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Article

# Hygroscopicity in Epoxy Powder Composites

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**Abstract:** Epoxy powders offer a low-cost means of manufacturing thick section composite parts, such as those found in wind and tidal turbines. Currently, their processing cycle includes a lengthy drying stage ( $\geq 15$  h) to remove ambient moisture. This prevents void defect formation and, thereby, a reduction in mechanical properties, however, it constitutes up to 60% of the processing time. Little research has been published on the study of this process or its optimisation. Experimental and simulated analyses are used to investigate the effects of hygroscopicity in epoxy powder composites. In particular, focus is given to the drying process, which is used to prevent void defect formation and, thereby, a reduction in mechanical properties. As such, tests are performed to quantify the void content of dried and undried laminates, and to measure its impact on transverse flexural strength. Dynamic vapour sorption analysis is used to study the sorption behaviour of the epoxy powder. Sorption data is fitted to a modified linear driving force model, and then implemented in existing process simulations tools. The drying of a thick epoxy powder composite section is simulated to investigate the influence of powder sintering on the duration required for drying. It is shown that the epoxy powder is slightly hygroscopic (1.36 wt%) and exhibits sorption behaviour that is characteristic of glassy polymers. This results in up to 4.8% voids (by volume) if processed in an undried state, leading to a 43% reduction in transverse flexural strength. Process simulations reveal that a standard drying cycle prematurely sinters the powder; inhibiting moisture release. By maintaining a powder state, simulations show that the drying cycle can be reduced to 5 h.

**Keywords:** hygroscopicity; epoxy powder; polymer composites; drying; sintering

## 1. Introduction

Advanced composite materials have become an important global commodity due to their use in light-weighting critical infrastructure. Their high stiffness/strength to weight ratio facilitates reduced energy consumption in transport sectors and increased energy production for renewable energy sources. For example, the Boeing 787 Dreamliner contains 50% composite materials by weight [1], while several companies have been successful in deploying 100+ m length composite wind turbine blades [2].

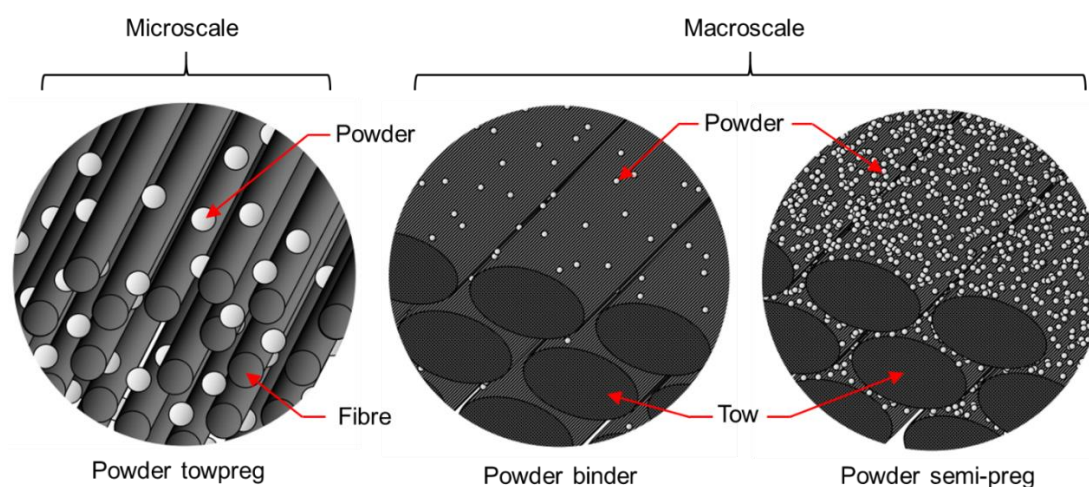
Generally, fibre-reinforced composites are composed of a fibre bed (carbon, glass, basalt, etc.) impregnated with a polymer matrix (thermoset or thermoplastic). Cost and performance dictate fibre choice as carbon fibres offer higher specific strength and stiffness than glass fibres but also come at an increased cost [3]. Polymer selection, on the other hand, is often driven by the ease of manufacturing; for example, low viscosity thermosets (0.1 – 100 Pa.s) allow large components to be infused in a cost-effective manner [4], whereas higher pressures and temperatures are typically required for processing thermoplastics ( $> 100$  Pa.s).

In the context of advanced composite materials, powder-based systems occupy several niches within the market: powder binder for preforming [5–9], powder towpregging [10–14], and powder semi-pregging [15–19]; each of which is shown in Figure 1.

In the case of powder binders, typically, only 3 – 9 wt% of polymer powder is added to dry reinforcing fabric. The fabric can be draped and formed prior to melting the powder, which then binds the fabric layers and fixes them into their formed shape. Subsequently, this “preformed” fabric can be infused with a low viscosity resin via resin transfer moulding or a similar process [5,6].

In contrast, for powder towpregging and powder semi-pregging, the powder acts as the primary polymer matrix for the composite. For towpregging, the powder is typically dispersed between spread reinforcing fibres in an automated production process using electrostatic deposition or similar [20,21]. This is particularly attractive for thermoplastic powders due to their high viscosity, i.e., dispersion between the fibres reduces the distance that molten polymer must flow to achieve full impregnation. As such, thermoplastic powder towpregging systems have undergone significant development in the last four decades [10,13,21,22]. Despite this, the high viscosity of thermoplastics means that towpreg quality plays an important role in subsequent composite manufacturing processes, such as automated tape placement [23], i.e., it is difficult to remove void defects without the use of expensive high-pressure equipment, such as autoclaves and heat presses. For this reason, recent developments in powder towpreg production have introduced the use of low viscosity (< 10 Pa s) epoxy powders, which can be reprocessed under low pressure conditions to improve final part quality [24]. Reprocessing is a possibility for these epoxy powders because they contain latent, heat-activated curing agents and have a glass transition temperature above 40°C. This means that they require no refrigerated storage to prevent curing, i.e., the epoxy powder is stable at ambient conditions for several months, unlike conventional liquid epoxy systems which undergo ageing [25,26].

Likewise, epoxy powders have undergone significant development for powder semi-pregs; a form of vacuum-bag-only (VBO) prepreg developed for low-cost out-of-autoclave (OoA) processing [16,17,19,27,28]. Vacuum-bag-only (VBO) prepregs differ from conventional prepregs in that the fibre bed is only partially impregnated with resin. This allows entrapped air and moisture to be evacuated during processing via dry fibre pathways [29]. Through-thickness permeability is particularly desirable for evacuation as the through-thickness flow paths tend to be significantly shorter than the in-plane flow paths [30]. As such, several recent studies have been dedicated to studying how resin deposition can improve gas evacuation [19,31–33]. Powder semi-pregs have inherent three-dimensional gas permeability, assuming the powder is left unsintered.



**Figure 1.** Illustrations of powder-based composite systems. (Left) Microstructure of powder towpreg with powder dispersed between fibres. (Middle) Macrostructure of fibre reinforcement coated with powder binder (note: tows are bundles of fibres used to create fabrics). (Right) Macrostructure of fibre reinforcement which has been partially impregnated with powder (i.e., powder semi-preg).

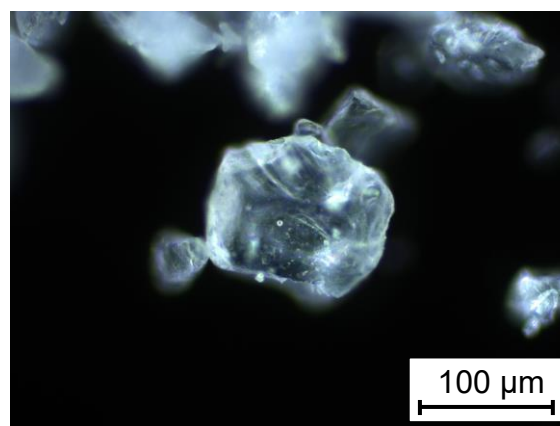
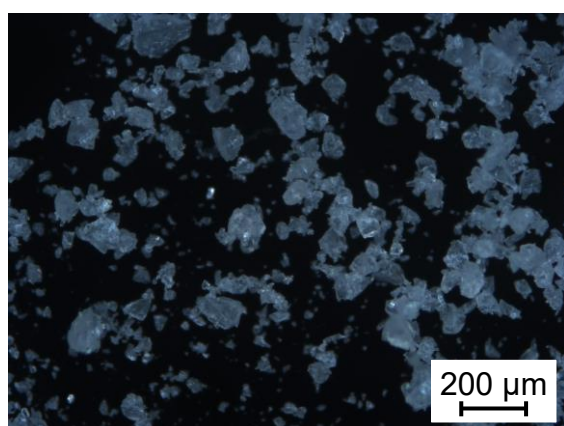
While gas permeability is important for evacuating VBO prepregs, moisture transport in these systems is largely driven by diffusion [34]. Many polymers used in composites manufacturing can be categorised as slightly hygroscopic (0.2 – 2% w/w) or moderately hygroscopic (2 – 15% w/w) [35] meaning that they attract moisture from the atmosphere during storage, cutting, lay-up, etc. It has been shown that entrapped moisture leads to significant void growth and reductions in thermal and mechanical properties [34,36]. As a result, vacuum holds of up to 16 hr are often used for drying VBO prepregs. In the case of polymer powders, however, their high surface area-to-volume ratio means that sorption kinetics play a large role in the drying process [37], with desorption being several orders of magnitude faster than diffusion. For example, Padaki and Drzal [38] modelled the drying of powder towpreg as it was being consolidated. Their simulations suggested that the drying process was in the order of several minutes rather than several hours, and that this drying time was a function of particle size. Despite this, the drying process for powder semi-pregs has not been optimised in industry e.g., drying times are still in the range of 15 hours for thick section parts of wind and tidal turbine blades [39].

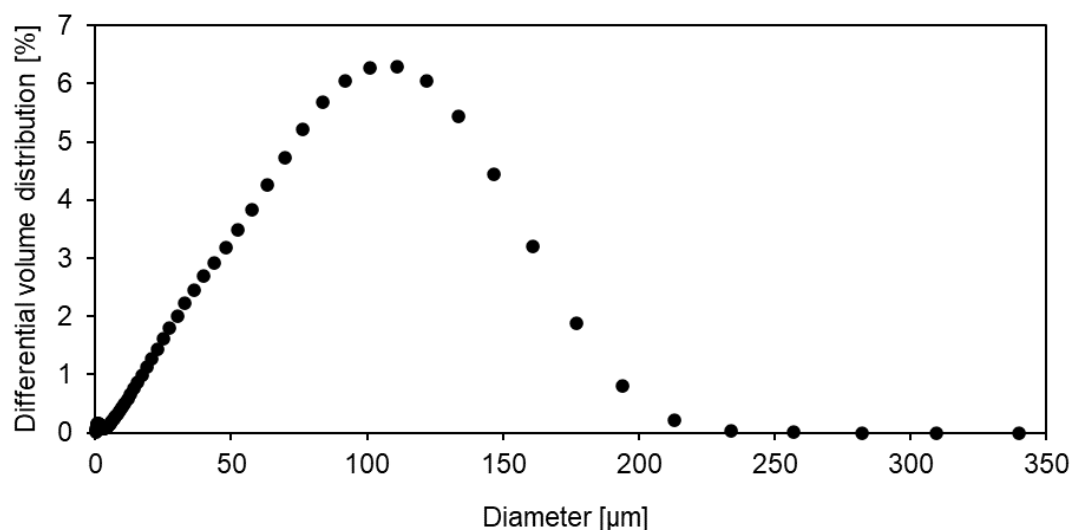
In this work, the effect of hygroscopicity is explored for epoxy powder composites. Mechanical testing and microscopy are performed on dried and undried epoxy powder composites to demonstrate the effect of drying on the composite properties. Dynamic vapour sorption (DVS) is used to analyse the sorption behaviour of the epoxy powder, considering the effect of both relative humidity and temperature, as well as the impact of powder sintering. The desorption kinetics are fitted to a semi-empirical model to perform first order simulations of the drying process. These simulations are used to determine optimal drying conditions for thick epoxy powder composite sections.

## 2. Materials and methodology

### 2.1. Materials

Epoxy powder was supplied by ÉireComposites Teo. under the product number GRN 918. Note, this was the same epoxy powder used in other works [14,20,24] under its original product number PE6405. Optical micrographs of the epoxy powder are shown in Figure 2, as well as the differential volume distribution of particle sizes. Optical microscopy was performed using a Zeiss Axioskop 2 fitted with an AxioCam MRc 5 camera. The particle size analysis was performed using a Beckmann Coulter LS100, which uses laser diffraction to measure grain sizes in a liquid suspension. For mechanical testing, the epoxy powder was combined with a 1200 g/m<sup>2</sup>, stitched unidirectional glass fabric (UD-GF) supplied by Johns Manville.



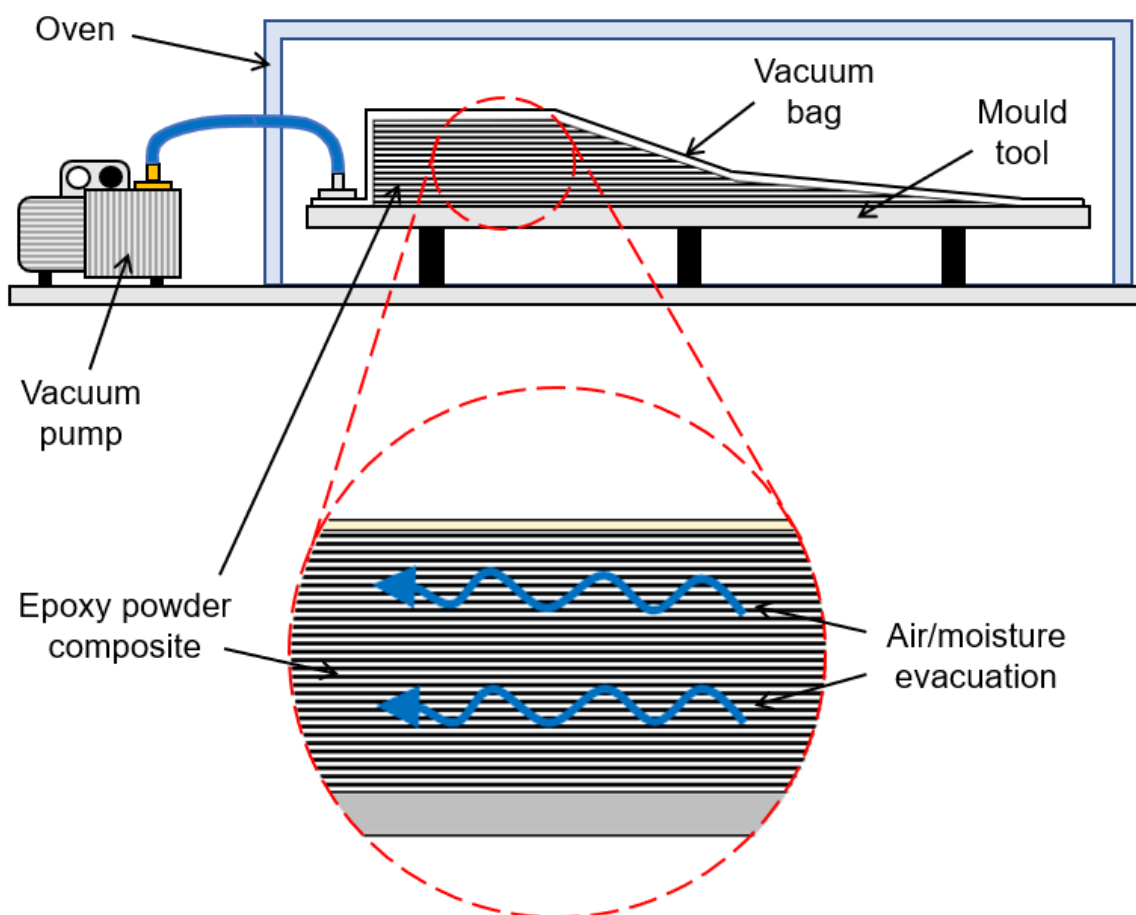


**Figure 2.** Details of epoxy powder particle size. (Top left) Micrograph of epoxy powder at  $\times 5$  magnification. (Top right) Micrograph of epoxy powder at  $\times 20$  magnification. (Bottom) Differential volume distribution of epoxy particles based on size (i.e., diameter).

## 2.2. Experimental

### 2.2.1. Composite manufacturing

A schematic of the VBO process is shown in Figure 3 for the manufacture of a thick epoxy powder composite part. This is representative of the process simulated later in this work (discussed in sections 2.3.2 and 3.3) as well as the process used to manufacture composite test laminates (discussed in sections 2.2.2 and 3.1). For VBO processing, plies (i.e., layers) of powder semi-preg are stacked on a metallic mould tool and then sealed in a flexible vacuum bag. The mould is placed in an oven and heated to the desired drying temperature while air/moisture are evacuated via a vacuum pump. When the drying stage is complete, the temperature is increased to lower the viscosity of the epoxy so that it will infuse through the dry fibre reinforcement. Finally, the temperature is increased again to cure the epoxy.



**Figure 3.** Schematic of a thick epoxy powder composite part being manufactured in an oven using VBO processing. Air/moisture is drawn out of the part using a vacuum pump connected to the vacuuming bag.

Two UD-GF/Epoxy test laminates were manufactured using VBO processing in an oven. In the A drying stage was included (16 h at 45°C) for one laminate and excluded in the other laminate. Both laminates were subsequently processed with the following temperature cycle:

- Ramp to 120°C at 1.5°C/min
- Soak at 120°C for 30 min
- Ramp to 180°C at 1.5°C/min
- Soak at 180°C for 60 min

### 2.2.2. Mechanical testing

Transverse flexural test specimens were extracted from the composite laminate using a diamond-coated wet saw. Three-point bending tests were performed using a Zwick 10 kN test frame to the specifications of BS ISO EN 14125. For each laminate, 5 specimens were tested at a crosshead speed of 5 mm/min. Test specimens had dimensions of 60 × 15 × 2 mm (length × width × thickness), with a span of 40 mm.

### 2.2.3. Void content

The fibre volume fraction and void content of the composite laminates were determined by the acid digestion method, in accordance with ASTM D 3171 - 09. Additionally, scanning electron microscopy (SEM) was performed on the fracture surface of the transverse flexural test specimens using a Hitachi S-4700 with an acceleration voltage of 15 kV. The fracture surface was sputter-coated with gold to improve image quality.

### 2.2.4. Dynamic vapour sorption

Dynamic vapour sorption (DVS) was performed on epoxy powder samples using an Aquadyne DVS-2 from Quantachrome Instruments. As the Aquadyne DVS-2 is a dual-gravimetric system, all tests were performed in duplicate with deionized water. Samples were weighed in glass crucibles at a variety of isothermal conditions (e.g., 23, 35, and 45°C) across a range of relative humidity (RH), i.e., 1 – 90%. Weight calibration was performed for each test temperature. At ambient conditions, each powder sample had a mass of  $60 \pm 13$  mg. The nitrogen gas flow rate was limited to a minimum and maximum of 50 cm<sup>3</sup>/min and 150 cm<sup>3</sup>/min, respectively.

At the start of each test, the RH was set as low as possible (i.e., 1-2% RH) until the powder mass reached an equilibrium. After equilibrium was achieved, the RH level was increased in increments of 15% RH up to 90% RH, and then decreased again in 15% RH increments. For each test, the equilibrium criterion was set as mass change  $\leq 0.0005\%/min$ . Time limits were also set in the event that equilibrium was not achieved within a given duration.

The only exception to the above procedure were samples tested at 45°C. These samples fully sintered above 60% RH, resulting in a drastic change to the sorption characteristics. Consequently, the following additional tests were carried out:

- Sintered samples – tested at 35°C using the above procedure
- Powder samples – tested at 45°C and 50°C, with the RH increasing from 1-2% to 90% in increments of approx. 1% RH every 6 mins, then decreasing at the same rate.

## 2.3. Modelling

### 2.3.1. Sorption kinetics

In the context of composites manufacturing, the key sorption process occurs during the drying cycle, i.e., desorption from ambient conditions. As such, only the first step of the DVS data is considered for modelling the drying cycle. In this step, the RH is reduced from circa 57% to 1-2% and water is desorbed from the polymer. The linear driving force (LDF) model, a pseudo first-order model, is an efficient means of analysing the sorption kinetics [40],

$$\frac{dq}{dt} = k \cdot (q_0 - q) \quad (1)$$

where  $q$  is water content of the powder particle [% by weight],  $k$  is the effective mass transfer coefficient [h<sup>-1</sup>], and  $q_0$  is the equilibrium water content of the powder particle for a given relative humidity and time.

For an initial water content of  $q_m$ , Equation 1 can be integrated to determine an analytical solution for desorption kinetics,

$$\int_{q_m}^q \frac{dq}{(q_0 - q)} = \int_0^t k \cdot dt \quad (2)$$

$$-\ln(q_0 - q) + \ln(q_0 - q_m) = k \cdot t \quad (3)$$

Assuming  $q_0 = 0$ , Equation 3 becomes,

$$q = q_m \cdot e^{-k \cdot t} \quad (4)$$

In this form, Equation 4 can be fitted to DVS data at a given temperature, however, several considerations must be made:

1. Geometry: The LDF model was originally developed for analysing the kinetics of a packed adsorbent column with beads or pellets (i.e., spherical or cylindrical geometries – not composite systems with irregular particles as shown in Figure 1 and Figure 2).

2. Effect of temperature and isotherm non-linearity:
  - a. If the experiment is not isothermal (e.g., due to the endothermic enthalpy of desorption), the desorption kinetics will appear to be slower due to the combined effect of shifted equilibrium and slower diffusion at lower temperatures.
  - b. The diffusivity also depends on the shape of isotherm. If the experiment is performed over the linear part of the isotherm, the diffusivity can be assumed to be constant. Otherwise, more careful treatment is required and the Darken correction factor can be used to account for the isotherm non-linearity [40].
3.  $q_0$  is the equilibrium loading with RH at a given time. The derivation from Equation 3 to Equation 4 assumes that RH drops instantaneously to almost 0, which is not the case for DVS experiments. As described in [40], solutions have been derived for constant pressure / constant volume experiments (for an initial step change in pressure in an infinite medium / finite medium, respectively). To take into account the varying RH, however, a more complex analysis would be required.

Given the above considerations, the LDF model was modified with an additional term,  $J$ , to enable semi-empirical fitting,

$$q^* = q_m \cdot J \cdot e^{-k \cdot t} \quad (5)$$

$$J = 1 + e^{C \cdot (t - t_c)} \quad (6)$$

where  $C$  is a rate coefficient [ $\text{h}^{-1}$ ], and  $t_c$  is a time constant [h].

In this instance,  $k$  and  $C$  vary with temperature,  $T$  [ $^{\circ}\text{C}$ ], according to the following relations,

$$k = A_k e^{B_k \cdot T} \quad (7)$$

$$C = A_C e^{B_C \cdot T} \quad (8)$$

The parameters for Equations 5 – 8 were fitted to the DVS data using MATLAB's nonlinear least-squares curve fitting solver, *lsqcurvefit*. The fitting parameters are shown in Table 1.

**Table 1.** Fitting parameters for the modified linear driving force model.

Parameter [units]	Value
$t_c$ [h]	0.170
$A_k$ [ $\text{h}^{-1}$ ]	4.937
$B_k$ [ $^{\circ}\text{C}^{-1}$ ]	0.030
$A_C$ [ $\text{h}^{-1}$ ]	4.580
$B_C$ [ $^{\circ}\text{C}^{-1}$ ]	0.031

As will be described in the next section, the sorption kinetics model must be solved numerically along with a system of equations for heat transfer, powder sintering, and thickness to simulate the drying stage of the composite manufacturing cycle. To solve the model numerically, its derivative must be determined. Equation 5 can be expanded to the form,

$$q^* = q_m \cdot e^{-k \cdot t} (1 + e^{C \cdot (t - t_c)}) \quad (9)$$

$$q^* = q_m(e^{-k \cdot t} + e^{C \cdot (t-t_c) - k \cdot t}) \quad (10)$$

Differentiating with respect to time,

$$\frac{dq^*}{dt} = q_m[(C - k)e^{C \cdot (t-t_c) - k \cdot t} - k \cdot e^{-k \cdot t}] \quad (11)$$

This derivative can then be rearranged as follows,

$$\frac{dq^*}{dt} = q_m[Ce^{-k \cdot t}e^{C \cdot (t-t_c)} - ke^{-k \cdot t}e^{C \cdot (t-t_c)} - k \cdot e^{-k \cdot t}] \quad (12)$$

$$\frac{dq^*}{dt} = q_mCe^{-k \cdot t}e^{C \cdot (t-t_c)} - k \cdot q_m \cdot e^{-k \cdot t}(1 + e^{C \cdot (t-t_c)}) \quad (13)$$

Substituting in Equation 9, the derivative becomes,

$$\frac{dq^*}{dt} = \frac{q^*Ce^{C \cdot (t-t_c)}}{1 + e^{C \cdot (t-t_c)}} - k \cdot q^* \quad (14)$$

### 2.3.2. Process simulations

Using experimentally validated process simulation tools [39,41], the drying stage of the manufacturing cycle is simulated for a 100-ply thick composite laminate. Such a laminate is representative of the root section of large wind and tidal turbine blades. As previously mentioned, the process simulation tools combine the modified LDF model (Equation 14) with a through-thickness heat transfer model and powder sintering model to predict the behaviour of the system during drying. This heat transfer model is based on the following one-dimensional (1D) heat conduction equation,

$$\rho_{ply}c_{p,c} \frac{dT}{dt} = \kappa \nabla^2 T \quad (15)$$

Where  $\rho_{ply}$  is the ply density [kg/m<sup>3</sup>],  $c_{p,c}$  is the specific heat capacity of the composite [J/kg K],  $\kappa$  is the through-thickness thermal conductivity [W/m K].

During the drying cycle, the thickness of each ply,  $h_{ply}$  [m], and thereby  $\rho_{ply}$ , can vary as a function of the powder void fraction,  $\chi$  [-],

$$h_{ply} = h_{fab} + h_r \quad (16)$$

Where  $h_{fab}$  is the fabric thickness [m] and  $h_r$  is the thickness of the resin layer [m],

$$h_r = \frac{h_r^*}{1 - \chi} \quad (17)$$

Where  $h_r^*$  is the thickness of the fully sintered resin.

The powder void fraction,  $\chi$ , tends towards zero as the epoxy powder sinters according to the following semi-empirical relationship [41],

$$\frac{d\chi}{dt} = -\chi_E \exp\left(\frac{C_{\chi 1}[T - T_\theta]}{C_{\chi 2} + T - T_\theta}\right)(\chi - \chi_\infty)^B \quad (18)$$

where  $\chi_E$  is a pre-exponential rate constant,  $\chi_\infty$  is the powder void fraction at  $t = \infty$ ,  $T_\theta$  is the onset temperature for melting [K], and  $C_{\chi 1}$ ,  $C_{\chi 2}$  [K], and  $B$  are fitting constants.

As will be shown for the DVS results, sintering also had a large effect on the drying kinetics of the epoxy, however, fully modelling the complex interaction was outside the scope of the current work. Rather, the modified LDF model (Equation 9) was fitted to DVS data for sintered epoxy flakes at 35°C ( $k = 2.0964$  [h<sup>-1</sup>],  $C = 1.9784$  [h<sup>-1</sup>], and  $t_c = -0.7829$  [h]), and subsequently implemented in the simulation via the following relationship,

$$\frac{dq^*}{dt} = \left[ \frac{\chi}{\chi_0} \right] \cdot \frac{dq^*}{dt} \Big|_{pow} + \left[ 1 - \frac{\chi}{\chi_0} \right] \cdot \frac{dq^*}{dt} \Big|_{sin} \quad (19)$$

Where  $\chi_0$  is the initial powder fraction.

While this doesn't capture the temperature-dependency of the drying process for sintered epoxy, nor the exact relationship between desorption and powder void fraction, it was deemed sufficient to illustrate the undesirable effect of sintering on drying times i.e., for a given temperature, the rate of drying is up to 7 times slower for sintered epoxy than it is for epoxy powder. It should also be noted that air evacuation is not modelled in the simulations as it is assumed that  $t_{drying} \gg t_{evacuation}$ . This is based on experimental observations that a  $400 \times 400 \times 60$  mm laminate can be fully evacuated within 1 min, similar to dry fabric, whereas drying is in the order of hours.

The above system of equations was solved in MATLAB R2019a. Equation 15 was solved using the Euler method for a time step of 0.5 s. For the simulations, it was assumed that the composite section was heated in a forced convection oven (heat transfer coefficient:  $40 \text{ W/m}^2\text{K}$ ) on a 10 mm thick steel tool under vacuum bag pressure, as shown in Figure 3 and described in previous works [39,41]. While the process simulation tools are also capable of predicting through-thickness resin infusion and curing, only the drying stage has been simulated due to its immediate relevance to the current work. Interested readers are directed to previous works [16,39,41] for details of the resin infusion and curing stages of the process cycle.

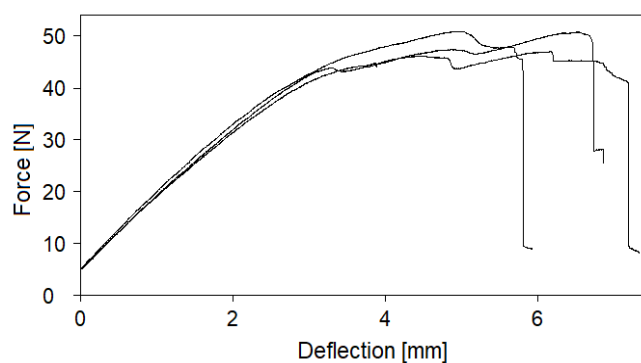
### 3. Results and discussion

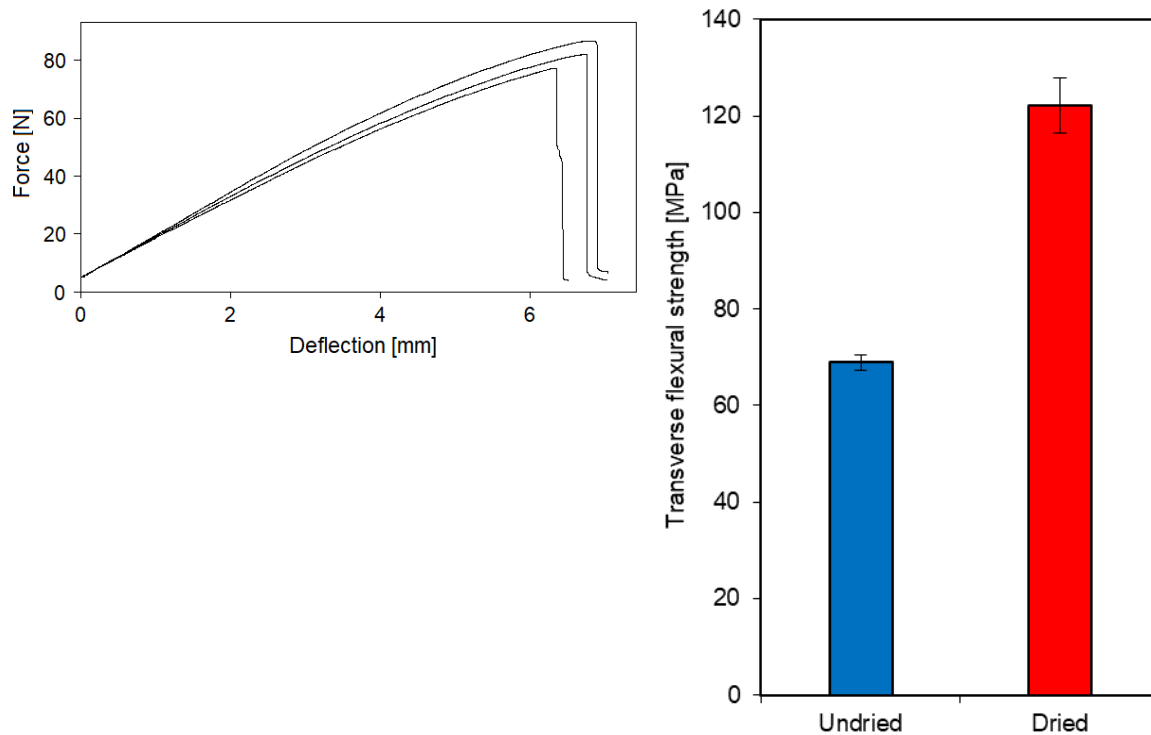
#### 3.1. Effect of entrapped moisture on epoxy powder composite properties

While epoxies tend to be only slightly hygroscopic, even small amounts of moisture can have significant effects on the void content of cured composites. Grunenfelder and Nutt [34] studied this effect by first conditioning VBO prepreg samples at  $35^\circ\text{C}$  with 70, 80, and 90% RH, and then by measuring their moisture contents using both thermogravimetric analysis and Fischer titration. Under autoclave pressures (e.g., 6 atm) they found that void growth was easily suppressed. For VBO conditions (i.e., 1 atm), however, the vapour pressure of entrapped moisture was sufficient form up to 2.62% voids by volume. Moreover, the void content increased as a function of the initial moisture content.

**Table 2.** Results of the acid digestion analysis.

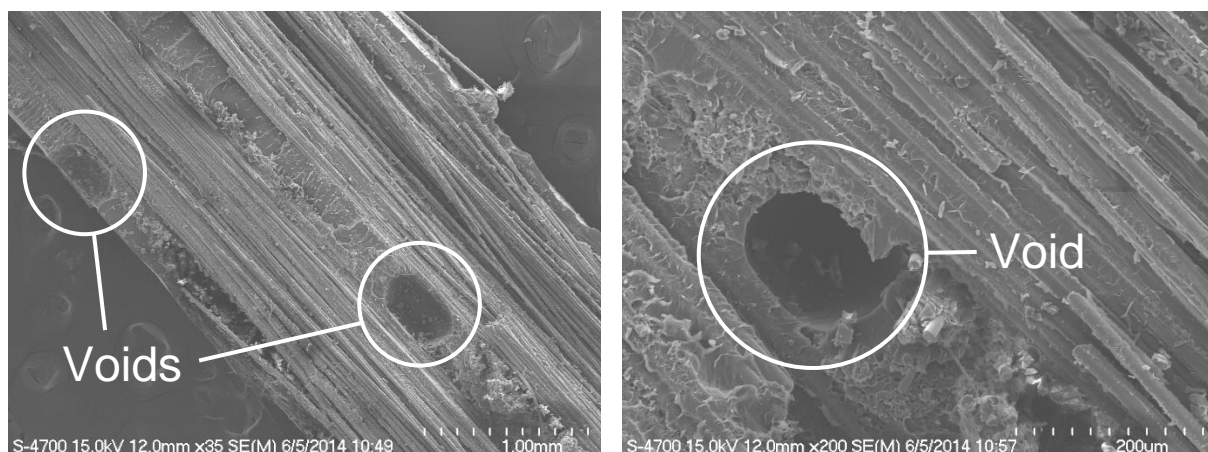
Laminate	Fibre volume fraction [%]	Void content [%]
Undried	47.7	4.80
Dried	48.1	0.91

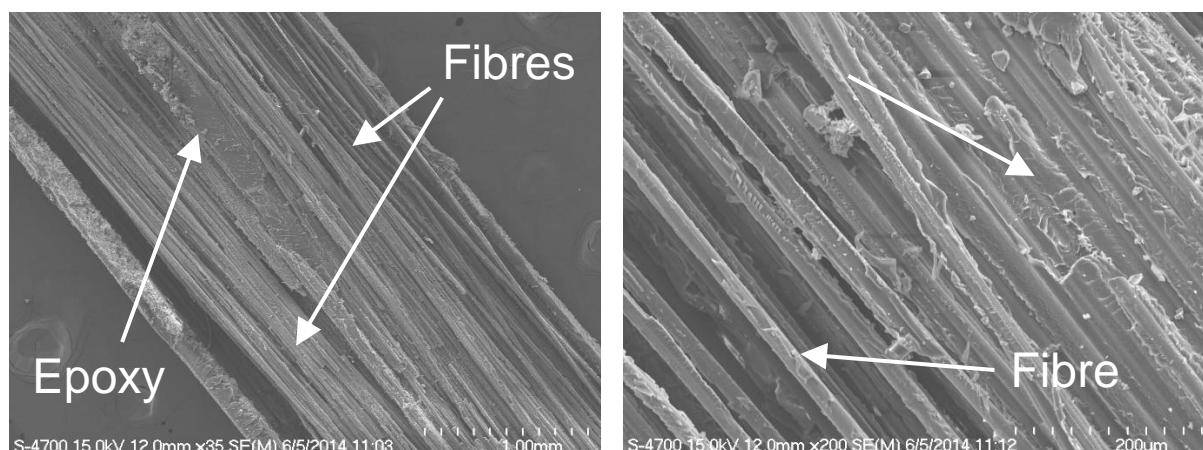




**Figure 4.** Results of the transverse flexural testing. (Top left) Force-deflection data for undried test specimens. (Bottom left) Force-deflection data for the dried test specimens. (Right) Mean transverse flexure strengths for both sets of specimens, with error bars representing  $\pm 1$  standard deviation.

As described in sections 2.2.1 – 2.2.3, two UD-GF/epoxy powder laminates were manufactured and tested to determine the effect of moisture on the composite properties. One laminate was manufactured with a drying cycle, while the other was manufactured without. Upon visual inspection, the undried laminate had visible voids on the surface of the laminate. The results of the acid digestion analysis (Table 2) revealed that, while the laminates had similar FVF (circa 48%), the void content of the undried laminate was 5 times higher than that of the dried laminate.





**Figure 5.** Scanning electron micrographs showing the fracture surface of the transverse flexural test specimens. (Top) Microscale voids were visible at the fracture surface of the undried test specimens, while none were visible for the dried test specimens (bottom). Note, for both top and bottom, the left micrograph shows  $\times 35$  magnification, while the right shows  $\times 200$  magnification.

As shown in Figure 4, the presence of voids resulted in a significant reduction in the transverse flexural strength (i.e., 43.4%). This reduction is unsurprising as void defects affect load transfer between polymer and fibres, and can aid crack growth [42]. Using SEM, voids were also observed at the fracture surface of the undried test specimens, confirming their influence on mechanical failure (see Figure 5). In contrast, the absence of void defects at the fracture surface of the dried specimens indicated that failure did not occur due to voids.

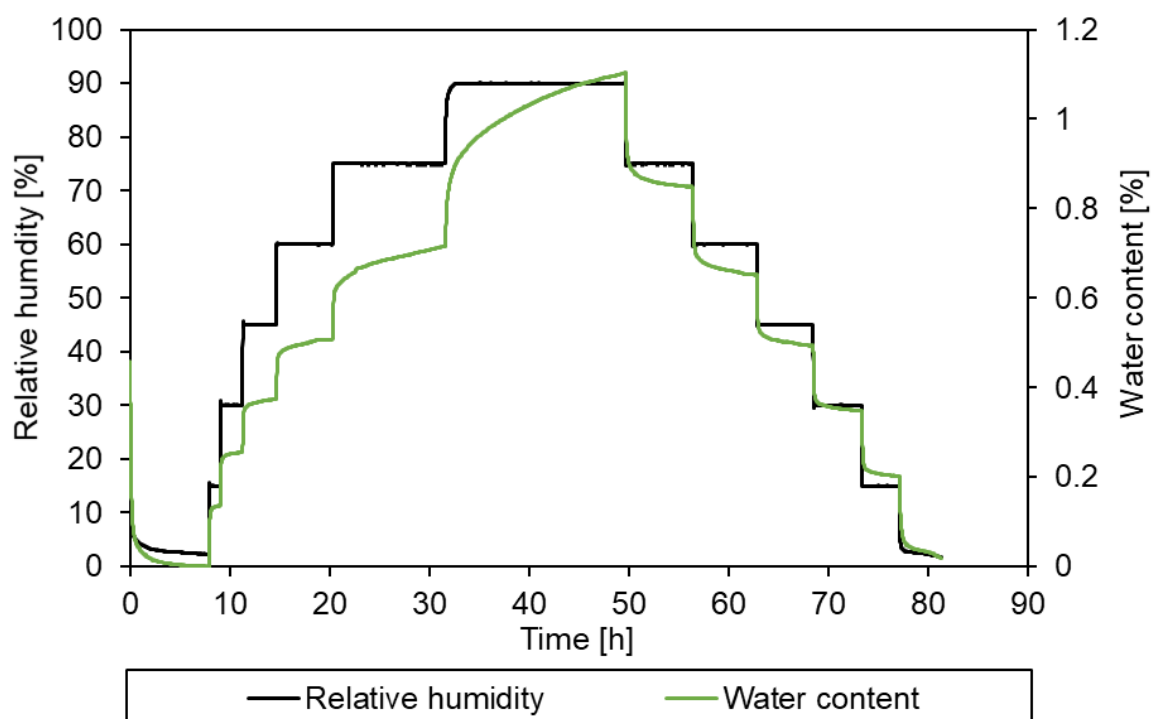
### 3.2. Sorption behaviour of epoxy powder

For polymer powders, adsorption occurs via electrostatic interaction with functional groups on the polymer chains [37]. This can be achieved both on the outer surface of the powder particles and within the bulk polymer. The latter requires diffusion through the polymer chains to reach the adsorption sites. The adsorption process varies as a function of numerous parameters such as time, temperature, relative humidity (RH), chemical structure, etc.

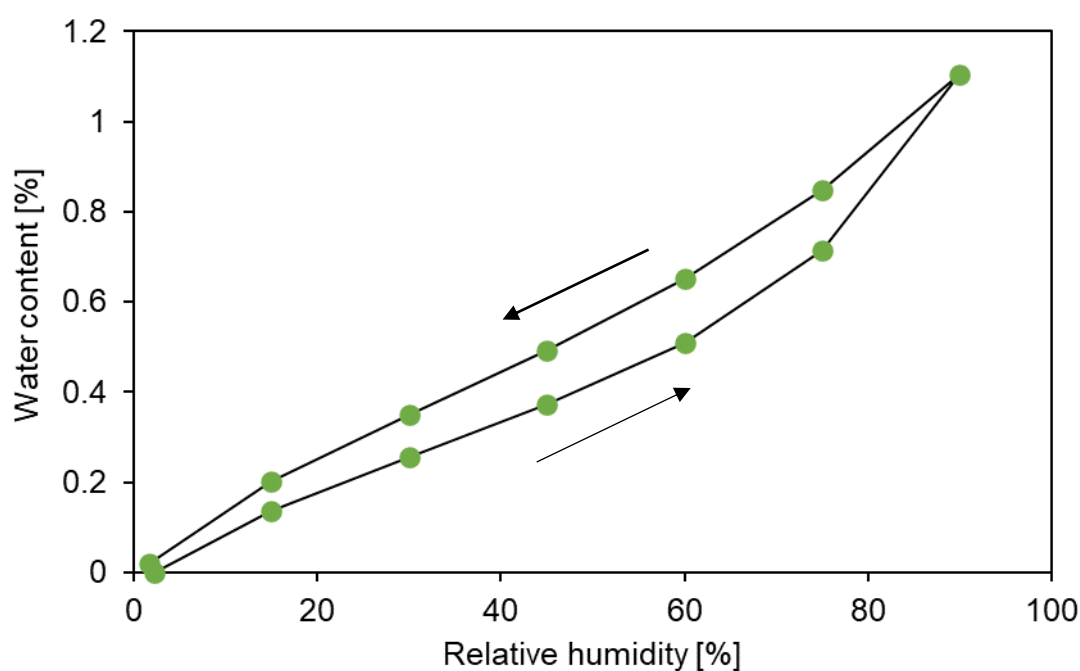
To investigate the sorption behaviour of epoxy powder, DVS analysis was performed for a range of conditions, as described in section 2.2.4. An initial analysis was performed at ambient temperature ( $23^{\circ}\text{C}$ ) to determine its behaviour for typical storage conditions (see Figure 6).

For each step, the initial step change response in water content indicated that water vapour was being adsorbed/desorbed to/from the surface of the epoxy powder particles, however, equilibrium was not achieved at 75% RH or 90% RH. The gradual increase in water content at higher % RH was indicative of continued water diffusion into the powder particles. In relation to this latter point, plotting water content against relative humidity (see Figure 7) revealed hysteresis in the  $23^{\circ}\text{C}$  isotherm. It should also be noted that Figure 7 is a type II isotherm. This is typical behaviour for polymers, which are nonporous networks of tangled macromolecules [37].

To investigate how the sorption behaviour varied with temperature, additional isothermal tests were run at  $35^{\circ}\text{C}$  and  $45^{\circ}\text{C}$ . Figure 8 shows that temperature had a strong effect on the rate of sorption: at  $35^{\circ}\text{C}$ , equilibrium was reached in 30 – 60 mins; at  $45^{\circ}\text{C}$ , equilibrium was reached within several minutes. The water content at each RH also changed with temperature e.g., at  $35^{\circ}\text{C}$ , 1.36% was reached. As such, for the range of conditions tested, the epoxy powder can be categorised as slightly hygroscopic [35].



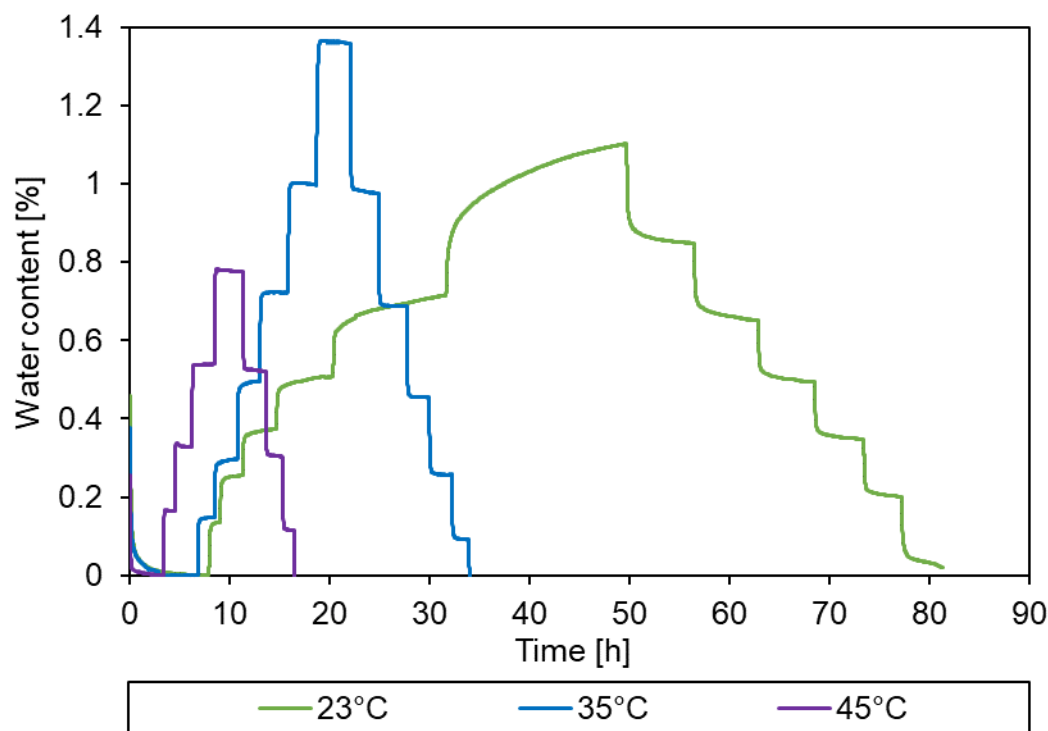
**Figure 6.** DVS data for epoxy powder under isothermal conditions (23°C). The water content changes as a function of relative humidity (RH) due to adsorption and desorption of water vapour.



**Figure 7.** Sorption isotherm for epoxy powder at 23°C.

It should be noted that for 45°C, the epoxy powder was only tested up to 60% RH because, above this point, the epoxy passed through its glass transition and the powder began to sinter. This phenomenon has been reported by others for polymer powders [43], i.e., increases in the RH cause a reduction in the polymer's glass transition temperature ( $T_g$ ), resulting in the 'caking' and sintering of powders as the  $T_g$  approaches the test temperature. Even in the 'caked' state, handling becomes difficult as the powder particles have already begun to melt and adhere together. This can be

problematic for processes like powder towpregging, where a high degree of control is required for uniform powder deposition [44]. As such, the relationship between the  $T_g$  and RH is important for the storage stability of epoxy powders.

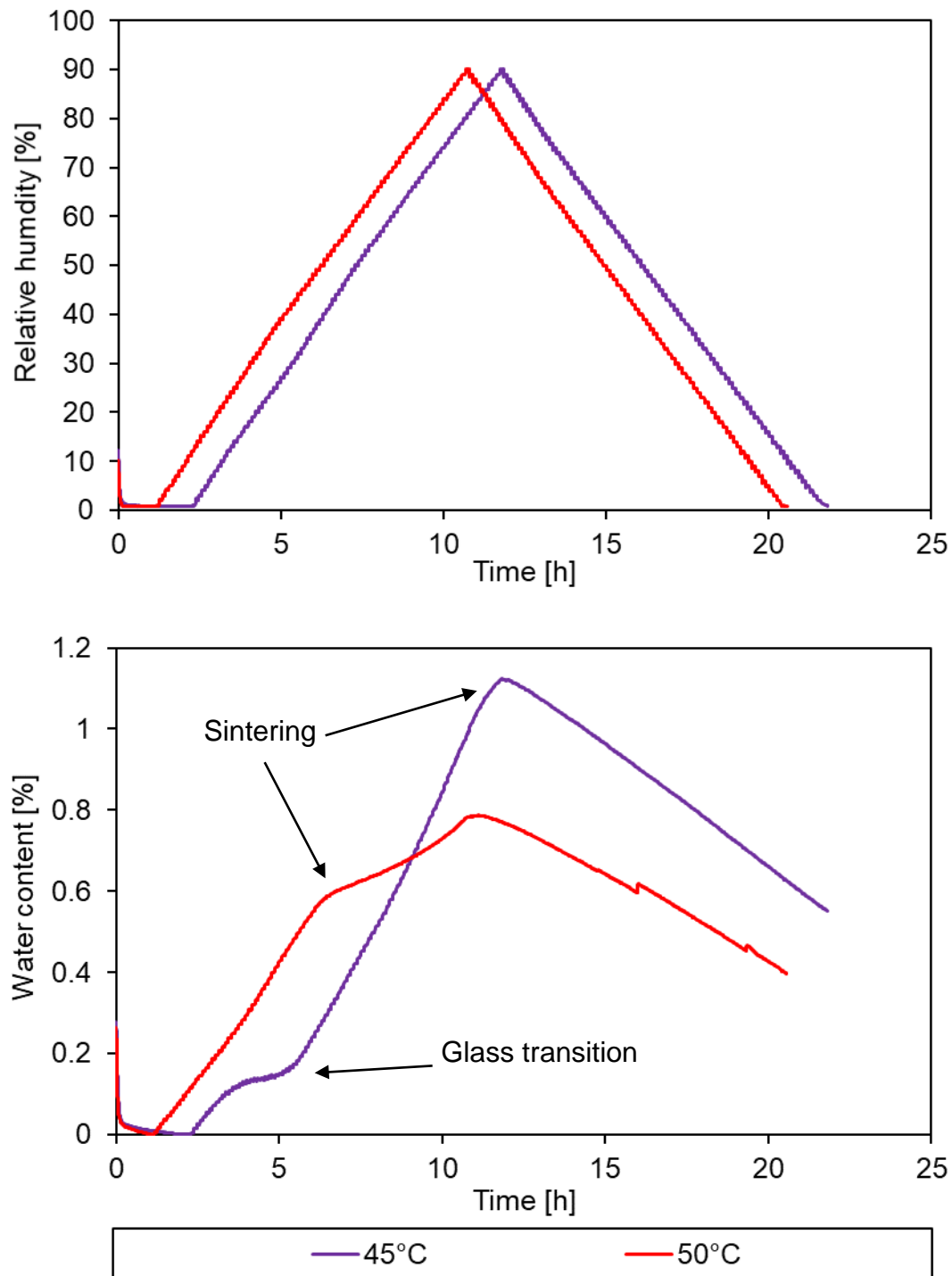


**Figure 8.** DVS data for the epoxy powder at three different temperatures. The sorption behaviour was highly temperature dependent. Note, for 45°C, epoxy powder was only tested up to 60% RH.

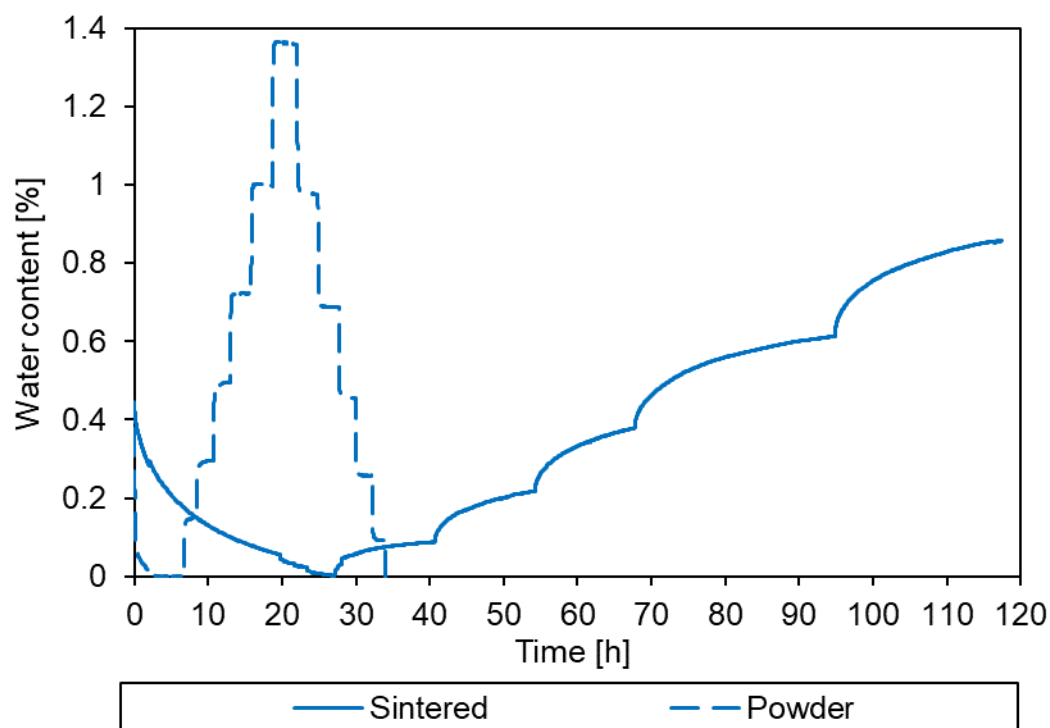
To further explore the effects of caking and sintering, additional DVS analyses were performed at higher temperatures with smaller RH increments. The test data for 45°C and 50°C are shown in Figure 9. At 45°C, the water content of the powder temporarily equilibrated between 16% RH and 26% RH, which is indicative of the glass transition. This was followed by continued water uptake until sintering occurred due to the collapse of the powder structure under its own weight. The sintering process was clearer for the test at 50°C, during which the slope of the water content curve changed suddenly at approx. 50% RH. Post-test, visual observation confirmed that both sets of powder samples had completely sintered. This confirmed that the glass transition, and thereby sintering process, was dependent on RH as well as temperature. Furthermore, it showed that the form of the epoxy (i.e., powder or sintered) had a significant impact on the sorption behaviour, with epoxy powder having a greater surface area-to-volume ratio than sintered epoxy.

Padaki and Drzal [38] also studied this phenomenon when developing powder towpreg. They modelled moisture diffusion in powder particles and showed that the diffusion time increased for increasing particle size. Although their study did not consider sorption phenomena, it stands to reason that moisture removal for smaller particles was dominated by desorption due to their higher surface area-to-volume ratio. In contrast, moisture diffusion through the bulk polymer would have played a larger role as the particle size increased. As noted above, temperature also plays a significant role, however, temperature dependencies were not accounted for in their model.

As a final analysis, sintered flakes of epoxy were tested at 35°C, as shown in Figure 10. The characteristics of the water uptake differed greatly from the previous epoxy powder samples. This was most likely due to the reduced surface area of the epoxy, which impacted the sorption mechanism, forcing water to diffuse through the polymer to find adsorption sites. Consequently, equilibrium was not achieved at each RH and the test was stopped prematurely due to time limitations.



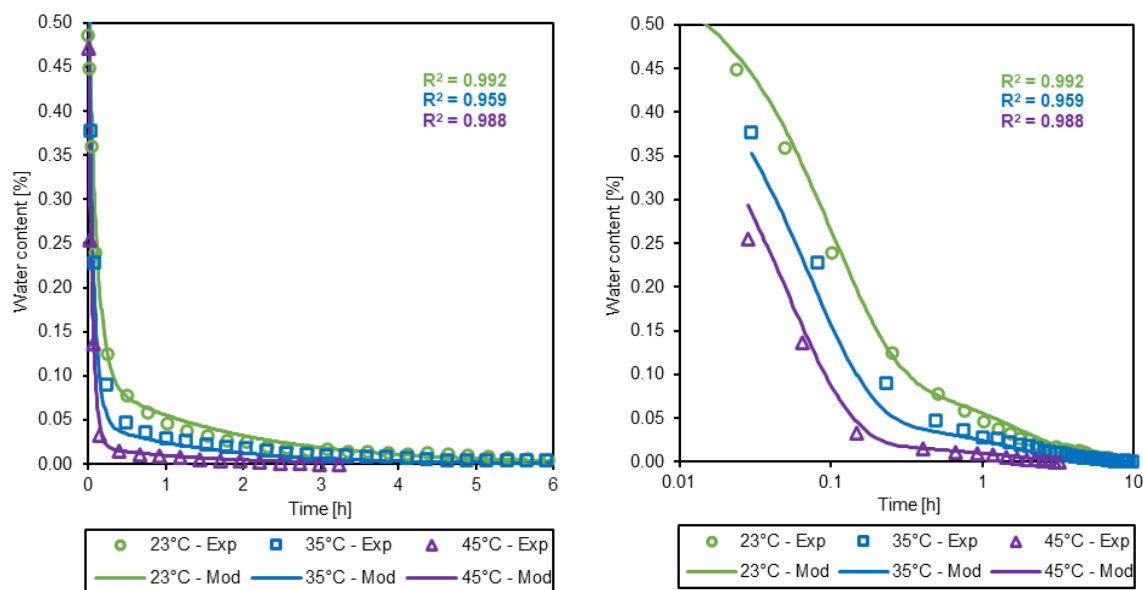
**Figure 9.** DVS data (bottom) for epoxy powder at 45°C and 50°C using smaller increments of RH (top). For 45°C, the glass transition was observed in the water content curve at approx. 10% RH. At approx. 85% RH, powder sintering caused a second transition in water uptake as the epoxy became a rubbery liquid. In this latter form, there was a dramatic change in sorption behaviour, both in terms of adsorption and desorption. This effect was more evident for the 50°C data, where the slope of the water content curve suddenly changed at 50% RH, and did not recover during desorption.



**Figure 10.** DVS data for flakes of sintered epoxy at 35°C, which have been overlapped with data for powder at the same temperature. The water uptake was much slower for the sintered flakes, and equilibrium was not achieved at any RH. Consequently, the test was terminated due to time constraints.

The behaviour displayed by sintered epoxy in Figure 10 is directly linked to the lengthiness of drying cycles for conventional VBO prepregs (i.e., > 16 hr for large laminates [45]). It suggests that, by using powder semi-prepregs, the drying process can be transitioned away from being diffusion-controlled towards being sorption-controlled. In doing so, manufacturers may be able to reduce their drying times significantly.

While the results of the DVS analyses were promising, further research was required to test the hypothesis that the drying cycle time could be reduced significantly. To do this, the initial desorption step of each DVS analysis was fit to the modified LDF model described in section 2.3.1. The results of the model are shown plotted along with the DVS data in Figure 11.

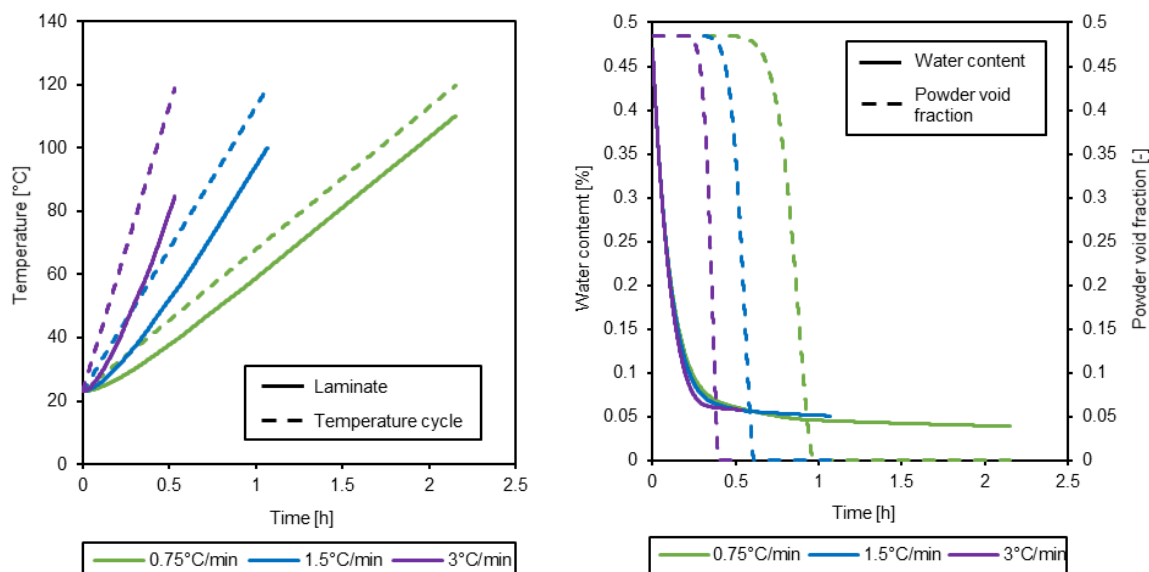


**Figure 11.** (Left) DVS data plotted against the results of the modified linear driving force model. (Right) DVS data and model results plotted on a log time scale.

As previously discussed, the DVS data displayed high rates of desorption initially (0.4 % within 30 min or less), followed by gradual water loss (i.e., 0.1 % or less) over a period of hours as the RH reached equilibrium. Note, the gradual equilibration of RH can be observed within the first 8 h of the test in Figure 6. This effect at low RH, along with the other considerations outlined in section 2.3.1, meant that a modified LDF model was used to achieve a semi-empirical fit for the DVS data, with an  $R^2$  value above 0.95 in each case. While the model did not capture the physics of the behaviour, it was deemed sufficient for predicting water content during the drying stage of the composite manufacturing process. In this way, the model could be combined with an existing process simulation tool to investigate the drying stage holistically i.e., accounting for heat transfer and powder sintering.

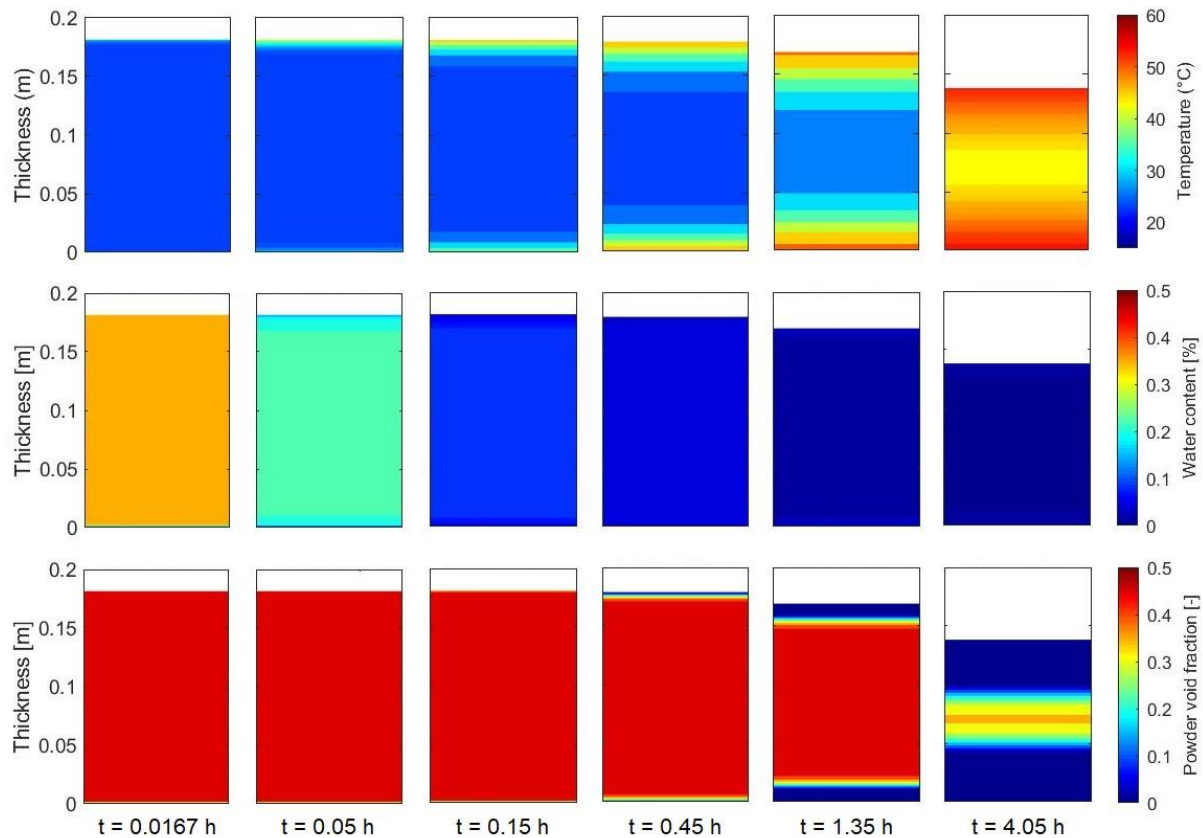
### 3.3. Simulation of the drying process

As an initial investigation, a 2-ply laminate was simulated for 3 linear temperature ramps (0.75, 1.5, and 3°C/min) from 23°C to 120°C. These simulations were performed to predict the water content of the undried laminate described in section 3.1, and determine how it would be influenced by the temperature ramp rate. As shown in Figure 12, the epoxy powder was not fully dried for any of the simulated heating rates (plateauing near 0.05% in each case), thus confirming that a low-temperature dwell period was necessary to fully dry the composite. Predominantly, this was due to the powder sintering above 40°C, which inhibited the release of water. It should be noted that the 1.5°C/min simulation replicated the process cycle used for the undried composite test laminate described in section 2.2.1, i.e., 1.5°C/min from 23°C to 120°C with no drying stage. As such, it can be inferred from the simulation that as little as 0.05% water content was sufficient to produce a void content (by volume) of up to 5% in the cured composite, as observed in Table 2 and Figure 5.

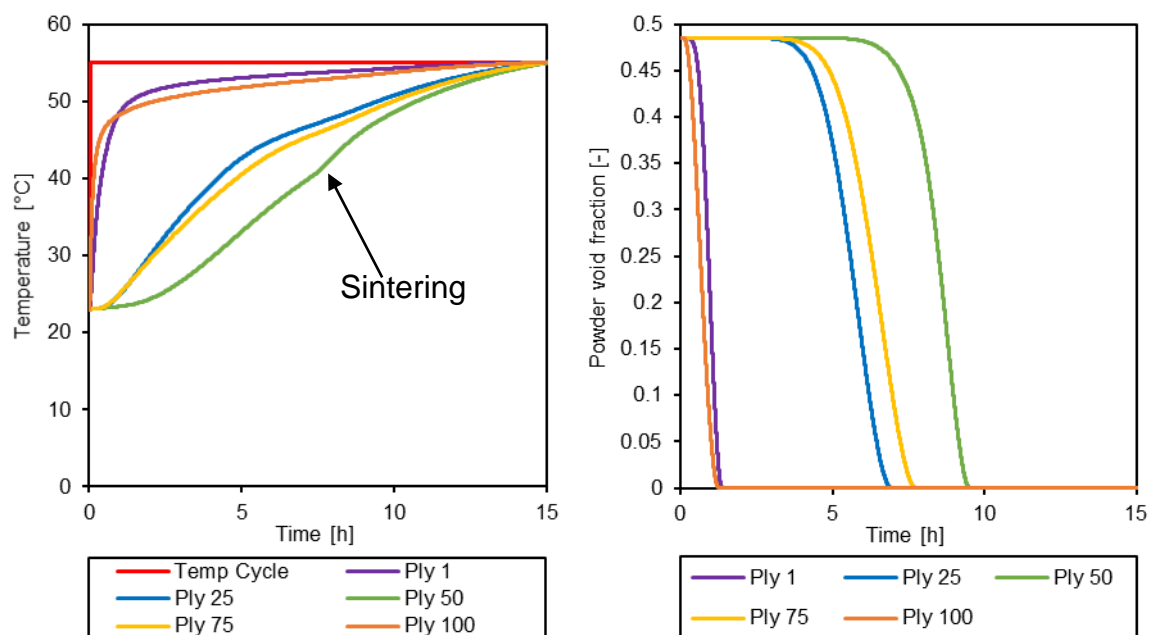


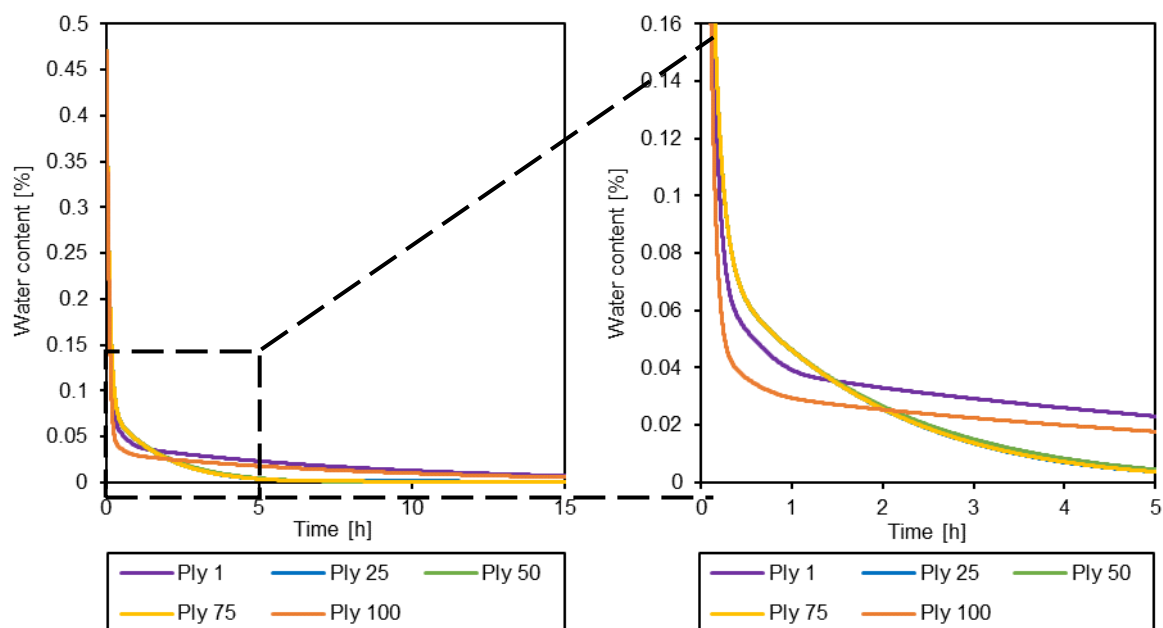
**Figure 12.** Simulation results for a 2-ply thick UD-GF/epoxy powder laminate. Three simulations were performed at three heating rates. The water content plateaued at approx. 0.05 % in each case. Note, the water content is a weight percentage of the epoxy powder, not of the whole laminate.

To investigate the drying stage under realistic conditions, a 100-ply laminate was simulated. As previously mentioned, this thickness is representative of a large blade root section. Figure 13 shows contour plots of the simulation at various time steps within the first 4 h of the drying stage. While temperature and powder void fraction were slow to change in the first hour, the water content was reduced to 0.05% within that time. Moreover, the latter was largely uniform as desorption could occur as soon as vacuum pressure was applied. In reality, this profile may be less uniform if gas evacuation was modelled, as moisture on the outside of the laminate has a shorter path to evacuation. In a similar vein, the contour plots of temperature and powder void fraction displayed an outside-to-inside profile that is characteristic of temperature-dependent processes in this material system [16,39,41]. Nevertheless, as previously mentioned, it is expected that gas evacuation would be in the order of seconds/minutes due to the high permeability of the epoxy powder and fibres. As such, large gradients would not be expected to develop for water content, provided sintering does not occur before the powder is fully dried.



**Figure 13.** Contour plots for a 1D simulation of a 100-ply laminate processed in an oven, with time progressing from left to right. A standard drying stage was applied to the laminate (i.e., 15 h at 55°C). (Top) The temperature change was slow and non-uniform (i.e., outside-to-inside profile) due to the low thermal conductivity of the epoxy powder and glass fibres. (Middle) In contrast, a large, uniform change in water content was predicted early in the drying stage (i.e., within 1 h). (Bottom) The sintering process followed the temperature profile and resulted in significant thickness change after 1 h.

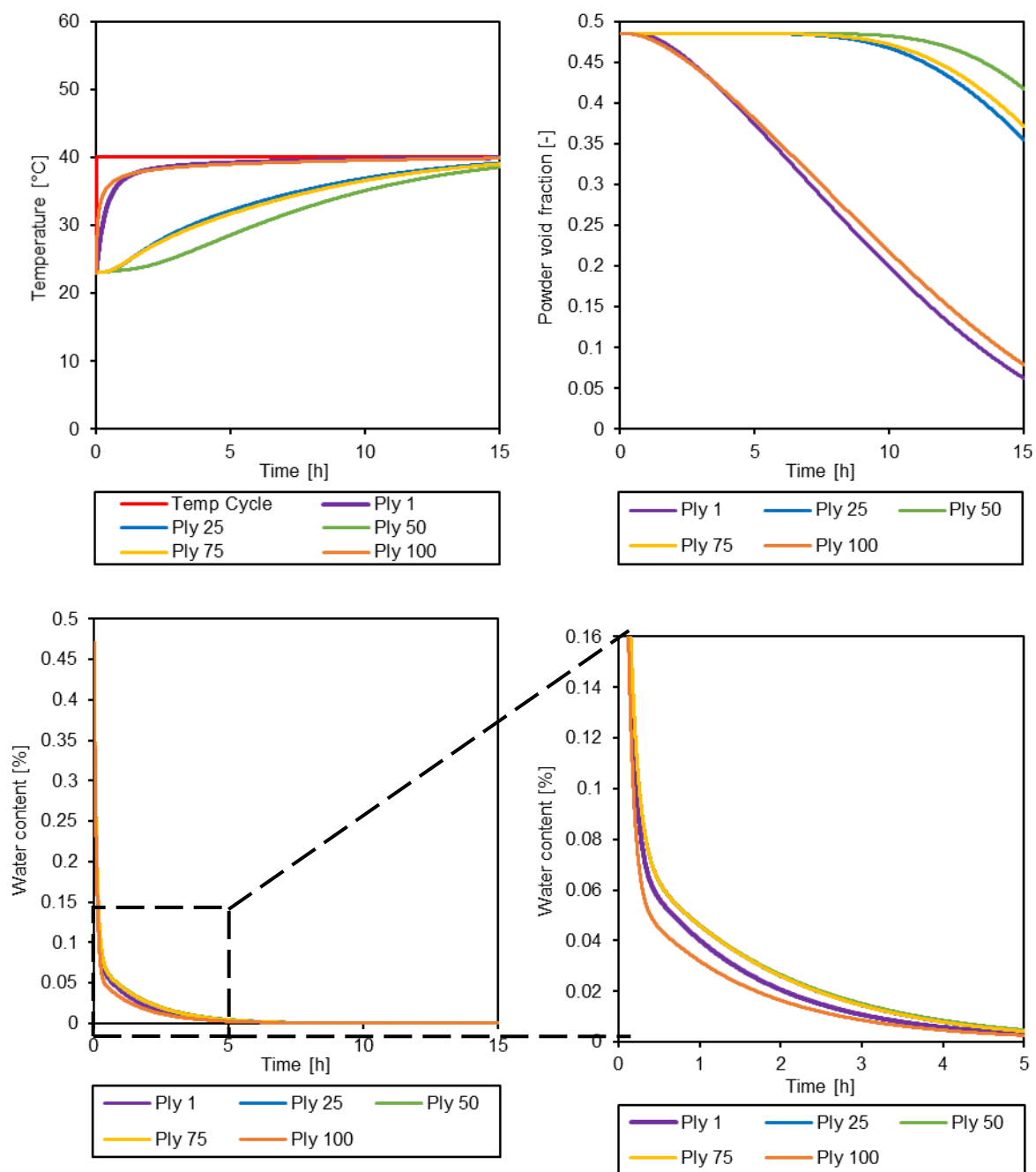




**Figure 14.** Simulated results for a 100-ply laminate processed using a standard drying stage (i.e. 55°C for 15 h). Data was taken from equispaced locations through the thickness of the laminate. (Top left) Temperature plots show that heat was slow to transfer through the laminate when in powder form, but the rate increased as the powder sintered (top right). (Bottom left) Most of the moisture desorbed before the powder sintered; however, magnifying the plot (bottom right) revealed that the outside of the laminate (Plies 1 and 100) sintered before they could be dried completely.

While the laminate appeared to be fully dried in Figure 13, closer inspection (see Figure 14) revealed that the outer plies of the laminate sintered before the water content could reach zero. By magnifying the water content plot, it was clear to see that the outer plies plateaued initially between 0.03% and 0.04%. Consequently, the entire 15 h dwell was required to remove the remaining entrapped moisture. As observed in previous work [41], powder sintering improved heat transfer because liquid epoxy has a higher thermal conductivity than powder, however, powder presented better characteristics for drying. Although the water diffusion from sintered/liquid epoxy was not fully modelled, the data presented in Figure 14 clearly indicated that the standard processing cycle used in industry was not efficient for drying epoxy powder composites and that sintering should be delayed until drying is complete.

To delay sintering, a second simulation was performed with a drying temperature of 40°C; the results of which are shown in Figure 15. Relatively little sintering was predicted to occur within the first 5 h due to the temperature dependency of the sintering process. As a result, the powder in the laminate was dried to a water content of  $\leq 0.005\%$  i.e., the same water content achieved after 15 h of drying at 55°C. This indicated that significant time savings can be made if the powder format is maintained during the drying stage. In the context of the standard processing cycle used by industry, resin infusion and curing may account for another 9 h of processing time. Assuming those times remain similar, shortening the drying time by 10 h would constitute a reduction of 38%. Not only would this allow for faster blade production, but drying for 5 h at 40°C, rather than 15 h at 55°C, would also enable energy savings within the production process. This is important considering the production process requires heating large ovens and moulds as well as the composite itself (as shown in Figure 3).



**Figure 15.** Simulated results for a 100-ply laminate processed using a modified drying temperature (i.e., 40°C). Data was taken from equispaced locations through the thickness of the laminate. Lowering the drying temperature (top left) helped to delay sintering (top right). (Bottom) By keeping the epoxy in its powder form, the water content of the powder was reduced to  $\leq 0.005\%$  within 5 h.

#### 4. Conclusions

An investigation of hygroscopicity in epoxy powder composites has been performed. It has been shown that the hygroscopicity of the powder gave rise to void defects (up to 5% by volume) when epoxy powder composites were manufactured in an undried state. This had a negative effect on the mechanical properties of the composite; in particular, the transverse flexural strength (i.e., 43.4% reduction). Via simulation, it was shown that moisture became entrapped in the composite (approximately 0.05% by mass) regardless of the heating rate due to powder sintering. As such, it was concluded that a drying stage is always required for this material system to avoid void defects.

Dynamic vapour sorption analysis was performed on the epoxy powder to better understand its sorption behaviour. This provided useful information, both for understanding the drying process and for understanding the effect of storage conditions on the epoxy powder handling. The epoxy powder displayed typical behaviour for a glassy polymer (i.e., type II isotherm), with temperature dependent sorption kinetics. It was also shown that the epoxy powder's glass transition temperature varied with relative humidity, with the powder sintering above the glass transition temperature. This had significant effects on the sorption behaviour of the epoxy as the surface area-to-volume ratio was drastically altered by the sintering process. From this, it was concluded that storage conditions should be controlled sufficiently to avoid powder 'caking' or sintering due to their detrimental effects on handling.

It was also considered that sintering should be avoided or delayed during the drying stage of composite manufacturing to ensure adequate drying. To investigate this further, data from the initial drying stage of the dynamic vapour sorption analysis was fit to a modified linear driving force model. Subsequently, this model was implemented into existing process simulation tools to simulate the drying stage. The simulations predicted that the standard drying cycle (15 h at 55°C) used in industry would sinter the outer plies of a 100-ply thick laminate before all moisture could be removed. As a result, the full 15 h of drying was required to achieve an adequately low water content (i.e.,  $\leq 0.005\%$ ) throughout the laminate. In contrast, the same simulation performed with a drying temperature of 40°C achieved a water content of  $\leq 0.005\%$  in all plies within 5 hours. This means that the total manufacturing cycle time could be reduced by as much as 10 hours for thick section composite parts, such as those found in the roots and spars of wind and tidal turbine blades. For this reason, it can be concluded that, to maximise the advantages of epoxy powder composites, their powder format should be maintained during the drying stage of manufacturing.

**Author Contributions:** James M. Maguire: Conceptualisation, Methodology, Software, Validation, Formal analysis, Investigation, Writing – Original Draft, Visualisation, Project administration. Jinyu Wang: Methodology, Writing – Review & Editing. Conchúr M. Ó Brádaigh: Conceptualisation, Resources, Writing – Review & Editing, Supervision, Project administration, Funding acquisition

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**Conflicts of interest:** The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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