

Article

Not peer-reviewed version

---

# Theory for Electrochemical Heat Sources and Exothermic Explosions: Akbari-Ganji's Method

---

Ramalingam Vanaja , Ponraj Jeyabarathi , [Lakshmanan Rajendran](#) \* , [Michael Edward Gerard Lyons](#) \*

Posted Date: 21 July 2023

doi: 10.20944/preprints2023071500.v1

Keywords: electrochemical heat sources; exothermic explosions; mathematical modelling; nonlinear equation; Akbari-Ganji's method



Preprints.org is a free multidiscipline platform providing preprint service that is dedicated to making early versions of research outputs permanently available and citable. Preprints posted at Preprints.org appear in Web of Science, Crossref, Google Scholar, Scilit, Europe PMC.

Copyright: This is an open access article distributed under the Creative Commons Attribution License which permits unrestricted use, distribution, and reproduction in any medium, provided the original work is properly cited.

Article

# Theory for Electrochemical Heat Sources and Exothermic Explosions: Akbari-Ganji's Method

Ramalingam. Vanaja <sup>1</sup>, Ponraj. Jeyabarathi <sup>2</sup>, Lakshmanan. Rajendran <sup>1,\*</sup> and Michael E. G. Lyons <sup>3,\*</sup>

<sup>1</sup> Department of Mathematics, AMET, Deemed to be University, Chennai, India.

<sup>2</sup> Department of Mathematics, Bharath Institute of Higher Education and Research, Chennai, India.

<sup>3</sup> School of Chemistry and AMBER National Centre, University of Dublin, Trinity College Dublin, Dublin 2, Ireland

\* Correspondence: melyons@tcd.ie (Michael E. G. Lyons) raj\_sms@rediffmail.com (L.Rajendran).

**Abstract:** A device that transforms chemical energy into electrical energy is an electrochemical cell. The reaction type inside the cell will determine whether it is exothermic or endothermic. This paper discusses the mathematical modelling of exothermic explosions in a slab. A nonlinear differential equation is used as a model in which a nonlinear term is related to the bimolecular, sensitised, and Arrhenius laws of reaction kinetics. The absolute temperature can be obtained by solving the nonlinear equation using Akbari-Ganji's method. The influence of the parameters Frank-Kamenetskii, activation energy and numerical exponent on temperature is discussed. The predicted results are validated with previous available analytical and numerical results (Matlab). An acceptable agreement is indicated. The appropriate consent is indicated.

**Keywords:** electrochemical heat sources; exothermic explosions; mathematical modelling; nonlinear equation; Akbari-Ganji's method

## 1. Introduction

In explosive applications, the safety of combustible materials during transport and storage is essential. Self-ignition is a common occurrence with certain materials. This interior heating occurs when an explosive chemical is heated to a temperature where the decomposition process begins to cause significant exothermic effects. A thermal runaway effect occurs when the temperature rises rapidly, resulting in a fast thermal breakdown. Understanding the components that control this occurrence in many industrial processes is essential.

Many authors have provided models to explain thermal runaway and abusive behaviour. Hatchard et al. [1] make the first attempts to explain the exothermic reaction kinetics. In the works of Peng et al. [3,4] and Kim et al. [2,] a simplified reaction-diffusion model is presented. There is also a discussion of an electrochemical model of lithium-ion battery nail absorption [5]. Wang et al. [6] present a catastrophe theoretic approach using a reduced ordinary differential equation model as a foundation. In [7], this model has been expanded. One must identify the primary exothermic chemical reactions to describe the thermal runaway of LIBs. Rising temperature can be used to describe the overall mechanism that causes a thermal runaway [1,3,4,8,9].

The equilibrium voltage and the method by which the equilibrium voltage is derived from the temperature are crucial factors in the electrochemical heat source [10]. The mechanisms of thermal abuse inside the Lithium-iron battery are directly related to modelling the thermal runaway and exothermic heat sources. As the temperature rises inside a battery, many exothermic chemical reactions may occur. If there is insufficient heat transmission to the environment [11] or if the rate of heat creation is higher than the heat dissipation rate, this could produce heat that accumulates inside the cell and speeds up the chemical reaction between the components of the cell. Any external factors, including outer heating, high or low voltage/current, nail piercing, exterior shorts, and others, might cause a temperature increase. Cells can be destroyed by a thermal runaway that can be brought on

by an air leak, cigarette smoke, gas combustion, fires, etc. In 1930, Semonov, Zeldovich, and Frank Kamenetskii described this behaviour first, and their pioneering contributions are presented in [12]. Frank-Kamenetskii also proposed the steady-state theory of thermal explosion. This idea has been applied to various combustible material geometries in the literature. For the infinite slab, Boddington et al. [13-15] reviewed the case of two-step parallel exothermic processes, and they extended their research to include the geometries of the sphere and the circular cylinder.

Graham-Eagle et al. [16] studied a system of exothermic processes co-occurring. The critical values of the Frank-Kamenetskii parameter and the maximum temperature were calculated using a variational technique. The analysis of simultaneous processes [17] was expanded by the same authors to exothermic and endothermic reactions. Gelfand et al. [18] numerically determined the parameter's values.

Ajadi and Gol'dshtein [19] used a three-step kinetics of reactions model including steps for initiation, transmission, and cessation. The computation was performed using an approximation of the effective activation energy. The critical values for several geometries, including infinite square, rod, and cube, have been determined by Balakrishnan et al. [20] employing the finite difference method.

Makinde et al. [21] used the perturbation technique and Hermite-Pade approximants to arrive at the analytical solutions to the governing nonlinear boundary-value problem. They also explored the fundamental characteristics of the thermodynamic field, such as heat and bifurcations. Ananthasamy et al. [22] derived the analytical expression of temperature in exothermic explosions in a slab by solving the nonlinear equation using HAM. It is time-consuming since this contains an infinite number of convergence-control parameters.

Er-Riani and Chetehouna [23] apply the homotopy perturbation method for solving the steady-state nonlinear equation in an exothermic chemical reaction. This method was introduced by He [24-26]. In this communication, we derive the simple analytical expression for the temperature field for three kinds of reactions by solving the nonlinear equation using Akbari-Ganji's method.

## 2. Problem Formulation and Analysis

Considering the steady-state of an exothermic chemical reaction in a combustible slab with the potential of heat loss to the environment. Frank-Kamenetskii [12] first proposed the classical formulation of this problem. The heat balance equation for steady-state conditions is given as follows:

$$k \frac{d^2 T(Y)}{dY^2} + Q C_0 A \left( \frac{K T(Y)}{v h} \right)^m e^{\frac{-E}{RT(Y)}} = 0 \quad (1)$$

The boundary conditions are

$$\frac{dT}{dY} = 0 \quad \text{at} \quad Y = 0, \quad (2)$$

$$T = T_0 \quad \text{at} \quad Y = a, \quad (3)$$

The material's thermal conductivity is denoted by the letters  $k$ , while  $T$  represents the absolute temperature. The other parameters have the same standard meaning as in the reference [12]. Additionally, the numerical exponent for Arrhenius, bimolecular, and sensitised kinetics is  $m = 2, 0, 1/2$ . To reduce the complexity, we make the nonlinear Eq. (1) into dimensionless form by defining the following dimensionless parameters.

$$\theta = \frac{E(T-T_0)}{RT_0^2}, \quad \varepsilon = \frac{RT_0}{E}, \quad y = \frac{Y}{a}, \quad \lambda = \frac{Q E A a^2 C_0 K^m T_0^{m-2} e^{\frac{E}{RT_0}}}{v^m h^m R k} \quad (4)$$

where  $\theta$  is the dimensionless temperature field,  $\lambda$  represents the Frank-Kamenetskii constant,  $\varepsilon$  denotes the activation energy. Using Eq. (4), the Eq. (1) reduces to the following dimensionless form.

$$\frac{d^2 \theta(y)}{d y^2} + \lambda (1 + \varepsilon \theta(y))^m e^{\frac{\theta(y)}{1 + \varepsilon \theta(y)}} = 0 \quad (5)$$

The boundary conditions (2) and (3) can be reduced as follows:

$$\frac{d\theta}{dy} = 0 \quad \text{at} \quad y = 0, \quad (6)$$

$$\theta = 0 \quad \text{at} \quad y = 1, \quad (7)$$

### 3. Analytical Expression of the Temperature using Akbari-Ganji's method

Recently, a variety of asymptotic techniques for solving nonlinear differential equations have been established such as the Adomian decomposition [27,28], Variational iteration [29,30], Taylor series [31,32] and Akbari-Ganji method (AGM)[33-40]. Among these techniques, AGM might be recognised as a useful algebraic (semi-analytic) method of resolving such problems. According to the AGM, a solution function with unidentified constant coefficients is supposed to satisfy the differential equation and the initial conditions. Then, the unknown coefficients are calculated using algebraic equations derived from initial conditions and derivatives.

We can assume that the trial solution of the Eq. (5) is

$$\theta(y) = \sum_{i=0}^2 \theta_i y^i = \theta_0 + \theta_1 y + \theta_2 y^2 \quad (8)$$

where  $\theta_0, \theta_1$  and  $\theta_2$  are constants. We obtain the constant  $\theta_0$  and  $\theta_1$  using the boundary conditions (6) and (7) as follows:

$$\theta_1 = 0, \quad \theta_0 = -\theta_2 \quad (9)$$

Now define the function  $G$  by

$$G(y) = \frac{d^2\theta}{dy^2} + \lambda(1 + \varepsilon\theta)^m e^{\left(\frac{\theta}{1+\varepsilon\theta}\right)} = 0 \quad (10)$$

Using Eq. (8), the Eq. (10) at  $y = 0$  becomes

$$G(y = 0) = 2\theta_2 + \lambda(1 - \varepsilon\theta_2)^m e^{\left(\frac{-\theta_2}{1-\varepsilon\theta_2}\right)} = 0 \quad (11)$$

Using eq. (9), the eq. (8) can be rewritten as follows:

$$\theta(y) = \theta_2(y^2 - 1) \quad (12)$$

The parameter  $\theta_2$  is obtained by solving the nonlinear equation

$$2\theta_2 + \lambda(1 - \varepsilon\theta_2)^m e^{\left(\frac{-\theta_2}{1-\varepsilon\theta_2}\right)} = 0 \quad (13)$$

The unidentified parameter  $\theta_2$  in the equation (13) can be obtained with the Ying Buzu technique [41]. The value of this parameter was also determined using the regular false method and the secant algorithm. The Ying Buzu algorithm approach provides a convergent solution very quickly.

## 4. Previous analytical results

### 4.1. Homotopy analysis method

Anathaswamy et al. [11] used the homotopy analysis method (HAM) to solve Eq. (5) with boundary conditions (6) and (7). They obtained that the analytical expression for the temperature field

$$\theta(y, \lambda, \varepsilon, m) = \frac{\lambda(1-y^2)}{2} - h \left[ \frac{-\lambda^2(1+\varepsilon m)}{2} \left( \frac{y^2}{2} - \frac{y^4}{12} \right) - \frac{\lambda^3 \varepsilon(1-m)}{4} \left( \frac{y^2}{2} - \frac{y^4}{6} + \frac{y^6}{30} \right) + \frac{5\lambda^3(1+\varepsilon m)}{24} + \frac{11\lambda^3 \varepsilon(1-m)}{120} \right] \quad (14)$$

It takes a very long time since the convergence-control parameter  $h$  are unbounded.

### 4.2. Perturbation method

Makinde et al [10] solved Eq. (5) with boundary conditions (6) and (7) using the perturbation approach. According to their computations, the temperature was:

$$\theta(y, \lambda, \varepsilon, m = -2) = \frac{\lambda(1-y^2)}{2} - \frac{\lambda^2}{24}(y^2-1)(y^5-5)(2\varepsilon-1) + \frac{\lambda^3}{360}(y^2-1)(-11y^4\varepsilon + 2y^4 + 11y^4\varepsilon^2 + 64y^2\varepsilon - 13y^2 - 64y^2\varepsilon^2 + 221\varepsilon^2 - 221\varepsilon + 47) \quad (15)$$

$$\theta(y, \lambda, \varepsilon, m = 0) = \frac{\lambda(1-y^2)}{2} + \frac{\lambda^2}{24}(y^2-1)(y^5-5) + \frac{\lambda^3}{360}(y^2-1)(-2y^4 + 3y^4\varepsilon - 12y^2\varepsilon + 13y^2 + 33\varepsilon - 47) \quad (16)$$

$$\theta(y, \lambda, \varepsilon, m = 0.5) = \frac{\lambda(1-y^2)}{2} - \frac{\lambda^2}{48}(y^2-1)(y^5-5)(2+\varepsilon) + \frac{\lambda^3}{1440}(y^2-1)(4y^4\varepsilon - 8y^4 + y^4\varepsilon^2 + 4y^2\varepsilon + 52y^2 + y^2\varepsilon^2 - 14\varepsilon^2 - 56\varepsilon - 188) \quad (17)$$

These approximate solutions are obtained by carrying out expansions in terms of a small parameter ( $\varepsilon$ ). In addition to this, perturbation method is not always to generate a continuous family of solutions in terms of the small parameter.

## 5. Discussion

Equation (12) represents the simplest analytical expression of the temperature profile. The thermal decomposition of the reacting combustible material depends on the parameters  $\lambda$ ,  $\varepsilon$  and  $m$ , which are of great importance for applications in explosives handling and industrial safety.

### 5.1. Numerical Simulation

This section validates the above theoretical results using numerical simulation for physically realistic values of various embedded parameters. The function `bvp4c` in Matlab/Scilab software, which solves non-linear boundary value problems for ordinary differential equations, is used to solve these equations numerically. The present (AGM) and previous (HAM, PM) analytical results are compared to this numerical solution in Tables (1–4). The maximum average relative error between our result and the simulation result is 1.44. But the maximum error between numerical results and HAM and PM is 1.86% and 4.92%.

**Table 1. Comparison of the analytical results with numerical and earlier analytical results for the temperature  $\theta(y)$  when  $\lambda = 0.1$ ,  $\varepsilon = 0.1$ ,  $m = -2$  and  $\theta_2 = -0.05175$ .**

y	$\theta(y)$						
	Num.	AGM Eq. (12). This work	HAM [11] Eq. (14)	PM [10] Eq. (15)	Error % AGM Eq. (12) This work	Error % HAM [11] Eq. (14)	Error % PM [10] Eq. (15)
0	0.0517	0.0517	0.0517	0.0516	0.0000	0.0000	0.1934
0.2	0.0496	0.0496	0.0496	0.0495	0.0000	0.0000	0.2016
0.4	0.0432	0.0436	0.0434	0.0433	0.9259	0.0230	0.4629
0.6	0.0327	0.0324	0.0330	0.0329	0.9174	0.0303	0.6116
0.8	0.0179	0.0180	0.0185	0.0185	0.5586	3.3519	3.3519
1	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
	Average error (%)				0.3493	0.5675	0.8036

**Table 2. Comparison of the analytical results with numerical and earlier analytical results for the temperature  $\theta(y)$  when  $\lambda = 0.5$ ,  $\varepsilon = 0.1$ ,  $m = -2$ ,  $\theta_2 = -0.320092$ .**

y	$\theta(y)$						
	Num.	AGM Eq. (12).	HAM [11]	PM [10]	Error %	Error % HAM [11]	Error % PM [10]

		This work	Eq. (14)	Eq. (15)	AGM Eq. (12) This work	Eq. (14)	Eq. (15)
0	0.3045	0.3201	0.2951	0.2823	4.8133	3.0870	7.2906
0.2	0.2916	0.3001	0.2829	0.2707	2.8000	2.9835	7.1673
0.4	0.2532	0.2548	0.2466	0.2363	0.6319	2.5671	6.6745
0.6	0.1899	0.1893	0.1869	0.1792	0.3159	1.5798	5.6334
0.8	0.1031	0.1030	0.1041	0.1002	0.0970	0.9699	2.8128
1	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Average error (%)					1.4430	1.8645	4.9298

**Table 3. Comparison of the analytical results with numerical and earlier analytical results for the temperature  $\theta(y)$  when  $\lambda = 0.1$  when  $\varepsilon = 0.1, m = 0, \theta_2 = -0.0523$  .**

y	$\theta(y)$						
	Num.	AGM Eq. (12). This work	HAM [11] Eq. (14)	PM [10] Eq. (16)	Error % AGM Eq. (12) This work	Error % HAM [11] Eq. (14)	Error % PM [10] Eq. (16)
0	0.0522	0.0523	0.0521	0.0522	0.1916	0.1916	0.0000
0.2	0.0501	0.0501	0.0500	0.0501	0.0000	0.1996	0.0000
0.4	0.0436	0.0437	0.0437	0.0438	0.2294	0.2294	0.4587
0.6	0.0329	0.0331	0.0332	0.0333	0.6079	0.9118	1.2158
0.8	0.0180	0.0181	0.0188	0.0187	0.5555	4.4444	3.8889
1	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Average error (%)					0.2641	0.9961	0.9272

**Table 4. Comparison of the analytical results with numerical and earlier analytical results for the temperature  $\theta(y)$  when  $\lambda = 0.4$  ,  $\varepsilon = 0.1, m = 0, \theta_2 = -0.32181$  .**

y	$\theta(y)$						
	Num.	AGM Eq. (12). This work	HAM [11] Eq. (14)	PM [10] Eq. (16)	Error % AGM Eq. (12) This work	Error % HAM [11] Eq. (14)	Error % PM [10] Eq. (16)
0	0.3255	0.3208	0.3192	0.3172	1.4439	1.9355	2.5499
0.2	0.3116	0.3077	0.3059	0.3040	1.2516	1.8292	2.4390
0.4	0.2701	0.2684	0.2662	0.2646	0.6294	1.4439	2.0363
0.6	0.2021	0.2030	0.2011	0.1994	0.4433	0.4948	1.3360
0.8	0.1093	0.1113	0.1117	0.1110	1.8230	2.1958	1.5553
1	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Average error (%)					0.9319	1.3163	1.6527

## 6. Limiting case

When the activation energy ( $\varepsilon$ ) or Arrhenius kinetics ( $m$ ) is very small, the equation (5) becomes

$$\frac{d^2\theta}{dy^2} + \lambda e^\theta = 0 \quad (18)$$

In this case, the temperature becomes,

$$\theta(y) = \log \left[ \frac{n - nT \tanh^2(0.5y\sqrt{n})}{2\lambda} \right] \quad (19)$$

where  $n$  is obtained from the equation

$$n - nT \tanh^2(0.5\sqrt{n}) = 2\lambda \quad (20)$$

We can notice that the average error percentage between AGM and an exact limiting case result (eqn.(19)) does not exceed 1.8% for the slab.

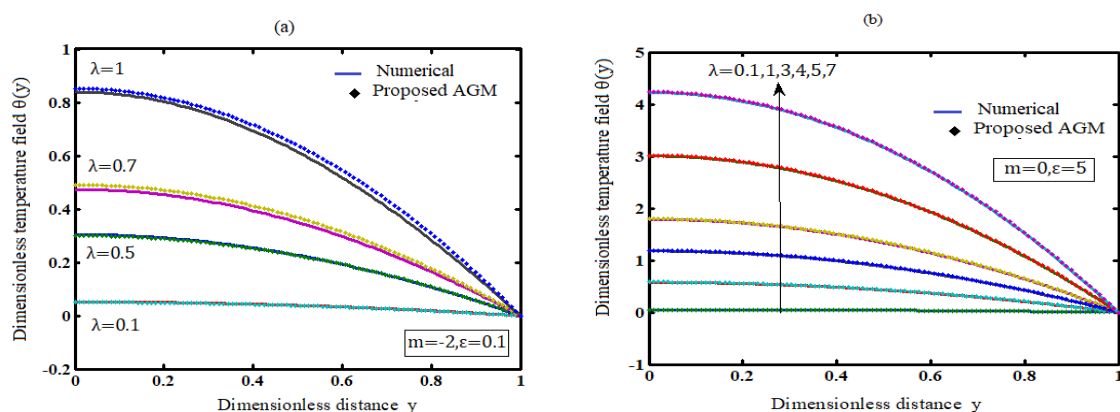
**Table 5.** Comparison of our approximate analytical result (12) with exact result (19) for the limiting case.

y	$\lambda = 0.1$			$\lambda = 0.3$			$\lambda = 0.5$		
	Exact solution	AGM Eq. (12)	Error%	Exact solution	AGM Eq. (12)	Error%	Exact solution	AGM Eq. (12)	Error%
0	0.0522	0.0527	0.9578	0.1733	0.1795	3.5776	0.3290	0.3474	5.5927
0.2	0.0501	0.0505	0.7984	0.1661	0.1689	1.6857	0.3148	0.3246	3.1131
0.4	0.0436	0.0439	0.6881	0.1443	0.1440	0.2079	0.2728	0.2768	1.4663
0.6	0.0329	0.0330	0.3039	0.1085	0.1087	0.1843	0.2040	0.2060	0.9804
0.8	0.0180	0.0180	0.0000	0.0590	0.0590	0.0000	0.1102	0.1102	0.0000
1	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
	Average error (%)		0.4580	Average error (%)		0.9426	Average error (%)		1.8587

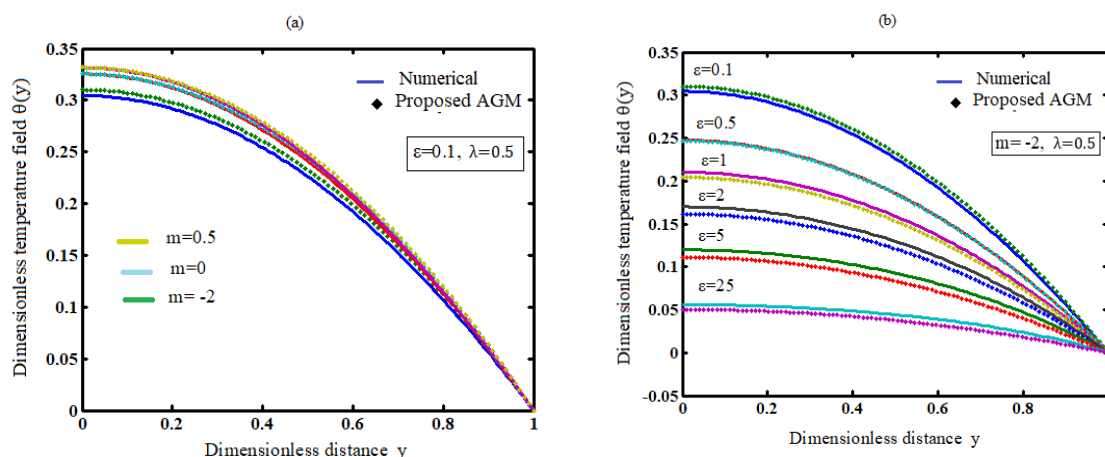
## 7. Influence of the parameters on temperature

### 7.1. Effect of the Frank-Kamenetskii parameter $\lambda$ on temperature

Figure (1) illustrates the effects of the Frank-Kamenetskii parameter on a temperature profile. Figure 2 shows that an increase in Frank-Kamenetskii leads to an increase in the rate of an exothermic reaction. The maximum temperature along the slab is at the centre line, and the minimum is at the slab surface.. The slab temperature will invariably rise as a result of this.



**Figure 1.** Comparison of analytical expression of temperature field  $\theta(y)$  with simulation results for different values of Frank-Kamenetskii parameter  $\lambda$  using eq. (12).



**Figure 2.** Comparison of temperature field  $\theta(y)$  with simulation results (a) for various values of  $m$  (Kinetics) and (b) for various values of  $\varepsilon$  (Activation energy).

### 7.2. Effect of the numerical exponent $m$ on temperature

The effects of numerical exponent  $m$  on temperature profiles are shown in Figure 2 (a). The figure shows that the temperature increases as the numerical exponent number  $m$  increases. Moreover, the tables and figures show that in a bimolecular ( $m = 0.5$ ) reaction, a thermal explosion occurs faster than in the Arrhenius ( $m = 0$ ), sensitised ( $m = -2$ ) reactions.

### 7.3. Effect of the activation energy parameter ( $\varepsilon$ ) on temperature

A similar effect of temperature is observed with increasing values of activation energy parameter ( $\varepsilon$ ) (Figure 2-b)). With rising values of the activation energy, a similar effect of temperature enhancement is observed. Increasing values of  $\varepsilon$  imply that the reacting slab's activation energy is insufficient, and thus the reacting slab's volatility characteristic is significantly reduced.

## 8. Conclusions

We studied the exothermic explosion of a viscous combustible in the slab under various laws of reactions. The exothermic chemical reaction in a slab of flammable material is considered. The expected outcomes reveal that this method provides an outstanding and highly accurate approximation of the solution of this nonlinear system. The effects of the parameters Frank-Kamenetskii, numerical exponent of temperature and activation energy on temperature profiles are discussed. This method can be applied to infinite cylindrical and spherical geometries.

**Funding:** The authors have not received any funds.

**Institutional Review Board Statement:** Not applicable.

**Informed Consent Statement:** Not applicable.

**Conflicts of Interest:** The author declare no conflicts of interest.

## References

1. Hatchard T.D.; MacNeil D.D.; Basu, A.; Dahn J.R. Thermal model of cylindrical and prismatic lithium-ion cells. *J. Electrochem. Soc* **2001**, *148* (7), A755–A761.
2. Kim G.H.; Pesaran A.; Spotnitz R. A three-dimensional thermal abuse model for lithium-ion cells. *J. Power Sources* **2007**, *170*, 476–489.
3. Peng P.; Sun Y.; Jiang F. Thermal analyses of LiCoO<sub>2</sub> lithium-ion battery during oven tests, *Heat Mass Transf* **2014**, *50*, 1405–1416.
4. Peng P.; Sun Y.; Jiang F. Numerical simulations and thermal behavior analysis for oven thermal abusing of LiCoO<sub>2</sub> lithium-ion battery, *CIESC J* **2014**, *65* (2), 647–657.

5. Chiu K.C.; Lin C.H.; Yeh S.F.; Lin Y.H.; Chen K.C. An electrochemical modeling of lithium-ion battery nail penetration, *J. Power Sources* **2014**, 251, 254–263.
6. Wang Q.; Ping P.; Sun J. Catastrophe analysis of cylindrical lithium ion battery, *Nonlinear Dyn* **2010**, 61, 763–772.
7. Wang Q.; Ping P.; Zhao X.; Chu G.; Sun J.; Chen C. Thermal runaway caused fire and explosion of lithium ion battery, *J. Power Sources* **2012**, 208, 210–224.
8. Lisbona D.; Snee T. A review of hazards associated with lithium and lithium-ion batteries. *Process Saf. Environ. Prot* **2011**, 89, 434–442.
9. Abraham D.P.; Roth E.P.; Kostecki R.; McCarthy K.; MacLaren S.; Doughty D.H. Diagnostic examination of thermally abused high-power lithium-ion cells. *J. Power Sources* **2006**, 161, 648–657.
10. C. Ziebert C.; Melcher A.; Lei B.; Zhao W.; Rohde M.; Seifert H.J. Chapter Six - Electrochemical-Thermal Characterization and Thermal Modeling for Batteries, *Emerging Nanotechnologies in Rechargeable Energy Storage Systems*, 2017, Micro and Nano Technologies, 195-229.
11. Guo G.; Long B.; Cheng B.; Zhou S.; Cao B.; Three-dimensional thermal finite element modeling of lithium-ion battery in thermal abuse application, *J. Power Sources* **2010**, 195, 2393–2398.
12. Frank-Kamenetskii D.A.; *Diffusion and Heat Transfer in Chemical Kinetics*. Plenum Press, New York, NY, USA **1969**.
13. Boddington T.; Gray P.; C. Robinson. Thermal explosions and the disappearance of criticality at small activation energies: exact results for the slab. *Proc. R. Soc. Lond* **1979**, **368**,441–461.
14. Boddington T.; Feng C.G.; Gray P. Thermal explosions, criticality and the disappearance of criticality in systems with distributed temperatures. I. arbitrary biot number and general reaction rate laws, *Proc. R. Soc. Lond* **1983**, 390, 247–264.
15. T. Boddington T.; P. Gray P.; Wake G.C. Theory of thermal explosions with simultaneous parallel reactions. I. foundations and the one-dimensional case. *Proc. R. Soc. Lond* **1984**, **393**,85–100.
16. Graham-Eagle J.G.; Wake G.C. Theory of thermal explosions with simultaneous parallel reactions. II. The two- and three-dimensional cases and the variational method, *Proc. R. Soc. Lond. A* **1820**, 401, 195–202.
17. Graham-Eagle J.G.; Wake G.C. The theory of thermal explosions with simultaneous parallel reactions.III. Disappearance of critical behaviour with one exothermic and one endothermic reaction. *Proc. R. Soc. Lond A* **1986**, 407, 183–198.
18. Gelfand I.M.; Fomin S.V. *Calculus of Variations*, Prentice Hall, Englewood Cliffs, NJ, USA. **1963**.
19. Ajadi S.O.; Gol'dshtein V. Critical behaviour in a three-step reaction kinetics model. *Combust. Theory Model* **2009**, 13 (1), 1–16.
20. Balakrishnan E.; Swift A.; ke G.C. Critical values for some nonclass A geometries in thermal ignition theory. *Mathl. Comput. Modelling* **1996**, 24, 1–10.
21. Makinde O.D. Exothermic explosions in a slab: A case study of series summation technique. *Int. Commun. Heat Mass Transf.* **2004**, 31(8), 1227-1231.
22. Ananthaswamy V.; Subha M. Analytical expressions for exothermic explosions in a slab. *Int. J. Res. Granthaalayah* **2014**, 1(2), 22-33.
23. Er-Riani M.; Chetehouna K. On the critical behaviour of exothermic explosions in class A geometries. *Math. Probl. Eng* **2011**, 536056, 1-14.
24. He J.H. A coupling method of a homotopy technique and a perturbation technique for non-linear problems. *Int J Non-Linear Mech* **2000**, 35(1), 37–43.
25. He J.H. Homotopy perturbation method: A new nonlinear analytical technique. *Appl. Math. Comput* **2003**, 135(1),73–79.
26. He, J.H.; Homotopy perturbation method for solving boundary value problems. *Phys. Lett. A* **2006**, 350(1-2), 87–88.
27. Jeyabarathi P.; Kannan M.; Rajendran L. Approximate analytical solutions of biofilm reactor problem in applied biotechnology. *Theor. Found. Chem. Eng* **2021**, 55(5), 851-861.
28. Jeyabarathi,P.; Rajendran,L.; Abukhaled,M.; Kannan,M.;Semi-analytical expressions for the concentrations and effectiveness factor for the three general catalyst shapes. *React. Kinet. Mech. Catal.***2022**, 1-16
29. Abukhaled M. Variational iteration method for nonlinear singular two-point boundary value problems arising in human physiology. *J. Math* **2013**, 1-4.
30. He J.H.; Wu X.H. Variational iteration method: new development and applications, *Comput. Math. with Appl* **2007**, 54(7-8), 881-894.

31. Vinolyn Sylvia S.; Joy Salomi R.; Rajendran L.; Abukhaled M. Solving nonlinear reaction–diffusion problem in electrostatic interaction with reaction-generated pH change on the kinetics of immobilized enzyme systems using Taylor series method. *J. Math. Chem* **2019**, *59*, 1332-1347.
32. He,JH.; Taylor series solution for a third order boundary value problem arising in Architectural Engineering. *Ain Shams Eng. J.* **2022**, *11*(4), 1411-141
33. Jeyabarathi P.; Rajendran L.; Lyons M. E. G.; Abukhaled M. Theoretical Analysis of Mass Transfer Behavior in Fixed-Bed Electrochemical Reactors: Akbari-Ganji’s Method. *Electrochem* **2022**, *3*, 699–712.
34. Joy Salomi R.; Vinolyn Sylvia S.; Rajendran L.; Abukhaled M. Electric potential and surface oxygen ion density for planar, spherical and cylindrical metal oxide grains. *Sens. Actuators B Chem* **2020**, *321*, 128576.
35. Manimegalai B.; Lyons M.E.G.; Rajendran L. A kinetic model for amperometric immobilized enzymes at planar, cylindrical and spherical electrodes: The Akbari-Ganji method. *J Electroanal Chem* **2021**, *880*, 114921.
36. Mary M.; Chitra Devi M.; Meena A.; Rajendran L.; Abukhaled M. Mathematical modeling of immobilized enzyme in porous planar, cylindrical, and spherical particle: a reliable semi-analytical approach. *React. Kinet. Mech. Catal* **2021**, 1-11.
37. Jeyabarathi P.; Rajendran L.; Lyons M.E.G. Reaction-diffusion in a packed-bed reactors: Enzymatic isomerization with Michaelis-Menten kinetics, *J Electroanal Chem* **2022**, *910*, 11618.
38. Akbari M.R.; Ganji D.D.; Goltabar A.R. Solving nonlinear differential equations of Vanderpol, Rayleigh and Duffing by AGM, *Front. Mech. Eng* **2014**, *9*, 177 – 190..
39. Rostami A.K.; Akbari M.R.; Ganji D.D.; Heydari S. Investigating Jeff ery-Hamel flow with high magnetic field and nanoparticle by HPM and AGM, *Cent. Eur. J. Eng* **2014**, *4*,357-370
40. Meresht NB.; Ganji D.D. Solving nonlinear differential equation arising in dynamical systems by AGM, *Int. J. Appl. Comput. Math* **2017**, *3*, 1507–1523
41. Manimegalai,B.; Swaminathan,R.; Lyons,MEG.; Rajendran,L. Application of Taylor’s series with Ying Buzu Shu algorithm for the nonlinear problem in amperometric biosensors. *Int. J. Electrochem. Sci.* **2022**, *17*, 22074

**Disclaimer/Publisher’s Note:** The statements, opinions and data contained in all publications are solely those of the individual author(s) and contributor(s) and not of MDPI and/or the editor(s). MDPI and/or the editor(s) disclaim responsibility for any injury to people or property resulting from any ideas, methods, instructions or products referred to in the content.