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Article

# A Numerical Simulation Study on the Critical Erosion of Laboratory-Scale Debris Flow

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#### **Abstract**

Debris-flow erosion is key to the potential escalation of hazards, which could endanger the adjacent ecosystem. However, studies pertaining to this issue are impeded by the intricate interactions of flow and sediment. Thus, this study introduces an unresolved CFD-DEM coupled simulation primarily relying on a classical numerical simulation and a physical experiment to study critical erosion process of debris flows on a dry basal sediment under laboratory-scale. Results indicate that three layers of substrate bed can be verified during the erosion process, and there is a positive correlation between the erosion depth and the particle size with the Froude number of debris flow, as well as between the erosion length and the critical entrainment transport with the total mass of debris flow. In addition, thresholds for the collisional point load and the impact energy of debris flow head, which are essential for predicting the attenuating rates of erosive depth and the critical entrainment transport, have been proposed based on data regressions derived from power functions. The coupled numerical approach is capable of accurately simulating the erosion behavior of debris flows similarly to physical model experiments, thereby providing both theoretical and practical insights into the dynamics of erosion.

Keywords: debris flow; numerical simulation; CFD-DEM; critical erosion

# 1. Introduction

Debris flows are typically classified as multi-phase mass movements characterized by distinctive shear dynamics, diverse particle composition, as well as variations in runout distance and volume [1-3]. The erosion of debris flow refers to complex flow-sediment interaction mechanisms that induces varied eroding magnitude, mobilization, and deposition [4–7]. The erosion dimension from the initiation of the flow should be taken into consideration to study how this phenomenon emerges or ends, which is vital to early-warning system and counter-measures [8,9]. Various methods, including quasi-theoretical analysis, physical model experiment, field testing, and numerical simulation, have been employed to study erosion, with the erosion or entrainment rate serving as a key indicator for sediment transport models e.g. [5,6,10–12]. Egashira et al. [13] conducted experiments in a flume and discovered that the erosion rate of debris flows is closely related to the grain size of the eroding bed particles, and it has no significant correlation with the solid volume fraction of the debris flow. Berger et al. [10] indicated the commencing of the erosion resulting from the collision between the debris flow head and the substrate by field measurements. This point was likewise emphasized by Choi and Song [14] and Jiang et al. [9], who both further asserted that the collisional stress associated with particle movements of the flow head is responsible for the erosion process of unsaturated or dry bed sediment. Besides, shearing stress is also proven to be one of the important parameters for entrainment models [12,15]. And Ning et al. [16] added the shearing stress and the peak discharge of debris flow are crucial to the erosion process of not only the substrate but also the bank if any. There seems insufficient evidence to determine which of the two types of stress is more potent in the erosion process. Furthermore, the critical erosion process that governs the run out of debris flow is still unclear.

Indeed, the erosion is supposed to be derived from the collision between flow head and bed sediment or bank, which can be defined by the collisional stress [9], while factors that affect the commencing of collision-induced erosion needed further understanding. Additionally, when the debris flow reaches maturity, the erosion rate is directly proportional to the net basal shear stress produced by the ensuing flow, which contains a great proportion of liquid [6]. Consequently, the erosion model of a debris flow is expected to demonstrate an initiation through particle collisions, followed by sediment transportation that is influenced by friction shearing on basal sediment [14]. In this matter, point loads denoting the initial collisional effects may be key to the model for anticipating the erosion. Such a hypothesis was verified by previous studies e.g. [17] but requires continuous data to backup its effectiveness. Numerical simulation from the perspective of fine observation is an emerging important means. The two-way coupling of CFD (Computation Fluid Dynamics) and DEM (Discrete Element Method) is expected to be a powerful and efficient tool for the numerical investigation of multi-phase flows [18,19]. The basic logic of the CFD-DEM coupling model, including the interactions among particles, between particles and CFD cells, and between particles and walls, is introduced through continuous and discrete algorithms. Various configuration is established based on the logic to meet different requirements, in aspects such as the dynamic viscosity associated with the nonlinear rheology of debris flow [7], the adopted smooth grid approach to refine the transfer of coupling information [20], and the coarse coupling without resolution in consideration of computation efficiency [21,22].

In comparison to physical model experiments, the documentation of erosion quantities without deposition effects, particle collisions and shearing frictions in a two-way coupling simulation is more feasible, as physical models primarily rely on indirect measurements and continuum-flow and/or depth-integrated estimations [11,23].

To address these issues, this paper introduces a CFD-DEM coupling method validated by a simple simulation and a physical model test. Then the methodology is adopted to simulate the erosion caused by debris flows on a dry bed sediment and to examine its correlation with various related factors. Factors for evaluating the collisional and shearing effects on erosion depth and longitudinal eroding range are mainly introduced and physically discussed.

# 2. Materials and Methods

#### 2.1. Coupling Logics

The coupled simulation is mainly focusing on interaction forces between spherical particles and fluid constrained in an impermeable and rigid facet geometries. And a dam breach approach herein is employed for the initiation of a debris flow and the flow propagation upon based on some criteria [7,22].

Above all, the CFD-DEM coupling in this study is unresolved, meaning the fluid cell size is larger than the maximal diameter of solid particles, for accurate resolution of the particle volume fraction and hydrodynamic forces on the fluid grid. This situation is also a trade-off made to achieve better computation efficiency. To comprehensively understand the CFD-DEM coupling model, it is necessary to go through the details about the continuous feature of fluid (including air and liquid), the discrete contacts among particles, and most importantly the interaction of fluid-particle media.

The CFD method is started with the continuity equation, considering both air and water fluids [18]:

$$\frac{\partial(\epsilon\rho)}{\partial t} + \nabla(\epsilon\rho\vec{u_f}) = 0 \tag{1}$$

where  $\varepsilon$  is the porosity of a CFD cell;  $\rho$  is the equivalent density of the fluid defined by air and liquid;  $\vec{u_f}$  is the mean velocity of the fluid through the cell. According to the above discrete-cell approach the averaged Navier-Stokes equation is introduced to solve the dynamics of fluid:

$$\frac{\partial(\varepsilon\rho)}{\partial t} + \nabla(\varepsilon\rho\vec{u_f}\otimes\vec{u_f}) = -\varepsilon\nabla\vec{p} + \nabla(\varepsilon\tau) - \vec{F_p} + \varepsilon\rho g \tag{2}$$

where  $\vec{p}$  denotes fluid pressure;  $\vec{F}_p$  is the interaction force on the fluid per unit cell volume.

As for the DEM side, the motion of a particular particle i (involving translation and rotation) is mainly based on the Newton's Second Law while the resultant force is derived from gravitational, particle-particle contact and particle-fluid interaction forces:

$$\begin{cases} m_i \frac{d\vec{u}}{dt} = m_i g + \Sigma \vec{F}_{ij} + \vec{F}_{fi} \\ I_t \frac{d\vec{\omega}}{dt} = \sum_{i=1}^{n_{ij}} \vec{T}_{ij} \end{cases}$$
(3)

where  $m_i$  and  $I_t$  are the mass and the rotational moment of inertia of particle i, respectively.  $\vec{T}_{ij}$  is the torque generated by other particles imposing rotation. Herein the Hertzian-Mindlin contact law is dominantly introduced to govern the inter-particle contact criteria in DEM and the force-deformation law, which won't be repeated in this study due to its reliability [7,18].  $\vec{F}_{ij}$  denotes the contact force exerted by other particles.  $\vec{F}_{fi}$  is the interaction force exerted from the fluid cell integrated with the drag force  $\vec{F}_d$ , buoyancy force  $\vec{F}_b$ , and lifting force  $\vec{F}_l$ . These forces are briefly introduced as follows:

$$\vec{F}_d = \frac{1}{2} C_d \rho \frac{\pi d_p^2}{4} |\vec{u}_f - \vec{u}_p| (\vec{u}_f - \vec{u}_p) \varepsilon^{-\chi + 1}$$
(4)

where  $d_p$  is the particle diameter,  $u_p$  the particle velocity, and  $\varepsilon^{-\chi+1}$  the correcting coefficient of porosity, representing the influence from other solid particles within the cell. And the  $\chi$  is computed by:

$$\chi = 3.7 - 0.65 \exp\left[-\frac{(1.5 - \lg Re_p)^2}{2}\right]$$
 (5)

where  $Re_p$  denotes the Reynolds number defined at the particle diameter scale, yielding:

$$Re_p = \rho d_p |\vec{u}_f - \vec{u}_p|/\mu \tag{6}$$

where  $\mu$  is the dynamic coefficient of viscosity. And  $C_D$  is the drag coefficient which can be computed according to [24]:

$$C_D = \begin{cases} \frac{24}{Re_p} (1.0 + 0.15Re_p^{0.687}) & (Re_p \le 1000) \\ 0.44 & (Re_p > 1000) \end{cases}$$
 (7)

The buoyancy force is defined by the affecting volume Vs and the gradient of the fluid pressure p:

$$\vec{F}_b = -V_s \nabla \vec{p} \tag{8}$$

Herein the lifting forces are introduced in the model in case the low solid fraction of debris flow.

$$\vec{F}_l = \frac{1}{8} \rho \vec{u_r}^2 \pi C_L d_p \frac{\vec{\omega_r} \cdot \vec{u_r}}{|\vec{\omega_r}| |\vec{u_r}|}$$

$$\tag{9}$$

where  $\vec{u_r}$  and  $\vec{\omega_r}$  are the relative linear and angular velocities between particles and fluid, respectively.  $C_L$  denotes lifting coefficient and has the following expression :

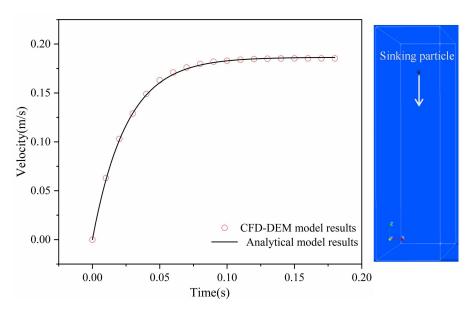
$$C_L = \begin{cases} \frac{|\vec{\omega_r}|}{|\vec{u_r}|} d_p & (Re_p \le 1) \\ \frac{|\vec{\omega_r}|}{|\vec{u_r}|} d_p (0.178 + 0.822Re_p^{-0.522}) & (1 < Re_p < 1000) \end{cases}$$
(10)

During the development of the two-phase movement, the negative term of the sum of  $\vec{F}_d$  and  $\vec{F}_l$  is distributed back to the fluid cell, becoming  $\vec{F}_p$ .

At last, the MPI criteria (Message Passing Interface) is utilized to implement fluid and particle media kinematic information exchange including interaction force and particle movements. The

frequency of the exchange is set to 10 time step in the CFD domain while it is one time step in the DEM.

The calibration of the model parameters is expected to be ensured following meticulous benchmarking procedures [18,25–27]. To do so, the CFD-DEM coupling herein is firstly benchmarked using a concise simulation plan involving a spherical particle (with a diameter of 1 mm) sinking in an initially static liquid under drag force, buoyancy force and gravity interpreted by the CFD domain. This approach was proven to be efficient in terms of quick benchmarking [28] and the coupling interaction governed by multiple parameters is then verified. The particle is descending in a 0.2\*0.2\*0.6 m CFD domain. The descending velocity of the particle  $U_d$  in this design scenario served as the dominant factor for comparison with the one solved by the empirical analytical model [7,20]. The analytical  $U_d$  varied with time computed according to [29], is added to compare with the numerical solution. As shown in Figure 1 the plotted data set of  $U_d$  fits the analytical model rather well, justifying the interaction forces set in the coupling framework.



**Figure 1.** (left) the data set of the velocity of the sinking particle varied with time from analytical model and numerical calculation and (right) the simulation scene.

**Table 1.** The configuration of parameters for numerical simulations.

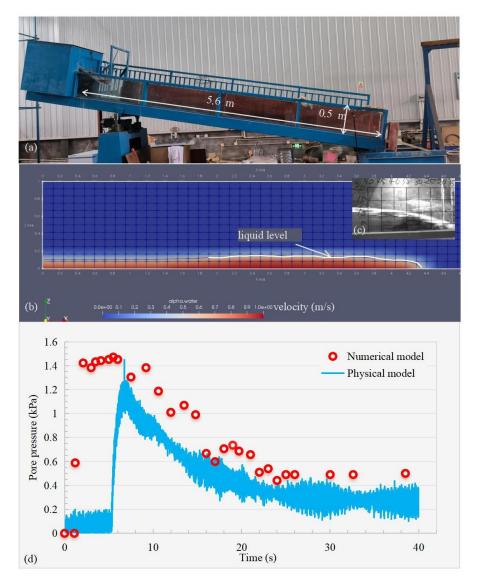
Parameters	Sinking sphere	Erodible bed	Debris flow
Cell size for CFD domain (mm)	20*20*20	60*100*60	60*100*60
Mean particle diameter (mm)	1	10	$20/30/40^1$
Gravity acceleration $(m/s^2)$	9.81	9.81	9.81
Dynamic viscosity of liquid ( $Pa \cdot s$ )	9.81	9.81	9.81
Message exchange resolution (time steps)	10	10	10
Friction coefficient	0.7	0.7	0.7
Rebound coefficient	0.4	0.4	0.4
Poisson's ratio	-	0.3	0.3
Time step (sec)	0.01	0.001	0.001
Solid fraction	-	1	$0.45/0.50/0.55^{2}$

<sup>1</sup> and <sup>2</sup> denote three different mean diameters and solid fractions, respectively.

#### 2.2. Experiments for Validation

Indeed, this simulation failed to fully capture the dynamic scenarios especially for the angular contacts and the porosity evolution among particles. Since the pore water pressure evolution is one of the essential indices that affect the debris-flow dynamics and transportation [12,30–33], we have added a series of physical flume model tests as prerequisite to further validate the numerical model of

debris flow. The pore pressure dissipation within the flow propagation of both physical and numerical approaches was compared.



**Figure 2.** comparative analysis of pore pressure evolution presented between (a) the physical flume model and (b) the numerical model (60\*60 mm per grid), as well as (c) the flow profile in the real model (50\*50 mm per grid) and (d) the data set obtained from the numerical computation and the actual sensor.

The flume which has the length and the width of 5.6 m and 0.3 m respectively is inclined by 20 degrees initially and the base-plate is paved without sediments serving as a rigid bed (Figure 2a). A mixture of sand gravel, clay and water with a solid fraction is mixed together to mimic real debris flows (76 % of grain, 24 % of water and clay), which has been already introduced by [34]. The mixture is firstly put and kept stirring in a hopper located at the top of the flume and then is released through the gate at the bottom of the hopper forming a moving slide on the rigid flume bottom. A pore pressure sensor is placed at the bottom plate 3 m downstream from the top trying to detect the pore pressure during the mature flow propagation and the sampling rate is 100 HZ. The right side of the flume is transparent, and a camera is employed to trace the flow process. On the other hand, the numerical model is established based on the physical flume model, except the distribution of the particle size was reduced to enhance computational efficiency, as specified in the Table 1. Based on the physical flume model, the whole motion during this numerical simulation is bounded by a box geometry (forming a chute inclined by 20 degrees) with 5.0 m length, 0.3 m width and 1.0 m height (Figure 2b). The debris flow mixture, referred to as a pack of DEM particles with a uniform diameter of 20 mm, is initially

confined within a box filled with the CFD fluid at the upper section of the chute (0.3\*0.5\*0.5 m), and is subsequently initiated in accordance with a dam-breach pattern. In this context, we emphasize the significance of pore pressure dissipation in comparison to the one in the physical model test, thus the pore pressure evolution data set is directly computed by the detected water level within the debris flow head, which gives:

$$p_0 = \rho g h \tag{11}$$

where h is the height from liquid surface to the bottom boundary. Note that the pore pressure here is considered as only the liquid flow propagation within debris flow and no excess pore pressure was taken into consideration due to the coarse grains-feature of the frontal head [35,36].

The numerical simulation trial here demonstrates close agreement with the physical model in terms of the maximum magnitude and the growth trend of the pore pressure, with both exhibiting a gradual dissipation process (Figure 2d). However, distinct temporal discrepancies are also observed: the numerical model sustains elevated pore water pressure for a longer duration (4.0 sec) compared to the physical model's 0.4 sec (as recorded by the pore pressure transducer), which still showed a continuing downward trend. The discrepancies could be resulted from different particle diameter distribution and porosity between the numerical and physical models. General findings indicate that the uniform spherical particle-pack setting in the coupled approach effectively captures the pore pressure dissipation patterns and provides a reliable representation of debris flow transport mechanisms. Besides the ratio  $\lambda$  of pore pressure to normal pressure of debris flow indicating the liquefaction was also compared. The values of  $\lambda$  are 0.5 for the numerical simulation and 0.7 for the physical test, respectively (Table 2), which are both within the appropriate range according to [37].

Results Physical model Numerical model Pore pressure dissipation time (s) 38 26 Mean flow velocity U (m/s) 1.32 2.30 Mean flow thickness  $h_d$  (m) 0.10 0.15 1.68 1.93 Fr Deposit depth (m) 0.150.160.7 0.5 λ

Table 2. representative results from physical and numerical models.

Moreover, as shown in Table 2, the comparison of the fluid kinematics of the numerical simulation with the physical experimental data set reveals that both the averaged velocity U and the thickness  $h_d$  of the debris flow head in the physical model are smaller, while the Froude number Fr as computed by Eqn. 12 and the final deposit depth are both quite close. This substantiates that the numerical simulation is able to effectively solve the flow kinematics driven by inertial forces.

$$Fr = \frac{U}{\sqrt{gh_d\cos\alpha}} \tag{12}$$

In conclusion, following the aforementioned verification, the adopted parameter values were determined and listed in the right-hand column of Table 1.

## 2.3. Procedure for Formal Simulation Experiments

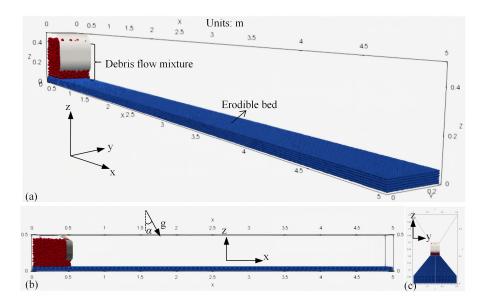
The formal simulation experiments adhere to the key perspectives from the validation experimental procedure, as detailed in the Section 2.2, including for instance the inclined (fixed 20 degrees) chute defined by wall geometries, the dam breach-like initiation of debris flow, and the CFD resolution etc. A notable distinction from the validation experiment is that in formal experiments an additional pack of DEM spherical particles with uniform diameter of 10 mm served as a layer of dry bed sediment, 0.06 m thick, is paved across the bottom-bound geometry (Figure 3).

Mixtures comprising three types of masses, grain size distributions, and solid fractions, respectively, are generated to produce debris flows with diverse flow regime or dynamics along the x-axis in Figure 3b and interacting with a dry basal sediment. The detailed configuration of experimental variables is presented in Table 3, and the experimental serial nomenclature is established based on the conditions. It is noteworthy that uniform grain diameter distribution of the debris mixture as well as the basal sediment is setup in each case as a representative of the mean grain diameter of in-situ debris flow, and the given diameter of debris particles is always larger than that of the bed sediment with a diameter of 10 mm (see Table 1).

**Table 3.** Experimental variables.

Solid fraction (%)	Uniform diameter of debris flow (cm)	Total mass (kg)	Serial ID.	
		115	D4M115V55	
55	4	150	D4M150V55	
		185	D4M185V55	
		115	D3M115V55	
55	3	150	D3M150V55	
		185	D3M185V55	
55		115	D2M115V55	
	2	150	D2M150V55	
		185	D2M185V55	
		115	D4M115V50	
50	4	150	D4M150V50	
		185	D4M185V50	
		115	D3M115V50	
50	3	150	D3M150V50	
		185	D3M185V50	
50		115	D2M115V50	
	2	150	D2M150V50	
		185	D2M185V50	
		115	D4M115V45	
45	4	150	D4M150V45	
		185	D4M185V45	
45		115	D3M115V45	
	3	150	D3M150V45	
		185	D3M185V45	
45		115	D2M115V45	
	2	150	D2M150V45	
		185	D2M185V45	

e.g. D2M150V45 D2, M150, and V45 denote grain size of 2 cm, total mass of 150 kg, and solid fraction of 45 %, respectively.



**Figure 3.** Numerical simulation setup of (a) the axonometric view, (b) the longitudinal view ( $\alpha$  inside means inclined angle of 20 degrees), and (c) the frontal view of the model.

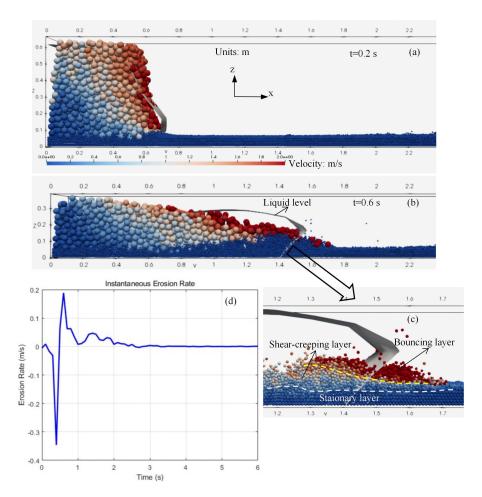
#### 3. Results

In this section, the erosion process is analysed progressively in relation to bed sediment surface morphology and its mesoscopic interactions with the flows. Along the flow direction (x-axis in Figure 3), by measuring the volume variation of the erodible bed along the z-axis within each 0.01 m interval ( $\Delta x = 0.01$  m) and dividing it by the base area, an averaged erosion depth is obtained. Accordingly, the dimension of the eroded material are quantified.

#### 3.1. Erosion Phases

The initiation of the dam-break of the mixture signifies the time of 0 seconds. Even with differing experimental conditions, the erosion process can be generally divided into three phases: i) incipient intrusion into the substrate, namely the initial phase; ii) the net erosion phase; and iii) flowing attenuation leading to deposition, namely the post erosion phase. Sediment transport varied slightly depending on experimental conditions. In the following content, case D4M185V55 is selected as the representative example for illustrating the phases of erosion resulting from the most pronounced findings under high-dose of conditions, and the remaining cases are presented in the Appendix A.

In the initiation phase, the time duration varies slightly under different conditions, but is generally constrained within the range from 0 to 0.3 s. Debris mixture descends and flows forward, with a nearly uniform distribution of particle velocity (Figure 4a). It is believed that the descending is more pronounced, and the extent in erosion depth is negligible (less than 0.1 mm). The debris flow head develops at around x=0.6 m and ultimately reaches maximum x=1.8 m downstream. The generation is dependent on the dam-breach pattern while there are multiple different kinds of initiations in practice. Analysis relying on the particular initiating model does not hold significant practical guidance. Therefore, the phase serves solely as a temporal basis for distinguishing between the subsequent erosion and deposition phases.



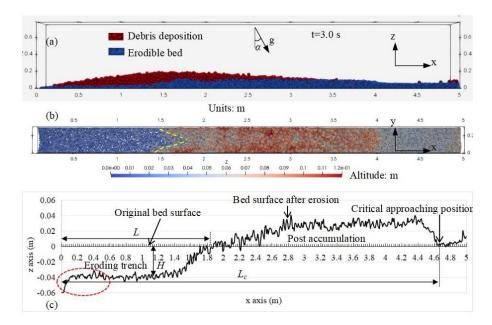
**Figure 4.** The erosion processes (taking D4M185V55 as an example): (a) initial phase, (b) the debris flow propagation and (c) the separated erodible bed at the net erosion phase, and (d) the erosion rate varying with time.

During the net erosion phase, the primary concern is focusing on the spatial range where x > 0.6 m. The liquid profile in Figure 4b, similar to a surge wave, indicates the formation of the debris flow head, and the flow head moved along the x-axis from 1.2 to 3.1 m, with the associated time interval ranging from 0.3 to 3.2 s. The velocity of debris flow is stratified, typically increasing from the lower rear layer to the upper front (Figure 4b), indicating the highest erosion potential of the flow head. The effect of erosion on the bed sediment can be described as a plough induced by particle collisions. The particles located on the surface of the basal bed are characterized as being eroded at a velocity that approximates that of the flow head (Figure 4c). This shallow layer of particles is called the stimulated bouncing layer, and further down they are defined as shear-creeping layer and stationary layer, respectively, according to the velocity distribution (Figure 4c). The erosion rate herein  $r_e$  (m/s) is determined according to the erosion depth measured along the y-axis at one certain position of  $x = x_0 \pm 0.1$  m:

$$r_e = \frac{H_2 - H_1}{t_2 - t_1} \tag{13}$$

where  $H_2$  and  $H_1$  are the erosion depths at the time  $t_2$  and  $t_1$ , respectively. The erosion rate at  $x=1.2\pm0.1$  m, as a function of time, exhibits a sharp increasing trend at the beginning, followed by a gentle decreasing trend toward the end of this phase (Figure 4d). As a result of the substantial collision between the debris flow and the surface particles, the particles from the eroded bed were incorporated into the initial erosion rate calculation (before time of 0.5 s). This led to a significantly large negative value for the erosion rate prior to reaching the peak value (Figure 4d). However, the subsequent curve can effectively represent the variation of the erosion rate over time. It can be deduced that the transient collision of particles contributes to the sharp increase in the erosion rate (at time of  $0.6\pm0.1$  s), allowing

partial particles of the bed move at a velocity nearly identical to that of the debris flow and form like a surge front (Figure 4c). And the gentle decreasing erosion from  $0.6\pm0.1$  to  $3.2\pm0.1$  s, indicating the shear-creeping layer of the bed, results from the shearing friction afterwards. The two layers of the erodible bed will be further discussed later on.



**Figure 5.** The post erosion phase (taking D4M185V55 as an example): (a) the longitudinal view, (b) the plan view, and (c) the profile of the bed after erosion (note that H, L, and  $L_c$  denote the erosion depth, the erosion length, and the critical bed sediment transport displacement, respectively).

On the other hand, the erosion rate fluctuates a little and tends to zero after 2.2 s (Figure 4d), indicating the onset of the attenuation phase. In a longitudinal perspective, there is a prevailing trend of thicker deposition observed in the rear segment, contrasted with thinner deposition in the front segment, while the flow body with the eroded materials extends to the farthest point of x = 4.63 m (Figure 5a). The erodible bed exhibits an arrow-like shape, with greater depth in the middle central region and shallower profiles at both lateral sides. This reveals that during the erosion process, the rheology of the debris flow still prevails, with a larger momentum in the centre and smaller momentum on the sides (Figure 5b). The particles of the bed upstream are evidently eroded, thereby leaving a shallow trench upstream while elevating the bed surface downstream (Figure 5c), and the demarcation line separating these two areas fluctuates between x=1.2 and x=1.8 m, depending on varying conditions (x=1.8 m in the case D4M185V55). It is noteworthy that the eroded interface of the bed material is presented as averaged values under unit width of the flume. Once again, we direct our attention to locations where the flow head has reached the net erosion state (x>0.6 m) to eliminate any potential bias that may arise from the initiation of the dam breach. As shown in the red dotted oval in Figure 5c, the erosion quantities in that area is neglected.

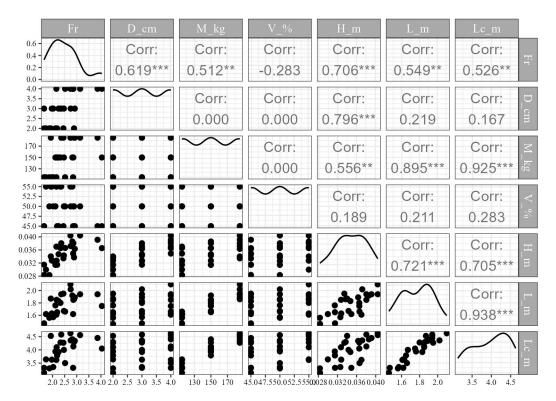
#### 3.2. Factors Contributing to Eroding Dynamics

In this context, the experimental variables, including the total mass, particle size, solid fraction of debris flows, and the derived kinematic parameters, were selected as factors to evaluate erosion. The analysis is mainly performed on the erosion depth at x = 1.2 - 1.4 m, where all the authorized debris flows transit into the net erosion phase and the flow heads shape up. According to sections 2.2 and 3.1, the Froude number Fr is primarily employed to assess the flow dynamics. The longitudinal erosion range as well as the entrainment is further evaluated. All data results in relation to experimental variables can be checked in Table A1.

Figure 6 illustrates that the particle size D of the debris flow exhibits a strong positive correlation with the final erosion depth H (correlation coefficient r = 0.796), whereas the total mass M and

the solid fraction V demonstrate weaker and the weakest correlations with H (r = 0.556 and 0.189), respectively. This trend is likewise observable in the relationship between the erosion length L and the aforementioned factors, whereas the correlation coefficient r between M and L is greater than that between M and M (0.895 compared with 0.556), and M between M and M (0.219 compared with 0.796). Moreover, M of the bed sediment, as indicated by the farthest approaching position of the post accumulation illustrated in Figure 5c, exhibits a stronger positive correlation with M, with M of 0.925. And the strongest positive correlation (M =0.938) between M and M indicates that the large erosion magnitude could significantly enhance the run out of debris flow. Meanwhile, M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M show very limited correlation with M and M and M and M show very limited correlation with M and M and M and M show very limited correlation with M and M and

It is also inferred from Figure 6 that a greater grain size D and mass M of debris flow, accompanied by a lower solid fraction V, may result in a larger Fr, and the positive correlations between Fr and H, L, and  $L_c$  remain valid (showing r = 0.706, 0.549, and 0.526, respectively). Therefore, the grain size D and the mass M of debris flow are both explicitly key variables in the erosion process, with the exception of the V. And D has more evident impact on H while M has more evident impact on L and  $L_c$ . In addition, the flow regime also has a considerable impact on the extent of the erosion. However, it is not reliable to directly compare the impacts of M and D on erosion with that of Fr, as M and D here have only three variations while Fr has P0 runs.



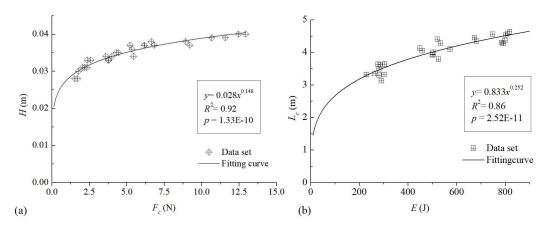
**Figure 6.** The correlation pairs between the variables including Fr, diameter D, total mass M, solid fraction V, the erosion depth H, the erosion length L, and the critical bed sediment transport displacement  $L_c$ .

#### 3.3. Mechanical Factors

To further study the critical mechanisms underlying erosion and propagation, contact forces with respect to the collisional effect between the flow head and the basal particles were detected. The detection is focused on the debris particles within the range x=  $1.2\pm0.1$  m where the flow head approaches at the commencing of the net erosion phase (when the time is  $0.6\pm0.1$  s). And the collisional force is computed as the scalar quantities of the contact forces exerted from the particles of the flow head per unit:

$$F_c = \frac{\sum \sqrt{F_x^2 + F_y^2 + F_z^2}}{n_i} \tag{14}$$

where  $F_x$ ,  $F_y$ , and  $F_z$  are the components in the x, y, and z directions of the contact force, respectively, and  $n_i$  is the number of the particles of the flow head reaching the given region. The contact force  $F_c$  here is documented using the numerical coupling method, which encompasses normal and tangential components, and is also referred to as point loads. In this matter, as  $F_c$  increases, it also increases H in proportion, meanwhile a curve indicated by power-law was able to match the data points with the coefficient of determination  $R^2$  being equal to 0.92 and p-value much less than 0.05 (Figure 7a), revealing a significant statistical relationship between the two variables. The power-law was predominantly applied because of the trend suggesting that H should equal zero when in the absence of force. The slope of the fitting curve exhibits a trend of transitioning from steep to gentle around a certain range ( $F_c = 2.5$  to 4 N), suggesting that this is a threshold of change in the erosion rate.



**Figure 7.** The erosion depth H (a) and the erosion length L (b) as functions of the point load  $F_c$  and the impact energy E of the flow head, respectively.

On the other hand, an impact energy approximation of debris flow head is introduced as an integrated factor affecting the length of the erosion, which leads to:

$$E = Mgh(1 + \frac{Fr^2}{2}) \tag{15}$$

Similarly, a power-law regression model effectively interprets the relationship between  $L_c$  and the impact energy E, and the increasing rate of  $L_c$  along E is slow after E reaches from 130 to 150 J (Figure 7b). Further validation may be needed through addition of data set within a smaller range of E (e.g. E < 200 J). Accordingly, the collisional force  $F_c$  is key to the erosion depth extent E0 while the impact energy E1 governs the critical erosion length E2. There are specific thresholds in E3 and E4 that distinguish between rapid and slow rates of increase for E3 and E4.

#### 4. Discussion

#### 4.1. Mechanisms of the Critical Erosion

This study particularly emphasizes on the net erosion process, specifically examining how the erosion develops under varied conditions. The erodible sediment presented was distinctively noted as comprising the layers of bouncing and creeping shear, which has the same feature of granular flow [39,40]. Note is made that the two-layer sediment is mobilized at an averaged velocity (denoted as erosion velocity  $U_e$ ) that is up to 9.1% of the one U of the flow head. When considered aside with the creeping shear layer, the bouncing layer can be classified as an instance of entrainment, as indicated by its mean velocity  $U_n = U - U_e$  [41] (refer to Table A1), which is approximately 90% of U. That is why the downward displacement of the entrained material is close to the run-out distance of the debris flow. Therefore, the entrainment in this context can be understood as being initiated by transit interplay between the granular head of the flow and the basal particles, which includes both collisions

and rapid increase in basal friction [42]. Subsequently the mobility of the flow body is maintained by the shearing friction [10,12,17].

The increase in grain size D and Froude number Fr enhances the erosion depth H linearly where the flow head interacts with the bed, justifying the granular-enrichment feature of the flow head [42] as well as the dependency of the two parameters on the collisional stress [14]. Besides, since the contact force  $F_c$  which denotes the point load follows a power-law with H (Figure 7a) and  $F_c$  was recorded concurrently with the onset of the net erosion (time of  $0.6 \pm 0.1$  s), the potential of the collision is supposed to prompt the normal-oriented excavation of the substrate [10]. A preliminary threshold of  $F_c$  that lies within the range of 2.5 to 4 N is proposed to define the erosion increasing from fast to slow with the increase in  $F_c$ , which is different from the frictional and/or collisional stresses proposed by [6,9,35]. The point load  $F_c$  offers a viable alternative for assessing the erosion caused by debris flow, and our subsequent study will concentrate on the practical computation of  $F_c$ .

The total mass M of the mixture being known as the magnitude or volume of debris flow has a positive effect on both the eroded length L and the critical entrainment migration  $L_c$ . This can be elucidated by stating that an increase in mass leads to a reduction in internal friction [42], thereby enhancing mobility. Accordingly, the energy-oriented factor E that integrates M and E (Eqn. 15) should be likely related to the critical eroding effects, and its regressive power-law relationship with E confirms the idea. Since the computation of E indicates averaged flow depth E along the whole flow body, the trend highlights the significance of friction in the eroding dynamics [12,17]. Again, there is a preliminary threshold of E (within the range from 130 to 150 J) in controlling the rate of increase of E from fast to slow according to Figure 7b, and E is more feasible to obtain in fields than E. In total, the critical erosion mechanism can be interpreted through a synthesis of both force-based and energy-based perspectives.

#### 4.2. Limitations of this Study

This paper is focusing on the erosion of debris flow head on a dry bed sediment under laboratory-scale, thus the effect should be discussed if transferring to large-scale events. Now that several dimensionless numbers such as Froude number  $F_r$ , Savage number  $N_{sav}$ , Bagnld number  $N_{bag}$ , and Friction number  $N_f$  et al. have been demonstrated valid in debris-flow dynamics [36,43], our study chooses  $F_r$  to preliminarily meet the similitude, meaning the Froude number of the model  $Fr_{(m)}$  equals that of the prototype  $Fr_{(p)}$ , expressed as follows: In the case where the geometric dimension ratio is set at 1 (model) to N (prototype), and where the density  $\rho$  and the gravity acceleration g are both equal, the scale ratios for both force and energy here are established as 1 to  $N^3$ .

For further exploration, angular particles and boundary conditions [44] on how the flow dynamics evolving more accurately are warranted. Indeed, intervals of the given variables need to be more refined [43] and flow attenuation affecting the energy estimation due to collisions or frictions should be added [45], in order to broaden the scope of the research.

## 5. Conclusions

Our study generally ascertains that the CFD-DEM coupled numerical simulations can effectively serve as an auxiliary or supplementary tool to physical model experiments, providing comprehensive feedback on the phenomenon of debris flow erosion, thus offering technical support for practical engineering or theoretical studies. The main results are listed as follows:

The process of erosion can be categorized into three distinct phases: the initial erosion phase, the net erosion phase, and the post-erosion phase, wherein the net erosion phase is responsible for the most significant erosive effects. Increasing both the grain size D and the Froude number Fr of debris flow can enhance the erosion depth normal to the bed, and the eroded length L and the critical transport  $L_c$  of the basal sediment are both positively correlated with the total mass M of the debris flow.

The erosion depth H is described by a power function that correlates with the collisional point load  $F_c$  computed by the normal impact force per unit of the debris-flow head. Furthermore, the critical

entrainment transport  $L_c$  is also represented as a power function of the impact energy E estimated by the averaged thickness of the debris flow head.

Furthermore, thresholds for both the collisional point load and the impact energy that predict the attenuated rates of the erosive depth and the critical transport of entrainment, respectively, are obtained through regression analyses.

The idea for the mechanisms of the erosion proposed by previous studies is verified by the presented coupled simulation that the collisional point load is key to initiating the net erosion process, while frictional shearing is the factor that sustains the flow mobility.

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# **Abbreviations**

The following abbreviations are used in this manuscript:

- D Uniform grain size of debris flow
- M Total mass of debris flow
- V Solid fraction of debris flow
- H Erosion depth
- L Erosion length
- $L_c$  Critical entrainment transport
- *Fr* Froude number
- U Velocity of the debris flow head
- *Ue* Velocity of the eroded material
- $U_n$  Velocity of the entrainment
- *h* Thickness of debris flow
- g Gravity acceleration
- *F<sub>c</sub>* Collisional point load
- E Impact energy of debris flow



# Appendix A Appendix for main results

**Table A1.** Main results from the numerical simulation.

Serial ID.	Fr	H (m)	L (m)	$L_c$ (m)	<i>U</i> (m/s)	<i>U<sub>e</sub></i> (m/s)	h (m)
D4M115V45	2.85	0.035	1.62	3.32	2.46	0.09	0.040
D4M115V50	2.52	0.037	1.66	3.5	2.54	0.12	0.060
D4M115V55	2.16	0.037	1.61	3.62	2.30	0.13	0.076
D4M150V45	4.04	0.037	1.75	4.05	2.37	0.15	0.034
D4M150V50	2.86	0.038	1.85	4.13	2.54	0.18	0.060
D4M150V55	2.82	0.039	1.92	4.40	2.46	0.20	0.071
D4M185V45	3.86	0.039	1.94	4.45	2.46	0.20	0.044
D4M185V50	3.14	0.040	1.94	4.56	2.51	0.23	0.070
D4M185V55	2.74	0.040	2.10	4.63	2.59	0.24	0.095
D3M115V45	1.65	0.031	1.47	3.32	2.15	0.08	0.113
D3M115V50	2.03	0.033	1.57	3.35	2.08	0.10	0.077
D3M115V55	1.97	0.033	1.63	3.63	2.24	0.11	0.083
D3M150V45	2.25	0.035	1.83	3.92	2.13	0.13	0.097
D3M150V50	2.47	0.034	1.67	4.00	2.18	0.13	0.085
D3M150V55	2.33	0.037	1.80	4.28	2.21	0.17	0.098
D3M185V45	2.92	0.036	1.89	4.34	2.26	0.17	0.071
D3M185V50	2.75	0.037	2.02	4.36	2.13	0.18	0.092
D3M185V55	2.36	0.038	1.94	4.58	2.28	0.18	0.118
D2M115V45	1.65	0.028	1.46	3.13	1.65	0.07	0.109
D2M115V50	1.87	0.028	1.56	3.30	1.71	0.08	0.091
D2M115V55	1.73	0.030	1.62	3.64	1.72	0.10	0.108
D2M150V45	2.19	0.031	1.65	3.79	1.68	0.11	0.105
D2M150V50	2.12	0.031	1.76	3.94	1.70	0.13	0.105
D2M150V55	2.17	0.033	1.85	4.10	1.72	0.14	0.116
D2M185V45	2.45	0.033	1.95	4.27	1.73	0.14	0.109
D2M185V50	2.89	0.034	1.86	4.30	1.87	0.15	0.084
D2M185V55	1.93	0.034	1.87	4.53	1.81	0.16	0.154

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