mobility, and UV-Vis spectroscopy analysis, as described in the previous section. Due to the colloidal nature of the polymer particles, the study of a suitable polymerization process for the



monomers and crosslinkers could not be conducted using conventional methods like FT-IR spectroscopy and FT-Raman spectroscopy, which had been employed in previous studies [17, 51-54]. Instead, experiments of acid-base titration of the polymers were performed. The variation in the pH was accomplished in order to study the dependence of NIPAM-co-AEMA colloidal microgels to the external stimulus pH, analyzing the NH<sub>2</sub> group of AEMA. The results indicate that the polymerization reaction was successful, as the AEMA percentage obtained by titration closely matches the theoretical value (0.91%). Table 1 summarizes the results obtained for the characterization of the two synthesized polymers in terms of effective diameter and electrophoretic mobility (determined by DLS analysis) as well as the AEMA composition (acid-base titration).

**Table 1.** Effective diameter and Electrophoretic mobility in different pH, for colloidal microgels.

Characterization Data		NIPAM-co-AEMA	NIPAM-co-AEMA-RB
Effective diameter (nm)	pH = 3	732	724
	Natural pH of microgel	655	669
	pH = 7	631	634
	pH = 11	488	498
Electrophoretic mobility (m <sup>2</sup> s <sup>-1</sup> V <sup>-1</sup> )	pH = 3	0.15	0.18
	Natural pH of microgel	0.02	0.07
	pH = 7	0.01	0.03
	pH = 11	-0.09	-0.32
% AEMA (titration)		0.92 %	0.92 %
RB loading (titration)		0	33 μmol RB /g polym.
RB loading (UV-Vis)		0	33 μmol RB /g polym.

Table 1 shows the natural pH values of the hydrogels: 6.69 for NIPAM-co-AEMA and 6.45 for NIPAM-co-AEMA-RB. These results are consistent with expectations, as the natural pH of PNIPAM in pure water is close to 7. The slightly lower experimental values in both cases are due to the mild acidity introduced by the functional groups in the polymeric network contributed by the ≈ 1% AEMA comonomer. That is, the amino group exclusively for NIPAM-co-AEMA, and the non-functionalized amino group along with the Rose Bengal for NIPAM-co-AEMA-RB.

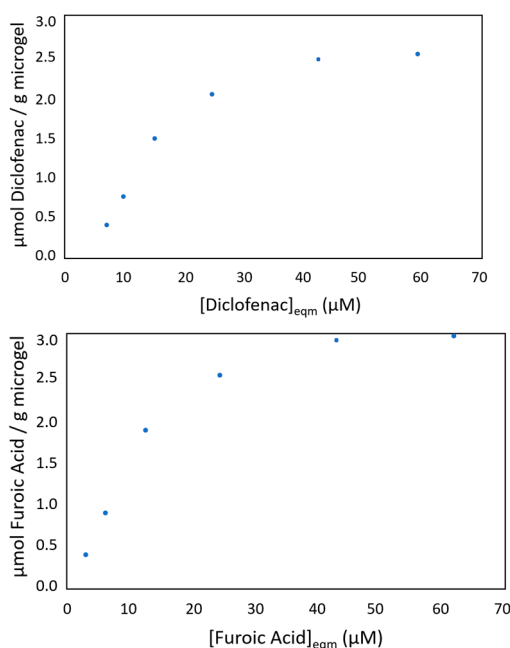
On the other hand, a dependence of the effective diameter and electrophoretic mobility on pH can be observed. The effective diameter of the microgels is larger in acidic pH due to increased swelling caused by electrostatic repulsion from the positive charges contributed by AEMA. As the pH increases, the effective diameter decreases, indicating a gradual contraction of the polymeric network. At the natural pH of the microgels, which is near neutral, the structure achieves its most balanced state between swelling and contraction, promoting optimal substrate adsorption within this pH range. Regarding electrophoretic mobility, both microgels display positive values at acidic pH, near zero at neutral pH, and negative values at basic pH. In the case of NIPAM-co-AEMA-RB, the mobility values are more pronounced compared to NIPAM-co-AEMA, particularly at acidic and basic pH. This heightened response is due to the amino groups from AEMA contributing to positive mobility at acidic pH and the negatively charged groups from Rose Bengal dominating at basic pH.

The particle size of the polymeric microgels was determined using dynamic light scattering, with the effective diameter calculated from diffusion coefficients using the Stokes-Einstein equation:  $D = kT / (6\pi\eta R)$ . This equation relates the diffusion coefficient (D) to the particle radius (R), accounting for temperature (25°C, in this study), the Boltzmann constant (k), and the solvent viscosity (water, in this study) [58].

Regarding the calculation of RB loading in NIPAM-co-AEMA-RB using the acid-base titration method, the carboxylate group of RB is the one that binds to the amino group through the carbodiimide coupling reaction. However, under basic pH conditions, RB can lose a proton from its hydroxyl group, the value obtained using this method is 33 μmol RB/g microgel, as presented in

Table 1. Moreover, as mentioned in the methodology section, the amount of Rose Bengal covalently attached to NIPAM-co-AEMA-RB was also calculated by analyzing the unreacted supernatant after prior calibration using UV-Vis spectroscopy ( $\lambda=549$  nm). The acquired value was  $33 \mu\text{mol RB/g}$  microgel, which is the same result obtained using the acid-base titration method. All results of the titration studies can be found in the supplementary material.

Finally, adsorption studies were conducted to evaluate the adsorption capacity of microgel NIPAM-co-AEMA-RB using three different substrates (ADPA, Diclofenac, and Furoic Acid), which will be employed in subsequent experiments. These studies not only validated the microgels' ability to adsorb the substrates but also determined the optimal microgel-to-substrate ratio required for effective adsorption in the medium.



**Figure 3.** Graphics of substrate adsorption in the microgel NIPAM-co-AEMA-RB (Diclofenac, left and Furoic Acid, right) in  $\mu\text{mol}$  substrate /g microgel as function of the equilibrium substrate concentration at  $25^\circ\text{C}$  and  $\text{pH}=6.45$ .

The results obtained were  $0.69 \mu\text{mol ADPA/g}$  microgel,  $2.55 \mu\text{mol Diclofenac/g}$  microgel, and  $3.01 \mu\text{mol Furoic Acid/g}$  microgel. The highest adsorption was observed for furoic acid, while the lowest was for ADPA, with a difference of half an order of magnitude. This difference is attributed to their chemical properties: furoic acid is smaller, has a single carboxyl group, and its furan ring facilitates effective electrostatic and hydrophobic interactions with the protonated amino groups of the microgel, especially at slightly acidic or neutral pH. In contrast, ADPA, being larger and bearing two carboxylate groups, experiences greater charge repulsion, limiting its adsorption. Diclofenac, with an intermediate molecular weight and a single carboxyl group that remains deprotonated at slightly acidic pH, also interacts effectively with the microgel, resulting in adsorption values slightly lower than furoic acid but higher than ADPA.

### 3.2. Evaluation the Photo-Oxidation Kinetics of the Photoactive Colloidal Microgels

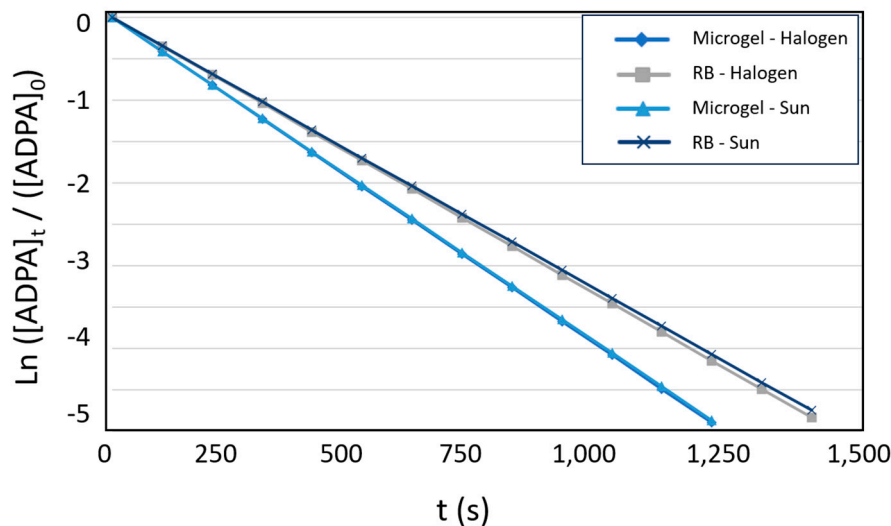
The production efficiency of singlet oxygen by the polymeric photosensitizers was evaluated using the standard photooxidation reaction of anthracene-9,10-dipropionic acid (ADPA). In this process, ADPA reacts with  $\text{O}_2(^1\Delta_g)$  forming ADPA endoperoxide. The photooxidation experiments were conducted as outlined in section 2.4, using  $86.95 \text{ mg}$  of microgel added to a solution of  $1.2 \times 10^{-4} \text{ M}$  ADPA in Milli-Q water. The reactions were performed in a  $500 \text{ mL}$  jacketed reactor surrounded by the  $\text{FeCl}_3$  ( $\lambda < 450\text{nm}$  filter) solution, under constant stirring and equilibrated with air. The temperature control system was activated to maintain the reaction temperature between  $23^\circ\text{C}$  and

25°C. At regular intervals, 3 mL aliquots were collected and analyzed in a quartz spectrophotometer cuvette, monitoring the decrease in the ADPA absorption band at 398 nm. The experiments were performed using two different irradiation sources: (1) a 50 W halogen lamp and (2) natural sunlight. The irradiation at the surface of the reaction medium was measured. For the halogen lamp experiments, the vials were positioned at a distance where the lamp's emission matched the average natural irradiation than in solar experiments. To evaluate the effect of the microgel, comparable experiments were carried out without the microgel, using only Rose Bengal at a concentration equivalent to that of the covalently anchored RB in the microgel, specifically  $5.74 \times 10^{-3}$  M. Control experiments without irradiation were also performed, with no decrease observed in the ADPA absorption band. Table 2 summarizes the study on ADPA conversion, including the reaction rate constants ( $k_{obs}$ ) and a comparison between the different irradiation sources and the performance of microgel-anchored RB versus free RB. In all cases, the decrease in ADPA concentration follows first-order kinetics, according to the literature [17, 31, 32, 50].

**Table 2.** Kinetic parameters ( $k_{obs}$ , half-reaction time and time for >99% conversion) for ADPA conversion under different irradiation sources and comparison of microgel-anchored RB vs. free RB.

Photosensitizer		$t_{1/2}$ (s)	$t$ (>99%) (s)	$k_{obs}$ ( $10^{-5} s^{-1}$ )
Halogen lamp (sol simulated)	Blank	-	-	-
	NIPAM-co-AEMA	-	-	-
	NIPAM-co-AEMA-RB	170	1,128	408
	Free RB	200	1,332	346
Sun natural irradiation (May 2024)	Blank	-	-	-
	NIPAM-co-AEMA	-	-	-
	NIPAM-co-AEMA-RB	171	1,135	406
	Free RB	204	1,357	339

The average solar irradiation in both experiments (halogen lamp and natural solar light) was 6.9 kWh/m<sup>2</sup>, aligning with expected values for May sunlight in Murcia [59]. The reaction temperature remained consistently between 24 and 25°C, with no use of the temperature control system; this was due to the short reaction times and the initial temperature of the Milli-Q water being 25°C, contributing to the overall energy efficiency of the process. The key findings are that microgel NIPAM-co-AEMA-RB effectively generate singlet oxygen with equivalent efficiency under both sunlight and laboratory conditions when exposed to identical irradiation levels. Additionally, the kinetic parameters of RB anchored in the microgel surpass those of free RB, as illustrated in Figure 4. This enhancement is attributed to the local concentration effect caused by the substrate adsorption onto the polymeric matrix, supported by the micellar colloidal structure of PNIPAM at the given temperature [23, 36].



**Figure 4.** Comparison of first-order kinetic parameters for singlet oxygen production between microgel-anchored RB and free RB.

3.3. Studies of Diclofenac Pollutant Photo-Degradation

The degradation capacity of the NIPAM-co-AEMA-RB microgel for the pollutant Diclofenac was investigated following a similar approach to the ADPA studies. Experiments were conducted as described in Section 2.5, under both 50 W halogen lamp irradiation and natural solar irradiation conditions. For the latter, experiments were performed at different times of the year to assess the impact of seasonal sun-light variations. In both setups, the irradiation on the surface of the 500 mL jacketed reactor was monitored, and the temperature was controlled to remain within the range of 23–25°C. The jacketed section of the reactor was filled with the filter solution for wavelengths below 450 nm, preventing direct photodegradation of RB, the microgels and Diclofenac. Inside the reactor, 3.31 g of microgel were added to a 5 ppm Diclofenac solution. For control experiments with free RB, the dye solution concentration was adjusted to  $2.2 \times 10^{-4}$  M, equivalent to the amount of RB anchored to the microgel.

Table 3 presents the results, demonstrating that both NIPAM-co-AEMA-RB and free RB achieved complete degradation of Diclofenac within approximately 3 hours of reaction. As observed previously, the supported dye in the microgel exhibited better reaction kinetics than the free dye, with a clear local concentration effect due to substrate adsorption.

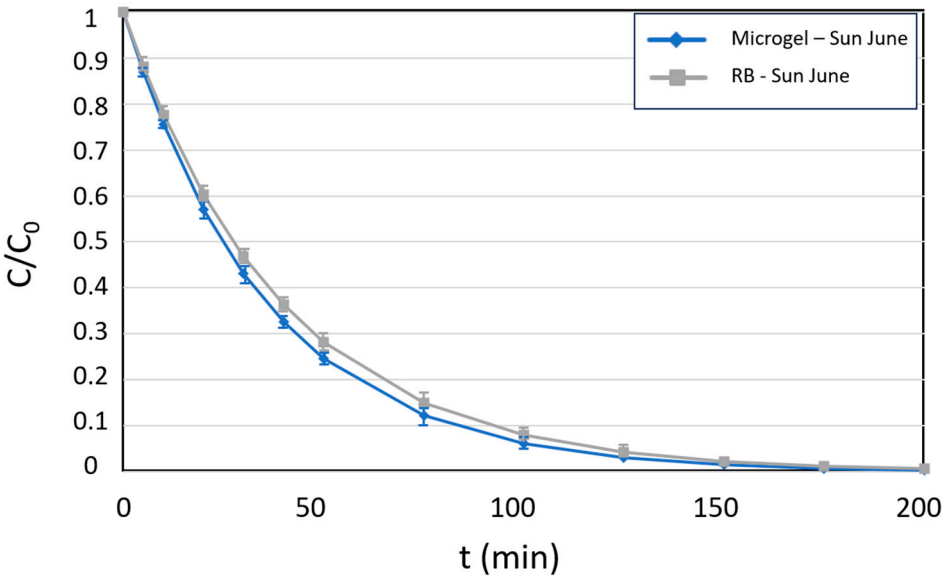
**Table 3.** Measured solar irradiation values and kinetic parameters ( $k_{obs}$  and time for >99% conversion) for Diclofenac degradation conversion under different irradiation scenarios.

Photosensitizer		Solar irradiation (kWh/m <sup>2</sup> )	t (>99%) (min)	k <sub>obs</sub> (min <sup>-1</sup> )
Halogen lamp (sun simulated)	Blank	6.9	-	-
	NIPAM-co-AEMA		-	-
	NIPAM-co-AEMA-RB		164	0.02808
	RB		182	0.02530
Sun natural irradiation June	Blank	7.2	-	-
	NIPAM-co-AEMA		-	-
	NIPAM-co-AEMA-RB		165	0.02791
	RB		181	0.02544
Sun natural irradiation September	Blank	6.1	-	-
	NIPAM-co-AEMA		-	-
	NIPAM-co-AEMA-RB		165	0.02788
	RB		184	0.02532



Sun natural irradiation December	Blank		-	-
	NIPAM-co-AEMA		-	-
	NIPAM-co-AEMA-RB	3.3	169	0.02725
	RB		188	0.02450

An analysis of the seasonal variation experiments indicates that the expected changes in solar irradiation had no impact on the reaction kinetics. This consistency can be attributed to the design of the microgels, which include a sufficient amount of RB to produce singlet oxygen even during periods of reduced solar irradiation [32]. Regarding temperature control, the average recorded temperatures across all experiments, including those with the halogen lamp, were consistently between 23°C and 25°C. The thermostat system in the jacketed reactor was used minimally, except during the experiments conducted in December. In the summer experiments, the initial temperature was 23°C and naturally increased to 25°C without the need for cooling. During winter experiments, the starting temperature was set at 25°C, and the heating system was only activated if the temperature dropped below 23,5°C. The experiments conducted in September and those with the halogen lamp required almost no use of the thermostat system, as the external temperature during these reactions was close to the desired range.



**Figure 5.** Degradation ratio of Diclofenac over time (C) relative to the initial concentration (C<sub>0</sub>), for free RB and NIPAM-co-AEMA-RB in triplicate-performed experiments carried out in June.

The reaction kinetics followed a first-order model in all cases, with half-life times of around 24–25 minutes for NIPAM-co-AEMA-RB and 27–28 minutes for free RB. No degradation of RB, either free or supported on the microgel, was detected during the experiments under either direct sunlight or simulated solar irradiation. Previous studies have reported that heterogeneous catalysis offers the advantage of preventing dye degradation, a phenomenon observed for free RB during Diclofenac degradation in recent works [43, 44]. Likely, the filter used in this design helped prevent the degradation of free RB; however, the primary goal is to ensure that the supported photocatalyst remains stable and active over multiple cycles. Recyclability studies of the NIPAM-co-AEMA-RB photosensitizer were conducted by recovering the photocatalyst via centrifugation and replacing the Diclofenac solution after each cycle. The results were remarkable, with the microgel maintaining its kinetic properties over 40 consecutive cycles without any loss in activity. This limit of 40 cycles was chosen for experimental proof-of-concept purposes and not because of observed performance degradation. In fact, the catalytic regeneration potential is much higher, as the NIPAM-co-AEMA-RB microgel demonstrated recyclability for up to 100 cycles in the photooxidation of ADPA without losing activity (ADPA experiments involved more cycles due to shorter degradation times compared

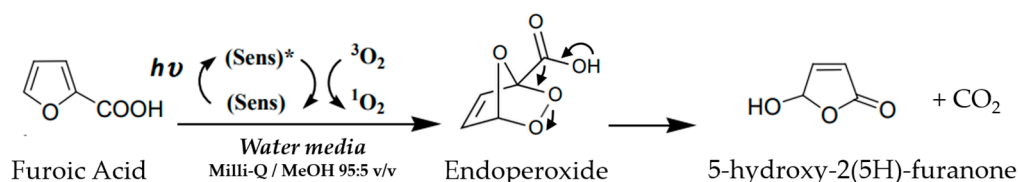
to Diclofenac). These findings confirm that the new colloidal microgels can function as efficient and robust photocatalysts for a large number of reaction cycles.

Finally, it is worth noting that both ADPA and Diclofenac experiments the kinetics suggest degradation via singlet oxygen photocatalysis [17, 31, 32]. However, in the case of Diclofenac photodegradation, the involvement of other reactive species cannot be entirely ruled out, although in this case the reaction kinetics strongly indicate that singlet oxygen is the main driver of the oxidation process. As supported by previous studies [43, 44], reactive species such as  $\bullet\text{OH}$  radicals may contribute to the mineralization of Diclofenac during later stages of degradation following singlet oxygen activity. Nevertheless, this proof-of-concept study aims to demonstrate the sustainable effectiveness of the newly designed green materials in removing contaminants. A detailed investigation into the specific degradation mechanism of Diclofenac and the precise identification of its degradation products falls beyond the scope of this work. Indeed, in the present study, HPLC analysis of the supernatant after Diclofenac degradation revealed no intermediate products such as nitroxides, quinones, or chlorophenols. This suggests that the ring-opening of the contaminant via photooxidation was successful. Nonetheless, due to the absence of comprehensive characterization, the complete mineralization of the drug cannot be definitively confirmed.

### 3.4. Studies of Photo-Oxidation of Furoic Acid and Green Synthesis 5-Hydroxy-2(5H)-Furanone

The green synthesis of 5-hydroxy-2(5H)-furanone was performed using singlet oxygen following the same protocol as with the previous substrates. For this reaction, 166.11 mg of microgel were added to a 500 mL jacketed reactor containing a  $10^{-3}$  M solution of 2-furoic acid in Milli-Q water with 5% methanol (95:5 v/v). The pH was adjusted to match the natural pH of the microgel due to slight acidification of the medium. The jacketed section of the reactor was filled with a  $\text{FeCl}_3$  solution, which acted as a filter for wavelengths below 450 nm and as a temperature regulator. The reaction was carried out under continuous stirring and aeration, with temperature monitored and controlled, and irradiation at the surface of the reaction medium recorded. The synthesis was performed under both simulated sunlight (using a 50 W halogen lamp) and natural sunlight, with experiments conducted at different times of the year to account for seasonal variations.

The mechanism of the photooxidation reaction, shown in Figure 6, has been extensively studied [10, 17, 18]. It involves the activation of molecular oxygen ( $^3\text{O}_2$ ) through light excitation ( $h\nu$ ) of a photosensitizer (*Sens*). The generated singlet oxygen ( $^1\text{O}_2$ ) binds to the furan ring and facilitates the formation of an endoperoxide intermediate, which subsequently leads to the production of 5-hydroxy-2(5H)-furanone. The presence of alcohol in the reaction medium enhances this mechanism. Notably, the 5% MeOH content does not alter the swelling, adsorption, or stability properties of the microgel. Control experiments were performed in the dark and with free Rose Bengal in a 0.011 M solution, equivalent to the concentration of RB anchored to the microgel.



**Figure 6.** Reaction pathway for the photooxidation of 2-furoic acid to 5-hydroxy-2(5H)-furanone via singlet oxygen. The process involves the formation of an endoperoxide intermediate.

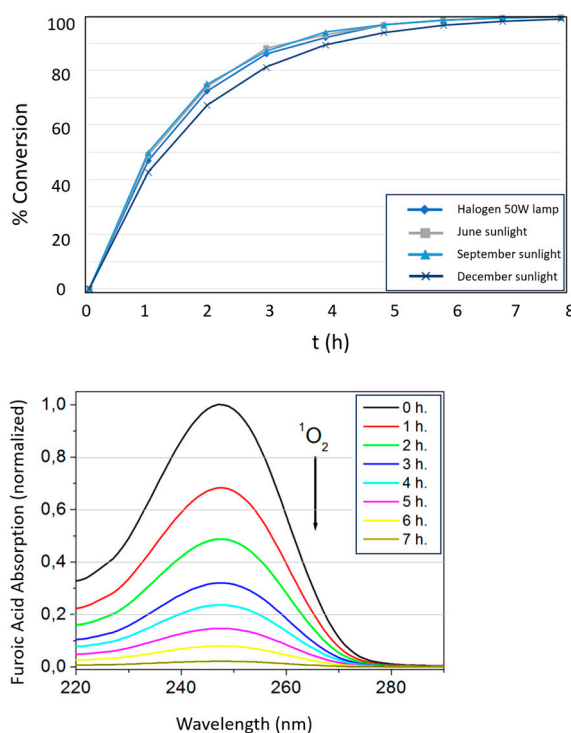
Table 4 presents the kinetic parameters for the different irradiation scenarios, showing that the supported photocatalyst achieved complete conversion of furoic acid to 5-hydroxy-2(5H)-furanone in approximately 7 hours of reaction time in all cases. Additionally, product characterization studies performed by HPLC chromatography confirm a pure conversion to 5-hydroxy-2(5H)-furanone, with no remaining reactants or byproducts detected, such as further oxidation to maleic acid or other compounds.

In this case, the performance difference between free RB and microgel-supported RB is significantly more pronounced than with the previous substrates. The heterogeneous photocatalyst NIPAM-co-AEMA-RB demonstrated enhanced efficiency due to the adsorption properties of the microgel, driven by its micellar structure. This local concentration effect facilitated the interaction between the substrate, the covalently anchored RB, and the MeOH in the system. The notably low reaction kinetics observed for free RB further confirm the importance of the adsorption effect provided by the microgel. According to the literature, this reaction with free RB is only effective in alcohol-based media and fails to proceed in aqueous environments [10, 18]. The use of heterogeneous catalysis and the adsorption effect of the microgel allowed for kinetic parameters in aqueous media that are comparable to those reported in previous studies conducted in 100% MeOH [17]. This result underscores the sustainable design and efficiency of this system.

**Table 4.** Kinetic parameters and conversion rates (t=420 min) for Furoic Acid photooxidation using heterogenous or homogeneous photosensitizers in different irradiation scenarios.

Photosensitizer		Conversion of Furoic Acid at t=420 min	t ½ (min)	k <sub>obs</sub> (min <sup>-1</sup> )
Halogen lamp Irradiation = 6.9 kWh/m <sup>2</sup>	Blank	-	-	-
	NIPAM-co-AEMA	-	-	-
	NIPAM-co-AEMA-RB	>99%	61	0.01143
	RB	12%	2,277	0.00030
June sunlight Irradiation = 7.5 kWh/m <sup>2</sup>	Blank	-	-	-
	NIPAM-co-AEMA	-	-	-
	NIPAM-co-AEMA-RB	>99%	60	0.01140
	RB	13%	2,090	0.00033
September sunlight Irradiation = 6.1 kWh/m <sup>2</sup>	Blank	-	-	-
	NIPAM-co-AEMA	-	-	-
	NIPAM-co-AEMA-RB	>99%	61	0.01134
	RB		2,498	0.00028
December sunlight Irradiation = 2.9 kWh/m <sup>2</sup>	Blank	-	-	-
	NIPAM-co-AEMA	-	-	-
	NIPAM-co-AEMA-RB	98%	74	0.00931
	RB	9%	3,087	0.00022

Within the first hour of reaction, the heterogeneous photocatalyst achieves approximately 50% 5-hydroxy-2(5H)-furanone conversion. Figure 7 depicts the kinetic profiles for the formation of the product under the four irradiation conditions studied. In December, a slightly longer time is required to reach >99% conversion (430 minutes), likely due to the lower average irradiation resulting from shorter daylight hours and the prolonged reaction duration.



**Figure 7.** Left: Conversion ratio of 5-hydroxy-2(5H)-furanone as a function of time under different irradiation scenarios. Right: Evolution of the absorption band ( $\lambda = 246$  nm) of furoic acid as a function of time under the December solar irradiation scenario. In both cases for NIPAM-co-AEMA-RB.

Recyclability studies were carried out during a period of moderate solar irradiation (September and October), spanning 25 complete cycles, equivalent to 175 hours of total irradiation. Due to the limitation of sunlight, each cycle was conducted on a different day, with each reaction lasting 7 hours. Notably, after 25 cycles, the NIPAM-co-AEMA-RB photocatalyst maintained its catalytic performance without any measurable loss of activity. On the other hand, the reaction demonstrates remarkable efficiency, achieving a high yield with excellent atomic economy, fully aligned with the principles of green chemistry and generating practically no by-products. The  $CO_2$  released during the process could be captured using an additional adsorption system, further enhancing its sustainability. Based on the catalytic performance and the mass balance of the 5-hydroxy-2(5H)-furanone synthesis, it is notable that under the studied conditions—representing a TRL of 4-5 and still far from industrial-scale operations—the 500 mL jacketed reactor, with a  $1 \times 10^{-3}$  M concentration of furoic acid, produces approximately 50 g of 5-hydroxy-2(5H)-furanone per cycle (1.25 kg of product in the 25 cycles studied).

### 3.5. Energy Cost-Effective Calculations for Industrial Scale-Up

The energy OPEX calculations for the two proposed systems—emerging contaminant removal and the green synthesis of 5-hydroxy-2(5H)-furanone—were conducted. Energy consumption for both processes was analyzed under two scenarios: halogen lamp irradiation and natural solar irradiation. The calculations were based on the average energy consumption per reaction cycle, determined from a minimum of 20 experiments for each scenario. Seasonal variations were also considered for the solar irradiation experiments. The energy consumption was calculated by multiplying the reaction time per cycle (approximately 3 hours for Diclofenac degradation and 7 hours for the synthesis of 5-hydroxy-2(5H)-furanone) by the power requirements of the equipment used. This included a 50 W lamp (excluded for solar irradiation experiments), a 5 W stirring system, temperature and solar irradiation sensors with a combined power of 8 W, a 1060 W heater (only accounted for the active heating time during each experiment), and a centrifuge, operated for 12 minutes at the end of each cycle to recover the photocatalyst. The results presented in Table 5 reveal



lower energy consumption for Diclofenac degradation compared to furoic acid oxidation, attributed to the longer reaction time required per cycle in the latter process. Importantly, energy consumption under lamp irradiation is more than twice that of direct solar irradiation for both scenarios. This underscores the significant impact of the lamp on overall energy usage. Substituting lamp irradiation with direct sunlight greatly improves the cost-effectiveness and enhances the economic and environmental sustainability of the process.

**Table 5.** Energy consumption across different reactor scales for Diclofenac degradation and Furoic Acid oxidation under halogen lamp and sunlight conditions. Scale-up comparison using Aspen and the Six-Tenths Rule methods (detailed calculations provided in the supplementary material).

Process	Energy consumption (kWh/m <sup>3</sup> ) Reactor 500 mL	Reactor scale-up 1 m <sup>3</sup> . Energy consp. (kWh/m <sup>3</sup> )		Reactor scale-up 100 m <sup>3</sup> . Energy consp. (kWh/m <sup>3</sup> )		Reactor scale-up 1 Hm <sup>3</sup> . Energy consp. (kWh/m <sup>3</sup> )	
		Aspen	Six-Tenths	Aspen	Six-Tenths	Aspen	Six-Tenths
Diclofenac (halogen lamp)	537	24.38	25.69	4.12	4.07	0.27	0.26
Diclofenac (sunlight)	253	12.48	12.09	2.01	1.92	0.12	0.12
Furoic Acid (halogen lamp)	1050	48.36	50.21	7.85	7.96	0.48	0.50
Furoic Acid (sunlight)	375	18.05	17.95	2.92	2.85	0.17	0.18

As detailed in the table, an energy OPEX cost analysis was performed at an economy-of-scale level to assess energy consumption per unit of treated volume. Two approaches were employed in this study to validate the extrapolated results. One method involved the use of the Aspen Plus Economic Evaluation tool, a well-established software widely recognized for its accuracy in estimating economy-of-scale costs from real chemical process data and its effectiveness in calculating operational expenses, including energy OPEX. The Rule of Six-Tenths, a widely recognized method in chemical engineering for estimating both CAPEX and OPEX costs across different scales, was also applied [60-63]. The results obtained from both approaches are closely aligned, demonstrating a clear and expected trend: as the treatment volume increases, the energy consumption per unit volume (kWh/m<sup>3</sup>) decreases. For instance, at a TRL 6-7 scale with a reactor volume of 1 m<sup>3</sup>, the energy OPEX for sunlight-driven treatments is approximately 12 kWh/m<sup>3</sup> for Diclofenac and 18 kWh/m<sup>3</sup> for Furoic Acid, which is notably lower than the energy consumption observed for the 500 mL experimental reactor at TRL 4-5. In an industrial-scale scenario, such as a treatment plant with a capacity of 1 hectometer cubed of water, the energy consumption further decreases to approximately 0.1–0.2 kWh/m<sup>3</sup> treated, representing a highly competitive energy demand for a water purification process [64].

Within the principles of Green Chemistry, the reactor operates without requiring any additional chemical compounds beyond the microgels. Furthermore, the natural pH of the microgels closely aligns with that of wastewater effluents from WWTPs, making the system well-suited for integration as an advanced tertiary or quaternary treatment in current water disinfection processes. While the use of direct sunlight for industrial-scale applications poses challenges—such as the spectral distribution of solar photons, interruptions due to the day/night cycle, and weather variability [45]—the proposed system can be designed for flexibility. It can utilize both solar and artificial light sources, with a preference for sunlight to enhance sustainability, while artificial light serves as a reliable alternative when sunlight is unavailable.

## 4. Conclusions

The microgels, designed following green chemistry principles, utilize a PNIPAM-based polymeric matrix with covalently anchored Rose Bengal, exhibiting properties to enhance substrate adsorption, reaction efficiency, and environmental sustainability. Their design supports sunlight-driven photocatalysis and sustainable applications in water treatment, achieving high polymerization efficiency, minimal waste, and reusability across multiple cycles. By using molecular oxygen from air as the oxidant and sunlight as the energy source, photocatalysis aligns with green chemistry principles, eliminating chemical oxidants and reducing energy barriers, thereby ensuring both environmental and economic benefits. NIPAM-co-AEMA-RB demonstrated effective adsorption properties for ADPA, Diclofenac, and furoic acid, attributed to its colloidal structure, which facilitates substrate adsorption within micellar-like configurations. The reaction kinetics were superior to those of free RB, driven by the local concentration effect enabled by the polymeric matrix's micellar colloidal structure at the reaction temperature. NIPAM-co-AEMA-RB achieved complete Diclofenac degradation in approximately 3 hours and the synthesis of 5-hydroxy-2(5H)-furanone within 7 hours. Recyclability studies demonstrated photosensitizer stability, maintaining kinetic properties over 25 cycles in 2-furoic acid photooxidation, 40 cycles in Diclofenac degradation, and 100 cycles in ADPA oxidation. The microgel's adsorption properties enabled the synthesis of 5-hydroxy-2(5H)-furanone in aqueous media using the supported photocatalyst, contrasting with free RB and previous studies requiring alcohol-based solvents. This underscores the sustainable design of these materials, facilitating green catalytic reactions in water. Industrial-scale studies of the proposed system estimate energy consumption at 0.1–0.2 kWh/m<sup>3</sup> for direct solar-driven reactions, confirming its energy efficiency and sustainability in water treatment applications. Future research should explore the photooxidative potential of these microgels for other environmentally and sustainably relevant reactions, investigate the degradation of additional CECs, and innovate in polymeric structure design and substrate adsorption properties.

**Supplementary Materials:** The following supporting information can be downloaded at the website of this paper posted on Preprints.org

**Author Contributions:** Conceptualization, V.F.; methodology, V.F.; formal analysis, V.F. and J.M.P.; investigation, V.F.; data curation, J.M.P.; writing—original draft, J.M.P.; writing—review & editing, V.F.; project administration, V.F. All authors have read and agreed to the published version of the manuscript.

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**Data Availability Statement:** Data is contained within the article.

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**Conflicts of Interest:** The authors declare no conflicts of interest.

## Abbreviations

The following abbreviations are used in this manuscript (ranked in order of appearance):

CECs	Contaminants of Emerging Concern
WWTPs	Wastewater treatment plants
PNIPAM	Poly(N-isopropylacrylamide)
RB	Rose Bengal
EPs	Emerging pollutants
ADPA	9,10-anthracenedipropionic acid
DLS	Dynamic light scattering
UV-Vis	Ultraviolet-visible spectroscopy
HPLC	High-Performance Liquid Chromatography

NIPAM	N-isopropylacrylamide
AEMA	Aminoethyl methacrylate
MBAM	N,N'-methylenebisacrylamide
EDC	1-[3-(dimethylamino)propyl]-3-ethylcarbodiimide
MeOH	Methanol
$t_{1/2}$	Half-reaction time
$k_{obs}$	Observed rate constant or observed $k$
$^1O_2$ or $O_2(^1\Delta g)$	Singlet oxygen
$^3O_2$	Molecular oxygen
$h\nu$	Light excitation or photon energy
TRL	Technology Readiness Level
CAPEX	Capital Expenditure
OPEX	Operational Expenditure

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